



Article

Influence of Water on the Oxidation of NO on Pd/TiO₂ Photocatalysts

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Abstract: Two series of new photocatalysts were synthesized based on modification with Pd of the commercial P25 photocatalyst (EVONIK®). Two techniques were employed to incorporate Pd nanoparticles on the P25 surface: photodeposition (series Pd-P) and impregnation (series Pd-I). Both series were characterized in depth using a variety of instrumental techniques: BET, DRS, XRD, XPS, TEM, FTIR and FESEM. The modified series exhibited a significant change in pore size distribution, but no differences compared to the original P25 with respect to crystalline phase ratio or particle size were observed. The Pd⁰ oxidation state was predominant in the Pd-P series, while the presence of the Pd²⁺ oxidation state was additionally observed in the Pd-I series. The photoactivity tests were performed in a continuous photoreactor with the photocatalysts deposited, by dip-coating, on borosilicate glass plates. A total of 500 ppb of NO was used as input flow at a volumetric flow rate of 1.2 L·min⁻¹, and different relative humidities from 0 to 65% were tested. The results obtained show that under UV-vis or Vis radiation, the presence of Pd nanoparticles favors NO removal independently of the Pd incorporation method employed and independently of the tested relative humidity conditions. This improvement seems to be related to the different interaction of the water with the surface of the photocatalysts in the presence or absence of Pd. It was found in the catalyst without Pd that disproportionation of NO₂ is favored through its reaction with water, with faster surface saturation. In contrast, in the catalysts with Pd, disproportionation took place through nitro-chelates and adsorbed NO₂ formed from the photocatalytic oxidation of the NO. This different mechanism explains the greater efficiency in NO_x removal in the catalysts with Pd. Comparing the two series of catalysts with Pd, Pd-P and Pd-I, greater activity of the Pd-P series was observed under both UV-vis and Vis radiation. It was shown that the Pd⁰ oxidation state is responsible for this greater activity as the Pd-I series improves its activity in successive cycles due to a reduction in Pd²⁺ species during the photoactivity tests.

Keywords: photocatalysis; NO_x; TiO₂; Pd; water; FTIR

1. Introduction

The continuing deterioration of the environment is a problem that has been acquiring ever greater relevance over the last few decades. In recent years, there has been growing concern about the

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deterioration in air quality. The emission of contaminating gases into the atmosphere—principally as a result of anthropogenic activity—is one of the issues that has generated the greatest concern. The legally established limits in various cities around the world are being exceeded on a regular basis. Among the most dangerous gases are ozone and nitrogen oxides or NO_x [1]. These atmospheric pollutants can provoke numerous harmful chemical reactions, making their elimination a priority [2]. Heterogeneous photocatalysis has been shown to be an effective tool for such elimination, as reported in several published studies [3–6]. Various articles have demonstrated its efficiency in the elimination of NO_x [7,8]. Nonetheless, it is also clear that its application with solar radiation needs to be improved as the current commercially available catalysts do not show significant photocatalytic activity in this wavelength range (400–700 nm) [9]. One of the techniques that can be used to enhance this aspect is the incorporation of metals into/onto the semiconductor [9]. In this respect, catalyst modification can be internal or surface-based. With surface modification, the metals are incorporated onto the surface of the catalyst without altering its internal structure and without affecting the arrangement of atoms in the crystalline lattice of the catalyst [10,11]. As a result of previous studies [12], it is known that the incorporation of Pd onto TiO2 can enhance photocatalyst absorption in the visible range (400–700 nm). Pd is one of the most extensively used noble metals in heterogeneous catalysis and photocatalysis after Pt and Au to improve photocatalytic efficiency in pollutant removal in water [13] and air [14]. Lee et al. [15] compared the results that they obtained according to the nature of the TiO₂ employed, the type of noble metal (Pd or Pt), the deposition method and the type of photocatalytic reaction. Some of the results were apparently contradictory, showing that the Pt-TiO₂ and Pd-TiO₂ systems were not always more effective than the unmodified TiO₂. The number of publications related to the study of the photoactivity of Pd-modified photocatalysts has grown in recent years [16-20]. However, very few studies have been published on NO elimination and none on in-depth analyses of the effect of the presence of Pd on the elimination mechanism. Some publications have focused very specifically on the synthesis of new materials modified with Pd [21,22], but without placing any importance on their reactivity, while others [14,23,24] have tested modified commercial materials under very specific conditions—including some not very common values for these conditions of radiation, temperature, humidity and NO concentrations. We consider that this present work constitutes an extension and completion of these previous studies. Consequently, taking as a starting point the knowledge acquired from these studies, this work evaluates the incorporation of Pd on TiO₂ by impregnation and photodeposition for NO_x removal at 500 ppb concentration, at a temperature of 25 °C and with and without humidity. Identification is made through infrared spectroscopy of the species that are formed in NO_x oxidation, and the influence of the water and palladium species on reactivity is discussed. In addition, visible (Vis) radiation was used as well as UV-vis, and photocatalyst stability was tested after long periods of radiation and reuse. This comprises one of the major goals of this study since photocatalyst reuse is one of the issues that need to be solved for the practical application of this technology.

2. Experimental

2.1. Synthesis of Photocatalysts

The modified TiO_2 catalyst was Aeroxide TiO_2 P25 (Evonik Degussa GmbH, Germany). The catalysts modified with Pd were obtained by photodeposition (P) and impregnation (I). The photodeposition of Pd was described previously by Maicu et al. [12]. The P25 was suspended in water at a concentration of 5 g·L⁻¹. A total of 400 mL of the suspension was taken, and 9.2 mL of isopropanol added, and 0.5% in weight of Pd with respect to the TiO_2 from palladium (II) nitrate dihydrate (Sigma-Aldrich). The mixture was placed under a low continuous flow of N_2 to maintain an inert atmosphere, illuminated for 6 h with a medium-pressure 400 W mercury lamp $(2.6 \times 10^{-7} \text{ Einstein} \cdot \text{s}^{-1} \cdot \text{L}^{-1})$ (Photochemical Reactors Ltd.) with emission principally in the UV-A region, and kept refrigerated at a temperature below 293 K. The suspensions were filtered using

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a 0.45 μ m filter and dried at 383 K for 24 h. Pd impregnation was described by Wu et al. [14]. In brief, 4 g of P25 were mixed with 50 mL of a Pd(NO₃)₂/HCl solution (40 mg in 100 mL HCl 36% v/v). Contact was maintained for 48 h under stirring, with subsequent drying at 333 K for 12 h.

2.2. Dip Coating

The catalysts were deposited onto previously washed 50 cm² borosilicate 3.3 plates with a dip-coating procedure (KSV-DC Dip-Coater). The plates were introduced into a 14 g·L⁻¹ suspension of the catalyst in methanol at a rate of 500 mm·min⁻¹, left in the suspension for 20 s and withdrawn at a rate of 120 mm·min⁻¹. These cycles were repeated in each case until the desired catalyst mass was reached (1.16 \pm 0.01 mg·cm⁻²). The plates were dried at 373 K for 2 h.

2.3. Analysis Techniques

Analyses of the crystalline structure were performed by X-ray diffraction (XRD Bruker D8 Advance) with a monochromatized source of Cu K α_1 radiation ($\lambda = 0.15406$ nm) at 1.6 kW (40 kV, 40 mA); samples were prepared by placing a drop of a concentrated ethanol dispersion of particles onto a single-crystal silicon plate. Crystal sizes in the different phases were estimated from line broadening of the corresponding X-ray diffraction peaks using the Scherrer equation. Anatase-rutile fractions were calculated, taking into account the relative diffraction peak intensities of crystalline planes (101) and (111) of anatase and rutile, respectively. The morphology of the samples was studied by transmission electron microscopy (TEM) using a Philips CM 200 instrument operating at 200 kV and a nominal structural resolution of ~0.25 nm. BET surface area, pore volume and pore size measurements were carried out by N₂ adsorption at 77 K using a Micromeritics 2010 instrument. Diffuse reflectance spectra were recorded on a Varian Cary 5 spectrometer equipped with an integrating sphere using PTFE (poly-tetra-fluoroethylene) as a reference to study light absorption properties of the samples [25]. Field emission scanning electron microscopy (FESEM) images were obtained using a Hitachi S-4800 microscope to determine the thickness of the deposit on the plates. Surface characterization by X-ray photoelectron (XPS) was conducted on a SPECS spectrometer, working with a constant pass energy of 40 eV. The spectrometer main chamber was maintained at a pressure of $5-6 \times 10^{-10}$ bar, and the machine was equipped with a PHOIBOS 150 9MCD hemispherical electron analyzer, using Al Kα (hv) 1486.6 eV at 250 W and 12.5 kV. The carbon 1 s signal (284.6 eV) was used as the internal energy reference in all measurements. All photoelectron spectra were analyzed using Casa-XPS software. A Thermo Scientific-Nicolet iS10 spectrophotometer was used for the FTIR studies. The catalyst was placed between two CaF₂ mirrors, and a 4000–1000 cm⁻¹ measurement range, 2 cm⁻¹ resolution and forward/backward mirror speeds of 10 kHz/6.2 kHz, respectively, were used.

2.4. Photoactivity Study

The photoactivity tests were performed as described in previous studies where a scheme of the setup is presented [26]. The 500 ppb concentration of NO was obtained from dilution with the air of a 100 ppm concentration of NO (supplied by Air Liquide). Humidity was added by passing the appropriate amount of dilution air through a thermostatic water bath and was controlled by means of a Rotronic HygroPalm probe. All workflows were controlled with mass flow controllers. The borosilicate glass plates were placed in a nylon reactor with a borosilicate window and a headspace of 0.5 cm. The total workflow was $1.2 \, \mathrm{L\cdot min^{-1}}$ at 1 atm. The light source employed was a $10 \, \mathrm{W\cdot m^{-2}}$ Osram Ultra Vitalux 300 W lamp. For the tests with visible light, a 420 nm Schott cutoff filter was placed between reactor and lamp. The NOx quantification was followed with a Horiba APNA-370 N/S analyzer. The results shown are the average of two tests with a maximum deviation of 5%. In all cases, the system is kept in the dark for 30 min to reach adsorption equilibrium and then the lamp is turned

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on (t = 0). The results are expressed as percentages of [NO] $_{removed}$, [NO2] $_{generated}$ and [NO $_{x}$] $_{removed}$ in accordance with the following equations:

$$NO_{removed} / \% = \frac{\int_0^t ([NO]_o - [NO]_t) dt}{\int_0^t [NO]_o dt} \cdot 100$$
 (1)

$$NO_{2_{\text{generated}}} / \% = \frac{\int_0^t ([NO_2]_t - [NO_2]_o) dt}{\int_0^t [NO]_o dt} \cdot 100$$
 (2)

$$NO_{x_{\text{removed}}} / \% = \frac{\int_{0}^{t} [([NO]_{o} + [NO_{2}]_{o}) - ([NO]_{t} + [NO_{2}]_{t})]dt}{\int_{0}^{t} [NO]_{o}dt} \cdot 100$$
(3)

where $[NO]_o$ and $[NO_2]_o$ are the concentrations are the concentrations at the inlet of the reactor once the adsorption equilibrium has been reached, and $[NO]_t$ and $[NO_2]_t$ are the concentrations at the outlet of the photoreactor at any time under illumination.

3. Results

3.1. Characterization of the Modified Catalysts

Table 1 shows the characterization of the P25 and Pd-modified catalysts. Modification of the P25 photocatalyst through the incorporation of Pd does not result in changes in the crystalline structure of the photocatalyst. The anatase percentage is maintained, and the anatase/rutile crystallite sizes barely vary. The diffractograms can be consulted in Supporting Information. The TiO_2 crystalline phases present in all the catalysts are anatase (A) and rutile (R), identified by the Crystallography Open Database (COD) as COD9015929 and COD9015662, respectively. No presence of metal is observed, as expected for the weight percentage of 0.5% of Pd, an amount which is difficult to detect using X-ray diffraction. Differences are observed in the colors of the Pd-modified photocatalysts (Figure 1). The Pd-P is grayish in color, whereas the Pd-I is more yellowish, indicating the presence of Pd⁰ in the Pd-P [14].

Table 1. Main characteristics of the catalysts.

Catalysts	% Anatase	Crystall	ite Size	Surface Area	Pore Volume (cm ³ ·g ⁻¹)	
		Anatase (nm)	Rutile (nm)	$(m^2 \cdot g^{-1})$		
P25	82.0	23.0	33.0	48.6	0.18	
Pd-P	79.4	21.2	35.4	49.8	0.41	
Pd-I	81.7	18.9	33.1	52.7	0.33	

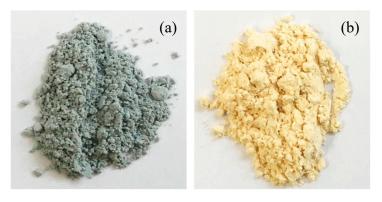


Figure 1. Photocatalysts Pd-P (**a**) and Pd-I (**b**).

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Figure 2a shows the DRS UV-vis for the Pd-modified photocatalysts. Comparing the P25 spectrum with the modified samples, similar behavior is observed with a slight shift from 400 nm to longer wavelengths ("redshift") in the sample order Pd-P > Pd-I > P25. Pd-I has a broad band between 450 and 550 nm centered at 470 nm due to a d-d transition of Pd^{2+} [27], responsible for the yellowish-brown color of the photocatalyst. Pd-P does not display bands characteristic of Pd in the visible range, although its absorbance is higher than for P25 in all the visible range due to its grayish color.

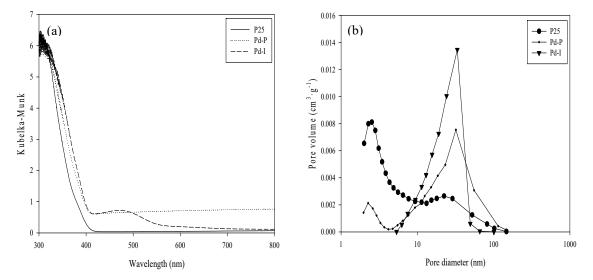


Figure 2. (a) UV-vis diffuse reflectance spectra and (b) Pore volume distribution of the catalysts.

Table 1 shows the surface area values obtained after modification of the P25 with Pd. No significant changes are observed, as also reported by other authors [24]. It is seen that the incorporation of metal particles at these low percentages does not entail any significant change in the surface area of the bare TiO₂ (P25). However, in the pore size distribution represented in Figure 2b, there can be seen an increase of the high interparticle mesoporosity in detriment to the low intraparticle mesoporosity, with this being more noticeable for Pd-I than for Pd-P. This would seem to suggest that the metal deposits have occupied the pores of lesser volume, as has also been observed for other metals such as Pt and Au in previous studies [28,29].

The TEM study enabled the identification of the deposits of Pd particles incorporated on the P25. It can be seen for both samples that the deposits are very small at the nanometer scale (Figure 3).

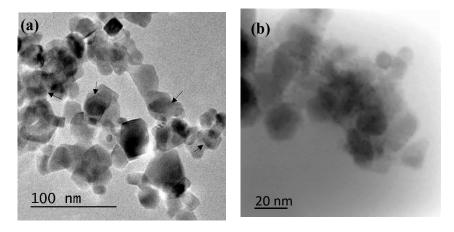


Figure 3. TEM of Pd-modified P25: Pd-P (**a**) and Pd-I (**b**). The latter was obtained using high-angle annular dark-field imaging (HAADF).

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The samples were analyzed by XPS in order to determine the oxidation states of the Pd incorporated on the surface of the titanium oxide. Table 2 shows the energies of the constituent elements of the different catalysts. For all the photocatalysts, the binding energy of the Ti was 458.0 ± 0.5 eV, corresponding to the Ti⁴⁺ signal of the TiO₂ (9). The O signal appears at values close to 529.5 ± 0.5 eV, attributable principally to the oxygen of the crystalline lattice of the TiO₂ [30]. A slight shift in the Ti and O signals was detected with respect to the P25 due to the surface inclusion of the Pd. This has previously been observed with the incorporation of other metals (Pt and Au) onto P25 [31]. The O_{lattice}/Ti ratio remained close to the theoretical value at around 2 in the modified photocatalysts. This indicates that the modification carried out in this work by means of the deposition of palladium particles is only superficial. An analysis of the oxidation state of the Pd can be made from Figure 4.

Catalysts	Binding Energy/eV (Ti)	% at. Ti	Binding Energy/eV (O)	% at. O	Binding Energy/eV Pd	% at. Pd	% wt. Pd	O _{lattice} /Ti
Pd-P	458.01	28.35	529.01	71.53	334.01	0.11	0.37	2.10
Pd-I	458.00	28 38	529.00	71 32	336.00	0.27	1.05	2 20

Table 2. XPS results of the Ti, O and Pd regions for the different modified photocatalysts.

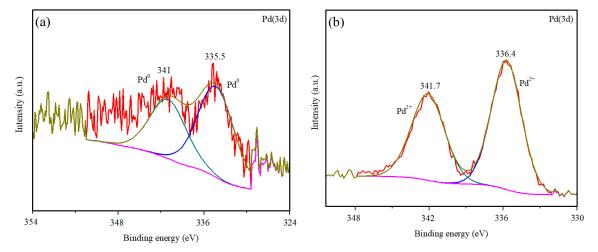


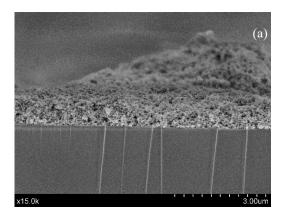
Figure 4. XPS of Pd-modified samples: (a) Pd (3d) of Pd-P and (b) Pd (3d) of Pd-I.

Figure 4a,b show the 3d spectra of the Pd for Pd-P and Pd-I, respectively. For Pd-P, the predominant species is the metallic Pd (335.5 eV ($3d_{5/2}$)) [32]. Despite the small amount of metal in the samples—which makes the peak-background ratio low—a certain asymmetry can be observed due to a shoulder at higher binding energies that could be due to the presence of Pd²⁺, as described in other samples obtained by photodeposition [12,14,21]. For Pd-I, it can be seen that the doublet corresponding to the Pd²⁺ (336.4 eV ($3d_{5/2}$)) is clearly defined, apparently in the form of PdO according to its value [30].

3.2. Characterization of the Deposits

The deposits of 1.16 mg·cm⁻² of P25 with Pd, independently of the modification method, display a continuous profile irregular in thickness, ranging between 198-1690 nm and 150–1437 nm, for Pd-P and Pd-I, respectively (Figure 5). Using ASTM Standard D3330/D3330M, it was determined that the Pd deposits show good adhesion, similar to the unmodified P25 deposit.

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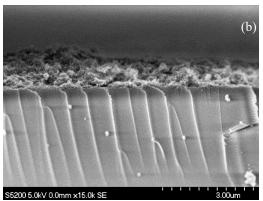


Figure 5. Deposit of 1.16 mg·cm⁻² of Pd-P (**a**) and Pd-I (**b**).

3.3. Comparison of Oxidation of the NO_x

Table 3 shows the photoactivity results obtained according to [NO] $_{removed}$, [NO2] $_{generated}$ and [NO $_{x}$] $_{removed}$ for Pd-P, Pd-I and P25 for comparison purposes. Reactivity was tested with different degrees of humidity. The test profiles are shown in Figure 6.

It can be observed from Table 3 that the presence of Pd entails an enhancement in NO_x removal both in the absence and presence of humidity. The percentage of removed NO remains practically unaltered for all the photocatalysts, independently of the relative humidity being tested. With respect to the generated NO_2 , it can be seen that, in general, as the humidity increases, more NO_2 is generated.

Longer studies of up to 24 h duration were undertaken of UV-vis irradiation under more adverse conditions of 65% RH (Figure 7a,c,e) in order to evaluate the capacity for NOx elimination of the catalysts before the occurrence of surface saturation by HNO_3 [33]. It was found that both Pd-I and Pd-P have a superior NOx removal capacity than that of P25. The P25 had a removal rate of 26% against the 35% of Pd-I and the 37% de Pd-P.

In the following subsection, an in-depth analysis is made using infrared spectroscopy studies of the effect of the presence of Pd on the changes in the reactivity of the P25.

Table 3. Percentages of NO removed, NO_2 generated, and NO_x removed for each of the tested photocatalyst samples for 5 h of UV-vis irradiation. RH stands for relative humidity.

	NO Removed (%)	NO ₂ Generated (%)	NO _x Removed (%)		NO Removed (%)	NO ₂ Generated (%)	NO _x Removed (%)
Pd-P 0% RH	96.23	1.17	95.06	Pd-I 0% RH	97.05	0.00	97.05
Pd-P 25% RH	95.04	3.61	91.43	Pd-I 25% RH	95.05	17.77	77.28
Pd-P 40% RH	89.69	20.74	68.95	Pd-I 40% RH	93.90	38.40	55.50
Pd-P 65% RH	91.27	21.19	70.08	Pd-I 65% RH	95.01	34.54	60.47
P25 0% RH	90.73	16.29	74.44	P25 65% RH	87.16	46.50	40.65

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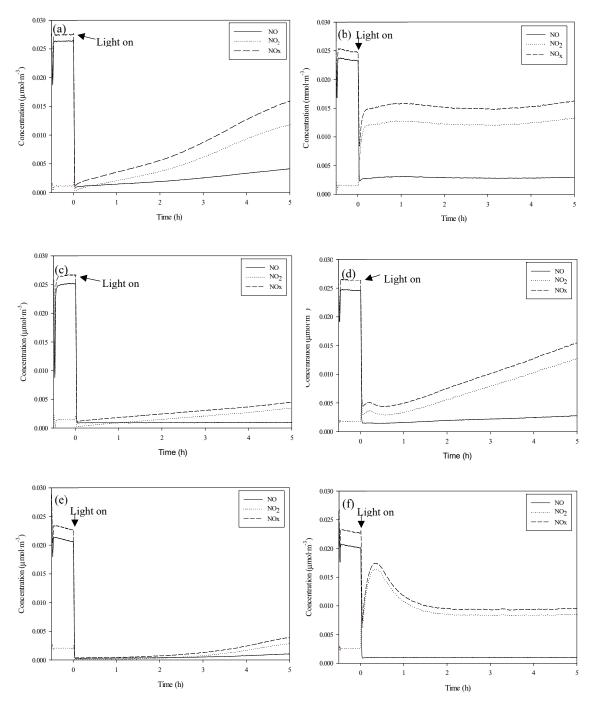


Figure 6. Evolution of species for P25 0% RH (**a**), P25 65% RH (**b**), Pd-P 0% RH (**c**), Pd-P 65% RH (**d**), Pd-I 0% RH (**e**) and Pd-I 65% RH (**f**).

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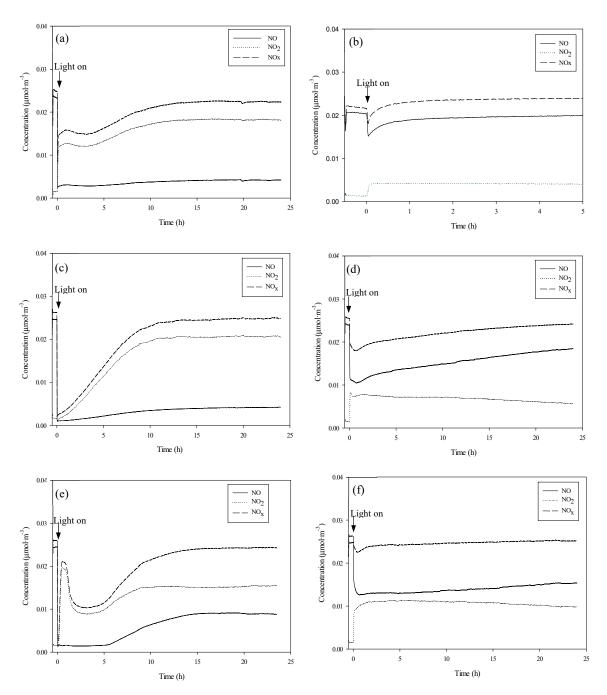


Figure 7. Evolution of species (65% RH): P25 UV-vis (a), P25 Vis (b), Pd-P UV-vis (c), Pd-P Vis (d), Pd-I UV-vis (e) and Pd-I Vis (f).

3.3.1. Influence of the Presence of Water on the Catalyst Surface on the Oxidation Mechanism

Figure 8 shows the spectra obtained of the surface of the P25, P25-P and P25-I catalysts after the NO elimination studies. The spectra obtained with the P25-P and P25-I catalysts are practically the same, with bands centered at 1615, 1585, 1490, 1289 and 1250 cm $^{-1}$. The P25-P spectrum additionally presents a shoulder over 1450 cm $^{-1}$. The P25 spectrum presents a band at 1620 cm $^{-1}$ with a shoulder at 1615 cm $^{-1}$ and bands at 1585, 1423 and 1309 cm $^{-1}$. These catalysts were left without illumination in an air atmosphere, and the progressive evolution of the bands observed initially was observed (Figure 8b–d). It could be seen in all cases that the initial bands progressively decreased at the same time as two new bands formed centered around 1416–1425 and 1330–1340 cm $^{-1}$.

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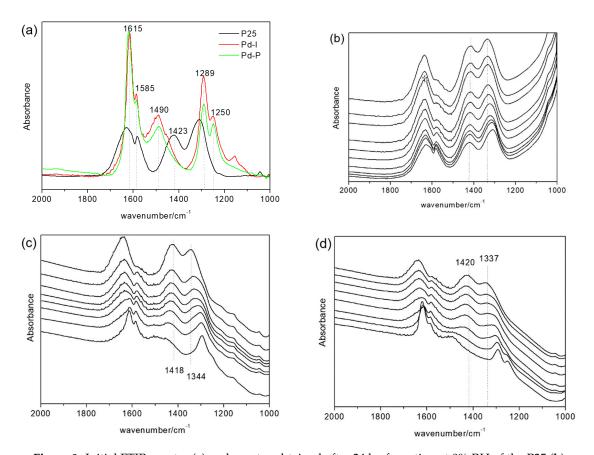


Figure 8. Initial FTIR spectra (**a**) and spectra obtained after 24 h of reaction at 0% RH of the P25 (**b**), Pd-P (**c**) and Pd-I (**d**).

The bands that can be seen in the P25-P and P25-I at 1490 and 1289 cm $^{-1}$ are attributed to nitro-chelates [34], while those observed at 1615, 1585 and 1250 cm $^{-1}$ can be attributed to adsorbed NO₂ [35,36]. The bands generated after concluding the test, centered around 1416–1425 and 1330–1340 cm $^{-1}$, are attributed to solvated nitrates [37]. The analysis of these spectra suggests that, in the P25, after the NO elimination studies, the surface is saturated with solvated nitrates and, to a lesser extent, with nitro-chelates and adsorbed NO₂. In contrast, in the catalysts with Pd, the surface is only saturated with nitro-chelates and adsorbed NO₂.

The reaction of the NO with oxygen surface ions gives rise to nitrites (4), and the reaction of nitrites with oxygen surface ions gives rise to NO_2 (5). Therefore, the nitrocompounds and the adsorbed NO_2 observed in the FTIR studies (Figure 8) are generated from the reactions. Ruggeri et al. [38] described how the reaction between nitrites and NO_2 to give nitrates, and NO_2 constitutes an equilibrium (6). Hence, during the NO_2 elimination studies in the catalysts with PO_2 , the reaction expressed in (6) does not take place until the catalysts are left in an air atmosphere, and the NO_2 concentration decreases. However, in the case of the PO_2 , the formation of nitrates is favored through another mechanism in which surface hydration of the catalyst is influential. This will be discussed below.

Of the catalyst is influential. This will be discussed below.
$$O_{br}^{-}(ads) + NO_{(ads)} \rightarrow NO_{2(ads)}^{-} +$$
Oxygen Vacancy

(4)

$$NO_{2(ads)}^{-} + O_{br(ads)}^{--} \rightarrow NO_{2(ads)} + O_{br}^{--}$$
 (5)

$$NO_{2(ads)} + NO_{2(ads)}^{-} \rightleftharpoons NO_{3(ads)}^{-} + NO_{(ads)}$$

$$(6)$$

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The FTIR spectra of the catalysts after 15 h of NO elimination at 65% RH are shown in Figure 9a). Bands are mainly observed centered at 1416 and 1330 cm⁻¹ attributed to solvated nitrates. These bands were more intense in the catalysts with Pd.

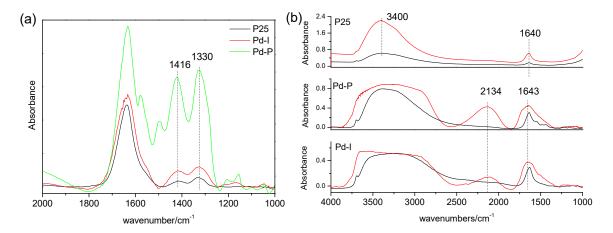


Figure 9. (a) FTIR spectra obtained after 15 h of the reaction of NO elimination at 65% RH. (b) FTIR spectra of the catalysts (black) and the catalysts subjected to a pure airflow at 65% RH (red).

In the presence of humidity, the NO₂ can be disproportionated through the following reaction:

$$2NO_{2(ads)} + H_2O_{(ads)} \rightarrow HONO_{(ads)} + HNO_{3(ads)}$$
(7)

It has been reported that the disproportionation of NO_2 with water requires the formation of a prior isomer [39]. The formation of this isomer and the subsequent disproportionation of NO_2 can be conditioned by the characteristics of the adsorbed water. Figure 9b shows the spectra of the catalysts and their spectra after subjecting them to a pure airflow at 65% RH. The P25 spectrum is represented by an intense band at 3400 cm⁻¹ and another at 1620 cm⁻¹ attributed to the stretching and bending modes of adsorbed water, respectively [40]. In contrast, in the catalysts with Pd, the spectrum is dominated by a broad band between 3600 and 2900 cm⁻¹, another at 2134 cm⁻¹ and a third at 1643 cm⁻¹, which are typical of liquid water. That is, the adsorption of water in these catalysts seems to be less intense than in the P25. The intense interaction of water in the P25 appears to favor the disproportionation of NO_2 through reaction (4).

These results are in agreement with those of previous studies made by our research team [41] in which it was found that the NO_2 is not photocatalytically degraded but rather adsorbed and disproportionated on the surface of the TiO_2 .

In short, the absence of high surface hydration favors the formation of nitro-chelates and the adsorption of NO_2 in the catalysts with Pd. This explains the greater eliminating capacity of this compound with the Pd-modified catalysts.

3.3.2. Influence of Palladium Oxidation State

The differences with respect to the Pd-I and Pd-P series of photocatalysts come from the amount of generated NO_2 . The increase of NO_2 generated with humidity is greater for the Pd-I series. This means that, in 5 h, NO_x removal is lower for Pd-I. Hence, in the absence of humidity, Pd-I and Pd-P function practically the same, but in the presence of humidity, the Pd-P series has greater photocatalytic efficiency. Although it was found for 65% RH that they have the same overall NOx removal capacity, the oxidation kinetics are faster for the Pd-P series (Figure 7c,e). Even though palladium deposition by photodeposition was less efficient (Table 2), the activity results of the P25-P series are better.

According to Sheng et al. [24], during irradiation, the formation of Pd⁴⁺ species takes place (8 and 9). The formation of these species is favored by the presence of humidity from the oxidation

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of Pd^{2+} . The formation of these species and the consequences for the adsorption of NO_x species may explain the changes in growth and decay in the NO_2 profile that takes place in the first hour of irradiation for the catalysts of the Pd-I series, which are the catalysts which have a higher amount of oxidized palladium (Figure 6f).

$$Pd^{2+} + 2HO_{ads}^{\cdot} \to Pd^{4+} + 2OH^{-}$$
 (8)

$$3Pd^{2+} + 2O_{2,ads}^{-} + 4H_2O \rightarrow 3Pd^{4+} + 8OH^{-}$$
 (9)

In order to clarify the results and the different evolution in the NO_x oxidation kinetics in Pd-I and Pd-P, an XPS analysis was undertaken of the evolution of the Pd-I sample for different test times of 5 h and 24 h (Figure 10a).

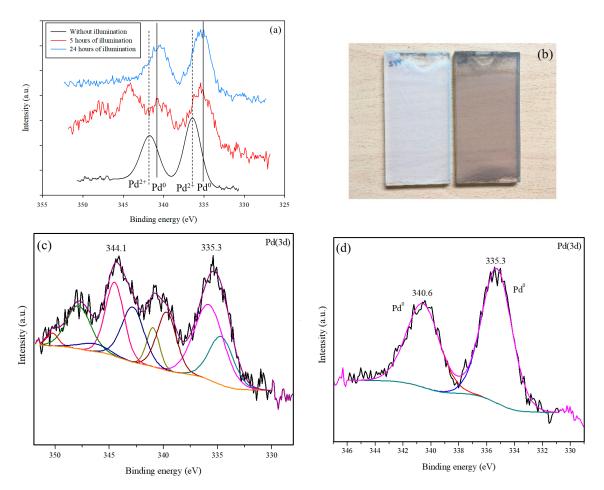


Figure 10. XPS spectra corresponding to the 3d region of the Pd-I: comparison at different exposure times (**a**) and deconvolution at 5 h (**c**) and 24 h of illumination (**d**). Appearance of the coatings of initial Pd-I and Pd-I after 24 h (**b**).

No appreciable differences were observed in the Ti and O signals compared to the initial sample. Figure 10c,d shows the deconvoluted Pd signals at 5 h and 24 h. A shift can be observed of the doublets corresponding to the Pd with the test time to lower binding energies (from 336.4 to 335.5 eV and from 341.7 to 340.6 eV). This corresponds to the reduction from Pd^{2+} to Pd^{0} . Figure 10b shows the initial deposit of Pd-I and after 24 h of radiation. A variation in color can be observed due to the majority appearance of Pd^{0} (grayish color). For Pd-I at 5 h, Pd presents a quite complex set of peaks, which indicates more species than Pd^{0} and PdO, which may be due to the Pd^{4+} (R5 and R6).

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Table 4 shows removed NO, generated NO_2 and removed NO_x for various cycles of photoactivity with intermediate washes for Pd-I. Enhancement of the activity after each radiation cycle is confirmed as the Pd is reduced. In the second cycle, similar values to those of the Pd-P sample are obtained, and in the third cycle, the results are even bettered as the Pd-P sample also initially contained some oxidized Pd.

Table 4. Percentages of NO removed, NO₂ generated, and NO_x removed for 4 reuse cycles of Pd-I and 5 h of UV-vis irradiation.

NO Removed (%)	NO ₂ Generated (%)	NO _x Removed (%)
95.01	34.54	60.47
92.18	20.53	71.65
92.33	9.18	83.14
94.16	8.11	86.05
	95.01 92.18 92.33	95.01 34.54 92.18 20.53 92.33 9.18

Activity was also tested with Vis radiation (Figure 7b,d,f). It can be seen that the incorporation of the metal improves P25 efficiency, especially for Pd-P with which more NO_x is removed and less NO_2 generated. Activity in the visible is attributable to the presence of Pd^{2+} and Pd^0 on the surface of the modified photocatalysts. Under visible radiation, the presence of Pd^0 gives rise to energy transitions between the TiO_2 valence band and localized energy levels due to metal clusters [42,43]. In addition, the PdO band gap, presumably formed in Pd-I, is low, at 0.8 eV [44], which could act as a Vis-photosensitizer [45].

4. Conclusions

The presence of Pd on the TiO_2 surface improves NO_x removal. This improvement appears to be related to the presence of Pd, giving rise to a different interaction of the water with the TiO_2 surface.

It is shown, as also indicated in previous studies, that NO_2 is not photocatalytically degraded but rather is adsorbed and disproportionated on the TiO_2 surface. In the present work, it was found that in the catalysts with Pd, the NO_2^- and NO_2 generated from the photocatalytic oxidation of the NO in the absence of humidity are adsorbed on the surface of the catalyst, and there is no disproportionation to give nitrates until the NO is eliminated from the reaction medium. However, in the P25, there is some NO_2 disproportionation due to the high surface hydration of the catalyst and less NO_2 adsorption.

The photodeposition method produces a higher quantity of Pd⁰ than impregnation. It seems to be that the Pd⁰ form is beneficial for the activity of the catalyst under both ultraviolet and visible radiation.

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