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Excess enthalpies of 72 binary liquid mixtures of methyl n-alkanoates (C4 - C16) + alkan-1-ols (C2 - C10) at 298.15 K

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Enthalpy-of-mixing measurements HE are reported at 298.15 K for 72 binary mixtures formed by eight methyl nalkanoates (propanoate, butanoate, pentanoate, heptanoate, nonanoate, undecanoate, tridecanoate, and pentadecanoate) with nine alkan-1-ols (ethanol through decan-1-ol). All the mixtures are endothermic with a regular increase of H^E as the chain length of the alkan-1ol increases, except the methyl nonanoate + butan-1-ol mixture. On the contrary, HE regulary decreases with the chain length of the methyl n-alkanoates, except for methyl butanoate + ethanol, + propan-1-ol, or + butan-1-ol. These exceptions are observed also in the variation of the molar excess volumes with the chain length of the molecules.

1. INTRODUCTION

In continuation of our systematic experimental studies on the excess molar enthalpies H^{E} of mixtures containing methyl n-alkanoates and n-alkanes [GONE0931], we present here measurements at 298.15 K for 72 binary mixtures formed by eight methyl nalkanoates (propanoate, butanoate, pentanoate, heptanoate, nonanoate, undecanoate, tridecanoate, and pentadecanoate) with nine alkan-1-ols (ethanol through decan-1-ol). The purpose of this investigation is to examine the effect of the chain length of each of the two linear molecules on the properties of the mixtures.

Several workers have reported H^{E} data for mixtures containing methyl ethanoate + alkan-1-ols [BENM1890];[GROJ1710];[NAGI0703];[NAGI0720]; see also [SINP0830]). In the literature we have found only a few H^{E} data for mixtures containing higher alkanoates + alkan-1-ols, all at 298.15 K: methyl propanoate + propan-1-ol [FERJ1850], + butan-1-ol, + hexan-1-ol, or + decan-1-ol [FERJ1830], methyl butanoate + propan-1-ol [FERJ1850], + butan-1-ol, + pentan-1-ol, + hexan-1-ol, heptan-1-ol, + octan-1-ol, + nonan-1-ol, or + decan-1-ol [FERJ1851], and methyl pentanoate + butan-1-ol, + hexan-1-ol, + octan-1-ol, or + decan-1-ol [FERJ1830].

2. EXPERIMENTAL SECTION

2.1. Apparatus and Procedure

The experimental data were taken at atmospheric pressure by means of a Calvet type microcalorimeter, model MS-80D (SETARAM, Lyon, France) with a stainless steel batch mixing cell (volume ca. 8 cm³) and with negligible vapor phase described in [ORTJ0921]. The temperature T was maintained constant to within 0.02 K at (298.15 \pm 0.02) K. All temperatures are on ITS-90. The microcalorimeter was calibrated electrically after each measurement (see [ORTJ0921]). Check measurements on cyclohexane + hexane and benzene + heptadecane are in agreement to within 1 % (over central range of concentration) with the data reported in [MCGM0690] and [DIAM0742]. The estimated uncertainties in the mole fraction composition x_i and $H^{\rm E}$ are, respectively, $\sigma(x_i) = 0.0005$ and $\sigma(H^E) = 0.02 |H^E|$ (over central range of concentration).

2.2. Materials

C₂H₆O, Ethanol (Ethyl alcohol). Fluka AG (Buchs, Switzerland) "puriss p. a." grade material of stated purity > 99.8 mole % degassed ultrasonically, dried over molecular sieves Type 3A (reference 69828, from Fluka), and used without further purification. n(D,298.15 K) = 1.3594; $\rho_i(298.15 \text{ K})/\text{kg m}^{-3} = 784.94$.

C₃H₈O, Propan-1-ol (Propyl alcohol). Fluka AG (Buchs, Switzerland) "puriss p. a." grade material of stated purity > 99.5 mole % purified as above. $n(D,298.15 \text{ K}) = 1.3833; \rho_i(298.15 \text{ K})/\text{kg m}^{-3} = 799.54.$

C₄H₈O₂, Methyl propanoate (Methyl propionate). Fluka AG (Buchs, Switzerland) "purum" grade material of stated GLC purity > 99.0 mole %, purified as above; n(D, 293.15 K) = 1.3745; $\rho_i(298.15 \text{ K})/\text{kg m}^{-3} = 909.30$.

C₄H₁₀O, Butan-1-ol (Butyl alcohol). Fluka AG (Buchs, Switzerland) "puriss p. a." grade material of stated purity > 99.5 mole % purified as above. $n(D,298.15 \text{ K}) = 1.3974; \rho_i(298.15 \text{ K})/\text{kg m}^{-3} = 805.93.$

C₅H₁₀O₂, Methyl butanoate (Methyl butyrate). Fluka AG (Buchs, Switzerland) "purum" grade material of stated GLC purity > 99.0 mole %, purified as above; n(D, 293.15 K) = 1.3849; $\rho_i(298.15 \text{ K})/\text{kg m}^{-3} = 892.31$.

C5H12O, Pentan-1-ol (Amyl alcohol). Fluka AG

(Buchs, Switzerland) "puriss p. a." grade material of stated purity > 99.0 mole % purified as above. $n(D,298.15 \text{ K}) = 1.4077; \rho_i(298.15 \text{ K})/\text{kg m}^{-3} = 810.40.$

C₆H₁₂O₂, Methyl pentanoate (Methyl valerate). Fluka AG (Buchs, Switzerland) "purum" grade material of stated GLC purity > 99.0 mole %, purified as above; n(D, 293.15 K) = 1.3947; $\rho_i(298.15 \text{ K})/\text{kg m}^{-3} = 884.52$.

C₆H₁₄O, Hexan-1-ol (Hexyl alcohol). Fluka AG (Buchs, Switzerland) "puriss" grade material of stated purity > 99.0 mole % purified as above. n(D,298.15 K) = 1.4160; $\rho_i(298.15 \text{ K})/\text{kg m}^{-3}$ = 815.26.

C₇H₁₆O, Heptan-1-ol (Heptyl alcohol). Fluka AG (Buchs, Switzerland) "puriss p. a." grade material of stated purity > 99.5 mole % purified as above. $n(D,298.15 \text{ K}) = 1.4223; \rho_i(298.15 \text{ K})/\text{kg m}^{-3} = 818.71.$

C₈H₁₆O₂, Methyl heptanoate (Methyl enanthate). Fluka AG (Buchs, Switzerland) "puriss" grade material of stated GLC purity > 99.0 mole %, purified as above; n(D, 293.15 K) = 1.4095; $\rho_i(298.15 \text{ K})/\text{kg m}^{-3} = 875.40$.

C₈H₁₈O, Octan-1-ol (Octyl alcohol). Fluka AG (Buchs, Switzerland) "puriss p. a." grade material of stated purity > 99.5 mole % purified as above. $n(D,298.15 \text{ K}) = 1.4270; \rho_i(298.15 \text{ K})/\text{kg m}^{-3} = 821.67.$

C₉**H**₂₀**O**, **Nonan-1-ol** (Nonyl alcohol). Fluka AG (Buchs, Switzerland) "purum" grade material of stated purity > 98.0 mole % purified as above. n(D,298.15 K) = 1.4315; $\rho_i(298.15 \text{ K})/\text{kg m}^{-3} = 824.78$.

C₁₀H₂₀O₂, Methyl nonanoate (Methyl pelargonate). Fluka AG (Buchs, Switzerland) "puriss" grade material of stated GLC purity > 99.0 mole %, purified as above; n(D, 293.15 K) = 1.4208; $\rho_i(298.15 \text{ K})/\text{kg m}^{-3} = 870.11$.

C₁₀H₂₂O, Decan-1-ol (Decyl alcohol). Fluka AG (Buchs, Switzerland) "puriss" grade material of stated purity > 99.0 mole % purified as above. n(D,298.15 K) = 1.4349; $\rho_i(298.15 \text{ K})/\text{kg m}^{-3}$ = 826.42.

C₁₂H₂₄O₂, Methyl undecanoate. Fluka AG (Buchs, Switzerland) "puriss" grade material of stated GLC purity > 98.0 mole %, purified as above; n(D, 293.15 K)= 1.4270; $\rho_i(298.15 \text{ K})/\text{kg m}^{-3} = 866.75$.

C₁₄H₂₈O₂, Methyl tridecanoate. Fluka AG (Buchs, Switzerland) "puriss" grade material of stated GLC purity > 98.0 mole %, purified as above; n(D, 293.15 K)= 1.4329; $\rho_i(298.15 \text{ K})/\text{kg m}^{-3}$ = 863.94.

C₁₆H₃₂O₂, Methyl pentadecanoate. Fluka AG (Buchs, Switzerland) 'puriss' grade material of stated GLC purity > 99.0 mole %, purified as above; n(D, 293.15 K) = 1.4370; $\rho_i(298.15 \text{ K})/\text{kg m}^{-3} = 862.35$.

3. RESULTS

The direct experimental $H^{\rm E}$ values of 48 systems (the alkanoates + ethanol, + propan-1-ol, + butan-1-ol, + hexan-1-ol, + octan-1-ol, and + decan-1-ol), are tabulated and graphed in the Appendix and all are saved on disk as Standard ELDATA Files **ORTJ0954.001** through **ORTJ0954.072**.

The data were fitted to Eq. (1):

$$H^{E}_{calo}/J \text{ mol}^{-1} = x_1 x_2 \Sigma A_i [x_1/(x_1 + k x_2)]^{i-1}$$
(1)

all points weighted equally. With an adjusted coefficient k and n = 4 coefficients A_i the standard deviations $\sigma(H^E)$, defined by Eq.(2):

$$\sigma(H^{\rm E}) = [\Sigma(H^{\rm E}_{\rm calc} - H^{\rm E})^2 / (N - n)]^{1/2}$$
(2)

where N is the number of experimental values, are less than 10 J mol⁻¹ (ca. 0.4 % at $x_1 = 0.5$).

4. DISCUSSION AND CONCLUSIONS

All the mixtures are endothermic with a regular increase of H^E as the chain length of the alkan-1-ol increases, except the methyl nonanoate + butan-1-ol mixture. On the contrary, H^E regulary decreases with the chain length of the methyl n-alkanoates, except for methyl butanoate + ethanol, + propan-1-ol, and + butan-1-ol. These exceptions are observed also in the variation of the molar excess volumes with the chain length of the molecules.

Our measurements are in rather poor agreement with the data reported by Fernandez et al. At equimolar composition our data are in general up to 5% higher than in [FERJ1830]. The mean deviations for all points range from 9 to 15% compared to [FERJ1850] and [FERJ1851].

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Copyright© 1995	[HMSD1000] H	EAT OF MIXIN	G AND SOLUTI	ON ORTJ0954.00
State:	Two-component	system, single-pl	ase liquid or two-	phase liquid-liquid (LL)
	Pure component	1, liquid		
	Pure component			
Parameters:	[P1] <i>T/</i> K,	Temperature		
Variables:	[X1] $x_{1/-}$,	Mole fraction	of component 1	
Method:	Direct low-press	Molar excess oure calorimetric	enthalpy measurement of H	T^{E} at variable x_{1} and constant T
Components:	1. C ₂ H ₆ O, Etha 2. C ₄ H ₈ O ₂ , Me			
[P1] = .29	8150E+03			[Y1]
[X1]	[Y1]			
.963000E-01	.479400E+03			○ [P1] = .298150E+03
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.280000E+00				
.358400E+00				00
.431300E+00 .497200E+00				.113E+04
.553900E+00	.124050E+04			
.603000E+00				à à
.644700E+00	.112220E+04			
.689800E+00				.750E+03
.734800E+00	.954700E+03			0
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	[HMSD1000] HE Two-component	EAT OF MIXING system, single-ph	G AND SOLUTIO	ON ORTJ0954.010 ORTJ0954.010
Property Code:	[HMSD1000] HE Two-component Pure component	EAT OF MIXINO system, single-ph 1, liquid	G AND SOLUTIO	
Property Code: State: Parameters:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K,	EAT OF MIXIN(system, single-ph 1, liquid 2, liquid Temperature	3 AND SOLUTIC ase liquid or two-p	
Property Code:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$,	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction	G AND SOLUTIO ase liquid or two-p of component 1	
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Property Code: State: Parameters: Variables: Method: Components:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C2H6O, Etha	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e are calorimetric n nol	G AND SOLUTIC ase liquid or two-p of component 1 anthalpy	
Property Code: State: Parameters: /ariables: Method: Components:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₂ H ₆ O, Ethan 2. C ₅ H ₁₀ O ₂ , Me	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e are calorimetric n nol	G AND SOLUTIC ase liquid or two-p of component 1 anthalpy	E at variable x_1 and constant T
Property Code: State: Parameters: Variables: Aethod: Components: [P1] = .298	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C_2H_6O , Ethan 2. $C_5H_{10}O_2$, Ma 150E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e are calorimetric n nol	G AND SOLUTIC ase liquid or two-p of component 1 anthalpy	The base liquid-liquid (LL) E at variable x_1 and constant T [Y1]
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Property Code: State: Parameters: /ariables: //ariabl	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₂ H ₆ O, Ethan 2. C ₅ H ₁₀ O ₂ , Me 150E+03 [Y1] .491700E+03 .827900E+03 .827900E+03 .104940E+04 .118520E+04 .113040E+04 .106790E+04 .997300E+03 .904400E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e are calorimetric n nol	G AND SOLUTIC ase liquid or two-p of component 1 anthalpy	E at variable x_1 and constant T [Y1] .160E+04 \circ [P1] = .298150E+03 .120E+04
Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₂ H ₆ O, Ethan 2. C ₅ H ₁₀ O ₂ , Me 150E+03 [Y1] .491700E+03 .827900E+03 .104940E+04 .116850E+04 .118520E+04 .118520E+04 .118520E+04 .1106790E+04 .997300E+03 .904400E+03 .804400E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e are calorimetric n nol	G AND SOLUTIC ase liquid or two-p of component 1 anthalpy	E at variable x_1 and constant T [Y1] .160E+04 \circ [P1] = .298150E+03 .120E+04 .800E+03
Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₂ H ₆ O, Ethan 2. C ₅ H ₁₀ O ₂ , Ma 150E+03 [Y1] .491700E+03 .827900E+03 .827900E+03 .104940E+04 .118520E+04 .118520E+04 .118520E+04 .118520E+04 .118520E+04 .106790E+03 .904400E+03 .804400E+03 .688100E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e are calorimetric n nol	G AND SOLUTIC ase liquid or two-p of component 1 anthalpy	E at variable x_1 and constant T [Y1] .160E+04 \circ [P1] = .298150E+03 .120E+04 .800E+03
Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C_2H_6O , Ethan 2. $C_5H_{10}O_2$, Mac 150E+03 [Y1] .491700E+03 .827900E+03 .827900E+03 .104940E+04 .116850E+04 .118520E+04 .113040E+04 .113040E+04 .106790E+03 .904400E+03 .804400E+03 .668100E+03 .560300E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e are calorimetric n nol	G AND SOLUTIC ase liquid or two-p of component 1 anthalpy	E at variable x_1 and constant T [Y1] .160E+04 \circ [P1] = .298150E+03 .120E+04 .800E+03
Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C_2H_6O , Ethan 2. $C_5H_{10}O_2$, Mac 150E+03 [Y1] .491700E+03 .827900E+03 .104940E+04 .116850E+04 .116850E+04 .118520E+04 .113040E+04 .106790E+04 .997300E+03 .904400E+03 .804400E+03 .668100E+03 .560300E+03 .423400E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e are calorimetric n nol	G AND SOLUTIC ase liquid or two-p of component 1 anthalpy	E at variable x_1 and constant T [Y1] .160E+04 \circ [P1] = .298150E+03 .120E+04 .800E+03 \circ \circ \circ \circ \circ \circ \circ \circ \circ \circ
Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C_2H_6O , Ethan 2. $C_5H_{10}O_2$, Mac 150E+03 [Y1] .491700E+03 .827900E+03 .827900E+03 .104940E+04 .116850E+04 .118520E+04 .113040E+04 .113040E+04 .106790E+03 .904400E+03 .804400E+03 .668100E+03 .560300E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e are calorimetric n nol	G AND SOLUTIC ase liquid or two-p of component 1 anthalpy	E at variable x_1 and constant T [Y1] .160E+04 \circ [P1] = .298150E+03 .120E+04 .800E+03 \circ \circ \circ \circ \circ \circ \circ \circ \circ \circ
Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C_2H_6O , Ethan 2. $C_5H_{10}O_2$, Me 150E+03 [Y1] .491700E+03 .827900E+03 .104940E+04 .120450E+04 .120450E+04 .113040E+04 .106790E+04 .106790E+04 .997300E+03 .804400E+03 .668100E+03 .560300E+03 .276300E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e are calorimetric n nol	G AND SOLUTIC ase liquid or two-p of component 1 anthalpy	E at variable x_1 and constant T [Y1] .160E+04 \circ [P1] = .298150E+03 .120E+04 .800E+03 \circ \circ \circ \circ \circ \circ \circ \circ \circ \circ
Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C_2H_6O , Ethan 2. $C_5H_{10}O_2$, Me 150E+03 [Y1] .491700E+03 .827900E+03 .104940E+04 .120450E+04 .120450E+04 .113040E+04 .106790E+04 .106790E+04 .997300E+03 .804400E+03 .668100E+03 .560300E+03 .276300E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e are calorimetric n nol	G AND SOLUTIC ase liquid or two-p of component 1 anthalpy	E at variable x_1 and constant T [Y1] .160E+04 .120E+04 .800E+03 .800E+03 .800E+03
Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C_2H_6O , Ethan 2. $C_5H_{10}O_2$, Me 150E+03 [Y1] .491700E+03 .827900E+03 .104940E+04 .120450E+04 .120450E+04 .113040E+04 .106790E+04 .106790E+04 .997300E+03 .804400E+03 .668100E+03 .560300E+03 .276300E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e are calorimetric n nol	G AND SOLUTIC ase liquid or two-p of component 1 anthalpy	E at variable x_1 and constant T [Y1] .160E+04 .120E+04 .800E+03 .400E+03
Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C_2H_6O , Ethan 2. $C_5H_{10}O_2$, Me 150E+03 [Y1] .491700E+03 .827900E+03 .104940E+04 .120450E+04 .120450E+04 .113040E+04 .106790E+04 .106790E+04 .997300E+03 .804400E+03 .668100E+03 .560300E+03 .276300E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e are calorimetric n nol	G AND SOLUTIC ase liquid or two-p of component 1 anthalpy	E at variable x_1 and constant T [Y1] .160E+04 \circ [P1] = .298150E+03 .120E+04 .800E+03 \circ \circ \circ \circ \circ \circ \circ \circ \circ \circ
Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C_2H_6O , Ethan 2. $C_5H_{10}O_2$, Me 150E+03 [Y1] .491700E+03 .827900E+03 .104940E+04 .120450E+04 .120450E+04 .113040E+04 .106790E+04 .106790E+04 .997300E+03 .804400E+03 .668100E+03 .560300E+03 .276300E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e are calorimetric n nol	G AND SOLUTIC ase liquid or two-p of component 1 anthalpy	$E \text{ at variable } x_1 \text{ and constant } T$ $[Y1] \\ .160E+04 \\ \circ [P1] = .298150E+03 \\ .120E+04 \\ .800E+03 \\ .400E+03 \\ .000E+00 \\ $
Property Code: itate: Parameters: fariables: fethod: components: [P1] = .298 [X1] .105900E+00 .211600E+00 .307000E+00 .307000E+00 .30700E+00 .603400E+00 .647800E+00 .647800E+00 .811900E+00 .854500E+00 .894900E+00 .934000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C_2H_6O , Ethan 2. $C_5H_{10}O_2$, Me 150E+03 [Y1] .491700E+03 .827900E+03 .104940E+04 .120450E+04 .120450E+04 .113040E+04 .106790E+04 .106790E+04 .997300E+03 .804400E+03 .668100E+03 .560300E+03 .276300E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e are calorimetric n nol	G AND SOLUTIC ase liquid or two-p of component 1 anthalpy	$E \text{ at variable } x_1 \text{ and constant } T$ $\begin{bmatrix} [Y1] \\ .160E+04 \\ 0 \text{ [P1]} = .298150E+03 \\ .120E+04 \\ .800E+03 \\ .400E+03 \\ .000E+00 \\ .50E+00 \end{bmatrix}$
roperty Code: tate: arameters: ariables: fethod: omponents: [P1] = .298 [X1] .105900E+00 .211600E+00 .307000E+00 .307000E+00 .393300E+00 .603400E+00 .647800E+00 .647800E+00 .811900E+00 .811900E+00 .811900E+00 .84500E+00 .894900E+00 .894900E+00 .934000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C_2H_6O , Ethan 2. $C_5H_{10}O_2$, Me 150E+03 [Y1] .491700E+03 .827900E+03 .104940E+04 .120450E+04 .120450E+04 .113040E+04 .106790E+04 .106790E+04 .997300E+03 .804400E+03 .668100E+03 .560300E+03 .276300E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e are calorimetric n nol	G AND SOLUTIC ase liquid or two-p of component 1 anthalpy	$E \text{ at variable } x_1 \text{ and constant } T$ $[Y1] \\ .160E+04 \\ \circ [P1] = .298150E+03 \\ .120E+04 \\ .800E+03 \\ .400E+03 \\ .000E+00 \\ $

	LDATA SARL Fran [HMSD1000] HE			T	ORTJ0954.019
State:			se liquid or two-ph		
	Pure component 1	l, liquid		iquia_iiqui	- ()
	Pure component 2	2, liquid			
Parameters:	[P1] <i>T/</i> K,	Temperature Mole fraction of	foomnoment 1		
Variables:	[X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$,	Mole fraction o	t component 1		
Method:	Direct low-pressu	re calorimetric m	easurement of H ^E	at variable x1 a	and constant T
Components:	1. C ₂ H ₆ O, Etha	nol			
[P1] = .298	2. C ₆ H ₁₂ O ₂ , Me	thyl pentanoate	Т		· · · · · · · · · · · · · · · · · · ·
[X1]	[Y1]			[Y1]	
		t to a transmission		.160E+04	
.121400E+00 .237500E+00	.591900E+03 .930600E+03	a stantin en New			\circ [P1] = .298150E+03
.341100E+00	.115760E+04				
.432100E+00	.124990E+04				
.509300E+00	.125520E+04			.120E+04	
.573600E+00 .627700E+00	.121190E+04 .114570E+04				, o o
.670600E+00					~ ~
.706400E+00	.990000E+03				
.747200E+00				.800E+03	•
.786800E+00 .827700E+00				.80012+03	
.867100E+00					o
.904900E+00					¢ A
.940200E+00					
.972700E+00	.129900E+03			.400E+03	-/ ò -
				.000E+00	
			¥ .*		.50E+00
					[X1]
L					
Convright© 1995					
		ance. All rights reser		N	ORT10954.028
Property Code:	[HMSD1000] HI	EAT OF MIXING	AND SOLUTIO		ORTJ0954.028
	[HMSD1000] HI	EAT OF MIXINC system, single-pha			
Property Code: State:	[HMSD1000] HI Two-component Pure component Pure component	EAT OF MIXINC system, single-ph 1, liquid 2, liquid	AND SOLUTIO		
Property Code: State: Parameters:	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/</i> K,	EAT OF MIXINC system, single-ph 1, liquid 2, liquid Temperature	AND SOLUTIO		
Property Code: State:	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/</i> K, [X1] x1/-,	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction	AND SOLUTIO ase liquid or two-pl of component 1		
Property Code: State: Parameters:	[HMSD1000] HI Two-component Pure component [P1] T/K, [X1] x1/-, [Y1] H ^E /Jmol ⁻¹ ,	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e	AND SOLUTIO ase liquid or two-pl of component 1	hase liquid-liqu	id (LL)
Property Code: State: Parameters: Variables:	[HMSD1000] HI Two-component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^-1$, Direct low-press 1. C ₂ H ₆ O, Eths	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n	AND SOLUTIO ase liquid or two-pl of component 1 nthalpy neasurement of H ^E	hase liquid-liqu	id (LL)
Property Code: State: Parameters: Variables: Method: Components:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. C ₂ H ₆ O, Ethe 2. C ₈ H ₁₆ O ₂ , M	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m	AND SOLUTIO ase liquid or two-pl of component 1 nthalpy neasurement of H ^E	hase liquid-liqu ³ at variable x ₁	id (LL)
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [X1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₂ H ₆ O, Eths 2. C ₈ H ₁₆ O ₂ , M 8150E+03	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n	AND SOLUTIO ase liquid or two-pl of component 1 nthalpy neasurement of H ^E	hase liquid-liqu	id (LL)
Property Code: State: Parameters: Variables: Method: Components:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. C ₂ H ₆ O, Ethe 2. C ₈ H ₁₆ O ₂ , M	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n	AND SOLUTIO ase liquid or two-pl of component 1 nthalpy neasurement of H ^E	hase liquid-liqu ⁵ at variable x ₁ [Y1]	and constant T
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .144700E+00 .276800E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₂ H ₆ O, Etha 2. C ₈ H ₁₆ O ₂ , M 8150E+03 [Y1] .713200E+03 .110460E+04	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n	AND SOLUTIO ase liquid or two-pl of component 1 nthalpy neasurement of H ^E	hase liquid-liqu ⁵ at variable x ₁ [Y1]	and constant <i>T</i>
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .144700E+00 .276800E+00 .367700E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₂ H ₆ O, Eths 2. C ₈ H ₁₆ O ₂ , M 8150E+03 [Y1] .713200E+03 .110460E+04 .129390E+04	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n	AND SOLUTIO ase liquid or two-pl of component 1 nthalpy neasurement of H ^E	hase liquid-liqu ⁵ at variable x ₁ [Y1]	and constant <i>T</i>
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .144700E+00 .276800E+00 .367700E+00 .444400E+00	[HMSD1000] HI Two-component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> 1/-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C2H6O, Etha 2. C8H16O2, M 8150E+03 [Y1] .713200E+03 .110460E+04 .129390E+04 .135260E+04	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n	AND SOLUTIO ase liquid or two-pl of component 1 nthalpy neasurement of H ^E	hase liquid-liqu 3 at variable x ₁ [Y1] .160E+04	and constant <i>T</i>
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .144700E+00 .276800E+00 .367700E+00 .444400E+00 .508000E+00	[HMSD1000] HI Two-component Pure component [P1] T/K, [X1] x1/-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C2H ₆ O, Eths 2. C8H ₁₆ O ₂ , M 8150E+03 [Y1] .713200E+03 .110460E+04 .135260E+04 .134690E+04	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n	AND SOLUTIO ase liquid or two-pl of component 1 nthalpy neasurement of H ^E	hase liquid-liqu ⁵ at variable x ₁ [Y1]	and constant <i>T</i>
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .144700E+00 .276800E+00 .367700E+00 .444400E+00	[HMSD1000] HI Two-component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> 1/-, [Y1] <i>H^E</i> /Jmol ⁻¹ , Direct low-press 1. C2H6O, Eths 2. C8H16O2, M 8150E+03 [Y1] .713200E+03 .110460E+04 .135260E+04 .134690E+04 .131010E+04	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n	AND SOLUTIO ase liquid or two-pl of component 1 nthalpy neasurement of H ^E	hase liquid-liqu 3 at variable x ₁ [Y1] .160E+04	and constant T \circ [P1] = .298150E+03
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .144700E+00 .276800E+00 .367700E+00 .444400E+00 .561500E+00 .604600E+00 .642100E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> 1/-, [Y1] <i>HE/Jmol-1</i> , Direct low-press 1. C2H6O, Etha 2. C8H16O2, M 8150E+03 [Y1] .713200E+03 .110460E+04 .129390E+04 .135260E+04 .131010E+04 .125510E+04 .119590E+04	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n	AND SOLUTIO ase liquid or two-pl of component 1 nthalpy neasurement of H ^E	hase liquid-liqu 3 at variable x ₁ [Y1] .160E+04	and constant T \circ [P1] = .298150E+03
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .144700E+00 .276800E+00 .367700E+00 .444400E+00 .508000E+00 .604600E+00 .642100E+00 .711100E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> 1/-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₂ H ₆ O, Etha 2. C ₈ H ₁₆ O ₂ , M 8150E+03 [Y1] .713200E+03 .110460E+04 .129390E+04 .135260E+04 .131010E+04 .125510E+04 .106850E+04	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n	AND SOLUTIO ase liquid or two-pl of component 1 nthalpy neasurement of H ^E	hase liquid-liqu 3 at variable x ₁ [Y1] .160E+04	and constant T \circ [P1] = .298150E+03
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .144700E+00 .276800E+00 .367700E+00 .444400E+00 .508000E+00 .604600E+00 .642100E+00 .711100E+00 .747700E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> 1/-, [Y1] <i>HE/Jmol-1</i> , Direct low-press 1. C2H6O, Ethe 2. C3H16O2, M 8150E+03 [Y1] .713200E+03 .110460E+04 .135260E+04 .135260E+04 .131010E+04 .125510E+04 .106850E+04 .958000E+03	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n	AND SOLUTIO ase liquid or two-pl of component 1 nthalpy neasurement of H ^E	hase liquid-liqu 3 at variable x ₁ [Y1] .160E+04	and constant T \circ [P1] = .298150E+03
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .144700E+00 .276800E+00 .367700E+00 .444400E+00 .508000E+00 .604600E+00 .644100E+00 .711100E+00 .747700E+00 .782500E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₂ H ₆ O, Ethe 2. C ₈ H ₁₆ O ₂ , M 8150E+03 [Y1] .713200E+03 .110460E+04 .135260E+04 .134690E+04 .134690E+04 .131010E+04 .135510E+04 .106850E+04 .106850E+04 .958000E+03 .856200E+03	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n	AND SOLUTIO ase liquid or two-pl of component 1 nthalpy neasurement of H ^E	hase liquid-liqu at variable x ₁ [Y1] .160E+04 .120E+04	and constant T \circ [P1] = .298150E+03
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .144700E+00 .276800E+00 .367700E+00 .444400E+00 .508000E+00 .604600E+00 .642100E+00 .711100E+00 .747700E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C2H6O, Etha 2. C8H16O2, M 8150E+03 [Y1] .713200E+03 .110460E+04 .129390E+04 .135260E+04 .134690E+04 .1300E+04 .106850E+04 .106850E+04 .856200E+03 .856200E+03 .752700E+03	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n	AND SOLUTIO ase liquid or two-pl of component 1 nthalpy neasurement of H ^E	hase liquid-liqu at variable x ₁ [Y1] .160E+04 .120E+04	and constant T \circ [P1] = .298150E+03
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .144700E+00 .276800E+00 .367700E+00 .444400E+00 .561500E+00 .604600E+00 .642100E+00 .711100E+00 .747700E+00 .817600E+00 .850700E+00 .884500E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> 1/-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C2H6O, Eths 2. C8H16O2, M 8150E+03 [Y1] .713200E+03 .110460E+04 .13260E+04 .13260E+04 .134690E+04 .13680E+04 .13680E+04 .19590E+04 .106850E+04 .19590E+03 .856200E+03 .856200E+03 .520000E+03 .520000E+03	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n	AND SOLUTIO ase liquid or two-pl of component 1 nthalpy neasurement of H ^E	hase liquid-liqu at variable x ₁ [Y1] .160E+04 .120E+04	and constant T \circ [P1] = .298150E+03
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .144700E+00 .276800E+00 .276800E+00 .444400E+00 .561500E+00 .604600E+00 .642100E+00 .711100E+00 .747700E+00 .817600E+00 .850700E+00 .884500E+00 .917097E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> 1/-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-press 1. C2H6O, Etha 2. C8H16O2, M 8150E+03 [Y1] .713200E+03 .110460E+04 .135260E+04 .135260E+04 .135260E+04 .136800E+04 .125510E+04 .19590E+04 .106850E+04 .19590E+04 .106850E+04 .520000E+03 .856200E+03 .520000E+03 .520000E+03 .388900E+03	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n	AND SOLUTIO ase liquid or two-pl of component 1 nthalpy neasurement of H ^E	hase liquid-liqu at variable x ₁ [Y1] .160E+04 .120E+04 .800E+03	and constant T \circ [P1] = .298150E+03
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .144700E+00 .276800E+00 .367700E+00 .444400E+00 .561500E+00 .604600E+00 .642100E+00 .711100E+00 .747700E+00 .817600E+00 .817600E+00 .817600E+00 .817600E+00 .917097E+00 .947595E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> 1/-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C2H6O, Ethat 2. C8H16O2, M 8150E+03 [Y1] .713200E+03 .110460E+04 .129390E+04 .135260E+04 .135260E+04 .131010E+04 .125510E+04 .13010E+04 .125510E+04 .106850E+04 .106850E+04 .52000E+03 .856200E+03 .52200E+03 .388900E+03 .255200E+03	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n	AND SOLUTIO ase liquid or two-pl of component 1 nthalpy neasurement of H ^E	hase liquid-liqu at variable x ₁ [Y1] .160E+04 .120E+04	and constant T \circ [P1] = .298150E+03
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .144700E+00 .276800E+00 .276800E+00 .444400E+00 .561500E+00 .604600E+00 .642100E+00 .711100E+00 .747700E+00 .817600E+00 .850700E+00 .884500E+00 .917097E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> 1/-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C2H6O, Etha 2. C8H16O2, M 8150E+03 [Y1] .713200E+03 .110460E+04 .135260E+04 .135260E+04 .13690E+04 .136850E+04 .125510E+04 .106850E+04 .106850E+04 .106850E+04 .106850E+04 .106850E+04 .3856200E+03 .52200E+03 .522000E+03 .388900E+03 .255200E+03	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n	AND SOLUTIO ase liquid or two-pl of component 1 nthalpy neasurement of H ^E	hase liquid-liqu at variable x ₁ [Y1] .160E+04 .120E+04 .800E+03	and constant T \circ [P1] = .298150E+03
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .144700E+00 .276800E+00 .367700E+00 .444400E+00 .561500E+00 .604600E+00 .642100E+00 .711100E+00 .747700E+00 .817600E+00 .817600E+00 .817600E+00 .817600E+00 .917097E+00 .947595E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> 1/-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C2H6O, Ethat 2. C8H16O2, M 8150E+03 [Y1] .713200E+03 .110460E+04 .129390E+04 .135260E+04 .135260E+04 .131010E+04 .125510E+04 .13010E+04 .125510E+04 .106850E+04 .106850E+04 .52000E+03 .856200E+03 .52200E+03 .388900E+03 .255200E+03	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n	AND SOLUTIO ase liquid or two-pl of component 1 nthalpy neasurement of H ^E	hase liquid-liqu at variable x ₁ [Y1] .160E+04 .120E+04 .800E+03	and constant T \circ [P1] = .298150E+03
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .144700E+00 .276800E+00 .367700E+00 .444400E+00 .561500E+00 .604600E+00 .642100E+00 .711100E+00 .747700E+00 .817600E+00 .817600E+00 .817600E+00 .817600E+00 .917097E+00 .947595E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> 1/-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C2H6O, Ethat 2. C8H16O2, M 8150E+03 [Y1] .713200E+03 .110460E+04 .129390E+04 .135260E+04 .135260E+04 .131010E+04 .125510E+04 .13010E+04 .125510E+04 .106850E+04 .106850E+04 .52000E+03 .856200E+03 .52200E+03 .388900E+03 .255200E+03	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n	AND SOLUTIO ase liquid or two-pl of component 1 nthalpy neasurement of H ^E	hase liquid-liqu at variable x ₁ [Y1] .160E+04 .120E+04 .800E+03	and constant T
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .144700E+00 .276800E+00 .367700E+00 .444400E+00 .561500E+00 .604600E+00 .642100E+00 .711100E+00 .747700E+00 .817600E+00 .817600E+00 .817600E+00 .817600E+00 .917097E+00 .947595E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> 1/-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C2H6O, Ethat 2. C8H16O2, M 8150E+03 [Y1] .713200E+03 .110460E+04 .129390E+04 .135260E+04 .135260E+04 .131010E+04 .125510E+04 .13010E+04 .125510E+04 .106850E+04 .106850E+04 .52000E+03 .856200E+03 .52200E+03 .388900E+03 .255200E+03	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n	AND SOLUTIO ase liquid or two-pl of component 1 nthalpy neasurement of H ^E	hase liquid-liqu at variable x ₁ [Y1] .160E+04 .120E+04 .800E+03	and constant T
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .144700E+00 .276800E+00 .367700E+00 .444400E+00 .561500E+00 .604600E+00 .642100E+00 .711100E+00 .747700E+00 .817600E+00 .817600E+00 .817600E+00 .817600E+00 .917097E+00 .947595E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> 1/-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C2H6O, Ethat 2. C8H16O2, M 8150E+03 [Y1] .713200E+03 .110460E+04 .129390E+04 .135260E+04 .135260E+04 .131010E+04 .125510E+04 .13010E+04 .125510E+04 .106850E+04 .106850E+04 .52000E+03 .856200E+03 .52200E+03 .388900E+03 .255200E+03	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n	AND SOLUTIO ase liquid or two-pl of component 1 nthalpy neasurement of H ^E	hase liquid-liqu at variable x ₁ [Y1] .160E+04 .120E+04 .800E+03 .400E+03	and constant T
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .144700E+00 .276800E+00 .367700E+00 .444400E+00 .561500E+00 .604600E+00 .642100E+00 .711100E+00 .747700E+00 .817600E+00 .817600E+00 .817600E+00 .817600E+00 .917097E+00 .947595E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> 1/-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C2H6O, Ethat 2. C8H16O2, M 8150E+03 [Y1] .713200E+03 .110460E+04 .129390E+04 .135260E+04 .135260E+04 .131010E+04 .125510E+04 .13010E+04 .125510E+04 .106850E+04 .106850E+04 .52000E+03 .856200E+03 .52200E+03 .388900E+03 .255200E+03	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n	AND SOLUTIO ase liquid or two-pl of component 1 nthalpy neasurement of H ^E	hase liquid-liqu at variable x ₁ [Y1] .160E+04 .120E+04 .800E+03 .400E+03	and constant T
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .144700E+00 .276800E+00 .367700E+00 .561500E+00 .604600E+00 .604600E+00 .642100E+00 .711100E+00 .747700E+00 .817600E+00 .817600E+00 .817600E+00 .817600E+00 .817600E+00 .817600E+00 .917097E+00 .947595E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> 1/-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C2H6O, Ethat 2. C8H16O2, M 8150E+03 [Y1] .713200E+03 .110460E+04 .129390E+04 .135260E+04 .135260E+04 .131010E+04 .125510E+04 .13010E+04 .125510E+04 .106850E+04 .106850E+04 .52000E+03 .856200E+03 .52200E+03 .388900E+03 .255200E+03	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n	AND SOLUTIO ase liquid or two-pl of component 1 nthalpy neasurement of H ^E	hase liquid-liqu at variable x ₁ [Y1] .160E+04 .120E+04 .800E+03 .400E+03	and constant T

		AT OF MIXING A			n fra Granden singer som en der eine en der er ander der eine der Granden einen alle eine sinderen gesenen auf	ORTJ0954.037
State:	Two-component s	system, single-phase	liquid or two-phase	liquid-liqui	d (LL)	OR130754.057
	Pure component	l, liquid				
	Pure component					
Parameters:	[P1] <i>T/</i> K,	Temperature	component 1			
ariables:	[X1] $x_{1/-}$, [X1] $HE/Imol-1$	Mole fraction of Molar excess entl	component 1			
fethod:	Direct low-pressu	re calorimetric mea	surement of $H^{\rm E}$ at v	variable x_1 a	nd constant T	
Components:	1. C ₂ H ₆ O, Ethan					4
(7)11 000	2. C ₁₀ H ₂₀ O ₂ , M	ethyl nonanoate	<u> </u>		р. 	
[P1] = .298				[Y1]		
[X1]	[Y1]			.160E+04		
.145300E+00 .272000E+00	.808000E+03 .121530E+04				○ [P1] = .298150E+03	
.372800E+00	.121350E+04				0 ₀	
.453100E+00	.143820E+04				, · · · · · · · · · · · · · · · · · · ·	
.517500E+00	.142180E+04		· · · ·	.120E+04	o 0.	
.573400E+00	.137790E+04					
.618200E+00	.131340E+04				A	
.654300E+00 .721200E+00	.124590E+04 .108750E+04				<u> </u>	
.753200E+00	.108730E+04				/	5.
.785100E+00				.800E+03	- ¢	å -
.816900E+00					/	·.
.847600E+00					/	
.877900E+00						0
.905000E+00 .933100E+00					/	o
.958000E+00				.400E+03	• /	6
.981000E+00	.112200E+03					Ť.
						Q
					/	0
				.000E+00		
				.00012+001	.50E+00	
						[X1]
						[AI]
		nce. All rights reserved		and the second secon		
Property Code:	[HMSD1000] HE	EAT OF MIXING	AND SOLUTION		and the second s	ORTJ0954.04
	[HMSD1000] HE Two-component	EAT OF MIXING A system, single-phase		e liquid-liqu	id (LL)	
Property Code:	[HMSD1000] HE Two-component Pure component	EAT OF MIXING A system, single-phase 1, liquid	AND SOLUTION	liquid-liqu	id (LL)	
Property Code:	[HMSD1000] HE Two-component Pure component Pure component	EAT OF MIXING A system, single-phase 1, liquid 2, liquid Temperature	AND SOLUTION e liquid or two-phase	liquid-liqu	id (LL)	
Property Code: State:	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-,	EAT OF MIXING A system, single-phase 1, liquid 2, liquid Temperature Mole fraction of	AND SOLUTION e liquid or two-phase component 1	liquid-liqu	id (LL)	
Property Code: State: Parameters: Variables:	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ ,	EAT OF MIXING A system, single-phase 1, liquid 2, liquid Temperature Mole fraction of Molar excess ent	AND SOLUTION e liquid or two-phase component 1 halpy			
Property Code: State: Parameters: Variables: Method:	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressu	EAT OF MIXING A system, single-phase 1, liquid 2, liquid Temperature Mole fraction of Molar excess ent Ire calorimetric mea	AND SOLUTION e liquid or two-phase component 1			
Property Code: State: Parameters: Variables: Method:	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₂ H ₆ O, Etha	EAT OF MIXING A system, single-phase 1, liquid 2, liquid Temperature Mole fraction of Molar excess ent Ire calorimetric mea	AND SOLUTION e liquid or two-phase component 1 halpy asurement of H ^E at y			
Property Code: State: Parameters: Variables: Method:	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₂ H ₆ O, Etha 2. C ₁₂ H ₂₄ O ₂ , M	EAT OF MIXING A system, single-phase 1, liquid 2, liquid Temperature Mole fraction of Molar excess ent are calorimetric mean nol	AND SOLUTION e liquid or two-phase component 1 halpy asurement of H ^E at y	variable x_1 a		
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1]	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₂ H ₆ O, Etha 2. C ₁₂ H ₂ 4O ₂ , M B150E+03 [Y1]	EAT OF MIXING A system, single-phase 1, liquid 2, liquid Temperature Mole fraction of Molar excess ent are calorimetric mean nol	AND SOLUTION e liquid or two-phase component 1 halpy asurement of H ^E at y			
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .195700E+00	[HMSD1000] HH Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₂ H ₆ O, Etha 2. C ₁₂ H ₂₄ O ₂ , M B150E+03 [Y1] .983400E+03	EAT OF MIXING A system, single-phase 1, liquid 2, liquid Temperature Mole fraction of Molar excess ent are calorimetric mean nol	AND SOLUTION e liquid or two-phase component 1 halpy asurement of H ^E at y	variable x ₁ a	o (B1) - 202150E + 02	ORTJ0954.04
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .195700E+00 .351400E+00	[HMSD1000] HH Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₂ H ₆ O, Etha 2. C ₁₂ H ₂₄ O ₂ , M B150E+03 [Y1] .983400E+03 .138450E+04	EAT OF MIXING A system, single-phase 1, liquid 2, liquid Temperature Mole fraction of Molar excess ent are calorimetric mean nol	AND SOLUTION e liquid or two-phase component 1 halpy asurement of H ^E at y	variable x ₁ a	o (B1) - 202150E + 02	ORTJ0954.04
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .195700E+00 .351400E+00 .439000E+00	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-pressu 1. C ₂ H ₆ O, Etha 2. C ₁₂ H ₂ 4O ₂ , M B150E+03 [Y1] .983400E+03 .138450E+04 .148220E+04	EAT OF MIXING A system, single-phase 1, liquid 2, liquid Temperature Mole fraction of Molar excess ent are calorimetric mean nol	AND SOLUTION e liquid or two-phase component 1 halpy asurement of H ^E at y	variable x ₁ a	o (B1) - 202150E + 02	ORTJ0954.04
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .195700E+00 .351400E+00 .439000E+00 .473400E+00	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-pressu 1. C ₂ H ₆ O, Etha 2. C ₁₂ H ₂ 4O ₂ , M B150E+03 [Y1] .983400E+03 .138450E+04 .148220E+04 .150290E+04	EAT OF MIXING A system, single-phase 1, liquid 2, liquid Temperature Mole fraction of Molar excess ent are calorimetric mean nol	AND SOLUTION e liquid or two-phase component 1 halpy asurement of H ^E at y	/ariable x ₁ a [Y1] .180E+04	o (B1) - 202150E + 02	ORTJ0954.04
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .195700E+00 .351400E+00 .439000E+00 .514900E+00	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-pressu 1. C ₂ H ₆ O, Etha 2. C ₁₂ H ₂ 4O ₂ , M B150E+03 [Y1] .983400E+03 .138450E+04 .148220E+04 .149720E+04	EAT OF MIXING A system, single-phase 1, liquid 2, liquid Temperature Mole fraction of Molar excess ent are calorimetric mean nol	AND SOLUTION e liquid or two-phase component 1 halpy asurement of H ^E at y	variable x ₁ a	o (B1) - 202150E + 02	ORTJ0954.04
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .195700E+00 .351400E+00 .439000E+00 .473400E+00 .514900E+00 .564200E+00	[HMSD1000] HETwo-componentPure componentPure component[P1] T/K,[X1] x1/-,[Y1] HE/Jmol-1,Direct low-pressu1. C2H6O, Etha2. C12H24O2, MB150E+03[Y1].983400E+03.138450E+04.148220E+04.149720E+04.149720E+04.147640E+04	EAT OF MIXING A system, single-phase 1, liquid 2, liquid Temperature Mole fraction of Molar excess ent are calorimetric mean nol	AND SOLUTION e liquid or two-phase component 1 halpy asurement of H ^E at y	/ariable x ₁ a [Y1] .180E+04	o (B1) - 202150E + 02	ORTJ0954.04
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .195700E+00 .351400E+00 .439000E+00 .473400E+00 .514900E+00 .564200E+00 .637600E+00	[HMSD1000] HETwo-componentPure componentPure component[P1] T/K,[X1] x1/-,[Y1] HE/Jmol-1,Direct low-pressu1. C2H6O, Etha2. C12H24O2, MB150E+03[Y1].983400E+03.138450E+04.148220E+04.149720E+04.149720E+04.149760E+04.139160E+04	EAT OF MIXING A system, single-phase 1, liquid 2, liquid Temperature Mole fraction of Molar excess ent are calorimetric mean nol	AND SOLUTION e liquid or two-phase component 1 halpy asurement of H ^E at y	/ariable x ₁ a [Y1] .180E+04	o (B1) - 202150E + 02	ORTJ0954.04
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .195700E+00 .351400E+00 .439000E+00 .473400E+00 .514900E+00 .564200E+00	[HMSD1000] HETwo-componentPure componentPure component[P1] T/K,[X1] x1/-,[Y1] HE/Jmol-1,Direct low-pressu1. C2H6O, Etha2. C12H24O2, MB150E+03[Y1].983400E+03.138450E+04.148220E+04.149720E+04.149720E+04.147640E+04	EAT OF MIXING A system, single-phase 1, liquid 2, liquid Temperature Mole fraction of Molar excess ent are calorimetric mean nol	AND SOLUTION e liquid or two-phase component 1 halpy asurement of H ^E at y	/ariable x ₁ a [Y1] .180E+04	o (B1) - 202150E + 02	ORTJ0954.04
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .195700E+00 .351400E+00 .439000E+00 .473400E+00 .564200E+00 .667800E+00 .705300E+00 .729000E+00	[HMSD1000] HETwo-componentPure componentPure component[P1] T/K,[X1] x1/-,[Y1] HE/Jmol-1,Direct low-pressu1. C2H6O, Etha2. C12H24O2, MB150E+03[Y1].983400E+03.138450E+04.138450E+04.149720E+04.149720E+04.139160E+04.131720E+04.121980E+04.114770E+04	EAT OF MIXING A system, single-phase 1, liquid 2, liquid Temperature Mole fraction of Molar excess ent are calorimetric mean nol	AND SOLUTION e liquid or two-phase component 1 halpy asurement of H ^E at y	[Y1] .180E+04 .135E+04	o (B1) - 202150E + 02	ORTJ0954.04
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .195700E+00 .351400E+00 .439000E+00 .514900E+00 .54200E+00 .637600E+00 .667800E+00 .705300E+00 .729000E+00 .757400E+00	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₂ H ₆ O, Etha 2. C ₁₂ H ₂₄ O ₂ , M 3150E+03 [Y1] .983400E+03 .138450E+04 .148220E+04 .149720E+04 .139160E+04 .131720E+04 .121980E+04 .114770E+04 .106240E+04	EAT OF MIXING A system, single-phase 1, liquid 2, liquid Temperature Mole fraction of Molar excess ent are calorimetric mean nol	AND SOLUTION e liquid or two-phase component 1 halpy asurement of H ^E at y	/ariable x ₁ a [Y1] .180E+04	o (B1) - 202150E + 02	ORTJ0954.04
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .195700E+00 .351400E+00 .439000E+00 .564200E+00 .667800E+00 .667800E+00 .705300E+00 .729000E+00 .757400E+00 .786600E+00	[HMSD1000] HETwo-componentPure componentPure component[P1] T/K,[X1] x1/-,[Y1] HE/Jmol-1,Direct low-pressu1. C2H6O, Etha2. C12H24O2, MB150E+03[Y1].983400E+03.138450E+04.148220E+04.149720E+04.149720E+04.139160E+04.139160E+04.131720E+04.121980E+04.14770E+04.106240E+04.966000E+03	EAT OF MIXING A system, single-phase 1, liquid 2, liquid Temperature Mole fraction of Molar excess ent are calorimetric mean nol	AND SOLUTION e liquid or two-phase component 1 halpy asurement of H ^E at y	[Y1] .180E+04 .135E+04	o (B1) - 202150E + 02	ORTJ0954.04
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .195700E+00 .351400E+00 .439000E+00 .564200E+00 .667800E+00 .667800E+00 .705300E+00 .729000E+00 .757400E+00 .786600E+00 .815400E+00	[HMSD1000] HETwo-componentPure componentPure component[P1] T/K,[X1] x1/-,[Y1] HE/Jmol-1,Direct low-pressu1. C2H6O, Etha2. C12H24O2, M3150E+03[Y1].983400E+03.138450E+04.148220E+04.149720E+04.149720E+04.139160E+04.139160E+04.121980E+04.114770E+04.106240E+04.966000E+03.861300E+03	EAT OF MIXING A system, single-phase 1, liquid 2, liquid Temperature Mole fraction of Molar excess ent are calorimetric mean nol	AND SOLUTION e liquid or two-phase component 1 halpy asurement of H ^E at y	[Y1] .180E+04 .135E+04	o (B1) - 202150E + 02	ORTJ0954.04
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .195700E+00 .351400E+00 .473400E+00 .514900E+00 .637600E+00 .637600E+00 .705300E+00 .705300E+00 .757400E+00 .815400E+00 .844000E+00	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-pressu 1. C ₂ H ₆ O, Etha 2. C ₁₂ H ₂₄ O ₂ , M 3150E+03 [Y1] .983400E+03 .138450E+04 .148220E+04 .149720E+04 .149720E+04 .139160E+04 .131720E+04 .121980E+04 .114770E+04 .106240E+04 .106240E+04 .361300E+03 .661300E+03 .747600E+03	EAT OF MIXING A system, single-phase 1, liquid 2, liquid Temperature Mole fraction of Molar excess ent are calorimetric mean nol	AND SOLUTION e liquid or two-phase component 1 halpy asurement of H ^E at y	[Y1] .180E+04 .135E+04	o (B1) - 202150E + 02	ORTJ0954.04
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .195700E+00 .351400E+00 .439000E+00 .564200E+00 .667800E+00 .667800E+00 .705300E+00 .729000E+00 .757400E+00 .786600E+00 .815400E+00	[HMSD1000] HETwo-componentPure componentPure component[P1] T/K,[X1] x1/-,[Y1] HE/Jmol-1,Direct low-pressu1. C2H6O, Etha2. C12H24O2, M3150E+03[Y1].983400E+03.138450E+04.148220E+04.149720E+04.149720E+04.139160E+04.139160E+04.121980E+04.114770E+04.106240E+04.966000E+03.861300E+03	EAT OF MIXING A system, single-phase 1, liquid 2, liquid Temperature Mole fraction of Molar excess ent are calorimetric mean nol	AND SOLUTION e liquid or two-phase component 1 halpy asurement of H ^E at y	[Y1] .180E+04 .135E+04	o (B1) - 202150E + 02	ORTJ0954.04
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .195700E+00 .351400E+00 .439000E+00 .514900E+00 .564200E+00 .667800E+00 .705300E+00 .705300E+00 .757400E+00 .815400E+00 .844000E+00 .844000E+00 .844000E+00 .844000E+00 .844000E+00 .897800E+00 .922600E+00	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₂ H ₆ O, Etha 2. C ₁₂ H ₂₄ O ₂ , M B150E+03 [Y1] .983400E+03 .138450E+04 .148220E+04 .148220E+04 .149720E+04 .149720E+04 .139160E+04 .131720E+04 .131720E+04 .121980E+04 .1477600E+03 .861300E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03	EAT OF MIXING A system, single-phase 1, liquid 2, liquid Temperature Mole fraction of Molar excess ent are calorimetric mean nol	AND SOLUTION e liquid or two-phase component 1 halpy asurement of H ^E at y	[Y1] .180E+04 .135E+04	o (B1) - 202150E + 02	ORTJ0954.04
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .195700E+00 .351400E+00 .439000E+00 .514900E+00 .564200E+00 .667800E+00 .705300E+00 .705300E+00 .757400E+00 .815400E+00 .815400E+00 .844000E+00 .844000E+00 .8471700E+00 .897800E+00 .922600E+00 .945800E+00	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₂ H ₆ O, Etha 2. C ₁₂ H ₂₄ O ₂ , M 3150E+03 [Y1] .983400E+03 .138450E+04 .148220E+04 .148220E+04 .149720E+04 .149720E+04 .149720E+04 .131720E+04 .121980E+04 .121980E+04 .121980E+04 .106240E+04 .56000E+03 .861300E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03	EAT OF MIXING A system, single-phase 1, liquid 2, liquid Temperature Mole fraction of Molar excess ent are calorimetric mean nol	AND SOLUTION e liquid or two-phase component 1 halpy asurement of H ^E at y	[Y1] .180E+04 .135E+04	o (B1) - 202150E + 02	ORTJ0954.04
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .195700E+00 .351400E+00 .439000E+00 .514900E+00 .564200E+00 .564200E+00 .667800E+00 .729000E+00 .757400E+00 .815400E+00 .815400E+00 .844000E+00 .844000E+00 .844000E+00 .844000E+00 .897800E+00 .922600E+00 .945800E+00 .945800E+00 .945800E+00	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₂ H ₆ O, Etha 2. C ₁₂ H ₂₄ O ₂ , M 3150E+03 [Y1] .983400E+03 .138450E+04 .148220E+04 .148220E+04 .149720E+04 .149720E+04 .149720E+04 .139160E+04 .139160E+04 .121980E+04 .121980E+04 .121980E+04 .106240E+04 .56000E+03 .645900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .507100E+03	EAT OF MIXING A system, single-phase 1, liquid 2, liquid Temperature Mole fraction of Molar excess ent are calorimetric mean nol	AND SOLUTION e liquid or two-phase component 1 halpy asurement of H ^E at y	[Y1] .180E+04 .135E+04	o (B1) - 202150E + 02	ORTJ0954.04
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .195700E+00 .351400E+00 .439000E+00 .514900E+00 .564200E+00 .564200E+00 .667800E+00 .729000E+00 .757400E+00 .815400E+00 .815400E+00 .844000E+00 .871700E+00 .897800E+00 .922600E+00 .945800E+00	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₂ H ₆ O, Etha 2. C ₁₂ H ₂₄ O ₂ , M 3150E+03 [Y1] .983400E+03 .138450E+04 .148220E+04 .148220E+04 .149720E+04 .149720E+04 .149720E+04 .131720E+04 .121980E+04 .121980E+04 .121980E+04 .106240E+04 .56000E+03 .861300E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03	EAT OF MIXING A system, single-phase 1, liquid 2, liquid Temperature Mole fraction of Molar excess ent are calorimetric mean nol	AND SOLUTION e liquid or two-phase component 1 halpy asurement of H ^E at y	[Y1] .180E+04 .135E+04	o (B1) - 202150E + 02	ORTJ0954.04
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .195700E+00 .351400E+00 .439000E+00 .514900E+00 .564200E+00 .564200E+00 .667800E+00 .729000E+00 .757400E+00 .815400E+00 .815400E+00 .844000E+00 .844000E+00 .844000E+00 .844000E+00 .897800E+00 .922600E+00 .945800E+00 .945800E+00 .945800E+00	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₂ H ₆ O, Etha 2. C ₁₂ H ₂₄ O ₂ , M 3150E+03 [Y1] .983400E+03 .138450E+04 .148220E+04 .148220E+04 .149720E+04 .149720E+04 .149720E+04 .139160E+04 .139160E+04 .121980E+04 .121980E+04 .121980E+04 .106240E+04 .56000E+03 .645900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .507100E+03	EAT OF MIXING A system, single-phase 1, liquid 2, liquid Temperature Mole fraction of Molar excess ent are calorimetric mean nol	AND SOLUTION e liquid or two-phase component 1 halpy asurement of H ^E at y	[Y1] .180E+04 .135E+04	ind constant T	ORTJ0954.04
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .195700E+00 .351400E+00 .439000E+00 .514900E+00 .564200E+00 .564200E+00 .667800E+00 .729000E+00 .757400E+00 .815400E+00 .844000E+00 .844000E+00 .844000E+00 .871700E+00 .897800E+00 .922600E+00 .945800E+00 .945800E+00 .945800E+00	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₂ H ₆ O, Etha 2. C ₁₂ H ₂₄ O ₂ , M 3150E+03 [Y1] .983400E+03 .138450E+04 .148220E+04 .148220E+04 .149720E+04 .149720E+04 .149720E+04 .139160E+04 .139160E+04 .121980E+04 .121980E+04 .121980E+04 .106240E+04 .56000E+03 .645900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .507100E+03	EAT OF MIXING A system, single-phase 1, liquid 2, liquid Temperature Mole fraction of Molar excess ent are calorimetric mean nol	AND SOLUTION e liquid or two-phase component 1 halpy asurement of H ^E at y	(Y1) .180E+04 .135E+04 .900E+03 .450E+03	o (B1) - 202150E + 02	ORTJ0954.04
Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₂ H ₆ O, Etha 2. C ₁₂ H ₂₄ O ₂ , M 3150E+03 [Y1] .983400E+03 .138450E+04 .148220E+04 .148220E+04 .149720E+04 .149720E+04 .149720E+04 .139160E+04 .139160E+04 .121980E+04 .121980E+04 .121980E+04 .106240E+04 .56000E+03 .645900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .540900E+03 .507100E+03	EAT OF MIXING A system, single-phase 1, liquid 2, liquid Temperature Mole fraction of Molar excess ent are calorimetric mean nol	AND SOLUTION e liquid or two-phase component 1 halpy asurement of H ^E at y	(Y1) .180E+04 .135E+04 .900E+03 .450E+03	$\circ [P1] = .298150E + 03$	ORTJ0954.04

	THMSD10001 HF.	ce. All rights reserve AT OF MIXING	AND SOLUTION	han and she was the		ORTJ0954.055
State:	Two-component s	vstem, single-phas	e liquid or two-pha	se liquid-liquid (10 No.
	Pure component 1					
	Pure component 2					
	[P1] <i>T/</i> K,	Temperature				
ariables:	$[X1] x_{1/-},$	Mole fraction of				
lethod:	[Y1] HE/Jmol ⁻¹ ,	Molar excess en	thalpy easurement of H ^E a	t unriable x. and	constant T	
	1. C ₂ H ₆ O, Ethan		asurement or m- a	a variable x1 and	constant 1	in the second
omponents.	2. $C_{14}H_{28}O_2$, M	ethyl tridecanoat	e			
[P1] = .298	150E+03			[Y1]		
[X1]	[Y1]	the second second second		.180E+04		
.160900E+00	.955900E+03	A the second of the	*		[P1] = .298150E+03	
.287600E+00	.138610E+04	and the second sec	1 			
.389100E+00	.156330E+04				······································	
.467000E+00	.160210E+04		4		0,00	
.534200E+00	.158290E+04	1	States &	.135E+04	P	-
.587800E+00 .634800E+00	.151760E+04 .142360E+04				<u> </u>	
.695200E+00	.127630E+04					à
.740700E+00	.114240E+04				/	A
.795700E+00	.943000E+03				ö	ò
.832000E+00	.813300E+03		가 가 있는 것은 가 있었다. 	.900E+03	- I	
.864700E+00	.697400E+03					٩
.896400E+00 .924700E+00	.575800E+03 .451600E+03					à
.947100E+00	.340600E+03				1	o l
.966400E+00	.230800E+03		1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1	.450E+03		
.986400E+00	.108700E+03					
						Q
						ò
	Sector States	See Sec. A		.000E+00	1	
		4			.50E+00	
						[X1]
						[X1]
	ELDATA SARL Fra			N		
	[HMSD1000] HI Two-component	EAT OF MIXING system, single-pha	AND SOLUTION		(LL)	[X1] ORTJ0954.064
Property Code:	[HMSD1000] HI Two-component Pure component	EAT OF MIXING system, single-pha 1, liquid			(LL)	
Property Code: State:	[HMSD1000] HI Two-component Pure component Pure component	EAT OF MIXING system, single-pha 1, liquid 2, liquid	AND SOLUTION		(LL)	
Property Code: State: Parameters:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K,	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature	AND SOLUTIO ase liquid or two-ph		(LL)	
Property Code: State: Parameters:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-,	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of	AND SOLUTION ase liquid or two-ph of component 1		(LL)	
Property Code: State: Parameters: Variables:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ .	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e	AND SOLUTION ase liquid or two-ph of component 1	ase liquid-liquid		
Property Code: State: Parameters: Variables: Method:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₂ H ₆ O, Ethe	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m	AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid		
Property Code: State: Parameters: Variables: Method: Components:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/$ -, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. C ₂ H ₆ O, Etha 2. C ₁₆ H ₃₂ O ₂ , M	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m	AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	hase liquid-liquid a		
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C ₂ H ₆ O, Eths 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m	AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	hase liquid-liquid x_1 and x_1 and $[Y1]$		
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1]	[HMSD1000] HI Two-component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₂ H ₆ O, Etha 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1]	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m	AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid at variable x_1 and [Y1] .200E+04	l constant T	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .172900E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₂ H ₆ O, Etha 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .107430E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m	AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid at variable x_1 and [Y1] .200E+04		
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .172900E+00 .305400E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₂ H ₆ O, Eths 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .107430E+04 .152230E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m	AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid at variable x_1 and [Y1] .200E+04	l constant T	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .172900E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₂ H ₆ O, Eths 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .107430E+04 .152230E+04 .169910E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m	AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid at variable x_1 and [Y1] .200E+04	<pre>constant T o [P1] = .298150E+03</pre>	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .172900E+00 .305400E+00 .410100E+00 .498800E+00 .567200E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₂ H ₆ O, Eths 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .107430E+04 .152230E+04 .169910E+04 .166500E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m	AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid at variable x_1 and [Y1] .200E+04	<pre>constant T o [P1] = .298150E+03</pre>	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .172900E+00 .305400E+00 .410100E+00 .498800E+00 .567200E+00 .624300E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₂ H ₆ O, Eths 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .107430E+04 .152230E+04 .169910E+04 .166500E+04 .158440E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m	AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid at variable x ₁ and [Y1] .200E+04	<pre>constant T o [P1] = .298150E+03</pre>	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .172900E+00 .305400E+00 .410100E+00 .498800E+00 .567200E+00 .624300E+00 .666600E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₂ H ₆ O, Eths 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .107430E+04 .152230E+04 .169910E+04 .166500E+04 .158440E+04 .148660E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m	AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid at variable x ₁ and [Y1] .200E+04	<pre>constant T o [P1] = .298150E+03</pre>	ORTJ0954.064
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .172900E+00 .305400E+00 .410100E+00 .498800E+00 .567200E+00 .624300E+00 .666600E+00 .706900E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₂ H ₆ O, Eths 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .107430E+04 .152230E+04 .169910E+04 .166500E+04 .158440E+04 .148660E+04 .137130E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m	AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid at variable x ₁ and [Y1] .200E+04	<pre>constant T o [P1] = .298150E+03</pre>	ORTJ0954.064
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .172900E+00 .305400E+00 .410100E+00 .498800E+00 .567200E+00 .624300E+00 .666600E+00 .706900E+00 .766300E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₂ H ₆ O, Eths 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .107430E+04 .152230E+04 .169910E+04 .166500E+04 .158440E+04 .137130E+04 .116630E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m	AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid at variable x ₁ and [Y1] .200E+04	<pre>constant T o [P1] = .298150E+03</pre>	ORTJ0954.064
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .172900E+00 .305400E+00 .410100E+00 .498800E+00 .667200E+00 .666600E+00 .706900E+00 .801960E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₂ H ₆ O, Etha 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .107430E+04 .152230E+04 .152230E+04 .166500E+04 .158440E+04 .137130E+04 .116630E+04 .104690E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m	AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid at variable x ₁ and [Y1] .200E+04	<pre>constant T o [P1] = .298150E+03</pre>	ORTJ0954.064
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .172900E+00 .305400E+00 .410100E+00 .498800E+00 .567200E+00 .624300E+00 .666600E+00 .706900E+00 .766300E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₂ H ₆ O, Etha 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .107430E+04 .152230E+04 .152230E+04 .166500E+04 .158440E+04 .158440E+04 .137130E+04 .116630E+04 .104690E+04 .888500E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m	AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid at variable x ₁ and [Y1] .200E+04 .150E+04	<pre>constant T o [P1] = .298150E+03</pre>	ORTJ0954.064
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .172900E+00 .305400E+00 .410100E+00 .498800E+00 .567200E+00 .666600E+00 .766300E+00 .801960E+00 .838600E+00 .83860E+00 .874200E+00 .909100E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> 1/-, [Y1] <i>HE/Jmol-1</i> , Direct low-press 1. C2H60, Eths 2. C16H3202, M 8150E+03 [Y1] .107430E+04 .152230E+04 .169910E+04 .166500E+04 .166500E+04 .137130E+04 .16630E+04 .116630E+04 .104690E+04 .3737100E+03 .737100E+03 .582700E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m	AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid at variable x ₁ and [Y1] .200E+04 .150E+04	<pre>constant T o [P1] = .298150E+03</pre>	ORTJ0954.064
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .172900E+00 .305400E+00 .410100E+00 .498800E+00 .567200E+00 .666600E+00 .706900E+00 .838600E+00 .838600E+00 .838600E+00 .874200E+00 .999100E+00 .940600E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₂ H ₆ O, Eths 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .107430E+04 .152230E+04 .169910E+04 .166500E+04 .166500E+04 .18440E+04 .18440E+04 .137130E+04 .116630E+04 .104690E+04 .888500E+03 .737100E+03 .582700E+03 .421300E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m Inol Aethyl pentadeca	AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid at variable x ₁ and [Y1] .200E+04 .150E+04	<pre>constant T o [P1] = .298150E+03</pre>	ORTJ0954.064
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .172900E+00 .305400E+00 .410100E+00 .498800E+00 .567200E+00 .666600E+00 .706900E+00 .838600E+00 .838600E+00 .874200E+00 .99100E+00 .99100E+00 .957900E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₂ H ₆ O, Eths 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .107430E+04 .152230E+04 .169910E+04 .166500E+04 .166500E+04 .18440E+04 .18440E+04 .188400E+04 .104690E+04 .888500E+03 .737100E+03 .582700E+03 .421300E+03 .315900E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m Inol Aethyl pentadeca	AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid at variable x ₁ and [Y1] .200E+04 .150E+04 .100E+04	<pre>constant T </pre> ○ [P1] = .298150E+03	ORTJ0954.064
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .172900E+00 .305400E+00 .410100E+00 .498800E+00 .567200E+00 .666600E+00 .706900E+00 .838600E+00 .838600E+00 .838600E+00 .874200E+00 .909100E+00 .940600E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₂ H ₆ O, Eths 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .107430E+04 .152230E+04 .169910E+04 .166500E+04 .166500E+04 .18440E+04 .18440E+04 .188500E+03 .737100E+03 .582700E+03 .421300E+03 .315900E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m Inol Aethyl pentadeca	AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid at variable x ₁ and [Y1] .200E+04 .150E+04	<pre>constant T </pre> ○ [P1] = .298150E+03	ORTJ0954.064
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .172900E+00 .305400E+00 .410100E+00 .498800E+00 .567200E+00 .666600E+00 .706900E+00 .838600E+00 .838600E+00 .838600E+00 .99100E+00 .99100E+00 .957900E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₂ H ₆ O, Eths 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .107430E+04 .152230E+04 .169910E+04 .166500E+04 .166500E+04 .18440E+04 .18440E+04 .188400E+04 .104690E+04 .888500E+03 .737100E+03 .582700E+03 .421300E+03 .315900E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m Inol Aethyl pentadeca	AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid at variable x ₁ and [Y1] .200E+04 .150E+04 .100E+04	<pre>constant T </pre> ○ [P1] = .298150E+03	ORTJ0954.064
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .172900E+00 .305400E+00 .410100E+00 .498800E+00 .567200E+00 .666600E+00 .706900E+00 .838600E+00 .838600E+00 .838600E+00 .99100E+00 .99100E+00 .957900E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₂ H ₆ O, Eths 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .107430E+04 .152230E+04 .169910E+04 .166500E+04 .166500E+04 .18440E+04 .18440E+04 .188400E+04 .104690E+04 .888500E+03 .737100E+03 .582700E+03 .421300E+03 .315900E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m Inol Aethyl pentadeca	AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid at variable x ₁ and [Y1] .200E+04 .150E+04 .100E+04	<pre>constant T </pre> ○ [P1] = .298150E+03	ORTJ0954.064
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .172900E+00 .305400E+00 .410100E+00 .498800E+00 .567200E+00 .666600E+00 .706900E+00 .838600E+00 .838600E+00 .874200E+00 .99100E+00 .99100E+00 .957900E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₂ H ₆ O, Eths 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .107430E+04 .152230E+04 .169910E+04 .166500E+04 .166500E+04 .18440E+04 .18440E+04 .188400E+04 .104690E+04 .888500E+03 .737100E+03 .582700E+03 .421300E+03 .315900E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m Inol Aethyl pentadeca	AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid at variable x ₁ and [Y1] .200E+04 .150E+04 .100E+04	<pre>constant T </pre> ○ [P1] = .298150E+03	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .172900E+00 .305400E+00 .410100E+00 .498800E+00 .567200E+00 .666600E+00 .706900E+00 .838600E+00 .838600E+00 .8374200E+00 .990100E+00 .940600E+00 .957900E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₂ H ₆ O, Eths 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .107430E+04 .152230E+04 .169910E+04 .166500E+04 .166500E+04 .18440E+04 .18440E+04 .188400E+04 .104690E+04 .888500E+03 .737100E+03 .582700E+03 .421300E+03 .315900E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m Inol Aethyl pentadeca	AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	100E+04 .150E+04 .100E+04	<pre>constant T </pre> ○ [P1] = .298150E+03	ORTJ0954.064
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .172900E+00 .305400E+00 .410100E+00 .498800E+00 .567200E+00 .624300E+00 .666600E+00 .706900E+00 .838600E+00 .838600E+00 .999100E+00 .999100E+00 .957900E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₂ H ₆ O, Eths 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .107430E+04 .152230E+04 .169910E+04 .166500E+04 .166500E+04 .18440E+04 .18440E+04 .188400E+04 .104690E+04 .888500E+03 .737100E+03 .582700E+03 .421300E+03 .315900E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m Inol Aethyl pentadeca	AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid at variable x ₁ and [Y1] .200E+04 .150E+04 .100E+04	○ [P1] = .298150E+03	ORTJ0954.064
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .172900E+00 .305400E+00 .410100E+00 .498800E+00 .567200E+00 .624300E+00 .666600E+00 .706900E+00 .838600E+00 .838600E+00 .999100E+00 .999100E+00 .957900E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₂ H ₆ O, Eths 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .107430E+04 .152230E+04 .169910E+04 .166500E+04 .166500E+04 .18440E+04 .18440E+04 .188400E+04 .104690E+04 .888500E+03 .737100E+03 .582700E+03 .421300E+03 .315900E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m Inol Aethyl pentadeca	AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	100E+04 .150E+04 .100E+04	<pre>constant T </pre> ○ [P1] = .298150E+03	ORTJ0954.064

Property Code:	[HMSD1000] HE	AT OF MIXING	G AND SOLUTION		ORTJ0954.002
tate:	Two-component s	ystem, single-pha	ase liquid or two-pha	se liquid-liquid (LL)	
	Pure component 1 Pure component 2				
arameters:	[P1] <i>T/</i> K,	Temperature			
ariables:	[X1] x ₁ /-,	Mole fraction of	of component 1		
a dha dh	[Y1] HE/Jmol ⁻¹ ,	Molar excess e	nthalpy	at variable x_1 and constant T	
Components:	1. C3HgO, Propa	an-1-ol	leasurement of 112 a	and constant 1	
[P1] = .298	2. C4H8O2, Met	hyl propanoate	T		
[X1]250	[Y1]		1	[Y1] .180E+04	
.783000E-01	.449400E+03				
.159300E+00	.821700E+03			○ [P1] = .298150E+03	
.239400E+00	.112030E+04			 	
.313800E+00 .384100E+00	.134550E+04			<u> </u>	
.447600E+00	.147760E+04 .153120E+04			.135E+04 o c	×, -
.505500E+00	.153400E+04				
.547700E+00	.149020E+04			, o	ò
.590100E+00 .640400E+00	.142780E+04		- 1		
.640400E+00	.134210E+04 .123120E+04			.900E+03	<u>م</u> ا
.737400E+00	.110390E+04			ø	
.794400E+00	.930900E+03				0
.842400E+00 .898400E+00	.751400E+03 .513000E+03				N I
.952600E+00	.260300E+03		$\rho = -i\epsilon$.450E+03	0
				Ĭ	\setminus
					0
			,		
				.000E+00	A A
				.00015+00	
			1	.50E+00	
				.50E+00	[X1]
				.50E+00	[X1]
	LDATA SARL Fra				
Property Code:	[HMSD1000] HE	EAT OF MIXING	G AND SOLUTION	1	[X1] ORTJ0954.011
	[HMSD1000] HE Two-component	EAT OF MIXING	G AND SOLUTION		
Property Code: State:	[HMSD1000] HE Two-component Pure component Pure component	EAT OF MIXING system, single-ph 1, liquid 2, liquid	G AND SOLUTION	1	
Property Code: State: Parameters:	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K,	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature	G AND SOLUTION ase liquid or two-ph	1	
Property Code: State: Parameters:	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$,	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction	G AND SOLUTION ase liquid or two-ph of component 1	1	
Property Code: State: Parameters: /arlables: Method:	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu	AT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e rre calorimetric n	G AND SOLUTION ase liquid or two-ph: of component 1 enthalpy	1	
Property Code: State: Parameters: /ariables: Method:	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$,	AT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n an-1-ol	G AND SOLUTION ase liquid or two-ph: of component 1 enthalpy	ł ase liquid-liquid (LL)	
Property Code: State: Parameters: /ariables: /dethod: Components: [P1] = .298	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^{E}/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₅ H ₁₀ O ₂ , Ma B150E+03	AT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n an-1-ol	G AND SOLUTION ase liquid or two-ph: of component 1 enthalpy	ase liquid-liquid (LL) at variable x_1 and constant T [Y1]	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1]	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₅ H ₁₀ O ₂ , Me B150E+03 [Y1]	AT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n an-1-ol	G AND SOLUTION ase liquid or two-ph: of component 1 enthalpy	ase liquid-liquid (LL) at variable x_1 and constant T	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .877000E-01	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₅ H ₁₀ O ₂ , Me B150E+03 [Y1] .534100E+03	AT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n an-1-ol	G AND SOLUTION ase liquid or two-ph: of component 1 enthalpy	ase liquid-liquid (LL) at variable x_1 and constant T [Y1] .160E+04	ORTJ0954.011
Property Code: State: Parameters: Variables: Variables: Method: Components: [P1] = .298 [X1] .877000E-01 .178300E+00	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^{E}/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₅ H ₁₀ O ₂ , Me B150E+03 [Y1] .534100E+03 .904400E+03	AT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n an-1-ol	G AND SOLUTION ase liquid or two-ph: of component 1 enthalpy	ase liquid-liquid (LL) at variable x_1 and constant T [Y1] .160E+04	ORTJ0954.011
Property Code: State: Parameters: Variables: Variables: Method: Components: [P1] = .298 [X1] .877000E-01 .178300E+00 .263800E+00	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₅ H ₁₀ O ₂ , Me B150E+03 [Y1] .534100E+03 .904400E+03 .119630E+04	AT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n an-1-ol	G AND SOLUTION ase liquid or two-ph: of component 1 enthalpy	ase liquid-liquid (LL) at variable x_1 and constant T [Y1]	ORTJ0954.011
Property Code: State: Parameters: Variables: Variables: Method: Components: [P1] = .298 [X1] .877000E-01 .178300E+00 .263800E+00 .342600E+00 .414500E+00	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^{E}/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₅ H ₁₀ O ₂ , Me B150E+03 [Y1] .534100E+03 .904400E+03	AT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n an-1-ol	G AND SOLUTION ase liquid or two-ph: of component 1 enthalpy	ase liquid-liquid (LL) at variable x_1 and constant T [Y1] .160E+04	ORTJ0954.011
Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C3H8O, Prop 2. C5H10O2, Me B150E+03 [Y1] .534100E+03 .904400E+03 .119630E+04 .137480E+04 .146340E+04 .148720E+04	AT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n an-1-ol	G AND SOLUTION ase liquid or two-ph: of component 1 enthalpy	ase liquid-liquid (LL) at variable x_1 and constant T [Y1] .160E+04	ORTJ0954.011
Property Code: State: Parameters: Variables: Variables: Vethod: Components: [P1] = .298 [X1] .877000E-01 .178300E+00 .263800E+00 .342600E+00 .414500E+00 .477500E+00 .534300E+00	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. C3H8O, Prop 2. C5H10O2, Me B150E+03 [Y1] .534100E+03 .904400E+03 .119630E+04 .137480E+04 .146340E+04 .148720E+04 .147110E+04	AT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n an-1-ol	G AND SOLUTION ase liquid or two-ph: of component 1 enthalpy	ase liquid-liquid (LL) at variable x_1 and constant T [Y1] .160E+04	ORTJ0954.011
Property Code: State: Parameters: Variables: Variables: Method: Components: [P1] = .298 [X1] .877000E-01 .178300E+00 .263800E+00 .342600E+00 .342600E+00 .34300E+00 .534300E+00 .583900E+00	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₅ H ₁₀ O ₂ , Ma B150E+03 [Y1] .534100E+03 .119630E+04 .137480E+04 .146340E+04 .148720E+04 .142410E+04	AT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n an-1-ol	G AND SOLUTION ase liquid or two-ph: of component 1 enthalpy	ase liquid-liquid (LL) at variable x_1 and constant T [Y1] .160E+04	ORTJ0954.011
Property Code: State: Parameters: Variables: Variables: Method: Components: [P1] = .298 [X1] .877000E-01 .178300E+00 .263800E+00 .342600E+00 .414500E+00 .534300E+00	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. C3H8O, Prop 2. C5H10O2, Me B150E+03 [Y1] .534100E+03 .904400E+03 .119630E+04 .137480E+04 .146340E+04 .148720E+04 .147110E+04	AT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n an-1-ol	G AND SOLUTION ase liquid or two-ph: of component 1 enthalpy	ase liquid-liquid (LL) at variable x_1 and constant T [Y1] .160E+04 .120E+04	ORTJ0954.011
Property Code: State: Parameters: Variables: Variables: Method: Components: [P1] = .298 [X1] .877000E-01 .178300E+00 .263800E+00 .414500E+00 .534300E+00 .534300E+00 .534300E+00 .626800E+00 .664300E+00 .675900E+00	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol-1, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₅ H ₁₀ O ₂ , Ma 3150E+03 [Y1] .534100E+03 .19630E+04 .19630E+04 .146340E+04 .146340E+04 .147110E+04 .142410E+04 .142670E+04 .128880E+04 .125790E+04	AT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n an-1-ol	G AND SOLUTION ase liquid or two-ph: of component 1 enthalpy	ase liquid-liquid (LL) at variable x_1 and constant T [Y1] .160E+04	ORTJ0954.011
Property Code: State: Parameters: /arlable: /arlables: /arlables: /arlable: /a	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₅ H ₁₀ O ₂ , Ma 3150E+03 [Y1] .534100E+03 .19630E+04 .19630E+04 .146340E+04 .146340E+04 .147110E+04 .142410E+04 .142670E+04 .128880E+04 .125790E+04 .113930E+04	AT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n an-1-ol	G AND SOLUTION ase liquid or two-ph: of component 1 enthalpy	ase liquid-liquid (LL) at variable x_1 and constant T [Y1] .160E+04 .120E+04	ORTJ0954.011
Property Code: State: Parameters: /arlable: /arlable: /arl	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] HE/Jmol-1, Direct low-pressu 1. C3H8O, Prop 2. C5H10O2, Me 3150E+03 [Y1] .534100E+03 .119630E+04 .137480E+04 .146340E+04 .146340E+04 .146720E+04 .147110E+04 .142410E+04 .128880E+04 .125790E+04 .125790E+04 .13930E+04 .992800E+03	AT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n an-1-ol	G AND SOLUTION ase liquid or two-ph: of component 1 enthalpy	ase liquid-liquid (LL) at variable x_1 and constant T [Y1] .160E+04 .120E+04	ORTJ0954.011
Property Code: State: Parameters: Variables: Variables: Variables: [P1] = .298 [X1] .877000E-01 .178300E+00 .263800E+00 .414500E+00 .447050E+00 .534300E+00 .626800E+00 .626800E+00 .626800E+00 .626800E+00 .723000E+00 .772300E+00 .870400E+00	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₅ H ₁₀ O ₂ , Ma 3150E+03 [Y1] .534100E+03 .19630E+04 .19630E+04 .146340E+04 .146340E+04 .147110E+04 .142410E+04 .142670E+04 .128880E+04 .125790E+04 .113930E+04	AT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n an-1-ol	G AND SOLUTION ase liquid or two-ph: of component 1 enthalpy	ase liquid-liquid (LL) at variable x_1 and constant T [Y1] .160E+04 .120E+04	ORTJ0954.011
Property Code: State: Parameters: Variables: Variables: Variables: [P1] = .298 [X1] .877000E-01 .178300E+00 .263800E+00 .263800E+00 .414500E+00 .583900E+00 .626800E+00 .664300E+00 .675900E+00 .72300E+00 .72300E+00 .870400E+00 .870400E+00 .918600E+00	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C3H8O, Prop 2. C5H10O2, Me 3150E+03 [Y1] .534100E+03 .904400E+03 .119630E+04 .146340E+04 .146340E+04 .148720E+04 .148720E+04 .142410E+04 .142410E+04 .12880E+04 .125790E+04 .125790E+04 .113930E+04 .992800E+03 .825400E+03 .632800E+03 .632800E+03 .632800E+03	AT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n an-1-ol	G AND SOLUTION ase liquid or two-ph: of component 1 enthalpy	ase liquid-liquid (LL) at variable x_1 and constant T [Y1] .160E+04 .120E+04	ORTJ0954.011
Property Code: State: Parameters: Variables: Variables: Variables: [P1] = .298 [X1] .877000E-01 .178300E+00 .263800E+00 .414500E+00 .447050E+00 .534300E+00 .626800E+00 .626800E+00 .626800E+00 .626800E+00 .723000E+00 .772300E+00 .870400E+00	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₅ H ₁₀ O ₂ , Me 150E+03 [Y1] .534100E+03 .119630E+04 .146340E+04 .146340E+04 .146340E+04 .148720E+04 .148720E+04 .148720E+04 .146770E+04 .128880E+04 .128880E+04 .125790E+04 .13930E+04 .992800E+03 .632800E+03 .632800E+03	AT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n an-1-ol	G AND SOLUTION ase liquid or two-ph: of component 1 enthalpy	at variable x_1 and constant T [Y1] .160E+04 .120E+04 .800E+03 .800E+03	ORTJ0954.011
Property Code: State: Parameters: Variables: Variables: Variables: [P1] = .298 [X1] .877000E-01 .178300E+00 .263800E+00 .263800E+00 .414500E+00 .583900E+00 .626800E+00 .664300E+00 .675900E+00 .72300E+00 .72300E+00 .870400E+00 .870400E+00 .918600E+00	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C3H8O, Prop 2. C5H10O2, Me 3150E+03 [Y1] .534100E+03 .904400E+03 .119630E+04 .146340E+04 .146340E+04 .148720E+04 .148720E+04 .142410E+04 .142410E+04 .12880E+04 .125790E+04 .125790E+04 .113930E+04 .992800E+03 .825400E+03 .632800E+03 .632800E+03 .632800E+03	AT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n an-1-ol	G AND SOLUTION ase liquid or two-ph: of component 1 enthalpy	A ase liquid-liquid (LL) at variable x_1 and constant T [Y1] .160E+04 .120E+04 .800E+03 .400E+03	ORTJ0954.011
Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C3H8O, Prop 2. C5H10O2, Me 3150E+03 [Y1] .534100E+03 .904400E+03 .119630E+04 .146340E+04 .146340E+04 .148720E+04 .148720E+04 .142410E+04 .142410E+04 .12880E+04 .125790E+04 .125790E+04 .113930E+04 .992800E+03 .825400E+03 .632800E+03 .632800E+03 .632800E+03	AT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n an-1-ol	G AND SOLUTION ase liquid or two-ph: of component 1 enthalpy	at variable x_1 and constant T [Y1] .160E+04 .120E+04 .800E+03 .800E+03	ORTJ0954.011
Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C3H8O, Prop 2. C5H10O2, Me 3150E+03 [Y1] .534100E+03 .904400E+03 .119630E+04 .146340E+04 .146340E+04 .148720E+04 .148720E+04 .142410E+04 .142410E+04 .12880E+04 .125790E+04 .125790E+04 .113930E+04 .992800E+03 .825400E+03 .632800E+03 .632800E+03 .632800E+03	AT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n an-1-ol	G AND SOLUTION ase liquid or two-ph: of component 1 enthalpy	A ase liquid-liquid (LL) at variable x_1 and constant T [Y1] .160E+04 .120E+04 .800E+03 .400E+03 .400E+03 .0 [P1] = .298150E	ORTJ0954.011
Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C3H8O, Prop 2. C5H10O2, Me 3150E+03 [Y1] .534100E+03 .904400E+03 .119630E+04 .146340E+04 .146340E+04 .148720E+04 .148720E+04 .142410E+04 .142410E+04 .12880E+04 .125790E+04 .125790E+04 .113930E+04 .992800E+03 .825400E+03 .632800E+03 .632800E+03 .632800E+03	AT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n an-1-ol	G AND SOLUTION ase liquid or two-ph: of component 1 enthalpy	Image: selection of the s	ORTJ0954.011
Property Code: itate: Parameters: /ariables: /aria	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C3H8O, Prop 2. C5H10O2, Me 3150E+03 [Y1] .534100E+03 .904400E+03 .119630E+04 .146340E+04 .146340E+04 .148720E+04 .148720E+04 .142410E+04 .142410E+04 .12880E+04 .125790E+04 .125790E+04 .113930E+04 .992800E+03 .825400E+03 .632800E+03 .632800E+03 .632800E+03	AT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n an-1-ol	G AND SOLUTION ase liquid or two-ph: of component 1 enthalpy	A ase liquid-liquid (LL) at variable x_1 and constant T [Y1] .160E+04 .120E+04 .800E+03 .400E+03 .400E+03 .0 [P1] = .298150E	ORTJ0954.011

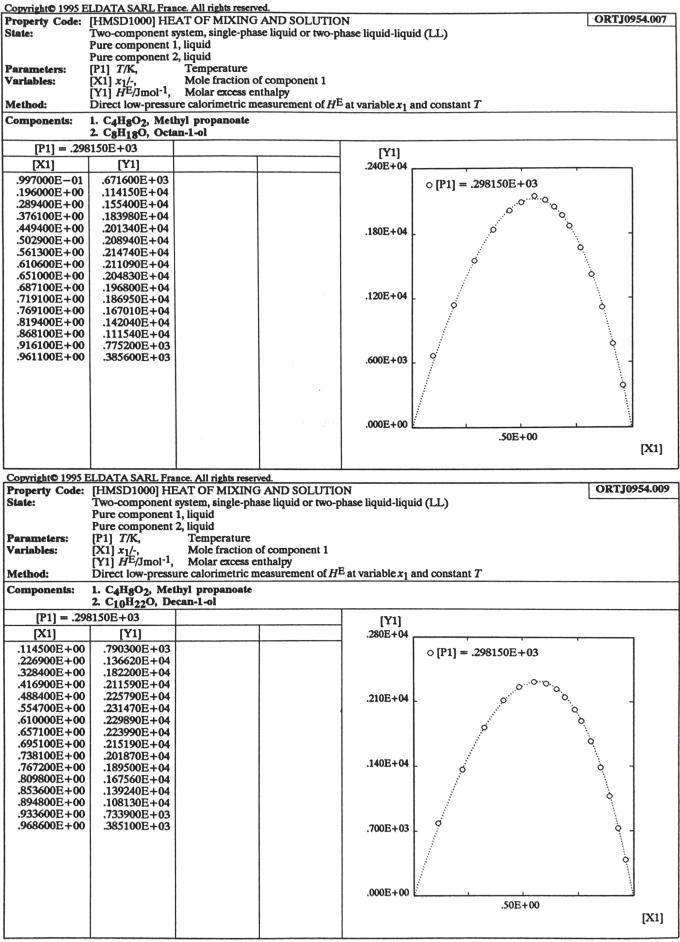
		ace. All rights reserve		r	ORTJ0954.02
State:		system, single-phas			
	Pure component		e aquie er two pa	se iquia iqu	
	Pure component				
Parameters:	[P1] <i>T/</i> K,	Temperature			
Variables:	$[X1] x_1/-,$	Mole fraction of			
	$[Y1]$ $H^{E}/Jmol^{-1}$,	Molar excess ent	thalpy		
Method:	Direct low-pressu	re calorimetric me	asurement of $H^{\rm E}$ a	at variable x_1 a	and constant T
Components:	1. C3HgO, Propa	an-1-ol			
	2. C ₆ H ₁₂ O ₂ , Me	thyl pentanoate			
[P1] = .298	8150E+03		200	[Y1]	
[X1]	[Y1]			.180E+04	
		da da		.1001.704	
.850000E-01	.555100E+03 .977600E+03	· · · · · · · · · · · · · · · · · · ·	d.		\circ [P1] = .298150E+03
.179100E+00 .271500E+00	.128760E+04				
.345100E+00	.143760E+04				
.416000E+00	.151920E+04			.135E+04	,o ~o,
.474000E+00	.153270E+04			.13515+04	
.521300E+00	.151180E+04				
.566000E+00	.146530E+04				
.603100E+00	.141610E+04				ò.
.633700E+00	.135470E+04			0007	<u> </u>
.671500E+00	.126910E+04			.900E+03	t / 🤍 1
.709600E+00	.116970E+04				$ \rangle / \rangle = \langle \rangle \rangle \rangle \rangle \rangle \rangle \rangle \rangle \rangle \rangle$
.751800E+00	.104230E+04				
.799600E+00 .847100E+00	.890800E+03				$ \rangle$
.84/100E+00	.720000E+03 .533500E+03			1000 . 00	o [P1] = .298150E+03
.934000E+00			the state of the second	.450E+03	-/ \ 1
.971300E+00	.160900E+03				ė
	.1007002105		1995 - Sec. 1997 - Sec. 199	1	
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	and the second second second	makati se seri se se se se se se se se	s men state in the	.000E+00	
		(1, 1, 1, 2, 2, 3, 3, 3, 3, 3, 3, 3, 3, 3, 3, 3, 3, 3,			.50E+00
					[X1
		1 1			· · · ·
					L.
		nce. All rights reserve			
Property Code:	[HMSD1000] HI	EAT OF MIXING	AND SOLUTION		ORTJ0954.0
	[HMSD1000] HI Two-component	EAT OF MIXING system, single-pha	AND SOLUTION		ORTJ0954.0
Property Code:	[HMSD1000] HI Two-component Pure component	EAT OF MIXING system, single-phas 1, liquid	AND SOLUTION		ORTJ0954.0
Property Code: State:	[HMSD1000] HI Two-component Pure component Pure component	EAT OF MIXING system, single-pha 1, liquid 2, liquid	AND SOLUTION		ORTJ0954.0
Property Code: State: Parameters:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K,	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature	AND SOLUTION se liquid or two-ph		ORTJ0954.0
Property Code: State:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-,	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o	AND SOLUTION se liquid or two-ph f component 1		ORTJ0954.0
Property Code: State: Parameters:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ .	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en	AND SOLUTION se liquid or two-ph f component 1 athalpy	ase liquid-liqu	id (LL)
Property Code: State: Parameters: Variables: Method:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo	AND SOLUTION se liquid or two-ph f component 1 athalpy	ase liquid-liqu	id (LL)
Property Code: State: Parameters: Variables:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo	AND SOLUTION se liquid or two-ph f component 1 athalpy	ase liquid-liqu	id (LL)
Property Code: State: Parameters: Variables: Method:	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [X1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C3H8O, Prop 2. C8H16O2, M	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo aan-1-ol	AND SOLUTION se liquid or two-ph f component 1 athalpy	ase liquid-liqu at variable x_1 ;	id (LL)
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₈ H ₁₆ O ₂ , M 8150E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo aan-1-ol	AND SOLUTION se liquid or two-ph f component 1 athalpy	ase liquid-liqu at variable x ₁ ; [Y1]	id (LL)
Property Code: State: Parameters: Variables: Method: Components: [P1] = .294 [X1]	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₈ H ₁₆ O ₂ , M 8150E+03 [Y1]	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo aan-1-ol	AND SOLUTION se liquid or two-ph f component 1 athalpy	ase liquid-liqu at variable x_1 ;	id (LL) and constant T
Property Code: State: Parameters: Variables: Method: Components: [P1] = .294 [X1] .731000E-01	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₃ H ₁₆ O ₂ , M 8150E+03 [Y1] .521200E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo aan-1-ol	AND SOLUTION se liquid or two-ph f component 1 athalpy	ase liquid-liqu at variable x ₁ ; [Y1]	id (LL) and constant T
Property Code: State: Parameters: Variables: Method: Components: [P1] = .294 [X1] .731000E-01 .136300E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₈ H ₁₆ O ₂ , M 8150E+03 [Y1] .521200E+03 .853000E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo aan-1-ol	AND SOLUTION se liquid or two-ph f component 1 athalpy	ase liquid-liqu at variable x ₁ ; [Y1]	id (LL) and constant T
Property Code: State: Parameters: Variables: Method: Components: [P1] = .294 [X1] .731000E-01 .136300E+00 .214600E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₈ H ₁₆ O ₂ , M 8150E+03 [Y1] .521200E+03 .853000E+03 .116950E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo aan-1-ol	AND SOLUTION se liquid or two-ph f component 1 athalpy	ase liquid-liqu at variable x ₁ ; [Y1]	id (LL) and constant T
Property Code: State: Parameters: Variables: Method: Components: [P1] = .294 [X1] .731000E-01 .136300E+00 .214600E+00 .300900E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₈ H ₁₆ O ₂ , M 8150E+03 [Y1] .521200E+03 .853000E+03 .116950E+04 .140170E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo aan-1-ol	AND SOLUTION se liquid or two-ph f component 1 athalpy	ase liquid-liqu at variable x ₁ ; [Y1] .180E+04	id (LL) and constant T
Property Code: State: Parameters: Variables: Method: Components: [P1] = .294 [X1] .731000E-01 .136300E+00 .214600E+00 .300900E+00 .367900E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₈ H ₁₆ O ₂ , M 8150E+03 [Y1] .521200E+03 .853000E+03 .116950E+04 .140170E+04 .150170E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo aan-1-ol	AND SOLUTION se liquid or two-ph f component 1 athalpy	ase liquid-liqu at variable x ₁ ; [Y1]	id (LL) and constant T
Property Code: State: Parameters: Variables: Method: Components: [P1] = .294 [X1] .731000E-01 .136300E+00 .214600E+00 .300900E+00 .367900E+00 .435800E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₈ H ₁₆ O ₂ , M 8150E+03 [Y1] .521200E+03 .116950E+04 .140170E+04 .150170E+04 .156070E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo aan-1-ol	AND SOLUTION se liquid or two-ph f component 1 athalpy	ase liquid-liqu at variable x ₁ ; [Y1] .180E+04	id (LL) and constant T
Property Code: State: Parameters: Variables: Method: Components: [P1] = .299 [X1] .731000E-01 .136300E+00 .214600E+00 .300900E+00 .367900E+00 .435800E+00 .491100E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C₃H₈O , Prop 2. C₈H₁₆O₂, M 8150E+03 [Y1] .521200E+03 .853000E+03 .116950E+04 .140170E+04 .150170E+04 .156070E+04 .156040E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo aan-1-ol	AND SOLUTION se liquid or two-ph f component 1 athalpy	ase liquid-liqu at variable x ₁ ; [Y1] .180E+04	id (LL) and constant T
Property Code: State: Parameters: Variables: Method: Components: [P1] = .294 [X1] .731000E-01 .136300E+00 .214600E+00 .309900E+00 .367900E+00 .435800E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₈ H ₁₆ O ₂ , M 8150E+03 [Y1] .521200E+03 .116950E+04 .140170E+04 .150170E+04 .156070E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo aan-1-ol	AND SOLUTION se liquid or two-ph f component 1 athalpy	ase liquid-liqu at variable x ₁ ; [Y1] .180E+04	id (LL) and constant T
Property Code: State: Parameters: Variables: Method: Components: [P1] = .299 [X1] .731000E-01 .136300E+00 .214600E+00 .30990E+00 .367900E+00 .435800E+00 .491100E+00 .528100E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₈ H ₁₆ O ₂ , M 8150E+03 [Y1] .521200E+03 .853000E+03 .116950E+04 .140170E+04 .150170E+04 .156070E+04 .152450E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo aan-1-ol	AND SOLUTION se liquid or two-ph f component 1 athalpy	ase liquid-liqu at variable x ₁ [Y1] .180E+04 .135E+04	id (LL) and constant T
Property Code: State: Parameters: Variables: Method: Components: [P1] = .292 [X1] .731000E-01 .136300E+00 .214600E+00 .367900E+00 .435800E+00 .528100E+00 .578500E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₈ H ₁₆ O ₂ , M 8150E+03 [Y1] .521200E+03 .853000E+03 .116950E+04 .150170E+04 .156040E+04 .156040E+04 .152450E+04 .146150E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo aan-1-ol	AND SOLUTION se liquid or two-ph f component 1 athalpy	ase liquid-liqu at variable x ₁ ; [Y1] .180E+04	id (LL) and constant T
Property Code: State: Variables: Method: Components: [P1] = .294 [X1] .731000E-01 .136300E+00 .214600E+00 .300900E+00 .30900E+00 .491100E+00 .528100E+00 .578500E+00 .622000E+00 .647500E+00 .678900E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₈ H ₁₆ O ₂ , M 8150E+03 [Y1] .521200E+03 .853000E+03 .116950E+04 .140170E+04 .15070E+04 .156070E+04 .156070E+04 .152450E+04 .132240E+04 .132240E+04 .132440E+04 .125860E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo aan-1-ol	AND SOLUTION se liquid or two-ph f component 1 athalpy	ase liquid-liqu at variable x ₁ [Y1] .180E+04 .135E+04	id (LL) and constant T
Property Code: State: Parameters: Variables: Method: Components: [P1] = .294 [X1] .731000E-01 .136300E+00 .214600E+00 .300900E+00 .367900E+00 .435800E+00 .578500E+00 .622000E+00 .647500E+00 .678900E+00 .709200E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₈ H ₁₆ O ₂ , M 8150E+03 [Y1] .521200E+03 .853000E+03 .116950E+04 .140170E+04 .156070E+04 .156040E+04 .152450E+04 .138290E+04 .132440E+04 .125860E+04 .13270E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo aan-1-ol	AND SOLUTION se liquid or two-ph f component 1 athalpy	ase liquid-liqu at variable x ₁ [Y1] .180E+04 .135E+04	id (LL) and constant T
Property Code: State: Parameters: Variables: Method: Components: [P1] = .294 [X1] .731000E-01 .136300E+00 .214600E+00 .300900E+00 .367900E+00 .435800E+00 .528100E+00 .622000E+00 .678900E+00 .678900E+00 .751000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₈ H ₁₆ O ₂ , M 8150E+03 [Y1] .521200E+03 .853000E+03 .116950E+04 .150170E+04 .150170E+04 .156040E+04 .152450E+04 .132440E+04 .125860E+04 .118710E+04 .107660E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo aan-1-ol	AND SOLUTION se liquid or two-ph f component 1 athalpy	ase liquid-liqu at variable x ₁ [Y1] .180E+04 .135E+04	id (LL) and constant T
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .731000E-01 .136300E+00 .214600E+00 .300900E+00 .367900E+00 .578500E+00 .578500E+00 .622000E+00 .678900E+00 .799200E+00 .793100E+00 .793100E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₈ H ₁₆ O ₂ , M 8150E+03 [Y1] .521200E+03 .853000E+03 .116950E+04 .150170E+04 .150170E+04 .150640E+04 .152450E+04 .138290E+04 .132440E+04 .132440E+04 .132440E+04 .125860E+04 .118710E+04 .107060E+04 .936100E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo aan-1-ol	AND SOLUTION se liquid or two-ph f component 1 athalpy	ase liquid-liqu at variable x ₁ ; [Y1] .180E+04 .135E+04 .900E+03	id (LL) and constant T
Property Code: State: Parameters: Variables: Method: Components: [P1] = .292 [X1] .731000E-01 .136300E+00 .214600E+00 .214600E+00 .367900E+00 .367900E+00 .578500E+00 .578500E+00 .622000E+00 .678900E+00 .79100E+00 .79100E+00 .834900E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₈ H ₁₆ O ₂ , M 8150E+03 [Y1] .521200E+03 .853000E+03 .116950E+04 .150170E+04 .150170E+04 .156070E+04 .156040E+04 .152450E+04 .13240E+04 .13240E+04 .125860E+04 .18710E+04 .107060E+04 .782900E+03 .782900E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo aan-1-ol	AND SOLUTION se liquid or two-ph f component 1 athalpy	ase liquid-liqu at variable x ₁ [Y1] .180E+04 .135E+04	id (LL) and constant T
Property Code: State: Parameters: Variables: Method: Components: [P1] = .292 [X1] .731000E-01 .136300E+00 .214600E+00 .214600E+00 .367900E+00 .367900E+00 .578500E+00 .578500E+00 .622000E+00 .678900E+00 .79100E+00 .79100E+00 .834900E+00 .834900E+00 .881000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₈ H ₁₆ O ₂ , M 8150E+03 [Y1] .521200E+03 .853000E+03 .116950E+04 .150170E+04 .150170E+04 .156070E+04 .156040E+04 .152450E+04 .138290E+04 .132440E+04 .125860E+04 .18710E+04 .107060E+04 .382900E+03 .782900E+03 .593400E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo aan-1-ol	AND SOLUTION se liquid or two-ph f component 1 athalpy	ase liquid-liqu at variable x ₁ ; [Y1] .180E+04 .135E+04 .900E+03	id (LL) and constant T
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .731000E - 01 .136300E + 00 .214600E + 00 .300900E + 00 .30900E + 00 .435800E + 00 .578500E + 00 .622000E + 00 .678900E + 00 .709200E + 00 .709200E + 00 .793100E + 00 .834900E + 00 .831000E + 00 .831000E + 00 .831000E + 00 .926498E + 00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₈ H ₁₆ O ₂ , M 8150E+03 [Y1] .521200E+03 .853000E+03 .116950E+04 .140170E+04 .15070E+04 .156070E+04 .156070E+04 .152450E+04 .152450E+04 .132440E+04 .132440E+04 .132440E+04 .18710E+04 .10706E+03 .782900E+03 .593400E+03 .383400E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo aan-1-ol	AND SOLUTION se liquid or two-ph f component 1 athalpy	ase liquid-liqu at variable x ₁ ; [Y1] .180E+04 .135E+04 .900E+03	id (LL) and constant T \circ [P1] = .298150E+03 \circ \circ \circ \circ \circ \circ \circ \circ \circ \circ
Property Code: State: Parameters: Variables: Method: Components: [P1] = .292 [X1] .731000E-01 .136300E+00 .214600E+00 .214600E+00 .367900E+00 .367900E+00 .578500E+00 .578500E+00 .622000E+00 .678900E+00 .79100E+00 .79100E+00 .834900E+00 .834900E+00 .881000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₈ H ₁₆ O ₂ , M 8150E+03 [Y1] .521200E+03 .853000E+03 .116950E+04 .150170E+04 .150170E+04 .156070E+04 .156040E+04 .152450E+04 .138290E+04 .132440E+04 .125860E+04 .18710E+04 .107060E+04 .382900E+03 .782900E+03 .593400E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo aan-1-ol	AND SOLUTION se liquid or two-ph f component 1 athalpy	ase liquid-liqu at variable x ₁ ; [Y1] .180E+04 .135E+04 .900E+03	id (LL) and constant T \circ [P1] = .298150E+03 \circ \circ \circ \circ \circ \circ \circ \circ \circ \circ
Property Code: State: Parameters: Variables: Method: Components: [P1] = .290 [X1] .731000E-01 .136300E+00 .214600E+00 .367900E+00 .435800E+00 .528100E+00 .528100E+00 .578500E+00 .647500E+00 .678900E+00 .709200E+00 .793100E+00 .834900E+00 .834900E+00 .834900E+00 .831000E+00 .926498E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₈ H ₁₆ O ₂ , M 8150E+03 [Y1] .521200E+03 .853000E+03 .116950E+04 .140170E+04 .15070E+04 .156070E+04 .156070E+04 .152450E+04 .152450E+04 .132440E+04 .132440E+04 .132440E+04 .18710E+04 .10706E+03 .782900E+03 .593400E+03 .383400E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo aan-1-ol	AND SOLUTION se liquid or two-ph f component 1 athalpy	ase liquid-liqu at variable x ₁ ; [Y1] .180E+04 .135E+04 .900E+03	id (LL) and constant T
Property Code: State: Parameters: Variables: Method: Components: [P1] = .290 [X1] .731000E-01 .136300E+00 .214600E+00 .367900E+00 .435800E+00 .528100E+00 .528100E+00 .578500E+00 .647500E+00 .678900E+00 .709200E+00 .793100E+00 .834900E+00 .834900E+00 .834900E+00 .831000E+00 .926498E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₈ H ₁₆ O ₂ , M 8150E+03 [Y1] .521200E+03 .853000E+03 .116950E+04 .140170E+04 .15070E+04 .156070E+04 .156070E+04 .152450E+04 .152450E+04 .132440E+04 .132440E+04 .132440E+04 .18710E+04 .10706E+03 .782900E+03 .593400E+03 .383400E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo aan-1-ol	AND SOLUTION se liquid or two-ph f component 1 athalpy	ase liquid-liqu at variable x ₁ ; [Y1] .180E+04 .135E+04 .900E+03	id (LL) and constant T \circ [P1] = .298150E+03 \circ \circ \circ \circ \circ \circ \circ \circ \circ \circ
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .731000E - 01 .136300E + 00 .214600E + 00 .300900E + 00 .30900E + 00 .435800E + 00 .578500E + 00 .578500E + 00 .647500E + 00 .678900E + 00 .709200E + 00 .793100E + 00 .834900E + 00 .831000E + 00 .831000E + 00 .831000E + 00 .926498E + 00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₈ H ₁₆ O ₂ , M 8150E+03 [Y1] .521200E+03 .853000E+03 .116950E+04 .140170E+04 .15070E+04 .156070E+04 .156070E+04 .152450E+04 .152450E+04 .132440E+04 .132440E+04 .132440E+04 .18710E+04 .10706E+03 .782900E+03 .593400E+03 .383400E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo aan-1-ol	AND SOLUTION se liquid or two-ph f component 1 athalpy	ase liquid-liqu <u>at variable x1 ;</u> [Y1] .180E+04 .135E+04 .900E+03 .450E+03	id (LL) and constant T \circ [P1] = .298150E+03 \circ \circ \circ \circ \circ \circ \circ \circ \circ \circ
Property Code: State: Parameters: Variables: Method: Components: [P1] = .290 [X1] .731000E-01 .136300E+00 .214600E+00 .367900E+00 .435800E+00 .528100E+00 .528100E+00 .578500E+00 .647500E+00 .678900E+00 .79200E+00 .793100E+00 .834900E+00 .834900E+00 .834900E+00 .834900E+00 .834900E+00 .83490E+00 .8498E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₈ H ₁₆ O ₂ , M 8150E+03 [Y1] .521200E+03 .853000E+03 .116950E+04 .140170E+04 .15070E+04 .156070E+04 .156070E+04 .152450E+04 .152450E+04 .132440E+04 .132440E+04 .132440E+04 .18710E+04 .10706E+03 .782900E+03 .593400E+03 .383400E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo aan-1-ol	AND SOLUTION se liquid or two-ph f component 1 athalpy	ase liquid-liqu <u>at variable x1 ;</u> [Y1] .180E+04 .135E+04 .900E+03 .450E+03	id (LL) and constant T
Property Code: State: Parameters: Variables: Method: Components: [P1] = .290 [X1] .731000E-01 .136300E+00 .214600E+00 .367900E+00 .435800E+00 .528100E+00 .528100E+00 .578500E+00 .647500E+00 .678900E+00 .79200E+00 .793100E+00 .834900E+00 .834900E+00 .834900E+00 .834900E+00 .834900E+00 .83490E+00 .8498E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₈ H ₁₆ O ₂ , M 8150E+03 [Y1] .521200E+03 .853000E+03 .116950E+04 .140170E+04 .15070E+04 .156070E+04 .156070E+04 .152450E+04 .152450E+04 .132440E+04 .132440E+04 .132440E+04 .18710E+04 .10706E+03 .782900E+03 .593400E+03 .383400E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo aan-1-ol	AND SOLUTION se liquid or two-ph f component 1 athalpy	ase liquid-liqu <u>at variable x1 ;</u> [Y1] .180E+04 .135E+04 .900E+03 .450E+03	id (LL) and constant T

State: Pure component j, liquid Pure compo		ELDATA SARL Fra [HMSD1000] HI			N	ORTJ0954.038
Parameters: Param	State:	Two-component	system, single-pha	ase liquid or two-p	hase liquid-liquid (LL)	
Parameters [P1] T/S. Temperature Weinbod Temperature (Yil) Product of component 1 (Yil)				•		
Virtualities [X] z_{L/s} Mole fraction of component 1 (X1) YEALDACT Direct low pressure calorinetric measurement of H ^B at variable z ₁ and constant T components 1. CafigO, Propen-1-ol 2. CafigO, 2002, Methyl nonanoset [P1] = 298050E+03 [Y1] [X1] [Y1] [X1] [Y1] [X2300E+00] 1.3570E+04 [J3000E+00] 1.3570E+04 [J3000E+00] 1.3570E+04 [J3000E+00] 1.3570E+04 [J3000E+00] 1.3580E+04 [J3000E+00] 1.3580E+04 [J3000E+00] 1.3580E+04 [J3000E+00] 1.34400E+04 [J3000E+00] 1.34400E+04 [J300E+00] 1.34400E+04 [J300E+00] 1.3580E+04		Pure component	2, liquid			
Method [Y1] <i>HE</i> [mon ⁻¹ , Molar access entilably Cemponents: 1. C3H20,07 Prepar-1-01 2. C.(J220,02) Methyl monanosis [Y1] [X1] [Y1] [X1] [Y1] [J2200E+00] 37590E+04 [J2200E+00] 1.05210E+04 [J2200E+00] 1.05210E+04 [J2200E+00] 1.05250E+04 [J2700E+00] 1.05250E+04 [J200E+00] 1.05250E+04 [J200E+00] 1.05250E+04 [J200E+00] 1.05250E+04 [J200E+00] 1.05250E+04 [J200E+00] 1.05460E+04 [J200E+00] 1.05460E+04 [J200E+00] 1.0470E+04 [J200E+00] <td< td=""><td>Parameters:</td><td>[P1] <i>T/</i>K,</td><td></td><td></td><td></td><td></td></td<>	Parameters:	[P1] <i>T/</i> K,				
Method: Direct two-pressure colorimetric measurement of H^E at variable x1 and constant T Components: C. CJRG, Propensition C. CJRG, Propen	Variables:					
Components: 1. C 3H 50, Propun-1-ol 2. C (JB300-2, Methyl nonanoate [P1] 2.83150E+03 [P1] 2.85150E+03 [P1] [Y1] [J3000E+00 1.87550E+04 2.8550E+01 1.87550E+04 2.8550E+01 1.82516E+04 2.8550E+01 1.82516E+04 3.8550E+01 1.82516E+04 3.8550E+01 1.82516E+04 3.8550E+01 1.8450E+04 3.8550E+01 1.8550E+04 3.8550E+01 1.8550E+04 3.8550E+01 1.8550E+04 3.8550E+01 1.5570E+03 3.9560E+00 1.5570E+03 3.9560E+00 1.5570E+03 3.9560E+00 1.5570E+03 3.9560E+00 1.5570E+03 3.9560E+00 1.5570E+04 3.9550E+01 1.970E 1		$[Y1]$ $H^{E}/Jmol^{-1}$,	Molar excess e	nthalpy		
- 2. C ₁ /dE ₂ /dP ₂ /Methyl nonanosic [P1] = 298150E+03 [P1] = 298150E+04 [J2] 000E+00 57590E+04 J2000E+00 157590E+04 J2000E+00 157590E+04 J3000E+00 157590E+04 J4200E+01 15250E+04 J35200E+00 15250E+04 J35200E+00 15250E+04 J35200E+00 158940E+04 J35200E+00 158940E+04 J35200E+00 158940E+04 J35200E+00 158940E+04 J35200E+00 15750E+04 J35200E+00 15750E+04 J35200E+00 15750E+04 J35200E+00 15750E+03 J35200E+00 15750E+03 J35200E+00 15750E+03 J35200E+00 15750E+03 J35200E+00 15750E+03 J35200E+00 15750E+04 J35200E+00 15750E+04 J35200E+00 15770E+04 J35200E+00 15770E+03 J35200E+00 15770E+04 J35200E+00 15770E+04 J35200E+00 15770E+04 J27700E+01 </td <td>Method:</td> <td></td> <td></td> <td>easurement of HI</td> <td>z at variable x_1 and constant T</td> <td></td>	Method:			easurement of HI	z at variable x_1 and constant T	
[Ki] [Y]	-	2. C ₁₀ H ₂₀ O ₂ , M		•		1. st.p
12700E+00 A75800E+03 22300E+00 1.35730E+04 30100E+00 1.37730E+04 43220E+00 1.6230E+04 43220E+01 1.6230E+04 53200E+00 1.5540E+04 53200E+00 1.5640E+04 633700E+00 1.5640E+04 633700E+00 1.35460E+04 633700E+00 1.35460E+04 633700E+00 1.35460E+04 633700E+00 1.35460E+04 633700E+00 1.35170E+04 633700E+00 1.35170E+04 80500E+00 1.351774 80500E+00 1.35		1				
200500E+00 976400E+03 892100E+00 .351700E+03 973900E+00 .351700E+03 973900E+00 .351700E+03 973900E+00 .351700E+03 973900E+00 .351700E+03 973900E+00 .155700E+03 973900E+00 .155700E+03 propriatue 1995 ELDATA SARL Frace. All rizke reserved. prove component 3, liquid arameters: [P1] 7/K, Temperature price component 2, liquid arameters: [C1] H ² / ₂ / ₂ / ₂ / ₂ Methyl undecanoste [P1]298150E+03 [Y1] [X1] [Y1] [X2] [Y1] [X300E+00 .16310E+04 .33200E+00 .16310E+04 .33200E+00 .16310E+04 .33200E+00 .16310E+04 .33200E+00 .16310E+04				and the state	.180E+04	
200500E+00 976400E+03 892100E+00 .351700E+03 973900E+00 .351700E+03 973900E+00 .351700E+03 973900E+00 .351700E+03 973900E+00 .351700E+03 973900E+00 .155700E+03 973900E+00 .155700E+03 propriatue 1995 ELDATA SARL Frace. All rizke reserved. prove component 3, liquid arameters: [P1] 7/K, Temperature price component 2, liquid arameters: [C1] H ² / ₂ / ₂ / ₂ / ₂ Methyl undecanoste [P1]298150E+03 [Y1] [X1] [Y1] [X2] [Y1] [X300E+00 .16310E+04 .33200E+00 .16310E+04 .33200E+00 .16310E+04 .33200E+00 .16310E+04 .33200E+00 .16310E+04						
200500E+00 976400E+03 892100E+00 .351700E+03 973900E+00 .351700E+03 973900E+00 .351700E+03 973900E+00 .351700E+03 973900E+00 .351700E+03 973900E+00 .155700E+03 973900E+00 .155700E+03 propriatue 1995 ELDATA SARL Frace. All rizke reserved. prove component 3, liquid arameters: [P1] 7/K, Temperature price component 2, liquid arameters: [C1] H ² / ₂ / ₂ / ₂ / ₂ Methyl undecanoste [P1]298150E+03 [Y1] [X1] [Y1] [X2] [Y1] [X300E+00 .16310E+04 .33200E+00 .16310E+04 .33200E+00 .16310E+04 .33200E+00 .16310E+04 .33200E+00 .16310E+04					o ^o a.o	
200500E+00 976400E+03 892100E+00 .351700E+03 973900E+00 .351700E+03 973900E+00 .351700E+03 973900E+00 .351700E+03 973900E+00 .351700E+03 973900E+00 .155700E+03 973900E+00 .155700E+03 propriatue 1995 ELDATA SARL Frace. All rizke reserved. prove component 3, liquid arameters: [P1] 7/K, Temperature price component 2, liquid arameters: [C1] H ² / ₂ / ₂ / ₂ / ₂ Methyl undecanoste [P1]298150E+03 [Y1] [X1] [Y1] [X2] [Y1] [X300E+00 .16310E+04 .33200E+00 .16310E+04 .33200E+00 .16310E+04 .33200E+00 .16310E+04 .33200E+00 .16310E+04					, o Čo,	and the second sec
200500E+00 976400E+03 892100E+00 .351700E+03 973900E+00 .351700E+03 973900E+00 .351700E+03 973900E+00 .351700E+03 973900E+00 .351700E+03 973900E+00 .155700E+03 973900E+00 .155700E+03 propriatue 1995 ELDATA SARL Frace. All rizke reserved. prove component 3, liquid arameters: [P1] 7/K, Temperature price component 2, liquid arameters: [C1] H ² / ₂ / ₂ / ₂ / ₂ Methyl undecanoste [P1]298150E+03 [Y1] [X1] [Y1] [X2] [Y1] [X300E+00 .16310E+04 .33200E+00 .16310E+04 .33200E+00 .16310E+04 .33200E+00 .16310E+04 .33200E+00 .16310E+04					0 0	
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935600E+00 351700E+03 973900E+00 155700E+03 973900E+00 155700E+03 operiphic 1995 ELDATA SARL France. All rights reserved. [X1] operiphic 1995 ELDATA SARL France. All rights reserved. [X1] operiphic 1995 ELDATA SARL France. All rights reserved. [X1] operiphic 1995 ELDATA SARL France. All rights reserved. [X1] reperty Code: [HMSD1000] HEAT OF MIXING AND SOLUTION ORTJ0954.047 ate: Two-component system, single-phase liquid rewo-phase liquid.liquid (LL) Pure component 2, liquid arameters: [P1] 7/K, Temperature Temperature arameters: [P1] 7/K, Molar access enthalpy [Mathematic measurement of H ^E at variable x1 and constant T omponents: 1. C3H60, Propan-1-01 2. C12H24O2, MetHyl undecanosie [Y1] [P1] = 228150E+03 [Y1] [X1] [Y1] [X1] [Y1] [X2] [Y1] [X2] [Y1] [X3] [Y1] [X3] [Y1] [X1] [Y1] [X3] [Y1] [X3] [Y1] [X3] [Y1] [X4] [Y1] [X3]					.450E+03	
935600E+00 351700E+03 973900E+00 155700E+03 973900E+00 155700E+03 operiphic 1995 ELDATA SARL France. All rights reserved. [X1] operiphic 1995 ELDATA SARL France. All rights reserved. [X1] operiphic 1995 ELDATA SARL France. All rights reserved. [X1] operiphic 1995 ELDATA SARL France. All rights reserved. [X1] reperty Code: [HMSD1000] HEAT OF MIXING AND SOLUTION ORTJ0954.047 ate: Two-component system, single-phase liquid rewo-phase liquid.liquid (LL) Pure component 2, liquid arameters: [P1] 7/K, Temperature Temperature arameters: [P1] 7/K, Molar access enthalpy [Mathematic measurement of H ^E at variable x1 and constant T omponents: 1. C3H60, Propan-1-01 2. C12H24O2, MetHyl undecanosie [Y1] [P1] = 228150E+03 [Y1] [X1] [Y1] [X1] [Y1] [X2] [Y1] [X2] [Y1] [X3] [Y1] [X3] [Y1] [X1] [Y1] [X3] [Y1] [X3] [Y1] [X3] [Y1] [X4] [Y1] [X3]						o l
.973900E+00 .155700E+03 .000E+00 .000E+00 .000E+00 .973900E+00 .50E+00 [X1] sepretation 1995 ELDATA SARL France. All rights reserved. .000E+00 .000E+00 .000E+00 roperty Code: [HMSD1000] HEAT OF MIXING AND SOLUTION ORTJ0954.047 fast: Two-component system, single-phase liquid or two-phase liquid-liquid (LL) ORTJ0954.047 pure component 1, liquid Pure component 1, liquid ORTJ0954.047 arameters: [P1] 7/K, Temperature Two-component 1, liquid arameters: [P1] 7/K, Temperature .000E+00 2. C12H24O2, Methyl undecanoate .000E+00 .2012H24O2, Methyl undecanoate [P1] = .298150E+04 .32300E+00 .15640E+04 .135E+04 .232300E+00 .16310E+04 .135E+04 .000E+03 .32300E+00 .16310E+04 .000E+03 .000E+03 .32300E+00 .13300E+04 .33010E+04 .000E+03 .32300E+00 .1330E+04 .000E+03 .000E+03 .32300E+00 .13300E+04 .000E+03 .000E+03 .32300E+00 .13300E+04 .000E+03 .000E+03					\circ (P11 - 208150E+03	
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oprizibit© 1995 ELDATA SARL France. All rights reserved. [X1] roperty Code: [HMSD1000] HEAT OF MIXING AND SOLUTION ORTJ0954.047 tale: Two-component system, single-phase liquid or two-phase liquid (LL) Pure component 2, liquid arameters: [P1] 7/K, Temperature Image: Calculation of component 1 tale: TXI, remperature Image: Calculation of component 1 Image: Calculation of component 1 tale: [X1] 7/K, Temperature Image: Calculation of component 1 Image: Calculation of component 1 tariables: [X1] 7/K, Mole fraction of component 1 Image: Calculation of component 1 Image: Calculation of component 1 tariables: [X1] 7/K, Mole fraction of component 1 Image: Calculation of component 1 tariables: [X1] 7/K, Mole fraction of component 1 Image: Calculation of component 1 tariables: [Y1] addition of component 1 [Y1] Image: Calculation of component 1 tariables: [Y1] addition of component 1 [Y1] Image: Calculation of component 1 tariables: [Y1] addition of component 1 Image: Calculation of component 1 tariables: [Y1]						
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opright@ 1995 ELDATA SARL France. All rights reserved. ORTJ0954.047 ase: [HMSD1000] HEAT OF MIXING AND SOLUTION ORTJ0954.047 tate: Two-component system, single-phase liquid or two-phase liquid-liquid (LL) Pure component 2, liquid arameters: [P1] T/K, Temperature Temperature ratables: [X1] x/j, Mole raction of component 1 [Y1] H ^E Jmol-1, Molar excess enthalpy feldd: Direct low-pressure calorimetric measurement of H ^E at variable x1 and constant T monponents: 1. C3H80, Propan-1-ol 1. C3H80, Propan-1-ol 1. C3H80, Propan-1-ol 1. RoBe+04 1.80E+04 1.83E+04 0.00E+03					.50E+00	
Image: Property Code: [HiNSD1000] HEAT OF MIXING AND SOLUTION ORTJ0954.047 fate: Two-component system, single-phase liquid or two-phase liquid (LL) Pure component 1, liquid Pure component 1, liquid Pure component 1, liquid Pure component 2, liquid ariables: [P1] 7/K, Temperature ariables: [X1] x ₁ /-, Mole fraction of component 1 [Y1] JK/, Temperature and constant T omponents: 1. C_3HgO, Propan-1-ol 2. C_12H2AO2, Methyl undecanoale [P1] = .298150E+03 [Y1] [X1] [Y1] 1.80E+04 .247500E+00 .137150E+04 .135E+04 .323400E+00 .166310E+04 .135E+04 .323500E+00 .166310E+04 .135E+04 .555900E+00 .163710E+04 .900E+03 .55900E+00 .137570E+04 .900E+03 .53800E+00 .131750E+04 .900E+03 .32300E+00 .131750E+04 .900E+03 .900E+00 .1317570E+04 .900E+03 .900E+00 .131750E+04 .900E+03 .900E+00 <td></td> <td></td> <td></td> <td></td> <td></td> <td>[X1]</td>						[X1]
Image: Property Code: [HiNSD1000] HEAT OF MIXING AND SOLUTION ORTJ0954.047 fate: Two-component system, single-phase liquid or two-phase liquid (LL) Pure component 1, liquid Pure component 1, liquid Pure component 1, liquid Pure component 2, liquid ariables: [P1] 7/K, Temperature ariables: [X1] x ₁ /-, Mole fraction of component 1 [Y1] JK/, Temperature and constant T omponents: 1. C_3HgO, Propan-1-ol 2. C_12H2AO2, Methyl undecanoale [P1] = .298150E+03 [Y1] [X1] [Y1] 1.80E+04 .247500E+00 .137150E+04 .135E+04 .323400E+00 .166310E+04 .135E+04 .323500E+00 .166310E+04 .135E+04 .555900E+00 .163710E+04 .900E+03 .55900E+00 .137570E+04 .900E+03 .53800E+00 .131750E+04 .900E+03 .32300E+00 .131750E+04 .900E+03 .900E+00 .1317570E+04 .900E+03 .900E+00 .131750E+04 .900E+03 .900E+00 <th></th> <th></th> <th></th> <th></th> <th></th> <th>. ,</th>						. ,
[Y1] H^E/mol^{-1} , Molar excess enthalpy Direct low-pressure calorimetric measurement of H^E at variable x_1 and constant T omponents: 2. C12H24O2, Methyl undecanoate [P1] = .298150E+03 [Y1] .130E+04 [P1] = .298150E+03 [Y1] .130E+04 [X1] [Y1] .130E+04	Property Code:	[HMSD1000] HI Two-component	EAT OF MIXING system, single-pha	AND SOLUTIO		ORTJ0954.047
omponents: 1. C_{3Hg0} , Propan-1-ol 2. $C_{12}H_{24}O_2$, Methyl undecanoate [P1] = .298150E+03 [Y1] [X1] [Y1] 1.41800E+00 .949200E+03 .247500E+00 .137150E+04 .324300E+00 .155640E+04 .324300E+00 .16680E+04 .447600E+00 .16680E+04 .439500E+00 .16680E+04 .439500E+00 .16310E+04 .532500E+00 .163710E+04 .532500E+00 .16310E+04 .532500E+00 .16140E+04 .532500E+00 .16140E+04 .59800E+00 .162130E+04 .663800E+00 .137570E+04 .734500E+00 .118540E+04 .900E+00 .32150E+04 .823900E+00 .92800E+03 .83400E+00 .330100E+03 .907300E+00 .330100E+03 .977600E+00 .147500E+03 .977600E+00 .147500E+03	Property Code: State: Parameters:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K,	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature	AND SOLUTIO		
Image: Sector 12 State 2000 Nethyl undecanoate [P1] = .298150E + 03 [Y1] [X1] [Y1] 1.41800E + 00 .949200E + 03 .247500E + 00 .137150E + 04 .324300E + 00 .164560E + 04 .393600E + 00 .164560E + 04 .447600E + 00 .166830E + 04 .439500E + 00 .166310E + 04 .532500E + 00 .163710E + 04 .532500E + 00 .163710E + 04 .532500E + 00 .163710E + 04 .532500E + 00 .16140E + 04 .559800E + 00 .16140E + 04 .559800E + 00 .137570E + 04 .664200E + 00 .137570E + 04 .664200E + 00 .137570E + 04 .794400E + 00 .101070E + 04 .833400E + 00 .30100E + 03 .997300E + 00 .303100E + 03 .997600E + 00 .147500E + 03 .997600E + 00 .900E + 03 .900E + 00	Property Code: State: Parameters: Variables:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$,	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess et	AND SOLUTIO ase liquid or two-p of component 1 nthalpy	hase liquid-liquid (LL)	
[P1] = .298150E+03 [Y1] [X1] [Y1] .141800E+00 .949200E+03 .247500E+00 .137150E+04 .324300E+00 .155640E+04 .339600E+00 .164560E+04 .447600E+00 .166880E+04 .447600E+00 .166880E+04 .447600E+00 .166310E+04 .505900E+00 .160140E+04 .505900E+00 .160140E+04 .505900E+00 .160140E+04 .509800E+00 .137570E+04 .734500E+00 .137570E+04 .734500E+00 .137570E+04 .794400E+00 .101070E+04 .823900E+00 .902800E+03 .833400E+00 .902800E+03 .833400E+00 .330100E+03 .977600E+00 .147500E+03 .977600E+00 .147500E+03 .977600E+00 .147500E+03	Property Code: State: Parameters: Variables: fethod:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [X1] $H^E/Jmol^{-1}$, Direct low-pressu	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m	AND SOLUTIO ase liquid or two-p of component 1 nthalpy	hase liquid-liquid (LL)	
141800E+00 .949200E+03 .247500E+00 .137150E+04 .324300E+00 .155640E+04 .393600E+00 .166880E+04 .447600E+00 .166880E+04 .493600E+00 .166310E+04 .535200E+00 .166310E+04 .535200E+00 .166310E+04 .535200E+00 .160140E+04 .535900E+00 .152130E+04 .635800E+00 .152130E+04 .663200E+00 .137570E+04 .734500E+00 .118540E+04 .664200E+00 .137570E+04 .794400E+00 .101070E+04 .832900E+00 .330100E+03 .863400E+00 .330100E+03 .9977600E+00 .147500E+03 .977600E+00 .147500E+03 .977600E+00 .147500E+03 .900E+00 .50E+00	Property Code: State: Parameters: Variables: Method: Components:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. CaHgO, Prop.	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en tre calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	hase liquid-liquid (LL)	
141800E+00 .949200E+03 .247500E+00 .137150E+04 .324300E+00 .155640E+04 .393600E+00 .166880E+04 .447600E+00 .166880E+04 .493600E+00 .166310E+04 .535200E+00 .166310E+04 .535200E+00 .166310E+04 .535200E+00 .160140E+04 .535900E+00 .152130E+04 .635800E+00 .152130E+04 .663200E+00 .137570E+04 .734500E+00 .118540E+04 .664200E+00 .137570E+04 .794400E+00 .101070E+04 .832900E+00 .330100E+03 .863400E+00 .330100E+03 .9977600E+00 .147500E+03 .977600E+00 .147500E+03 .977600E+00 .147500E+03 .900E+00 .50E+00	Property Code: State: Parameters: Variables: fethod: Components:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₁₂ H ₂₄ O ₂ , M	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en tre calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	hase liquid-liquid (LL) at variable x_1 and constant T	
.532500E+00 .163710E+04 .565900E+00 .160140E+04 .599800E+00 .152130E+04 .638800E+00 .137570E+04 .664200E+00 .137570E+04 .734500E+00 .118540E+04 .664200E+00 .101070E+04 .823900E+00 .902800E+03 .863400E+00 .740100E+03 .907300E+00 .536100E+03 .9077600E+00 .147500E+03 .977600E+00 .147500E+03 .977600E+00 .147500E+03 .000E+00 .50E+00	Property Code: State: Parameters: /ariables: /dethod: Components: [P1] = .298	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop. 2. C ₁₂ H ₂₄ O ₂ , M 150E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en tre calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	hase liquid-liquid (LL) $\frac{1}{2}$ at variable x_1 and constant T [Y1] .180E+04	ORTJ0954.047
.532500E+00 .163710E+04 .565900E+00 .160140E+04 .599800E+00 .152130E+04 .638800E+00 .137570E+04 .664200E+00 .137570E+04 .734500E+00 .118540E+04 .664200E+00 .101070E+04 .823900E+00 .902800E+03 .863400E+00 .740100E+03 .907300E+00 .536100E+03 .9077600E+00 .147500E+03 .977600E+00 .147500E+03 .977600E+00 .147500E+03 .000E+00 .50E+00	Property Code: State: Parameters: /ariables: Method: Components: [P1] = .298 [X1]	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^{E}/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1]	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en tre calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	hase liquid-liquid (LL) $\frac{1}{2}$ at variable x_1 and constant T [Y1] .180E+04	ORTJ0954.047
.532500E+00 .163710E+04 .565900E+00 .160140E+04 .599800E+00 .152130E+04 .638800E+00 .137570E+04 .664200E+00 .137570E+04 .734500E+00 .118540E+04 .664200E+00 .101070E+04 .823900E+00 .902800E+03 .863400E+00 .740100E+03 .907300E+00 .536100E+03 .9077600E+00 .147500E+03 .977600E+00 .147500E+03 .977600E+00 .147500E+03 .000E+00 .50E+00	Property Code: State: Parameters: /ariables:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^{E}/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .949200E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en tre calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	hase liquid-liquid (LL) $\frac{1}{2}$ at variable x_1 and constant T [Y1] .180E+04	ORTJ0954.047
.532500E+00 .163710E+04 .565900E+00 .160140E+04 .599800E+00 .152130E+04 .638800E+00 .137570E+04 .664200E+00 .137570E+04 .734500E+00 .118540E+04 .664200E+00 .101070E+04 .823900E+00 .902800E+03 .863400E+00 .740100E+03 .907300E+00 .536100E+03 .9077600E+00 .147500E+03 .977600E+00 .147500E+03 .977600E+00 .147500E+03 .000E+00 .50E+00	Property Code: State: Parameters: /ariable: /ariable: /ari	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .949200E+03 .137150E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en tre calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	hase liquid-liquid (LL) $\frac{1}{2}$ at variable x_1 and constant T [Y1] .180E+04	ORTJ0954.047
.532500E+00 .163710E+04 .565900E+00 .160140E+04 .599800E+00 .152130E+04 .638800E+00 .137570E+04 .664200E+00 .137570E+04 .734500E+00 .118540E+04 .664200E+00 .101070E+04 .823900E+00 .902800E+03 .863400E+00 .740100E+03 .907300E+00 .536100E+03 .9077600E+00 .147500E+03 .977600E+00 .147500E+03 .977600E+00 .147500E+03 .000E+00 .50E+00	Property Code: State: Parameters: Variables: Variables: (ethod: Components: [P1] = .298 [X1] .141800E+00 .247500E+00 .324300E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .949200E+03 .137150E+04 .155640E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en tre calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	hase liquid-liquid (LL) $\frac{1}{2}$ at variable x_1 and constant T [Y1] .180E+04	ORTJ0954.047
.532500E+00 .163710E+04 .565900E+00 .160140E+04 .599800E+00 .152130E+04 .638800E+00 .137570E+04 .664200E+00 .137570E+04 .734500E+00 .118540E+04 .664200E+00 .101070E+04 .823900E+00 .902800E+03 .863400E+00 .740100E+03 .907300E+00 .536100E+03 .9077600E+00 .147500E+03 .977600E+00 .147500E+03 .977600E+00 .147500E+03 .000E+00 .50E+00	Property Code: State: Parameters: Variables: Variables: (ethod: Components: [P1] = .298 [X1] .141800E+00 .247500E+00 .324300E+00 .393600E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^{E}/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .949200E+03 .137150E+04 .155640E+04 .164560E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en tre calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	hase liquid-liquid (LL) $\frac{1}{2}$ at variable x_1 and constant T [Y1] .180E+04	ORTJ0954.047
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	Property Code: State: Parameters: /ariables: /ariables: fethod: Components: [P1] = .298 [X1] .141800E+00 .247500E+00 .324300E+00 .393600E+00 .447600E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .949200E+03 .137150E+04 .155640E+04 .164560E+04 .166880E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en tre calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	hase liquid-liquid (LL) $\frac{1}{2}$ at variable x_1 and constant T [Y1] .180E+04	ORTJ0954.047
.599800E+00 .152130E+04 .635800E+00 .143790E+04 .664200E+00 .137570E+04 .734500E+00 .118540E+04 .734500E+00 .101070E+04 .823900E+00 .902800E+03 .863400E+00 .536100E+03 .907300E+00 .536100E+03 .9977600E+00 .147500E+03 .977600E+00 .147500E+03 .977600E+00 .147500E+03 .000E+00 .50E+00	Property Code: State: Parameters: Variables: Variables: Variables: (P1] = .298 [X1] .141800E+00 .247500E+00 .324300E+00 .393600E+00 .447600E+00 .493600E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .949200E+03 .137150E+04 .155640E+04 .166580E+04 .166310E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en tre calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	hase liquid-liquid (LL) x_{1} and constant T [Y1] .180E+04 .135E+04	ORTJ0954.047
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	Property Code: State: Parameters: Variables: Variables: Variables: Variables: (P1] = .298 [X1] .141800E+00 .247500E+00 .324300E+00 .447600E+00 .493600E+00 .532500E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .949200E+03 .137150E+04 .155640E+04 .166580E+04 .166310E+04 .163710E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en tre calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	hase liquid-liquid (LL) x_{1} and constant T [Y1] .180E+04 .135E+04	ORTJ0954.047
.794400E+00 .101070E+04 .823900E+00 .902800E+03 .863400E+00 .740100E+03 .907300E+00 .536100E+03 .907300E+00 .330100E+03 .977600E+00 .147500E+03 .000E+00 .50E+03	Property Code: State: Parameters: Variables: Variables: Variables: (P1] = .298 [X1] .141800E+00 .247500E+00 .324300E+00 .447600E+00 .493600E+00 .532500E+00 .565900E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .949200E+03 .137150E+04 .155640E+04 .166580E+04 .166310E+04 .166310E+04 .160140E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en tre calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	hase liquid-liquid (LL) x_{1} and constant T [Y1] .180E+04 .135E+04	ORTJ0954.047
.794400E+00 .101070E+04 .823900E+00 .902800E+03 .863400E+00 .740100E+03 .907300E+00 .536100E+03 .946400E+00 .330100E+03 .977600E+00 .147500E+03 .000E+00 .50E+00	Property Code: State: Parameters: Variables: Variables: (ethod: Components: [P1] = .298 [X1] .141800E+00 .247500E+00 .324300E+00 .447600E+00 .493600E+00 .532500E+00 .565900E+00 .599800E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .949200E+03 .137150E+04 .155640E+04 .166560E+04 .166880E+04 .166310E+04 .160140E+04 .152130E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en tre calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	hase liquid-liquid (LL) x_{1} and constant T [Y1] .180E+04 .135E+04	ORTJ0954.047
.794400E+00 .101070E+04 .823900E+00 .902800E+03 .863400E+00 .740100E+03 .907300E+00 .536100E+03 .907300E+00 .330100E+03 .977600E+00 .147500E+03 .000E+00 .50E+00	roperty Code: itate: arameters: aramete	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .949200E+03 .137150E+04 .155640E+04 .166560E+04 .166880E+04 .166310E+04 .166310E+04 .160140E+04 .152130E+04 .143790E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en tre calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	hase liquid-liquid (LL) x_1 and constant T [Y1] .180E+04 .135E+04 .135E+04	ORTJ0954.047
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	Property Code: State: Parameters: Variables: Variables: Variables: (ethod: Components: [P1] = .298 [X1] .141800E+00 .247500E+00 .324300E+00 .447600E+00 .493600E+00 .532500E+00 .565900E+00 .559800E+00 .635800E+00 .664200E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .949200E+03 .137150E+04 .155640E+04 .166880E+04 .166880E+04 .166310E+04 .166310E+04 .160140E+04 .152130E+04 .143790E+04 .137570E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en tre calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	hase liquid-liquid (LL) x_1 and constant T [Y1] .180E+04 .135E+04 .135E+04	ORTJ0954.047
.863400E+00 .740100E+03 .907300E+00 .536100E+03 .946400E+00 .330100E+03 .977600E+00 .147500E+03 .000E+00 .50E+00	roperty Code: itate: arameters: ariables: fethod: components: [P1] = .298 [X1] .141800E+00 .247500E+00 .324300E+00 .393600E+00 .447600E+00 .532500E+00 .565900E+00 .635800E+00 .635800E+00 .635800E+00 .635800E+00 .734500E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .949200E+03 .137150E+04 .155640E+04 .166560E+04 .166880E+04 .166310E+04 .166310E+04 .160140E+04 .152130E+04 .137570E+04 .137570E+04 .118540E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en tre calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	hase liquid-liquid (LL) x_1 and constant T [Y1] .180E+04 .135E+04 .135E+04	ORTJ0954.047
946400E+00 977600E+00 .147500E+03 .147500E+03 .000E+00 .000E+00	Property Code: State: Parameters: Variables: Varia	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .949200E+03 .137150E+04 .155640E+04 .166880E+04 .166880E+04 .166310E+04 .160140E+04 .160140E+04 .137570E+04 .137570E+04 .118540E+04 .101070E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en tre calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	hase liquid-liquid (LL) x_1 and constant T [Y1] .180E+04 .135E+04 .135E+04	ORTJ0954.047
946400E+00 977600E+00 .147500E+03 .147500E+03 .000E+00 .000E+00	Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .949200E+03 .137150E+04 .155640E+04 .166880E+04 .166880E+04 .166310E+04 .160140E+04 .160140E+04 .137570E+04 .137570E+04 .118540E+04 .101070E+04 .902800E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en tre calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	hase liquid-liquid (LL) x_1 and constant T [Y1] .180E+04 .135E+04 .135E+04	ORTJ0954.047
.147500E+00 .147500E+03 .000E+00 .50E+00	Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .949200E+03 .137150E+04 .155640E+04 .166880E+04 .166880E+04 .166310E+04 .166310E+04 .160140E+04 .163710E+04 .137570E+04 .137570E+04 .118540E+04 .101070E+04 .902800E+03 .740100E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en tre calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	hase liquid-liquid (LL) x_{1} and constant T [Y1] .180E+04 .135E+04 .900E+03 .900E+03	ORTJ0954.047
○ [P1] = .298150E+03	Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .949200E+03 .137150E+04 .155640E+04 .166310E+04 .166310E+04 .166310E+04 .160140E+04 .163710E+04 .137570E+04 .118540E+04 .101070E+04 .902800E+03 .740100E+03 .536100E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en tre calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	hase liquid-liquid (LL) x_{1} and constant T [Y1] .180E+04 .135E+04 .900E+03 .900E+03	ORTJ0954.047
.000E+00	Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .949200E+03 .137150E+04 .155640E+04 .166310E+04 .166310E+04 .166310E+04 .166310E+04 .163710E+04 .163710E+04 .137570E+04 .137570E+04 .137570E+04 .137570E+04 .1356100E+03 .330100E+03 .330100E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en tre calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	hase liquid-liquid (LL) x_{1} and constant T [Y1] .180E+04 .135E+04 .900E+03 .900E+03	ORTJ0954.047
.50E+00	Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .949200E+03 .137150E+04 .155640E+04 .166310E+04 .166310E+04 .166310E+04 .166310E+04 .163710E+04 .163710E+04 .137570E+04 .137570E+04 .137570E+04 .137570E+04 .1356100E+03 .330100E+03 .330100E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en tre calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	hase liquid-liquid (LL) $2 \text{ at variable } x_1 \text{ and constant } T$ [Y1] .180E+04 .135E+04 .900E+03 .450E+03 .450E+03 .450E+03 .450E+03 .450E+03 .450E+03 .450E+03 .450E+03 .450E+03 .450E+03 .450E+04 .450E+03 .450E+03 .450E+03 .450E+04	ORTJ0954.047
.50E+00	Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .949200E+03 .137150E+04 .155640E+04 .166310E+04 .166310E+04 .166310E+04 .166310E+04 .163710E+04 .163710E+04 .137570E+04 .137570E+04 .137570E+04 .137570E+04 .1356100E+03 .330100E+03 .330100E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en tre calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	hase liquid-liquid (LL) $2 \text{ at variable } x_1 \text{ and constant } T$ [Y1] .180E+04 .135E+04 .900E+03 .450E+03 .450E+03 .450E+03 .450E+03 .450E+03 .450E+03 .450E+03 .450E+03 .450E+03 .450E+03 .450E+04 .450E+03 .450E+03 .450E+03 .450E+04	ORTJ0954.047
.50E+00	Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .949200E+03 .137150E+04 .155640E+04 .166310E+04 .166310E+04 .166310E+04 .166310E+04 .163710E+04 .163710E+04 .137570E+04 .137570E+04 .137570E+04 .137570E+04 .1356100E+03 .330100E+03 .330100E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en tre calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	hase liquid-liquid (LL) $2 \text{ at variable } x_1 \text{ and constant } T$ [Y1] .180E+04 .135E+04 .900E+03 .450E+03 .450E+03 .450E+03 .450E+03 .450E+03 .450E+03 .450E+03 .450E+03 .450E+03 .450E+03 .450E+04 .450E+03 .450E+03 .450E+03 .450E+04	ORTJ0954.047
	Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .949200E+03 .137150E+04 .155640E+04 .166310E+04 .166310E+04 .166310E+04 .166310E+04 .163710E+04 .163710E+04 .137570E+04 .137570E+04 .137570E+04 .137570E+04 .1356100E+03 .330100E+03 .330100E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en tre calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	hase liquid-liquid (LL) x_{1} at variable x_{1} and constant T [Y1] .180E+04 .135E+04 .000E+03 .450E+03 .450E+03 .000E+03	ORTJ0954.047
[]	Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .949200E+03 .137150E+04 .155640E+04 .166310E+04 .166310E+04 .166310E+04 .166310E+04 .163710E+04 .163710E+04 .137570E+04 .137570E+04 .137570E+04 .137570E+04 .1356100E+03 .330100E+03 .330100E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en tre calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	hase liquid-liquid (LL) x_{1} at variable x_{1} and constant T [Y1] .180E+04 .135E+04 .900E+03 .450E+03 .000E+00 .000E+00	ORTJ0954.047
	Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₃ H ₈ O, Prop 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .949200E+03 .137150E+04 .155640E+04 .166310E+04 .166310E+04 .166310E+04 .166310E+04 .163710E+04 .163710E+04 .137570E+04 .137570E+04 .137570E+04 .137570E+04 .1356100E+03 .330100E+03 .330100E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en tre calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	hase liquid-liquid (LL) x_{1} at variable x_{1} and constant T [Y1] .180E+04 .135E+04 .900E+03 .450E+03 .000E+00 .000E+00	ORTJ0954.047

	[HMSD1000] HE	AT OF MIXING		N	u ¹ a da la fan de ante anno 1960 e se de ante anno 1860 e se de de de Berne (1860 e se de se de Berne).	ORTJ0954.056
State:	Two-component s	ystem, single-pha		ase liquid-liquid (LL)		
	Pure component 1					
	Pure component 2					
Parameters:	[P1] <i>T/</i> K,	Temperature				
Variables:	$[X1] x_{1/-},$	Mole fraction o	f component 1			
	$[Y1]$ $H^{E}/Jmol^{-1}$,	Molar excess en	thalpy			
			easurement of $H^{\rm L}$	at variable x_1 and con	stant T	
-	1. C ₃ H ₈ O, Propa 2. C ₁₄ H ₂₈ O ₂ , M	an-1-01 [ethyl tridecanoa)	te			
[P1] = .298	8150E+03			[Y1]		
[X1]	[Y1]			.180E+04		
.130700E+00	.848300E+03					
.130700E+00	.127310E+04				.o ^{o.} o.o	
.326800E+00	.127310E+04				, · · · · · · · · · · · · · · · · · · ·	
.400800E+00	.165350E+04					
.461200E+00	.168780E+04					
.509900E+00	.167710E+04			.135E+04	× *	-
.558400E+00	.165320E+04				o a	
.598500E+00	1 1				/ c	2
	.160190E+04				4	ò
.630900E+00	.154300E+04				/	
.693000E+00	.138630E+04		$(1,\ldots,m) \in \{1,\dots,m\}$.900E+03		ó, _
.720100E+00	.129120E+04			o		
.751400E+00 .783000E+00	.119910E+04 .108270E+04			/		0
.783000E+00						·
.817200E+00					o [P1] = .298150E+03	
.891300E+00						
.924600E+00				.450E+03		<u> </u>
.924000E+00						
.980300E+00	.139700E+03	State of the second sec			- (D1) - 202160E + 02	<u> </u>
.)003001+00	.1397002+03				\circ [P1] = .298150E+03	
				1		0
			and the second	.000E+00		3
					.50E+00	
Copyright© 1995 F	ELDATA SARL Fra	nce. All rights reserv	ved.			[X1]
		EAT OF MIXING system, single-pha	AND SOLUTIO	N hase liquid-liquid (LL))	[X1] ORTJ0954.065
Property Code:	[HMSD1000] HI Two-component Pure component	EAT OF MIXING system, single-pha 1, liquid	AND SOLUTIO)	
Property Code: State:	[HMSD1000] HE Two-component Pure component Pure component	EAT OF MIXING system, single-pha 1, liquid 2, liquid	AND SOLUTIO)	
Property Code: State: Parameters:	[HMSD1000] HE Two-component Pure component Pure component [P1] T/K,	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature	AND SOLUTIO ase liquid or two-p)	
Property Code: State:	[HMSD1000] HH Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-,	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of	AND SOLUTIO ase liquid or two-p)	
Property Code: State: Parameters: Variables:	[HMSD1000] HH Two-component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ ,	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess et	AND SOLUTIO ase liquid or two-p of component 1 nthalpy			
Property Code: State: Parameters: Variables: Method:	[HMSD1000] HH Two-component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess et ure calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-pi of component 1 nthalpy neasurement of H ^E	hase liquid-liquid (LL)		
Property Code: State: Parameters: Variables: Method: Components:	[HMSD1000] HH Two-component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₁₆ H ₃₂ O ₂ , M	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess et ure calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-pi of component 1 nthalpy neasurement of H ^E	hase liquid-liquid (LL) $\frac{1}{2}$ at variable x_1 and cor		
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29	[HMSD1000] HH Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess et ure calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-pi of component 1 nthalpy neasurement of H ^E	hase liquid-liquid (LL) $\frac{2}{3}$ at variable x_1 and cor [Y1]	nstant T	ORTJ0954.065
Property Code: State: Parameters: Variables: Method: Components: [P1] = .292 [X1]	[HMSD1000] HH Two-component Pure component [P1] <i>T/</i> K, [X1] <i>x</i> ₁ /-, [Y1] <i>HE/J</i> mol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1]	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess et ure calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-pi of component 1 nthalpy neasurement of H ^E	hase liquid-liquid (LL) $\frac{1}{2}$ at variable x_1 and cor	nstant T	ORTJ0954.065
Property Code: State: Parameters: Variables: Method: Components: [P1] = .292 [X1] .747000E-01	[HMSD1000] HH Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .563400E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess et ure calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-pi of component 1 nthalpy neasurement of H ^E	hase liquid-liquid (LL) $\frac{2}{3}$ at variable x_1 and cor [Y1]	nstant T	ORTJ0954.065
Property Code: State: Parameters: Variables: Method: Components: [P1] = .294 [X1] .747000E-01 .155100E+00	[HMSD1000] HH Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .563400E+03 .101630E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess et ure calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-pi of component 1 nthalpy neasurement of H ^E	hase liquid-liquid (LL) $\frac{2}{3}$ at variable x_1 and cor [Y1]	nstant T	ORTJ0954.065
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .747000E-01 .155100E+00 .289700E+00	[HMSD1000] HH Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> 1/-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .563400E+03 .101630E+04 .154190E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess et ure calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-pi of component 1 nthalpy neasurement of H ^E	hase liquid-liquid (LL) $\frac{2}{3}$ at variable x_1 and cor [Y1]	nstant T	ORTJ0954.065
Property Code: State: Parameters: Variables: Method: Components: [P1] = .294 [X1] .747000E-01 .155100E+00 .289700E+00 .403300E+00	[HMSD1000] HH Two-component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .563400E+03 .101630E+04 .154190E+04 .178360E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess et ure calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-pi of component 1 nthalpy neasurement of H ^E	hase liquid-liquid (LL) at variable x ₁ and cor [Y1] .200E+04	nstant T	ORTJ0954.065
Property Code: State: Parameters: Variables: Method: Components: [P1] = .290 [X1] .747000E-01 .155100E+00 .289700E+00 .403300E+00 .486400E+00	[HMSD1000] HH Two-component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .563400E+03 .101630E+04 .154190E+04 .178360E+04 .182490E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess et ure calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-pi of component 1 nthalpy neasurement of H ^E	hase liquid-liquid (LL) $\frac{2}{3}$ at variable x_1 and cor [Y1]	nstant T	ORTJ0954.065
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .747000E-01 .155100E+00 .289700E+00 .403300E+00 .403300E+00 .530300E+00	[HMSD1000] HH Two-component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .563400E+03 .101630E+04 .154190E+04 .178360E+04 .178790E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess et ure calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-pi of component 1 nthalpy neasurement of H ^E	hase liquid-liquid (LL) at variable x ₁ and cor [Y1] .200E+04	nstant T	ORTJ0954.065
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .747000E-01 .155100E+00 .289700E+00 .403300E+00 .403300E+00 .530300E+00 .566600E+00	[HMSD1000] HH Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .563400E+03 .101630E+04 .154190E+04 .178360E+04 .178790E+04 .174840E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess et ure calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-pi of component 1 nthalpy neasurement of H ^E	hase liquid-liquid (LL) at variable x ₁ and cor [Y1] .200E+04	nstant T	ORTJ0954.065
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .747000E-01 .155100E+00 .289700E+00 .403300E+00 .53030E+00 .53030E+00 .566600E+00 .600600E+00	[HMSD1000] HH Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .563400E+03 .101630E+04 .154190E+04 .178360E+04 .178790E+04 .174840E+04 .168560E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess et ure calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-pi of component 1 nthalpy neasurement of H ^E	hase liquid-liquid (LL) at variable x ₁ and cor [Y1] .200E+04	nstant T	ORTJ0954.065
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .747000E-01 .155100E+00 .289700E+00 .486400E+00 .530300E+00 .566600E+00 .600600E+00 .632700E+00	[HMSD1000] HH Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .563400E+03 .101630E+04 .154190E+04 .178360E+04 .178790E+04 .174840E+04 .168560E+04 .163320E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess et ure calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-pi of component 1 nthalpy neasurement of H ^E	hase liquid-liquid (LL) at variable x ₁ and cor [Y1] .200E+04	nstant T	ORTJ0954.065
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .747000E-01 .155100E+00 .289700E+00 .403300E+00 .403300E+00 .566600E+00 .6006600E+00 .632700E+00 .657700E+00	[HMSD1000] HH Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .563400E+03 .101630E+04 .154190E+04 .178360E+04 .178360E+04 .178360E+04 .168560E+04 .168560E+04 .166320E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess et ure calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-pi of component 1 nthalpy neasurement of H ^E	hase liquid-liquid (LL) at variable x ₁ and cor [Y1] .200E+04 .150E+04	nstant T	ORTJ0954.065
Property Code: State: Parameters: Variables: Method: Components: [P1] = .299 [X1] .747000E-01 .155100E+00 .289700E+00 .403300E+00 .530300E+00 .606600E+00 .632700E+00 .698700E+00	[HMSD1000] HH Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .563400E+03 .101630E+04 .154190E+04 .154190E+04 .178790E+04 .178790E+04 .168560E+04 .16320E+04 .156920E+04 .15930E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess et ure calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-pi of component 1 nthalpy neasurement of H ^E	hase liquid-liquid (LL) at variable x ₁ and cor [Y1] .200E+04	nstant T	ORTJ0954.065
Property Code: State: Parameters: Variables: Method: Components: [P1] = .290 [X1] .747000E-01 .155100E+00 .289700E+00 .403300E+00 .530300E+00 .530300E+00 .606600E+00 .632700E+00 .637700E+00 .698700E+00 .735300E+00	[HMSD1000] HH Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-presse 1. C ₃ H ₈ O, Prop 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .563400E+03 .101630E+04 .154190E+04 .178360E+04 .178790E+04 .178790E+04 .168560E+04 .163320E+04 .156920E+04 .145930E+04 .132700E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess et ure calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-pi of component 1 nthalpy neasurement of H ^E	hase liquid-liquid (LL) at variable x ₁ and cor [Y1] .200E+04 .150E+04	nstant T	ORTJ0954.065
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .747000E-01 .155100E+00 .289700E+00 .403300E+00 .403300E+00 .506600E+00 .606700E+00 .632700E+00 .639700E+00 .639700E+00 .753300E+00 .762600E+00	[HMSD1000] HH Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .563400E+03 .101630E+04 .1563400E+04 .178360E+04 .178360E+04 .163502E+04 .156920E+04 .132700E+04 .132700E+04 .122810E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess et ure calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-pi of component 1 nthalpy neasurement of H ^E	hase liquid-liquid (LL) at variable x ₁ and cor [Y1] .200E+04 .150E+04	nstant T	ORTJ0954.065
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .747000E-01 .155100E+00 .289700E+00 .403300E+00 .403300E+00 .566600E+00 .600600E+00 .600600E+00 .632700E+00 .698700E+00 .735300E+00 .732300E+00 .789300E+00	[HMSD1000] HH Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .563400E+03 .101630E+04 .154190E+04 .178360E+04 .178360E+04 .178790E+04 .174840E+04 .168560E+04 .163320E+04 .156920E+04 .132700E+04 .132700E+04 .122810E+04 .112090E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess et ure calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-pi of component 1 nthalpy neasurement of H ^E	hase liquid-liquid (LL) at variable x ₁ and cor [Y1] .200E+04 .150E+04	nstant T	ORTJ0954.065
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .747000E-01 .155100E+00 .289700E+00 .403300E+00 .530300E+00 .566600E+00 .600600E+00 .632700E+00 .698700E+00 .735300E+00 .735300E+00 .789300E+00 .817900E+00	[HMSD1000] HH Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .563400E+03 .101630E+04 .154190E+04 .178360E+04 .178360E+04 .178360E+04 .178790E+04 .17830E+04 .163320E+04 .156920E+04 .156920E+04 .122810E+04 .122810E+04 .101740E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess et ure calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-pi of component 1 nthalpy neasurement of H ^E	index index <td< td=""><td>nstant T</td><td>ORTJ0954.065</td></td<>	nstant T	ORTJ0954.065
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .747000E-01 .155100E+00 .289700E+00 .403300E+00 .506600E+00 .600600E+00 .606600E+00 .608700E+00 .698700E+00 .785300E+00 .789300E+00 .817900E+00 .848400E+00	[HMSD1000] HH Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .563400E+03 .101630E+04 .154190E+04 .154190E+04 .178360E+04 .178360E+04 .163320E+04 .163320E+04 .163320E+04 .163320E+04 .156920E+04 .16290E+04 .122810E+04 .101740E+04 .892600E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess et ure calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-pi of component 1 nthalpy neasurement of H ^E	hase liquid-liquid (LL) at variable x ₁ and cor [Y1] .200E+04 .150E+04	nstant T	ORTJ0954.065
Property Code: State: Parameters: Variables: Method: Components: [P1] = .299 [X1] .747000E-01 .155100E+00 .289700E+00 .403300E+00 .530300E+00 .600600E+00 .632700E+00 .632700E+00 .632700E+00 .735300E+00 .789300E+00 .817900E+00 .817900E+00 .84400E+00 .881600E+00	[HMSD1000] HH Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C3H80, Prop 2. C16H32O2, M 8150E+03 [Y1] .563400E+03 .101630E+04 .154190E+04 .154190E+04 .178360E+04 .178360E+04 .168560E+04 .168560E+04 .16320E+04 .156920E+04 .15290E+04 .122810E+04 .122810E+04 .101740E+04 .892600E+03 .741100E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess et ure calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-pi of component 1 nthalpy neasurement of H ^E	index index <td< td=""><td>nstant T</td><td>ORTJ0954.065</td></td<>	nstant T	ORTJ0954.065
Property Code: State: Parameters: Variables: Method: Components: [P1] = .294 [X1] .747000E-01 .155100E+00 .289700E+00 .403300E+00 .530300E+00 .606600E+00 .632700E+00 .637700E+00 .698700E+00 .753300E+00 .762600E+00 .789300E+00 .81600E+00 .81600E+00 .912200E+00	[HMSD1000] HH Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-presse 1. C ₃ H ₈ O, Prop 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .563400E+03 .101630E+04 .154190E+04 .154190E+04 .178360E+04 .178790E+04 .178790E+04 .163320E+04 .156920E+04 .156920E+04 .152700E+04 .122810E+04 .122810E+04 .12090E+04 .12090E+04 .12090E+04 .12090E+04 .12090E+04 .12090E+04 .12090E+04 .12090E+04 .12090E+04 .12090E+04 .12090E+04 .12090E+04 .12090E+04 .1100E+03 .741100E+03 .581300E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess et ure calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-pi of component 1 nthalpy neasurement of H ^E	index index <td< td=""><td>nstant T</td><td>ORTJ0954.065</td></td<>	nstant T	ORTJ0954.065
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .747000E-01 .155100E+00 .289700E+00 .289700E+00 .30300E+00 .530300E+00 .60600E+00 .632700E+00 .632700E+00 .657700E+00 .789300E+00 .881600E+00 .881600E+00 .881600E+00 .936700E+00 .936700E+00	[HMSD1000] HH Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-presse 1. C ₃ H ₈ O, Prop 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .563400E+03 .101630E+04 .154190E+04 .178360E+04 .178790E+04 .178790E+04 .178790E+04 .168560E+04 .168560E+04 .132700E+04 .122810E+04 .122810E+04 .101740E+04 .892600E+03 .741100E+03 .581300E+03 .439200E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess et ure calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-pi of component 1 nthalpy neasurement of H ^E	index index <td< td=""><td>nstant T</td><td>ORTJ0954.065</td></td<>	nstant T	ORTJ0954.065
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .747000E-01 .155100E+00 .289700E+00 .403300E+00 .403300E+00 .403300E+00 .506600E+00 .606600E+00 .698700E+00 .698700E+00 .789300E+00 .817900E+00 .81600E+00 .936700E+00 .936700E+00 .936700E+00 .936700E+00 .936700E+00 .936700E+00 .936700E+00 .936700E+00 .960000E+00	[HMSD1000] HH Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .563400E+03 .101630E+04 .154190E+04 .178360E+04 .178360E+04 .178360E+04 .178790E+04 .168560E+04 .156920E+04 .132700E+04 .122810E+04 .122810E+04 .122810E+04 .12090E+04 .12090E+04 .581300E+03 .439200E+03 .290800E+03 .290800E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess et ure calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-pi of component 1 nthalpy neasurement of H ^E	index index <td< td=""><td>nstant T</td><td>ORTJ0954.065</td></td<>	nstant T	ORTJ0954.065
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .747000E-01 .155100E+00 .289700E+00 .403300E+00 .403300E+00 .530300E+00 .632700E+00 .632700E+00 .637700E+00 .63700E+00 .789300E+00 .881600E+00 .881600E+00 .936700E+00 .936700E+00	[HMSD1000] HH Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-presse 1. C ₃ H ₈ O, Prop 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .563400E+03 .101630E+04 .154190E+04 .178360E+04 .178790E+04 .178790E+04 .178790E+04 .168560E+04 .168560E+04 .132700E+04 .122810E+04 .122810E+04 .101740E+04 .892600E+03 .741100E+03 .581300E+03 .439200E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess et ure calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-pi of component 1 nthalpy neasurement of H ^E	is at variable x1 and cor [Y1] .200E+04 .150E+04 .100E+04 .500E+03	nstant T	ORTJ0954.065
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .747000E-01 .155100E+00 .289700E+00 .403300E+00 .403300E+00 .403300E+00 .566600E+00 .566600E+00 .632700E+00 .638700E+00 .789300E+00 .817900E+00 .81600E+00 .81600E+00 .936700E+00 .936700E+00 .936700E+00 .936700E+00	[HMSD1000] HH Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .563400E+03 .101630E+04 .154190E+04 .178360E+04 .178360E+04 .178360E+04 .178790E+04 .168560E+04 .156920E+04 .132700E+04 .122810E+04 .122810E+04 .122810E+04 .12090E+04 .12090E+04 .581300E+03 .439200E+03 .290800E+03 .290800E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess et ure calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-pi of component 1 nthalpy neasurement of H ^E	index index <td< td=""><td>• [P1] = .298150E+03</td><td></td></td<>	• [P1] = .298150E+03	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .747000E-01 .155100E+00 .403300E+00 .403300E+00 .403300E+00 .403300E+00 .566600E+00 .566600E+00 .632700E+00 .632700E+00 .638700E+00 .789300E+00 .817900E+00 .81600E+00 .912200E+00 .936700E+00 .936700E+00 .936700E+00 .936700E+00	[HMSD1000] HH Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C ₃ H ₈ O, Prop 2. C ₁₆ H ₃₂ O ₂ , M 8150E+03 [Y1] .563400E+03 .101630E+04 .154190E+04 .178360E+04 .178360E+04 .178790E+04 .174840E+04 .168560E+04 .156920E+04 .132700E+04 .122810E+04 .122810E+04 .122810E+04 .12090E+04 .101740E+03 .581300E+03 .439200E+03 .290800E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess et ure calorimetric m an-1-ol	AND SOLUTIO ase liquid or two-pi of component 1 nthalpy neasurement of H ^E	is at variable x1 and cor [Y1] .200E+04 .150E+04 .100E+04 .500E+03	nstant T	ORTJ0954.065

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	[AT OF MIXING	AND SOLUTION	N ORTJ0954.00
State:	Two-component	system, single-pha	ise liquid or two-ph	ase liquid-liquid (LL)
	Pure component	1, liquid	-	
-	Pure component			
Parameters: Variables:	[P1] <i>T/</i> K,	Temperature Mole fraction of	of component 1	
A di mines:	[X1] $x_1/-$, [Y1] $H^{E}/Jmol^{-1}$.	Molar excess er	nthalpy	
Method:	Direct low-pressu	ure calorimetric m	leasurement of $H^{\rm E}$	at variable x_1 and constant T
Components:	1. C ₄ H ₈ O ₂ , Met 2. C ₄ H ₁₀ O, But	hyl propanoate an-1-ol		
[P1] = .298				[Y1]
[X1]	[Y1]			.200E+04
.626000E-01	.382900E+03			○ [P1] = .298150E+03
.115400E+00				
.185200E+00				
.254800E+00 .318700E+00	.120500E+04 .139500E+04			
.380600E+00			1 3 ² 1	.150E+04
.435500E+00				<u>o</u> 6
.486300E+00				
.516400E+00				0 0
.526800E+00	in the second second			
.566800E+00 .616100E+00				
.671200E+00	.163290E+04 .153660E+04			
.732100E+00				
.796500E+00	.116100E+04			ø
.867500E+00			11 - 17 G	.500E+03
.937500E+00	.450600E+03			.500E+03
	the man have been a		1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1	.000E+00
		1. SP		.50E+00
				[X1]
Copyright© 1995 F	ELDATA SARL Fra	nce. All rights reser	ved.	
Property Code:	[HMSD1000] HE	EAT OF MIXING	GAND SOLUTION	N ORTJ0954.00
State:			ase liquid or two-ph	ase liquid-liquid (LL)
	Pure component	1. liquid		
Parameters:	Dura component			
	Pure component	2, liquid		
	[P1] <i>T/K</i> ,	2, liquid Temperature	of component 1	
Variables:	[P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$,	2, liquid Temperature Mole fraction of Molar excess en	nthalpy	
Variables: Method:	[P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu	2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m	nthalpy	at variable x_1 and constant T
Variables: Method: Components:	[P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$,	2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m thyl propanoate	nthalpy	at variable x_1 and constant T
Variables: Method: Components: [P1] = .298	[P1] <i>T/</i> K, [X1] <i>x</i> ₁ /-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-pressu 1. C4H ₈ O ₂ , Met 2. C ₆ H ₁₄ O, Hex 3150E+03	2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m thyl propanoate	nthalpy	[Y1]
Variables: Method: Components: [P1] = .298 [X1]	[P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₄ H ₈ O ₂ , Met 2. C ₆ H ₁₄ O, Hex B150E+03 [Y1]	2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m thyl propanoate	nthalpy	[¥1] .220E+04
Variables: Method: Components: [P1] = .298 [X1] .802000E-01	[P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₄ H ₈ O ₂ , Met 2. C ₆ H ₁₄ O, Hex B150E+03 [Y1] .523100E+03	2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m thyl propanoate	nthalpy	[Y1]
Variables: Method: Components: [P1] = .298 [X1] .802000E-01 .162300E+00	[P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₄ H ₈ O ₂ , Met 2. C ₆ H ₁₄ O, Hex B150E+03 [Y1] .523100E+03 .953000E+03	2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m thyl propanoate	nthalpy	[Y1] .220E+04
Variables: Method: Components: [P1] = .298 [X1] .802000E-01 .162300E+00 .239900E+00	[P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₄ H ₈ O ₂ , Met 2. C ₆ H ₁₄ O, Hex B150E+03 [Y1] .523100E+03 .953000E+03 .130290E+04	2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m thyl propanoate	nthalpy	[Y1] .220E+04
Variables: Method: Components: [P1] = .298 [X1] .802000E-01 .162300E+00	[P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₄ H ₈ O ₂ , Met 2. C ₆ H ₁₄ O, Hex B150E+03 [Y1] .523100E+03 .953000E+03	2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m thyl propanoate	nthalpy	[Y1] .220E+04 \circ [P1] = .298150E+03 $\circ^{\circ\circ}$
Variables: Method: Components: [P1] = .298 [X1] .802000E-01 .162300E+00 .239900E+00 .318200E+00 .389600E+00 .453000E+00	[P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-pressu 1. C4H ₈ O ₂ , Met 2. C ₆ H ₁₄ O, Hex B150E+03 [Y1] .523100E+03 .953000E+03 .130290E+04 .157800E+04 .157800E+04 .186330E+04	2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m thyl propanoate	nthalpy	[Y1] .220E+04
Variables: Method: Components: [P1] = .298 [X1] .802000E-01 .162300E+00 .239900E+00 .318200E+00 .389600E+00 .453000E+00 .510300E+00	[P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₄ H ₈ O ₂ , Met 2. C ₆ H ₁₄ O, Hex B150E+03 [Y1] .523100E+03 .953000E+03 .130290E+04 .157800E+04 .157800E+04 .186330E+04 .191210E+04	2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m thyl propanoate	nthalpy	[Y1] .220E+04 \circ [P1] = .298150E+03 $\circ^{\circ\circ}$
Variables: Method: Components: [P1] = .298 [X1] .802000E-01 .162300E+00 .239900E+00 .318200E+00 .389600E+00 .453000E+00 .510300E+00 .584000E+00	[P1] <i>T/</i> K, [X1] <i>x</i> ₁ /-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₄ H ₈ O ₂ , Met 2. C ₆ H ₁₄ O, Hex B150E+03 [Y1] .523100E+03 .953000E+03 .130290E+04 .157800E+04 .157800E+04 .186330E+04 .191210E+04 .188490E+04	2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m thyl propanoate	nthalpy	[Y1] .220E+04 \circ [P1] = .298150E+03 $\circ^{\circ\circ}$
Variables: Method: Components: [P1] = .298 [X1] .802000E-01 .162300E+00 .239900E+00 .318200E+00 .389600E+00 .510300E+00 .584000E+00 .632900E+00	[P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₄ H ₈ O ₂ , Met 2. C ₆ H ₁₄ O, Hex B150E+03 [Y1] .523100E+03 .953000E+03 .130290E+04 .157800E+04 .157800E+04 .186330E+04 .188490E+04 .183190E+04	2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m thyl propanoate	nthalpy	$[Y1]$.220E+04 $\circ [P1] = .298150E+03$.165E+04 $\circ \circ $
Variables: Method: Components: [P1] = .298 [X1] .802000E-01 .162300E+00 .318200E+00 .389600E+00 .453000E+00 .510300E+00 .584000E+00 .632900E+00 .632900E+00 .683100E+00	[P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₄ H ₈ O ₂ , Met 2. C ₆ H ₁₄ O, Hex B150E+03 [Y1] .523100E+03 .953000E+03 .130290E+04 .157800E+04 .157800E+04 .186330E+04 .188490E+04 .183190E+04 .174960E+04	2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m thyl propanoate	nthalpy	[Y1] .220E+04 \circ [P1] = .298150E+03 $\circ^{\circ\circ}$
Variables: Method: Components: [P1] = .298 [X1] .802000E-01 .162300E+00 .239900E+00 .318200E+00 .389600E+00 .510300E+00 .584000E+00 .632900E+00	[P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_4H_8O_2$, Met 2. $C_6H_{14}O$, Hex 3150E+03 [Y1] .523100E+03 .953000E+03 .130290E+04 .157800E+04 .157800E+04 .186330E+04 .188490E+04 .183190E+04 .160140E+04 .140560E+04	2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m thyl propanoate	nthalpy	$[Y1]$.220E+04 $\circ [P1] = .298150E+03$.165E+04 $\circ \circ $
Variables: Method: Components: [P1] = .298 [X1] .802000E-01 .162300E+00 .239900E+00 .318200E+00 .389600E+00 .389600E+00 .510300E+00 .584000E+00 .632900E+00 .63100E+00 .734500E+00 .790900E+00 .847100E+00	[P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_4H_8O_2$, Met 2. $C_6H_{14}O$, Hex 3150E+03 [Y1] .523100E+03 .953000E+03 .130290E+04 .157800E+04 .157800E+04 .157800E+04 .188490E+04 .183190E+04 .180140E+04 .140560E+04 .112530E+04	2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m thyl propanoate	nthalpy	$[Y1]$.220E+04 $\circ [P1] = .298150E+03$.165E+04 $\circ \circ $
Variables: Method: Components: [P1] = .298 [X1] .802000E-01 .162300E+00 .239900E+00 .318200E+00 .389600E+00 .510300E+00 .584000E+00 .632900E+00 .632900E+00 .734500E+00 .734500E+00 .734500E+00 .734500E+00 .734500E+00 .790900E+00 .847100E+00 .902800E+00	[P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_4H_8O_2$, Met 2. $C_6H_{14}O$, Hex 3150E+03 [Y1] .523100E+03 .953000E+03 .130290E+04 .157800E+04 .157800E+04 .175930E+04 .188490E+04 .183190E+04 .174960E+04 .160140E+04 .140560E+04 .12530E+04 .775200E+03	2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m thyl propanoate	nthalpy	$[Y1]$.220E+04 $\circ [P1] = .298150E+03$.165E+04 $\circ \circ $
Variables: Method: Components: [P1] = .298 [X1] .802000E-01 .162300E+00 .239900E+00 .318200E+00 .389600E+00 .389600E+00 .510300E+00 .584000E+00 .683100E+00 .734500E+00 .790900E+00 .847100E+00	[P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_4H_8O_2$, Met 2. $C_6H_{14}O$, Hex 3150E+03 [Y1] .523100E+03 .953000E+03 .130290E+04 .157800E+04 .157800E+04 .157800E+04 .188490E+04 .183190E+04 .180140E+04 .140560E+04 .112530E+04	2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m thyl propanoate	nthalpy	$[Y1]$.220E+04 $\circ [P1] = .298150E+03$.165E+04 .110E+04
Variables: Method: Components: [P1] = .298 [X1] .802000E-01 .162300E+00 .239900E+00 .318200E+00 .389600E+00 .510300E+00 .584000E+00 .632900E+00 .632900E+00 .734500E+00 .734500E+00 .734500E+00 .734500E+00 .734500E+00 .790900E+00 .847100E+00 .902800E+00	[P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_4H_8O_2$, Met 2. $C_6H_{14}O$, Hex 3150E+03 [Y1] .523100E+03 .953000E+03 .130290E+04 .157800E+04 .157800E+04 .175930E+04 .188490E+04 .183190E+04 .174960E+04 .160140E+04 .140560E+04 .12530E+04 .775200E+03	2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m thyl propanoate	nthalpy	[Y1] .220E+04 .165E+04 .110E+04
Variables: Method: Components: [P1] = .298 [X1] .802000E-01 .162300E+00 .239900E+00 .318200E+00 .389600E+00 .510300E+00 .584000E+00 .632900E+00 .632900E+00 .734500E+00 .734500E+00 .734500E+00 .734500E+00 .734500E+00 .790900E+00 .847100E+00 .902800E+00	[P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_4H_8O_2$, Met 2. $C_6H_{14}O$, Hex 3150E+03 [Y1] .523100E+03 .953000E+03 .130290E+04 .157800E+04 .157800E+04 .175930E+04 .188490E+04 .183190E+04 .174960E+04 .160140E+04 .140560E+04 .12530E+04 .775200E+03	2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m thyl propanoate	nthalpy	$[Y1]$.220E+04 $\circ [P1] = .298150E+03$.165E+04 .110E+04
Variables: Method: Components: [P1] = .298 [X1] .802000E-01 .162300E+00 .239900E+00 .318200E+00 .389600E+00 .510300E+00 .584000E+00 .683100E+00 .734500E+00 .734500E+00 .790900E+00 .847100E+00 .902800E+00	[P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_4H_8O_2$, Met 2. $C_6H_{14}O$, Hex 3150E+03 [Y1] .523100E+03 .953000E+03 .130290E+04 .157800E+04 .157800E+04 .175930E+04 .188490E+04 .183190E+04 .174960E+04 .160140E+04 .140560E+04 .12530E+04 .775200E+03	2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m thyl propanoate	nthalpy	$[Y1]$.220E+04 $\circ [P1] = .298150E+03$.165E+04 .110E+04
Variables: Method: Components: [P1] = .298 [X1] .802000E-01 .162300E+00 .239900E+00 .318200E+00 .389600E+00 .584000E+00 .584000E+00 .632900E+00 .683100E+00 .734500E+00 .734500E+00 .799900E+00 .847100E+00 .902800E+00	[P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_4H_8O_2$, Met 2. $C_6H_{14}O$, Hex 3150E+03 [Y1] .523100E+03 .953000E+03 .130290E+04 .157800E+04 .157800E+04 .175930E+04 .188490E+04 .183190E+04 .174960E+04 .160140E+04 .140560E+04 .12530E+04 .775200E+03	2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m thyl propanoate	nthalpy	$[Y1]$.220E+04 $\circ [P1] = .298150E+03$.165E+04 .110E+04
Variables: Method: Components: [P1] = .298 [X1] .802000E-01 .162300E+00 .239900E+00 .318200E+00 .389600E+00 .584000E+00 .584000E+00 .632900E+00 .683100E+00 .734500E+00 .734500E+00 .799900E+00 .847100E+00 .902800E+00	[P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_4H_8O_2$, Met 2. $C_6H_{14}O$, Hex 3150E+03 [Y1] .523100E+03 .953000E+03 .130290E+04 .157800E+04 .157800E+04 .175930E+04 .188490E+04 .183190E+04 .174960E+04 .160140E+04 .140560E+04 .12530E+04 .775200E+03	2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m thyl propanoate	nthalpy	$[Y1]$.220E+04 \circ [P1] = .298150E+03 .165E+04 .165E+04 .110E+04 .550E+03 \circ
Variables: Method: Components: [P1] = .298 [X1] .802000E-01 .162300E+00 .239900E+00 .318200E+00 .389600E+00 .584000E+00 .584000E+00 .632900E+00 .683100E+00 .734500E+00 .734500E+00 .799900E+00 .847100E+00 .902800E+00	[P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_4H_8O_2$, Met 2. $C_6H_{14}O$, Hex 3150E+03 [Y1] .523100E+03 .953000E+03 .130290E+04 .157800E+04 .157800E+04 .175930E+04 .188490E+04 .183190E+04 .174960E+04 .160140E+04 .140560E+04 .12530E+04 .775200E+03	2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m thyl propanoate	nthalpy	$[Y1]$.220E+04 $\circ [P1] = .298150E+03$.165E+04 .110E+04
Yariables: fethod: Components: [P1] = .298 [X1] .802000E-01 .162300E+00 .239900E+00 .318200E+00 .389600E+00 .510300E+00 .584000E+00 .683100E+00 .734500E+00 .799900E+00 .847100E+00 .902800E+00	[P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_4H_8O_2$, Met 2. $C_6H_{14}O$, Hex 3150E+03 [Y1] .523100E+03 .953000E+03 .130290E+04 .157800E+04 .157800E+04 .175930E+04 .188490E+04 .183190E+04 .174960E+04 .160140E+04 .140560E+04 .12530E+04 .775200E+03	2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m thyl propanoate	nthalpy	$[Y1]$.220E+04 $\circ [P1] = .298150E+03$.165E+04 .110E+04 .550E+03 .000E+00



itale: ¹ Two-component s, liquid Pure component 1, liquid Pure component 2, liquid Pure component 3, liquid Pure 2, liquid Pure component 1, l			nce. All rights reserved. AT OF MIXING AN			ORTJ0954.01
Pure component 2, liquid Tamabtes: [X1] 77K, Mole fraction of component 1 [X1] 77K, Mole fraction of component 1 2 Capit (of particular constant T 2 Capit (of particular constant T) [X1] (V1] (V1) (1) (1) (1) (1) (1) (1) (1) (1) (1) (itate:	Two-component s	system, single-phase li			nid (LL)
Parameters: [P1] 7/K. Temperature availables: [P1] 7/K. Mole fraction of component 1 YTI [H2]mol-1. Mole fraction of component 1 YTI [H2]mol-1. Mole fraction of component 1 YTI [H2]mol-1. Mole fraction of component 1 2. C4B(100, Butan-1-01 2. C4B(100, Butan-1-01 2						
initiality Citi r_{i} , Mole factors of component it in the supersume calorinetric measurement of H^{E} at variable x_{1} and constant T components C. Citi (D), Baten 1-61 C. Citi (D), Baten 1-61 2. Citi (D), Distant-1-61 2. Citi (D), Baten 1-61 1360E+04 2. Citi (D), Baten 1-61 9 9 2. Citi (D), Baten 1-61 1360E+04 1360E+04 2. Citi (D), Baten 1-61 1350E+04 1350E+04 2. Symole+00 15330BE+04 135E+04 9 3. Symole+00 15320BE+04 9 9 3. Symole+00 15320BE+04 9 9 9 3. Symole+00 15320BE+04 9 9 9 9 9 3. Symole+00 1. Symole+04 9 <td< td=""><td></td><td></td><td></td><td></td><td></td><td></td></td<>						
detade [Y1] <i>HE</i> [morl-1, Molar access enhalp? Direct low-pressure advance in easurement of <i>HE</i> at variable x1 and constant <i>T</i> 2cmponents: 1. CqH1(p0, Butan-1-ol) 2. CqH1(p0, Butan-1-ol) [Y1] 23100E-01 50450E+03 23100E-01 50450E+03 225300E+00 119260E+04 337700E+01 15930E+04 34300E+01 15930E+04 35300E+00 13560E+04 727800E+01 13560E+04 35300E+00 13560E+04 727800E+00 13560E+04 35300E+00 13560E+04 36700E+00 13560E+04 36700E+00 13560E+04 36700E+00 13130E+04 36700E+00 284000E+03 37700E+00 284000E+03 37700E+00 284000E+03 39700E+00 12130E+04 39700E+00 1210K. Temperat				mnonont 1		
defaole Direct tow-pressure calorization measurement $ol H^E$ at variable x_1 and constant T components 1. C4H100, Batten-1-ol 2. C4H100, Batten-1-ol 1.3500E-01 504500E+03 [Y1] 1.3500E-01 504500E+03 [Y1] 1.3500E+04 1.35100E+04 1.35100E+04 29200E+01 1.40460E+04 1.35560E+03 29200E+01 1.35300E+04 1.35560E+04 4.3000E+01 1.55500E+04 1.35560E+04 5.35500E+00 1.35560E+04 900E+03 .35500E+00 1.35560E+04 900E+03 .35500E+00 1.35560E+04 900E+03 .4500E+00 .35500E+04 .500E+03 .622000E+00 .53500E+04 .500E+03 .951300E+00 .53500E+03 .500E+03 .951300E+00 .53500E+03 .00E+00 .951300E+00 .53500E+03 .00E+00 .951300E+00 .284000E+03 .00E+00 .951300E+00 .284000E+03 .00E+00 .951300E+01 .00E+00 .00E+00 .951300E+01	ariables:	$[X1] x_{1/-},$	Mole fraction of co	Inv		
Components: I. C (LF (p)). Butan-I-ol 2. C (SF (p)). Methy butanoate [P1] = 298150E+03 [X1] [Y1] [X3000E-01] SoldSolE-03 2.5300E+04 SoldSolE-03 2.5300E+04 SoldSolE-04 2.5300E+04 SoldSolE-04 2.5300E+06 SoldSolE-04 2.5300E+07 SoldSolE-03 SoldSolE-04 2.5300E+06 SoldSolE-03 SoldSolE-03 2.53100E+06 SoldSolE-03 SoldSolE-04 2.53100E+06 SoldSolE-03 SoldSolE-04	Method:	Direct low-pressu	re calorimetric measu	rement of HE	at variable r	and constant T
2. C3E1 (002), Methyl bulanoste [P1] = 298150E+03 [P1] = 298150E+04 [P1] = 298150E+03 [P1] = 298150E+04 [P1] = 298150E+03 [P1] = 298150E+04 [P1] = 298150E+03 [P1] = 298150E+03 [P1] = 298150E+03 [P1] = 298150E+04						
N1 Y1 Image: Constraint of the second secon						
[X1] [Y1]	[P1] = .298	8150E+03			[Y1]	
151700E+00 884500E+03 229200E+00 119200E+04 33050E+00 15380E+04 43010E+00 15930E+04 33050E+00 15330E+04 53050E+00 15330E+04 622302E+00 13550E+04 53050E+00 13530E+04 622302E+00 13550E+04 53050E+00 13230E+04 6233050E+00 13250E+04 53050E+00 13250E+04 53050E+00 13250E+04 53050E+00 35560E+03 571300E+00 352500E+03 571300E+00 352500E+03 571300E+00 352500E+03 571300E+00 35260E+03 72780E+00 12130E+04 571300E+00 12130E+04 571300E+00 12130E+04 571300E+00 12130E+04 900E+01 12130E+04 900E+02 224000E+03 900E+03 12130E+04 900E+03 12140E+04 900E+03 12140E+04 900E+03 135E+04 (P1] P1 14300D+04	[X1]	[Y1]		· · · ·		
151700E+00 884500E+03 229200E+00 119200E+04 33050E+00 15380E+04 43010E+00 15930E+04 33050E+00 15330E+04 53050E+00 15330E+04 622302E+00 13550E+04 53050E+00 13530E+04 622302E+00 13550E+04 53050E+00 13230E+04 6233050E+00 13250E+04 53050E+00 13250E+04 53050E+00 13250E+04 53050E+00 35560E+03 571300E+00 352500E+03 571300E+00 352500E+03 571300E+00 352500E+03 571300E+00 35260E+03 72780E+00 12130E+04 571300E+00 12130E+04 571300E+00 12130E+04 571300E+00 12130E+04 900E+01 12130E+04 900E+02 224000E+03 900E+03 12130E+04 900E+03 12140E+04 900E+03 12140E+04 900E+03 135E+04 (P1] P1 14300D+04	.735000E-01	.504500E+03				2 (B1) = 202150E + 02
2.12300E+00 1.1320E+04 0.72000E+00 1.13650E+04 0.72000E+00 1.1330E+04 .87000E+00 .12130E+04 .87000E+00 .53500E+03 .87000E+00 .53500E+03 .951300E+00 .53500E+03 .951300E+00 .234000E+03 .951300E+01 .900E+03 .951300E+01 .900E+03 .951300E+02 .900E+03 .951300E+03 .900E+03 .951300E+04 .900E+03 .951300E+00 .900E+03 .900E+03 .900E+03 </td <td>.151700E+00</td> <td>.884500E+03</td> <td></td> <td></td> <td></td> <td></td>	.151700E+00	.884500E+03				
2.12300E+00 1.1320E+04 0.72000E+00 1.13650E+04 0.72000E+00 1.1330E+04 .87000E+00 .12130E+04 .87000E+00 .53500E+03 .87000E+00 .53500E+03 .951300E+00 .53500E+03 .951300E+00 .234000E+03 .951300E+01 .900E+03 .951300E+01 .900E+03 .951300E+02 .900E+03 .951300E+03 .900E+03 .951300E+04 .900E+03 .951300E+00 .900E+03 .900E+03 .900E+03 </td <td></td> <td></td> <td></td> <td></td> <td></td> <td>o</td>						o
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ABORT OF AND TO AND TO AND TO AND TO AND TO AND SOLUTION 000E+00 [X1] Commission 1995 ELDATA SARL Frace. All rizhs reserved. 000E+00 [X1] Property Code: [HMSD1000] HEAT OF MIXING AND SOLUTION ORTJ0954.021 Site: Two-component system, single-phase liquid or two-phase liquid-liquid (LL) Pure component 2, liquid Parameters: [P1] 7/K, Mole fraction of component 1 [Y1] #E/Jmol-1, Method: Direct low-pressure calorimetric measurement of H ^E at variables x1 and constant T [Components: 1. C4H100, Batan-1-ol 2. C4H1202, Methyl pentanoate [Y1] .180E+04 [X1] [Y1] .180E+04 .180E+04 .135E+04 .303000E+00 .155670E+04 .135E+04 .00E+03 .00E+03 .227100E+00 .155670E+04 .135E+04 .00E+03 .00E+03 .59800E+00 .155670E+04 .500E+03 .00E+03 .00E+03 .00E+03 .59800E+00 .155670E+04 .500E+03 .00E+03 .00E+03 .00E+03 .59100E+00 .155670E+04 .500E+03 .00E+03 .00E+03 .00E+03 .59100E+00 .155670E+04 .500E+03						
Corright© 1995 ELDATA SARL Frace. All rights reserved. 000E+00					450E+03	¢.
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Corright® 1995 ELDATA SARL France. All rights reserved. [X1] Property Code: [HMSD1000] HEAT OF MIXING AND SOLUTION ORTJ9954.021 State: Two-component system, single-phase liquid or two-phase liquid-liquid (LL) ORTJ9954.021 Pure component J, liquid Pure component J, liquid ORTJ9954.021 Pure component J, liquid Pure component J, liquid ORTJ9954.021 Parameters: [X1] x/, Molar excess enthalpy Mole fraction of component I Transfer entry Variables: [X1] x/F, Molar excess enthalpy Mole fraction of Component I Transfer entry Verthod: Direct low-pressure calorimetric measurement of H ^E at variable x1 and constant T Components: 1. CqH100, Butan-1-ol 1 CqH100, Butan-1-ol 1/17200E+00 27100E+00 3/1400E+00 79000E+00				1. X S 43	.000E+00	
Image: Corright@ 1995 ELDATA SARL France. All rights reserved. ORTJ0954.021 Property Code: [HMSD1000] HEAT OF MIXING AND SOLUTION ORTJ0954.021 State: Two-component system, single-phase liquid or two-phase liquid-liquid (LL) Pure component 2, liquid Parameters: [P1] 7/K, Temperature Variables: [X1] x/-, Molar excess enthalpy Vethod: Direct low-pressure calorimetric measurement of H ^E at variable x1 and constant T Components: 1. CqH100, Butan-1-01 2. CqH1202, Methyl pentanoate [Y1]						
Property Code: [HMSD1000] HEAT OF MIXING AND SOLUTION State: Two-component system, single-phase liquid or two-phase liquid-liquid (LL) Pure component 1, liquid Pure component 2, liquid Pure component 2, liquid Pure component 2, liquid Pure component 1, liquid Pure component 2, liquid Pure component 2, liquid Direct low-pressure calorimetric measurement of H^E at variable x_1 and constant T Components: 1. C ₄ H ₁₀ O, Butan-1-ol 2. C ₆ H ₁₂ O ₂ , Methyl pentanoate [P1] = .298150E+03 [P1] = .298150E+03 .147200E+00 .123140E+04 .305300E+00 .150520E+04 .438200E+00 .150130E+04 .438200E+00 .15140E+04 .554500E+00 .15140E+04 .554500E+00 .15140E+04 .554500E+00 .15140E+04 .554500E+00 .15140E+04 .554500E+00 .151400E+04 .55670E+04 .1515670E+04 .50200E+00 .123150E+04 .450E+03 .900E+03 .000E+00 .211000E+03 .2000E+00 .2000E+03 .2000E+00 .2000E+03 .2000E+00 .2000E+03 .2000E+00 .2000E+03 .2000E+00 .2000E+03 .2000E+00 .2000E+03 .2000E+00 .2000E+03 .2000E+00 .2000E+03 .2000E+00 .2000E+03 .2000E+00						[X1]
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State: Two-component system, single-phase liquid or two-phase liquid-liquid (LL) Pure component 1, liquid Pure component 2, liquid Parameters: [P1] 7/K, Temperature Variables: [X1] x ₁ /-, [Y1] H ^E /Imol ⁻¹ , Molar excess enthalpy Vethod: Direct low-pressure calorimetric measurement of H ^E at variable x ₁ and constant T Components: 1. C4H ₁₀ O, Butan-1-ol 2. CdFl ₁₂ O ₂ , Methyl pentanoate [Y1] [R1] Software [Y1] [X1] [Y1] 1.7700E+00 [Y1] [Y1] [Y1] [Y1] [Y1] [Y1] [Y1] [Y1] [Y1]						
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Pure component 2, liquid Parameters: [P1] 7/K, Temperature Variables: [X1] $X_{1/-}$, Mole fraction of component 1 [Y1] H^2 /mol-1, Molar excess enthalpy Method: Direct low-pressure calorimetric measurement of H^E at variable x_1 and constant T Components: I. $C_{4}H_{10}O$, Butan-1-ol [Y1] Z. $C_{6}H_{12}O_2$, Methyl pentanoate [Y1] [P1] = .298150E+03 [Y1] [R1] x [Y1] [Y1] (A86000E-01] 505200E+03 [Y1] .123140E+04 .306300E+00 .161330E+04 .305300E+00 .161330E+04 .135E+04 $0^{\circ} O^{\circ} O_{\circ} O_$	Property Code:	[HMSD1000] HE	EAT OF MIXING AN			ORTJ0954.021
Wariables: $[X1] x_1/-,$ Mole fraction of component 1 $[Y1] H^E/Jmol^{-1}$, Molar excess enthalpy Method: Direct low-pressure calorimetric measurement of H^E at variable x_1 and constant T Components: 1. $C_4H_{10}O$, Butan-1-ol 2. $C_6H_{12}O_2$, Methyl penianoate [P1] = .298150E+03 [Y1] [R1] x/1/- [Y1] [Y1] [R1] x/200E+00 .090700E+03 [Y1] [X1] x/1/- [Y1] [R1] = .298150E+03 [Y1] [X1] x/1/- [Y1] [K1] x/1/- [Y1] [K1] x/1/- [Y1] [K1] x/1/- [Y1] [K1] x/1/- [Y1] [R1] x/200E+00		[HMSD1000] HE Two-component	EAT OF MIXING AN system, single-phase li			
Image: Text of the system of the s	Property Code: State:	[HMSD1000] HI Two-component Pure component Pure component	EAT OF MIXING AN system, single-phase li 1, liquid 2, liquid			
Method: Direct low-pressure calorimetric measurement of H^E at variable x_1 and constant T Components: 1. CqH ₁₀ O, Butan-1-ol 2. C ₆ H ₁₂ O ₂ , Methyl pentanoate [P1] = .298150E+03 [Y1] [X1] [Y1] [X2] [Y1] .86600E=01 .505200E+03 .123140E+04 .133440E+04 .306300E+00 .14910E+04 .306300E+00 .161420E+04 .305300E+00 .161420E+04 .519800E+00 .159440E+04 .537500E+00 .151140E+04 .530200E+00 .151140E+04 .50200E+00 .151250E+04 .50200E+00 .151400E+04 .50200E+00 .15140E+04 .50200E+00 .151570E+04 .50200E+00 .1515670E+04 .50200E+00 .132150E+04 .705700E+00 .132820E+04 .705700E+00 .18280E+04 .89100E+00 .889600E+03 .891100E+00 .889600E+03 .904200E+00 .211000E+03	Property Code: State: Parameters:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K,	EAT OF MIXING AN system, single-phase li 1, liquid 2, liquid Temperature	iquid or two-ph		
Components: 1. $C_{4}H_{10}O$, Butan-1-ol 2. $C_{6}H_{12}O_2$, Methyl pentanoate [P1] = .298150E+03 [X1] [Y1] .686000E-01 .505200E+03 .147200E+00 .907000E+03 .227100E+00 .123140E+04 .306300E+00 .124910E+04 .306300E+00 .161330E+04 .438200E+00 .161330E+04 .438200E+00 .161420E+04 .519800E+00 .155670E+04 .5354500E+00 .155670E+04 .530200E+00 .151140E+04 .672100E+00 .12820E+04 .765700E+00 .12820E+04 .705700E+00 .12820E+04 .819100E+00 .889600E+03 .811400E+00 .670300E+03 .92000E+00 .211000E+03 .92000E+00 .211000E+03	Property Code: State:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-,	EAT OF MIXING AN system, single-phase li 1, liquid 2, liquid Temperature Mole fraction of co	iquid or two-ph		
$\begin{tabular}{ c c c c c c c c c c c c c c c c c c c$	Property Code: State: Parameters: Variables:	[HMSD1000] HH Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ ,	EAT OF MIXING AN system, single-phase li 1, liquid 2, liquid Temperature Mole fraction of co Molar excess entha	iquid or two-ph omponent 1 lpy	ase liquid-liqu	id (LL)
[X1] [Y1] .686000E-01 .505200E+03 .147200E+00 .907000E+03 .227100E+00 .123140E+04 .306300E+00 .144910E+04 .306300E+00 .161330E+04 .482200E+00 .161330E+04 .47500E+00 .157050E+04 .519800E+00 .15940E+04 .519800E+00 .155670E+04 .59002e+00 .151140E+04 .509200E+00 .155670E+04 .509200E+00 .151140E+04 .509200E+00 .15140E+04 .57500E+00 .15140E+04 .6072100E+00 .12820E+04 .719200E+00 .12820E+04 .707300E+00 .12820E+04 .705700E+00 .212800E+03 .819100E+00 .670300E+03 .920000E+00 .211000E+03 .964200E+00 .211000E+03	Property Code: State: Parameters: Variables: Method:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^{E}/Jmol^{-1}$, Direct low-press 1. C4H10O, But	EAT OF MIXING AN system, single-phase li 1, liquid 2, liquid Temperature Mole fraction of co Molar excess entha ure calorimetric measu an-1-ol	iquid or two-ph omponent 1 lpy	ase liquid-liqu	id (LL)
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	Property Code: State: Parameters: Variables: Method: Components:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1}/-$, [Y1] H^{E}/Jmol^{-1} , Direct low-press 1. C ₄ H ₁₀ O, But 2. C ₆ H ₁₂ O ₂ , Mo	EAT OF MIXING AN system, single-phase li 1, liquid 2, liquid Temperature Mole fraction of co Molar excess entha ure calorimetric measu an-1-ol	iquid or two-ph omponent 1 lpy	ase liquid-liqui at variable x ₁ a	id (LL)
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.630700E+00 .144090E+04 .672100E+00 .135150E+04 .719200E+00 .122820E+04 .765700E+00 .108260E+04 .819100E+00 .889600E+03 .871400E+00 .670300E+03 .920000E+00 .437500E+03 .964200E+00 .211000E+03	Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .686000E-01 .147200E+00 .306300E+00 .309000E+00 .379000E+00 .48200E+00 .519800E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-press 1. C4H10O, But 2. C6H12O2, Mo 3150E+03 [Y1] .505200E+03 .123140E+04 .144910E+04 .157050E+04 .161330E+04 .161420E+04 .159440E+04	EAT OF MIXING AN system, single-phase li 1, liquid 2, liquid Temperature Mole fraction of co Molar excess entha ure calorimetric measu an-1-ol	iquid or two-ph omponent 1 lpy	ase liquid-liqui at variable x ₁ a [Y1] .180E+04	id (LL)
.719200E+00 .122820E+04 .765700E+00 .108260E+04 .819100E+00 .889600E+03 .871400E+00 .670300E+03 .920000E+00 .437500E+03 .964200E+00 .211000E+03 .964200E+00 .211000E+03 .964200E+00 .211000E+03	Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .686000E -01 .147200E +00 .306300E +00 .379000E +00 .48200E +00 .48200E +00 .519800E +00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₄ H ₁₀ O, But 2. C ₆ H ₁₂ O ₂ , Mo 3150E+03 [Y1] .505200E+03 .123140E+04 .144910E+04 .157050E+04 .161420E+04 .159440E+04 .155670E+04	EAT OF MIXING AN system, single-phase li 1, liquid 2, liquid Temperature Mole fraction of co Molar excess entha ure calorimetric measu an-1-ol	iquid or two-ph omponent 1 lpy	ase liquid-liqui at variable x ₁ a [Y1] .180E+04 .135E+04	id (LL) ind constant T \circ [P1] = .298150E+03 \circ \circ \circ \circ \circ \circ \circ \circ \circ \circ
.719200E+00 .122820E+04 .765700E+00 .108260E+04 .819100E+00 .889600E+03 .871400E+00 .670300E+03 .920000E+00 .437500E+03 .964200E+00 .211000E+03 .964200E+00 .211000E+03 .964200E+00 .211000E+03	Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .686000E -01 .147200E +00 .306300E +00 .379000E +00 .48200E +00 .519800E +00 .554500E +00 .590200E +00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] HE/Jmol-1, Direct low-press 1. C4H10O, But 2. C6H12O2, Ma 3150E+03 [Y1] .505200E+03 .123140E+04 .157050E+04 .161330E+04 .159440E+04 .155670E+04 .151140E+04	EAT OF MIXING AN system, single-phase li 1, liquid 2, liquid Temperature Mole fraction of co Molar excess entha ure calorimetric measu an-1-ol	iquid or two-ph omponent 1 lpy	ase liquid-liqui at variable x ₁ a [Y1] .180E+04 .135E+04	id (LL) ind constant T \circ [P1] = .298150E+03 \circ \circ \circ \circ \circ \circ \circ \circ \circ \circ
.879100E+00 .871400E+00 .920000E+00 .964200E+00 .211000E+03 .000E+00 .000E+00	Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .686000E-01 .147200E+00 .227100E+00 .306300E+00 .379000E+00 .54500E+00 .554500E+00 .590200E+00 .630700E+00 .672100E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressi 1. C ₄ H ₁₀ O, But 2. C ₆ H ₁₂ O ₂ , Ma 3150E+03 [Y1] .505200E+03 .907000E+03 .123140E+04 .144910E+04 .161330E+04 .161320E+04 .155670E+04 .155140E+04 .151140E+04 .151140E+04 .135150E+04	EAT OF MIXING AN system, single-phase li 1, liquid 2, liquid Temperature Mole fraction of co Molar excess entha ure calorimetric measu an-1-ol	iquid or two-ph omponent 1 lpy	ase liquid-liqui at variable x ₁ a [Y1] .180E+04 .135E+04	o [P1] = .298150E+03
.879100E+00 .871400E+00 .920000E+00 .964200E+00 .211000E+03 .000E+00 .000E+00	Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .686000E-01 .147200E+00 .227100E+00 .306300E+00 .379000E+00 .519800E+00 .554500E+00 .590200E+00 .630700E+00 .672100E+00 .719200E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-pressi 1. C4H ₁₀ O, But 2. C ₆ H ₁₂ O ₂ , Ma 3150E+03 [Y1] .505200E+03 .907000E+03 .123140E+04 .144910E+04 .157050E+04 .161330E+04 .159440E+04 .155670E+04 .155140E+04 .155150E+04 .122820E+04	EAT OF MIXING AN system, single-phase li 1, liquid 2, liquid Temperature Mole fraction of co Molar excess entha ure calorimetric measu an-1-ol	iquid or two-ph omponent 1 lpy	ase liquid-liqui at variable x ₁ a [Y1] .180E+04 .135E+04	id (LL) ind constant T \circ [P1] = .298150E+03 \circ \circ \circ \circ \circ \circ \circ \circ \circ \circ
.964200E+00 .211000E+03 .000E+00 .50E+00	Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .686000E-01 .147200E+00 .227100E+00 .306300E+00 .379000E+00 .519800E+00 .554500E+00 .590200E+00 .630700E+00 .672100E+00 .719200E+00 .765700E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressi 1. C4H10O, But 2. C6H12O2, Ma 3150E+03 [Y1] .505200E+03 .907000E+03 .123140E+04 .157050E+04 .161330E+04 .161330E+04 .155670E+04 .155670E+04 .151140E+04 .15150E+04 .122820E+04 .108260E+04	EAT OF MIXING AN system, single-phase li 1, liquid 2, liquid Temperature Mole fraction of co Molar excess entha ure calorimetric measu an-1-ol	iquid or two-ph omponent 1 lpy	ase liquid-liqui at variable x ₁ a [Y1] .180E+04 .135E+04	id (LL) ind constant T \circ [P1] = .298150E+03 \circ \circ \circ \circ \circ \circ \circ \circ \circ \circ
.964200E+00 .211000E+03 .000E+00 .50E+00	Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .686000E-01 .147200E+00 .227100E+00 .306300E+00 .379000E+00 .519800E+00 .554500E+00 .590200E+00 .630700E+00 .672100E+00 .765700E+00 .819100E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> 1/-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-press 1. C4H10O, But 2. C6H12O2, Mo 3150E+03 [Y1] .505200E+03 .907000E+03 .123140E+04 .144910E+04 .15130E+04 .161320E+04 .151140E+04 .155670E+04 .151140E+04 .155150E+04 .135150E+04 .122820E+04 .108260E+04 .889600E+03	EAT OF MIXING AN system, single-phase li 1, liquid 2, liquid Temperature Mole fraction of co Molar excess entha ure calorimetric measu an-1-ol	iquid or two-ph omponent 1 lpy	ase liquid-liqui at variable x1 a [Y1] .180E+04 .135E+04 .3900E+03	id (LL) ind constant T \circ [P1] = .298150E+03 \circ \circ \circ \circ \circ \circ \circ \circ \circ \circ
.000E+00	Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .686000E-01 .147200E+00 .227100E+00 .306300E+00 .379000E+00 .519800E+00 .519800E+00 .54500E+00 .50700E+00 .672100E+00 .719200E+00 .765700E+00 .819100E+00 .871400E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-presso 1. C4H10O, But 2. C6H12O2, Mo 3150E+03 [Y1] .505200E+03 .907000E+03 .123140E+04 .144910E+04 .161330E+04 .161330E+04 .161420E+04 .155670E+04 .155140E+04 .151140E+04 .151140E+04 .135150E+04 .108260E+04 .889600E+03 .670300E+03	EAT OF MIXING AN system, single-phase li 1, liquid 2, liquid Temperature Mole fraction of co Molar excess entha ure calorimetric measu an-1-ol	iquid or two-ph omponent 1 lpy	ase liquid-liqui at variable x1 a [Y1] .180E+04 .135E+04 .3900E+03	id (LL) ind constant T \circ [P1] = .298150E+03 \circ \circ \circ \circ \circ \circ \circ \circ \circ \circ
.000E+00	Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .686000E-01 .147200E+00 .306300E+00 .306300E+00 .379000E+00 .482500E+00 .519800E+00 .590200E+00 .590200E+00 .630700E+00 .630700E+00 .719200E+00 .819100E+00 .819100E+00 .871400E+00 .920000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-presse 1. C4H10O, But 2. C ₆ H12O ₂ , Ma 3150E+03 [Y1] .505200E+03 .907000E+03 .123140E+04 .144910E+04 .157050E+04 .161320E+04 .151140E+04 .155670E+04 .155140E+04 .151140E+04 .15250E+04 .15250E+04 .163260E+04 .889600E+03 .670300E+03 .670300E+03 .437500E+03	EAT OF MIXING AN system, single-phase li 1, liquid 2, liquid Temperature Mole fraction of co Molar excess entha ure calorimetric measu an-1-ol	iquid or two-ph omponent 1 lpy	ase liquid-liqui at variable x1 a [Y1] .180E+04 .135E+04 .3900E+03	id (LL) ind constant T \circ [P1] = .298150E+03 \circ \circ \circ \circ \circ \circ \circ \circ \circ \circ
.50E+00	Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .686000E-01 .147200E+00 .306300E+00 .306300E+00 .379000E+00 .482500E+00 .519800E+00 .590200E+00 .590200E+00 .630700E+00 .630700E+00 .719200E+00 .819100E+00 .819100E+00 .871400E+00 .920000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-presse 1. C4H10O, But 2. C ₆ H12O ₂ , Ma 3150E+03 [Y1] .505200E+03 .907000E+03 .123140E+04 .144910E+04 .157050E+04 .161320E+04 .151140E+04 .155670E+04 .155140E+04 .151140E+04 .15250E+04 .15250E+04 .163260E+04 .889600E+03 .670300E+03 .670300E+03 .437500E+03	EAT OF MIXING AN system, single-phase li 1, liquid 2, liquid Temperature Mole fraction of co Molar excess entha ure calorimetric measu an-1-ol	iquid or two-ph omponent 1 lpy	ase liquid-liqui at variable x1 a [Y1] .180E+04 .135E+04 .3900E+03	id (LL) ind constant T \circ [P1] = .298150E+03 \circ \circ \circ \circ \circ \circ \circ \circ \circ \circ
.50E+00	Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .686000E-01 .147200E+00 .306300E+00 .306300E+00 .379000E+00 .482500E+00 .519800E+00 .590200E+00 .590200E+00 .630700E+00 .630700E+00 .719200E+00 .819100E+00 .819100E+00 .871400E+00 .920000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-presse 1. C4H10O, But 2. C ₆ H12O ₂ , Ma 3150E+03 [Y1] .505200E+03 .907000E+03 .123140E+04 .144910E+04 .157050E+04 .161320E+04 .151140E+04 .155670E+04 .155140E+04 .151140E+04 .15250E+04 .15250E+04 .163260E+04 .889600E+03 .670300E+03 .670300E+03 .437500E+03	EAT OF MIXING AN system, single-phase li 1, liquid 2, liquid Temperature Mole fraction of co Molar excess entha ure calorimetric measu an-1-ol	iquid or two-ph omponent 1 lpy	ase liquid-liqui at variable x1 a [Y1] .180E+04 .135E+04 .3900E+03	id (LL) ind constant T \circ [P1] = .298150E+03 \circ \circ \circ \circ \circ \circ \circ \circ \circ \circ
	Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .686000E-01 .147200E+00 .306300E+00 .306300E+00 .379000E+00 .482500E+00 .519800E+00 .590200E+00 .590200E+00 .630700E+00 .630700E+00 .719200E+00 .819100E+00 .819100E+00 .871400E+00 .920000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-presse 1. C4H10O, But 2. C ₆ H12O ₂ , Ma 3150E+03 [Y1] .505200E+03 .907000E+03 .123140E+04 .144910E+04 .157050E+04 .161320E+04 .151140E+04 .155670E+04 .155140E+04 .151140E+04 .15250E+04 .15250E+04 .163260E+04 .889600E+03 .670300E+03 .670300E+03 .437500E+03	EAT OF MIXING AN system, single-phase li 1, liquid 2, liquid Temperature Mole fraction of co Molar excess entha ure calorimetric measu an-1-ol	iquid or two-ph omponent 1 lpy	ase liquid-liqui at variable x1 a [Y1] .180E+04 .135E+04 .900E+03 .450E+03	id (LL) ind constant T \circ [P1] = .298150E+03 \circ \circ \circ \circ \circ \circ \circ \circ \circ \circ
	Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .686000E-01 .147200E+00 .306300E+00 .306300E+00 .379000E+00 .482500E+00 .519800E+00 .590200E+00 .590200E+00 .630700E+00 .630700E+00 .719200E+00 .819100E+00 .819100E+00 .871400E+00 .920000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-presse 1. C4H10O, But 2. C ₆ H12O ₂ , Ma 3150E+03 [Y1] .505200E+03 .907000E+03 .123140E+04 .144910E+04 .157050E+04 .161320E+04 .151140E+04 .155670E+04 .155140E+04 .151140E+04 .15250E+04 .15250E+04 .163260E+04 .889600E+03 .670300E+03 .670300E+03 .437500E+03	EAT OF MIXING AN system, single-phase li 1, liquid 2, liquid Temperature Mole fraction of co Molar excess entha ure calorimetric measu an-1-ol	iquid or two-ph omponent 1 lpy	ase liquid-liqui at variable x1 a [Y1] .180E+04 .135E+04 .900E+03 .450E+03	id (LL) ind constant T \circ [P1] = .298150E+03 \circ \circ \circ \circ \circ \circ \circ \circ \circ \circ
	Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .686000E-01 .147200E+00 .306300E+00 .306300E+00 .379000E+00 .519800E+00 .59200E+00 .59200E+00 .630700E+00 .630700E+00 .719200E+00 .819100E+00 .819100E+00 .819100E+00 .871400E+00 .920000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-presse 1. C4H10O, But 2. C ₆ H12O ₂ , Ma 3150E+03 [Y1] .505200E+03 .907000E+03 .123140E+04 .144910E+04 .157050E+04 .161320E+04 .151140E+04 .155670E+04 .155140E+04 .151140E+04 .15250E+04 .15250E+04 .163260E+04 .889600E+03 .670300E+03 .670300E+03 .437500E+03	EAT OF MIXING AN system, single-phase li 1, liquid 2, liquid Temperature Mole fraction of co Molar excess entha ure calorimetric measu an-1-ol	iquid or two-ph omponent 1 lpy	ase liquid-liqui at variable x1 a [Y1] .180E+04 .135E+04 .900E+03 .450E+03	id (LL) ind constant T \circ [P1] = .298150E+03 \circ \circ \circ \circ \circ \circ \circ \circ \circ \circ

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opyright© 1995 EI roperty Code: [HMSD1000] HEA	AT OF MIXING A	AND SOLUTION	1		ORTJ0954.030
tate:	Two-component sy	stem, single-phase	e liquid or two-ph	ase liquid-liqui	d (LL)	
I	Pure component 1	, liquid				
	Pure component 2	, liquid				
	[P1] <i>T/</i> K,	Temperature				
ariables:	$[X1] x_1/-,$	Mole fraction of	component 1			
fethod:	[Y1] HE/Jmol ⁻¹ , Direct low-pressur	molar excess entre re calorimetric me	asurement of H ^E	at variable x1 a	nd constant T	
Components:	1. C ₄ H ₁₀ O, Buta	n-1-ol		1		
	2. C8H16O2, Me	hyl heptanoate				
[P1] = .298		T		[Y1]		
[X1]	[Y1]			.180E+04		
.890000E-01	.636500E+03				0,0,0,0,0,0,0,0,0,0,0,0,0,0,0,0,0,0,0,	
.184900E+00	.111440E+04				.OO.Q	
.262900E+00	.137940E+04				,o	
.339500E+00	.154840E+04				, o	
.402100E+00 .453900E+00	.162140E+04 .164040E+04		1	.135E+04	. <u>,</u> , , , , , , , , , , , , , , , , , ,	
.497600E+00	.163090E+04				۵.	
.536800E+00	.157230E+04				0	
.568600E+00	.152090E+04				0	
.595000E+00	.148670E+04					0
.623800E+00	.142900E+04			.900E+03	. /	$\langle -$
.655700E+00	.135990E+04					
.690800E+00	.127970E+04					0
.730200E+00 .785700E+00	.116940E+04				Ģ	
.850400E+00	.990600E+03 .743000E+03			4505.00		
.910800E+00	.472300E+03			.450E+03	- /	<u> </u>
.962600E+00	.216600E+03					
					○ [P1] = .298150E+03	, o
				.000E+00		
				.0002+00	50E+00	
Property Code:	Pure component	EAT OF MIXING system, single-pha 1, liquid	AND SOLUTIO	N	.50E+00	
	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-,	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of	AND SOLUTIO ise liquid or two-p	N		[X1] ORTJ0954.03
Property Code: State: Parameters: Variables:	[HMSD1000] HI Two-component Pure component [P1] T/K, [X1] x1/-, [Y1] H ^E Jmol ⁻¹ ,	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess et	AND SOLUTIO se liquid or two-p of component 1 nthalpy	N hase liquid-liqu	id (LL)	
Property Code: State: Parameters: Variables: Method:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m	AND SOLUTIO se liquid or two-p of component 1 nthalpy	N hase liquid-liqu	id (LL)	
Property Code: State: Parameters: Variables:	[HMSD1000] HI Two-component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₄ H ₁₀ O, But	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	N hase liquid-liqu	id (LL)	
Property Code: State: Parameters: Variables: Method: Components:	[HMSD1000] HI Two-component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₄ H ₁₀ O, But	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	N hase liquid-liqu ³ at variable x ₁	id (LL)	
Property Code: State: Parameters: Variables: Method: Components:	[HMSD1000] HI Two-component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> 1/-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C4H10O, But 2. C10H20O2, M	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	N hase liquid-liqu	id (LL)	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₄ H ₁₀ O, But 2. C ₁₀ H ₂₀ O ₂ , M 8150E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	N hase liquid-liqu ³ at variable x ₁ [Y1]	id (LL) and constant T	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1]	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C4H100, But 2. C10H2002, M 8150E+03 [Y1] .727500E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	N hase liquid-liqu ³ at variable x ₁ [Y1]	id (LL) and constant T	ORTJ0954.03
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .998000E-01	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-press 1. C ₄ H ₁₀ O, But 2. C ₁₀ H ₂₀ O ₂ , M 8150E+03 [Y1] .727500E+03 .121840E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	N hase liquid-liqu ³ at variable x ₁ [Y1]	id (LL) and constant T	ORTJ0954.03
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .998000E-01 .206500E+00 .289300E+00 .356700E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₄ H ₁₀ O, But 2. C ₁₀ H ₂₀ O ₂ , M 8150E+03 [Y1] .727500E+03 .121840E+04 .148650E+04 .161280E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	N hase liquid-liqu ³ at variable x ₁ [Y1]	id (LL) and constant T	ORTJ0954.03
Property Code: State: Variables: Method: Components: [P1] = .29 [X1] .998000E-01 .206500E+00 .289300E+00 .356700E+00 .417400E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₄ H ₁₀ O, But 2. C ₁₀ H ₂₀ O ₂ , M 8150E+03 [Y1] .727500E+03 .121840E+04 .148650E+04 .166980E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	N hase liquid-liqu ³ at variable x ₁ [Y1]	id (LL) and constant T	ORTJ0954.03
Property Code: State: Variables: Method: Components: [P1] = .29 [X1] .998000E-01 .206500E+00 .356700E+00 .417400E+00 .471600E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₄ H ₁₀ O, But 2. C ₁₀ H ₂₀ O ₂ , M 8150E+03 [Y1] .727500E+03 .121840E+04 .161280E+04 .168120E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	N hase liquid-liqu 3 at variable x ₁ [Y1] .180E+04	id (LL) and constant T	ORTJ0954.03
Property Code: State: Variables: Method: Components: [P1] = .29 [X1] .998000E-01 .206500E+00 .289300E+00 .356700E+00 .417400E+00 .471600E+00 .520500E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C4H ₁₀ O, But 2. C ₁₀ H ₂₀ O ₂ , M 8150E+03 [Y1] .727500E+03 .121840E+04 .161280E+04 .166980E+04 .166290E+04 .166290E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	N hase liquid-liqu 3 at variable x ₁ [Y1] .180E+04	id (LL) and constant T	ORTJ0954.03
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .998000E-01 .206500E+00 .289300E+00 .417400E+00 .520500E+00 .520500E+00 .571600E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C4H ₁₀ O, But 2. C ₁₀ H ₂₀ O ₂ , M 8150E+03 [Y1] .727500E+03 .121840E+04 .148650E+04 .166290E+04 .168120E+04 .168290E+04 .158510E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	N hase liquid-liqu 3 at variable x ₁ [Y1] .180E+04	id (LL) and constant T	ORTJ0954.03
Property Code: State: Variables: Method: Components: [P1] = .29 [X1] .998000E-01 .206500E+00 .289300E+00 .356700E+00 .417400E+00 .471600E+00 .520500E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> 1/-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C4H100, But 2. C10H2002, M 8150E+03 [Y1] .727500E+03 .121840E+04 .148650E+04 .161280E+04 .168120E+04 .168120E+04 .158510E+04 .152800E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	N hase liquid-liqu 3 at variable x ₁ [Y1] .180E+04 .135E+04	id (LL) and constant T	ORTJ0954.03
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .998000E-01 .206500E+00 .289300E+00 .356700E+00 .471600E+00 .520500E+00 .571600E+00 .601000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C4H100, But 2. C10H2002, M 8150E+03 [Y1] .727500E+03 .121840E+04 .148650E+04 .166980E+04 .166980E+04 .168200E+04 .158510E+04 .152800E+04 .146290E+04 .146290E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	N hase liquid-liqu 3 at variable x ₁ [Y1] .180E+04	id (LL) and constant T	ORTJ0954.03
Property Code: State: Variables: Method: Components: [P1] = .29 [X1] .998000E-01 .206500E+00 .356700E+00 .417400E+00 .471600E+00 .520500E+00 .61300E+00 .631300E+00 .64800E+00 .702200E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₄ H ₁₀ O, But 2. C ₁₀ H ₂₀ O ₂ , M 8150E+03 [Y1] .727500E+03 .121840E+04 .161280E+04 .166980E+04 .166980E+04 .166290E+04 .16290E+04 .152800E+04 .152800E+04 .138310E+04 .128470E+04 .128470E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	N hase liquid-liqu 3 at variable x ₁ [Y1] .180E+04 .135E+04	id (LL) and constant T	ORTJ0954.03
Property Code: State: Variables: Method: Components: [P1] = .29 [X1] .998000E-01 .206500E+00 .289300E-01 .206500E+00 .356700E+00 .417400E+00 .571600E+00 .571600E+00 .601000E+00 .601300E+00 .664800E+00 .702200E+00 .743600E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C4H100, But 2. C10H2002, M 8150E+03 [Y1] .727500E+03 .121840E+04 .161280E+04 .166980E+04 .166980E+04 .166290E+04 .166290E+04 .152800E+04 .146290E+04 .138310E+04 .128470E+04 .116010E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	N hase liquid-liqu 3 at variable x ₁ [Y1] .180E+04 .135E+04	id (LL) and constant T	ORTJ0954.03
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .998000E-01 .206500E+00 .289300E+00 .356700E+00 .417400E+00 .520500E+00 .571600E+00 .601000E+00 .601300E+00 .702200E+00 .743600E+00 .789900E+00	[HMSD1000] HI Two-component Pure component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> 1/-, [Y1] <i>HE/J</i> m0 ⁻¹ , Direct low-press 1. C4H100, But 2. C10H2002, M 8150E+03 [Y1] .727500E+03 .121840E+04 .166980E+04 .166980E+04 .166980E+04 .16690E+04 .166290E+04 .158510E+04 .152800E+04 .158510E+04 .16290E+04 .138310E+04 .128470E+04 .101090E+04 .101090E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m	AND SOLUTIO ase liquid or two-p of component 1 nthalpy leasurement of H ^E	N hase liquid-liqu 3 at variable x ₁ [Y1] .180E+04 .135E+04	id (LL) and constant T	ORTJ0954.03
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .998000E-01 .206500E+00 .289300E+00 .417400E+00 .417400E+00 .520500E+00 .571600E+00 .601000E+00 .601000E+00 .601300E+00 .743600E+00 .743600E+00 .789900E+00 .832000E+00	[HMSD1000] HI Two-component Pure component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> 1/-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-press 1. C4H100, But 2. C10H2002, M 8150E+03 [Y1] .727500E+03 .121840E+04 .166980E+04 .166980E+04 .166980E+04 .166980E+04 .166290E+04 .158510E+04 .158510E+04 .158510E+04 .160290E+04 .16010E+04 .101090E+04 .10	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m	AND SOLUTIO ase liquid or two-p of component 1 nthalpy reasurement of H ^E	N hase liquid-liqu 3 at variable x1 [Y1] .180E+04 .135E+04 .900E+03	id (LL) and constant T	ORTJ0954.03
Property Code: State: Variables: Variables: Method: Components: [P1] = .29 [X1] .998000E-01 .206500E+00 .289300E+00 .356700E+00 .417400E+00 .571600E+00 .601000E+00 .631300E+00 .664800E+00 .702200E+00 .789900E+00 .832000E+00 .872600E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C4H100, But 2. C10H2002, M 8150E+03 [Y1] .727500E+03 .121840E+04 .148650E+04 .166980E+04 .166980E+04 .166980E+04 .168120E+04 .168200E+04 .158510E+04 .158510E+04 .128470E+04 .116010E+04 .101090E+04 .855800E+03 .684800E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m	AND SOLUTIO ase liquid or two-p of component 1 nthalpy reasurement of H ^E	N hase liquid-liqu 3 at variable x ₁ [Y1] .180E+04 .135E+04	id (LL) and constant T	ORTJ0954.03
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .998000E-01 .206500E+00 .289300E+00 .417400E+00 .417400E+00 .520500E+00 .571600E+00 .601000E+00 .601000E+00 .601300E+00 .743600E+00 .743600E+00 .789900E+00 .832000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₄ H ₁₀ O, But 2. C ₁₀ H ₂₀ O ₂ , M 8150E+03 [Y1] .727500E+03 .121840E+04 .166980E+04 .166980E+04 .166980E+04 .166980E+04 .166980E+04 .168120E+04 .168120E+04 .168290E+04 .152800E+04 .128470E+04 .128470E+04 .128470E+04 .138310E+04 .128470E+04 .138310E+04 .13	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m	AND SOLUTIO ase liquid or two-p of component 1 nthalpy reasurement of H ^E	N hase liquid-liqu 3 at variable x1 [Y1] .180E+04 .135E+04 .900E+03	id (LL) and constant T	ORTJ0954.03
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .998000E-01 .206500E+00 .289300E+00 .356700E+00 .471600E+00 .520500E+00 .601000E+00 .631300E+00 .64800E+00 .743600E+00 .832000E+00 .832000E+00 .872600E+00 .910600E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E Jmol ⁻¹ , Direct low-press 1. C ₄ H ₁₀ O, But 2. C ₁₀ H ₂₀ O ₂ , M 8150E+03 [Y1] .727500E+03 .121840E+04 .161280E+04 .166980E+04 .166980E+04 .166980E+04 .16690E+04 .166290E+04 .16290E+04 .16290E+04 .16290E+04 .16290E+04 .16290E+04 .16010E+04 .128470E+04 .101090E+04 .503100E+03 .503100E+03 .503100E+03 .503100E+03 .503100E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m	AND SOLUTIO ase liquid or two-p of component 1 nthalpy reasurement of H ^E	N hase liquid-liqu 3 at variable x1 [Y1] .180E+04 .135E+04 .900E+03	id (LL) and constant T	ORTJ0954.03
Property Code: State: Variables: Method: Components: [P1] = .29 [X1] .998000E-01 .206500E+00 .356700E+00 .356700E+00 .417400E+00 .520500E+00 .601000E+00 .601000E+00 .631300E+00 .743600E+00 .789900E+00 .872600E+00 .910600E+00 .945400E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E Jmol ⁻¹ , Direct low-press 1. C ₄ H ₁₀ O, But 2. C ₁₀ H ₂₀ O ₂ , M 8150E+03 [Y1] .727500E+03 .121840E+04 .16280E+04 .166980E+04 .166980E+04 .166290E+04 .166290E+04 .152810E+04 .152800E+04 .152800E+04 .138310E+04 .128470E+04 .16010E+04 .101090E+04 .503100E+03 .503100E+03 .320200E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m	AND SOLUTIO ase liquid or two-p of component 1 nthalpy reasurement of H ^E	N hase liquid-liqu 3 at variable x1 [Y1] .180E+04 .135E+04 .900E+03	id (LL) and constant T	ORTJ0954.03
Property Code: State: Variables: Method: Components: [P1] = .29 [X1] .998000E-01 .206500E+00 .356700E+00 .356700E+00 .417400E+00 .520500E+00 .601000E+00 .601000E+00 .631300E+00 .743600E+00 .789900E+00 .872600E+00 .910600E+00 .945400E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E Jmol ⁻¹ , Direct low-press 1. C ₄ H ₁₀ O, But 2. C ₁₀ H ₂₀ O ₂ , M 8150E+03 [Y1] .727500E+03 .121840E+04 .16280E+04 .166980E+04 .166980E+04 .166290E+04 .166290E+04 .152810E+04 .152800E+04 .152800E+04 .138310E+04 .128470E+04 .16010E+04 .101090E+04 .503100E+03 .503100E+03 .320200E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m	AND SOLUTIO ase liquid or two-p of component 1 nthalpy reasurement of H ^E	N hase liquid-liqu 3 at variable x ₁ [Y1] .180E+04 .135E+04 .900E+03 .450E+03	id (LL) and constant T	ORTJ0954.03
Property Code: State: Variables: Method: Components: [P1] = .29 [X1] .998000E-01 .206500E+00 .356700E+00 .356700E+00 .417400E+00 .520500E+00 .601000E+00 .601000E+00 .631300E+00 .743600E+00 .789900E+00 .872600E+00 .910600E+00 .945400E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E Jmol ⁻¹ , Direct low-press 1. C ₄ H ₁₀ O, But 2. C ₁₀ H ₂₀ O ₂ , M 8150E+03 [Y1] .727500E+03 .121840E+04 .16280E+04 .166980E+04 .166980E+04 .166290E+04 .166290E+04 .152810E+04 .152800E+04 .152800E+04 .138310E+04 .128470E+04 .16010E+04 .101090E+04 .503100E+03 .503100E+03 .320200E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m	AND SOLUTIO ase liquid or two-p of component 1 nthalpy reasurement of H ^E	N hase liquid-liqu 3 at variable x1 [Y1] .180E+04 .135E+04 .900E+03	id (LL) and constant T	ORTJ0954.03
Property Code: State: Variables: Method: Components: [P1] = .29 [X1] .998000E-01 .206500E+00 .356700E+00 .356700E+00 .417400E+00 .520500E+00 .61300E+00 .631300E+00 .64800E+00 .743600E+00 .789900E+00 .872600E+00 .910600E+00 .945400E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E Jmol ⁻¹ , Direct low-press 1. C ₄ H ₁₀ O, But 2. C ₁₀ H ₂₀ O ₂ , M 8150E+03 [Y1] .727500E+03 .121840E+04 .16280E+04 .166980E+04 .166980E+04 .166290E+04 .166290E+04 .152810E+04 .152800E+04 .152800E+04 .138310E+04 .128470E+04 .16010E+04 .101090E+04 .503100E+03 .503100E+03 .320200E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess en ure calorimetric m	AND SOLUTIO ase liquid or two-p of component 1 nthalpy reasurement of H ^E	N hase liquid-liqu 3 at variable x ₁ [Y1] .180E+04 .135E+04 .900E+03 .450E+03	id (LL) and constant T	ORTJ0954.03

State:		AT OF MIXING	AND SOLUTION	ORTJ0954.04
				ase liquid-liquid (LL)
	Pure component	1, liquid	1	
	Pure component			
	[P1] <i>T/</i> K,	Temperature	f	
ariables:	[X1] $x_{1/-}$, [X1] $HE/Imol-1$	Mole fraction of Molar excess en	t component 1	
fethod:	Direct low-pressu	re calorimetric me	easurement of HE	at variable x_1 and constant T
	1. C4H10O, But			
P. V BO BERNON	2. C ₁₂ H ₂₄ O ₂ , M	lethyl undecanoa	le	
[P1] = .298				[Y1]
[X1]	[Y1]			.180E+04
.118900E+00	.828500E+03			
.237600E+00	.134240E+04			0 ^{.00} 0
.329100E+00	.157790E+04			° °
.400500E+00	.167670E+04			
.457400E+00	.170080E+04			.135E+04 - 0 - 0 - 0 - 0 - 0 - 0 - 0 - 0 - 0 -
.504700E+00 .544700E+00	.168970E+04 .165920E+04			
.604700E+00	.165920E+04			
.635800E+00	.149120E+04			
.664600E+00	.141690E+04			0
.695800E+00	.133560E+04			.900E+03
.729900E+00	.124410E+04			Y i i i i i i i i i i i i i i i i i i
.768300E+00 .811000E+00	.112390E+04 .967800E+03			
.858400E+00	.765200E+03			
.911900E+00	.507600E+03			.450E+03
.960400E+00	.251700E+03			
				○ [P1] = .298150E+03
				.000E+00
				.50E+00
				[X1
		nce. All rights reserv		
roperty Code:		EAT OF MIXING		
			and the set of the section of the se	
tate:			se liquid or two-pl	ase iquid-liquid (LL)
late:	Pure component	1, liquid	se liquid or two-pl	ase liquid-liquid (LL)
arameters:	Pure component Pure component [P1] T/K,	1, liquid 2, liquid Temperature		iase liquid-liquid (LL)
	Pure component Pure component [P1] T/K, [X1] x ₁ /-,	1, liquid 2, liquid Temperature Mole fraction o	of component 1	iase liquid-liquid (LL)
arameters: ariables:	Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$,	1, liquid 2, liquid Temperature Mole fraction of Molar excess er	of component 1 hthalpy	
arameters: ariables: ethod:	Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-press	1, liquid 2, liquid Temperature Mole fraction o Molar excess er ure calorimetric m	of component 1 hthalpy	at variable x_1 and constant T
arameters: ariables: ethod: omponents:	Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. C ₄ H ₁₀ O, But	1, liquid 2, liquid Temperature Mole fraction o Molar excess er ure calorimetric m an-1-ol	of component 1 nthalpy easurement of H ^E	
arameters: ariables: ethod: omponents:	Pure component Pure component [P1] T/K , [X1] $x_{1}/-$, [Y1] $H^{E}/Jmol^{-1}$, Direct low-press 1. C ₄ H ₁₀ O, But 2. C ₁₄ H ₂₈ O ₂ , M	1, liquid 2, liquid Temperature Mole fraction o Molar excess er ure calorimetric m	of component 1 nthalpy easurement of H ^E	at variable x_1 and constant T
arameters: ariables: ethod: omponents: [P1] = .298	Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-presso 1. C4H ₁₀ O, But 2. C ₁₄ H ₂₈ O ₂ , M B150E+03	1, liquid 2, liquid Temperature Mole fraction o Molar excess er ure calorimetric m an-1-ol	of component 1 nthalpy easurement of H ^E	at variable x ₁ and constant T [Y1]
arameters: ariables: ethod: omponents: [P1] = .298 [X1]	Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^{E}/Jmol^{-1}$, Direct low-presses 1. C4H ₁₀ O, But 2. C ₁₄ H ₂₈ O ₂ , M B150E+03 [Y1]	1, liquid 2, liquid Temperature Mole fraction o Molar excess er ure calorimetric m an-1-ol	of component 1 nthalpy easurement of H ^E	at variable x ₁ and constant T [Y1] .180E+04
rameters: riables: ethod: mponents: [P1] = .298 [X1] 138200E+00	Pure component Pure component [P1] T/K , [X1] $x_{1}/-$, [Y1] $H^{E}/Jmol^{-1}$, Direct low-presses 1. C4H ₁₀ O, But 2. C ₁₄ H ₂₈ O ₂ , M B150E+03 [Y1] .820500E+03	1, liquid 2, liquid Temperature Mole fraction o Molar excess er ure calorimetric m an-1-ol	of component 1 nthalpy easurement of H ^E	at variable x ₁ and constant T [Y1] .180E+04
rameters: riables: ethod: mponents: [P1] = .298 [X1] 138200E+00 179100E+00	Pure component Pure component [P1] T/K , [X1] $x_{1}/-$, [Y1] $H^{E}/Jmol^{-1}$, Direct low-presses 1. C4H ₁₀ O, But 2. C ₁₄ H ₂₈ O ₂ , M B150E+03 [Y1] .820500E+03 .992400E+03	1, liquid 2, liquid Temperature Mole fraction o Molar excess er ure calorimetric m an-1-ol	of component 1 nthalpy easurement of H ^E	at variable x ₁ and constant T [Y1] .180E+04
rameters: riables: ethod: mponents: [P1] = .298 [X1] 138200E+00 179100E+00 244800E+00	Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-presses 1. C4H ₁₀ O, But 2. C ₁₄ H ₂₈ O ₂ , M B150E+03 [Y1] .820500E+03 .992400E+03 .123810E+04	1, liquid 2, liquid Temperature Mole fraction o Molar excess er ure calorimetric m an-1-ol	of component 1 nthalpy easurement of H ^E	at variable x ₁ and constant T [Y1] .180E+04
rameters: riables: ethod: mponents: [P1] = .298 [X1] 138200E+00 179100E+00 244800E+00 333600E+00	Pure component Pure component [P1] T/K , [X1] $x_{1}/-$, [Y1] $H^{E}/Jmol^{-1}$, Direct low-presses 1. C4H ₁₀ O, But 2. C ₁₄ H ₂₈ O ₂ , M B150E+03 [Y1] .820500E+03 .992400E+03	1, liquid 2, liquid Temperature Mole fraction o Molar excess er ure calorimetric m an-1-ol	of component 1 nthalpy easurement of H ^E	at variable x_1 and constant T $[Y1]$.180E+04 0
rameters: riables: ethod: mponents: [P1] = .298 [X1] 138200E+00 179100E+00 244800E+00 333600E+00 341300E+00	Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-presses 1. $C_4H_{10}O$, But 2. $C_{14}H_{28}O_2$, M B150E+03 [Y1] .820500E+03 .992400E+03 .123810E+04 .148630E+04	1, liquid 2, liquid Temperature Mole fraction o Molar excess er ure calorimetric m an-1-ol	of component 1 nthalpy easurement of H ^E	at variable x_1 and constant T $[Y1]$.180E+04 0
rameters: riables: ethod: mponents: [P1] = .298 [X1] 138200E+00 179100E+00 244800E+00 333600E+00 341300E+00 426500E+00	Pure component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-presses 1. C4H10O, But 2. C14H28O2, M B150E+03 [Y1] .820500E+03 .992400E+03 .123810E+04 .148630E+04 .150230E+04	1, liquid 2, liquid Temperature Mole fraction o Molar excess er ure calorimetric m an-1-ol	of component 1 nthalpy easurement of H ^E	at variable x_1 and constant T $[Y1]$.180E+04 0
rameters: riables: ethod: mponents: [P1] = .298 [X1] 138200E+00 179100E+00 244800E+00 333600E+00 341300E+00 426500E+00 460400E+00 553400E+00	Pure component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-presses 1. C4H10O, But 2. C14H28O2, M B150E+03 [Y1] .820500E+03 .992400E+03 .123810E+04 .148630E+04 .163200E+04 .168220E+04 .167580E+04	1, liquid 2, liquid Temperature Mole fraction o Molar excess er ure calorimetric m an-1-ol	of component 1 nthalpy easurement of H ^E	at variable x_1 and constant T $[Y1]$.180E+04 0
rameters: riables: ethod: mponents: [P1] = .298 [X1] 138200E+00 179100E+00 244800E+00 333600E+00 341300E+00 426500E+00 460400E+00 553400E+00 619200E+00	Pure component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-presse 1. C4H10O, But 2. C14H28O2, M B150E+03 [Y1] .820500E+03 .992400E+03 .123810E+04 .148630E+04 .163200E+04 .168220E+04 .167580E+04 .159700E+04	1, liquid 2, liquid Temperature Mole fraction o Molar excess er ure calorimetric m an-1-ol	of component 1 nthalpy easurement of H ^E	at variable x_1 and constant T $[Y1]$.180E+04 0
rameters: riables: ethod: mponents: [P1] = .298 [X1] 138200E+00 179100E+00 244800E+00 333600E+00 341300E+00 426500E+00 460400E+00 553400E+00 656600E+00	Pure component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-presse 1. C4H10O, But 2. C14H28O2, M B150E+03 [Y1] .820500E+03 .992400E+03 .123810E+04 .148630E+04 .163000E+04 .168220E+04 .167580E+04 .150870E+04	1, liquid 2, liquid Temperature Mole fraction o Molar excess er ure calorimetric m an-1-ol	of component 1 nthalpy easurement of H ^E	at variable x_1 and constant T $[Y1]$.180E+04 0
rameters: riables: ethod: mponents: [P1] = .298 [X1] 138200E+00 179100E+00 244800E+00 333600E+00 341300E+00 426500E+00 460400E+00 553400E+00 656600E+00 740800E+00	Pure component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-presse 1. $C_4H_{10}O$, But 2. $C_{14}H_{28}O_2$, M 3150E+03 [Y1] .820500E+03 .992400E+03 .123810E+04 .148630E+04 .163000E+04 .168220E+04 .167580E+04 .150870E+04 .150870E+04 .127790E+04	1, liquid 2, liquid Temperature Mole fraction o Molar excess er ure calorimetric m an-1-ol	of component 1 nthalpy easurement of H ^E	at variable x_1 and constant T [Y1] .180E+04 .135E+04 .000E+03
rameters: riables: ethod: mponents: [P1] = .298 [X1] 138200E+00 179100E+00 244800E+00 333600E+00 341300E+00 426500E+00 460400E+00 553400E+00 656600E+00 740800E+00 780000E+00	Pure component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-presse 1. $C_4H_{10}O$, But 2. $C_{14}H_{28}O_2$, M 3150E+03 [Y1] .820500E+03 .992400E+03 .123810E+04 .148630E+04 .163200E+04 .163200E+04 .168220E+04 .167580E+04 .150870E+04 .127790E+04 .114450E+04	1, liquid 2, liquid Temperature Mole fraction o Molar excess er ure calorimetric m an-1-ol	of component 1 nthalpy easurement of H ^E	at variable x_1 and constant T [Y1] .180E+04 .135E+04 .000E+03
rameters: riables: ethod: mponents: [P1] = .298 [X1] 138200E+00 244800E+00 333600E+00 341300E+00 426500E+00 460400E+00 553400E+00 656600E+00 740800E+00 780000E+00 823500E+00	Pure component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-presse 1. $C_4H_{10}O$, But 2. $C_{14}H_{28}O_2$, M 3150E+03 [Y1] .820500E+03 .992400E+03 .123810E+04 .148630E+04 .163200E+04 .168220E+04 .167580E+04 .150870E+04 .150870E+04 .127790E+04 .114450E+04 .970000E+03	1, liquid 2, liquid Temperature Mole fraction o Molar excess er ure calorimetric m an-1-ol	of component 1 nthalpy easurement of H ^E	at variable x_1 and constant T [Y1] .180E+04 .135E+04 .900E+03
rameters: riables: ethod: mponents: [P1] = .298 [X1] 138200E+00 179100E+00 244800E+00 333600E+00 341300E+00 460400E+00 553400E+00 656600E+00 740800E+00 85500E+00 866000E+00	Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₄ H ₁₀ O, But 2. C ₁₄ H ₂₈ O ₂ , M 3150E+03 [Y1] .820500E+03 .992400E+03 .123810E+04 .148630E+04 .163200E+04 .168220E+04 .167580E+04 .150870E+04 .150870E+04 .127790E+04 .127790E+04 .127790E+04 .127790E+03 .782600E+03	1, liquid 2, liquid Temperature Mole fraction o Molar excess er ure calorimetric m an-1-ol	of component 1 nthalpy easurement of H ^E	at variable x_1 and constant T [Y1] .180E+04 .135E+04 .900E+03
rameters: riables: ethod: mponents: [P1] = .298 [X1] 138200E+00 179100E+00 244800E+00 333600E+00 341300E+00 460400E+00 553400E+00 656600E+00 780000E+00 823500E+00 866000E+00 906100E+00	Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₄ H ₁₀ O, But 2. C ₁₄ H ₂₈ O ₂ , M 3150E+03 [Y1] .820500E+03 .992400E+03 .123810E+04 .148630E+04 .150230E+04 .168220E+04 .168220E+04 .150870E+04 .150870E+04 .150870E+04 .127790E+04 .114450E+04 .970000E+03 .782600E+03 .585800E+03	1, liquid 2, liquid Temperature Mole fraction o Molar excess er ure calorimetric m an-1-ol	of component 1 nthalpy easurement of H ^E	at variable x_1 and constant T [Y1] .180E+04 .135E+04 .900E+03
rameters: riables: ethod: mponents: [P1] = .298 [X1] 138200E+00 179100E+00 244800E+00 333600E+00 341300E+00 426500E+00 656400E+00 656600E+00 740800E+00 823500E+00 866000E+00 906100E+00 942700E+00	Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₄ H ₁₀ O, But 2. C ₁₄ H ₂₈ O ₂ , M 3150E+03 [Y1] .820500E+03 .992400E+03 .123810E+04 .148630E+04 .163200E+04 .168220E+04 .167580E+04 .150870E+04 .150870E+04 .127790E+04 .127790E+04 .127790E+04 .127790E+03 .782600E+03	1, liquid 2, liquid Temperature Mole fraction o Molar excess er ure calorimetric m an-1-ol	of component 1 nthalpy easurement of H ^E	at variable x_1 and constant T [Y1] .180E+04 .135E+04 .900E+03
rameters: riables: ethod: mponents: [P1] = .298 [X1] 138200E+00 179100E+00 244800E+00 333600E+00 341300E+00 426500E+00 656400E+00 553400E+00 656600E+00 780000E+00 823500E+00 866000E+00 906100E+00 942700E+00	Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₄ H ₁₀ O, But 2. C ₁₄ H ₂₈ O ₂ , M 3150E+03 [Y1] .820500E+03 .992400E+03 .123810E+04 .148630E+04 .163000E+04 .163200E+04 .163200E+04 .150870E+04 .150870E+04 .127790E+04 .114450E+04 .970000E+03 .782600E+03 .585800E+03 .375900E+03	1, liquid 2, liquid Temperature Mole fraction o Molar excess er ure calorimetric m an-1-ol	of component 1 nthalpy easurement of H ^E	at variable x_1 and constant T [Y1] .180E+04 .135E+04 .000E+03
rameters: riables: ethod: mponents: [P1] = .298 [X1] 138200E+00 179100E+00 244800E+00 333600E+00 341300E+00 460400E+00 553400E+00 656600E+00 656600E+00 780000E+00 823500E+00 866000E+00 906100E+00 942700E+00	Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₄ H ₁₀ O, But 2. C ₁₄ H ₂₈ O ₂ , M 3150E+03 [Y1] .820500E+03 .992400E+03 .123810E+04 .148630E+04 .163000E+04 .163200E+04 .163200E+04 .150870E+04 .150870E+04 .127790E+04 .114450E+04 .970000E+03 .782600E+03 .585800E+03 .375900E+03	1, liquid 2, liquid Temperature Mole fraction o Molar excess er ure calorimetric m an-1-ol	of component 1 nthalpy easurement of H ^E	at variable x_1 and constant T [Y1] .180E+04 .135E+04 .900E+03 .450E+03 .450E+03 .0 [P1] = .298150E+03
rameters: riables: ethod: mponents: [P1] = .298 [X1] 138200E+00 179100E+00 244800E+00 333600E+00 341300E+00 426500E+00 656400E+00 656600E+00 740800E+00 823500E+00 866000E+00 906100E+00 942700E+00	Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₄ H ₁₀ O, But 2. C ₁₄ H ₂₈ O ₂ , M 3150E+03 [Y1] .820500E+03 .992400E+03 .123810E+04 .148630E+04 .163000E+04 .163200E+04 .163200E+04 .150870E+04 .150870E+04 .127790E+04 .114450E+04 .970000E+03 .782600E+03 .585800E+03 .375900E+03	1, liquid 2, liquid Temperature Mole fraction o Molar excess er ure calorimetric m an-1-ol	of component 1 nthalpy easurement of H ^E	at variable x_1 and constant T [Y1] .180E+04 .135E+04 .900E+03 .450E+03
ethod: [P1] = .298	Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₄ H ₁₀ O, But 2. C ₁₄ H ₂₈ O ₂ , M 3150E+03 [Y1] .820500E+03 .992400E+03 .123810E+04 .148630E+04 .163000E+04 .163200E+04 .163200E+04 .150870E+04 .150870E+04 .127790E+04 .114450E+04 .970000E+03 .782600E+03 .585800E+03 .375900E+03	1, liquid 2, liquid Temperature Mole fraction o Molar excess er ure calorimetric m an-1-ol	of component 1 nthalpy easurement of H ^E	at variable x_1 and constant T [Y1] .180E+04 .135E+04 .900E+03 .450E+03 \circ [P1] = .298150E+03
rameters: riables: ethod: mponents: [P1] = .298 [X1] 138200E+00 179100E+00 244800E+00 333600E+00 341300E+00 426500E+00 656400E+00 656600E+00 740800E+00 823500E+00 866000E+00 906100E+00 942700E+00	Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₄ H ₁₀ O, But 2. C ₁₄ H ₂₈ O ₂ , M 3150E+03 [Y1] .820500E+03 .992400E+03 .123810E+04 .148630E+04 .163000E+04 .163200E+04 .163200E+04 .150870E+04 .150870E+04 .127790E+04 .114450E+04 .970000E+03 .782600E+03 .585800E+03 .375900E+03	1, liquid 2, liquid Temperature Mole fraction o Molar excess er ure calorimetric m an-1-ol	of component 1 nthalpy easurement of H ^E	at variable x_1 and constant T [Y1] .180E+04 .135E+04 .900E+03 .450E+03 .450E+03 .0 [P1] = .298150E+03
rameters: riables: sthod: mponents: [P1] = .298 [X1] 138200E+00 179100E+00 244800E+00 333600E+00 341300E+00 341300E+00 553400E+00 553400E+00 556600E+00 780000E+00 823500E+00 906100E+00 942700E+00	Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₄ H ₁₀ O, But 2. C ₁₄ H ₂₈ O ₂ , M 3150E+03 [Y1] .820500E+03 .992400E+03 .123810E+04 .148630E+04 .163000E+04 .163200E+04 .163200E+04 .150870E+04 .150870E+04 .127790E+04 .114450E+04 .970000E+03 .782600E+03 .585800E+03 .375900E+03	1, liquid 2, liquid Temperature Mole fraction o Molar excess er ure calorimetric m an-1-ol	of component 1 nthalpy easurement of H ^E	at variable x_1 and constant T [Y1] .180E+04 .135E+04 .900E+03 .450E+03 .000E+00

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States	[HMSD1000] HE	AT OF MIXING AND SOLUTIO	ON ORTJ0954.066
State:	Two-component s Pure component 1	ystem, single-phase liquid or two-p	nase uquia-uquia (LL)
	Pure component 2	2 liquid	
Parameters:	[P1] <i>T/</i> K,	Temperature	
Variables:	$[X1] x_1/-,$	Mole fraction of component 1	
	[Y1] $H^{E}/Jmol^{-1}$,	Molar excess enthalpy	
Method:		re calorimetric measurement of H^2	^E at variable x_1 and constant $T_{$
Components:	1. C ₄ H ₁₀ O, Buta 2. C ₁₆ H ₃₂ O ₂ , Me	n-1-ol ethyl pentadecanoate	
[P1] = .298		· · · · · · · · · · · · · · · · · · ·	[Y1]
[X1]	[Y1]		.200E+04
.543000E-01	.478300E+03		4 1 ' ' ' 1
.148300E+00	.105030E+04		○ [P1] = .298150E+03
.276400E+00	.149440E+04		, o ^{o.,} o,
.376100E+00	.172070E+04		
.447200E+00	.177740E+04		150E+04
.507700E+00 .560000E+00	.178420E+04 .173630E+04		
.602700E+00			
.639700E+00	.160600E+04		
.670400E+00			1005.04
.698400E+00			.100E+04
.733600E+00 .768200E+00			○ [P1] = .298150E+03 .150E+04 - 0 .100E+04 - 0 .500E+03 - 0 .500E+04 - 0 .500E+05 - 0 .500E+0
.708200E+00			
.840700E+00			
.879300E+00	.736500E+03		.500E+03
.915800E+00			
.948700E+00 .976900E+00			0
.9/09002+00	.167200E+03		
			.000E+00
			.50E+00
			[X1]
Commisht@ 1005 I	LI DATA SADI Em	nce. All rights reserved.	
Property Code:	[HMSD1000] HE	EAT OF MIXING AND SOLUTIO	ON ORTJ0954.014
State:			
State:	Two-component Pure component	system, single-phase liquid or two- 1, liquid	
	Two-component Pure component Pure component	system, single-phase liquid or two- 1, liquid 2, liquid	
Parameters:	Two-component Pure component Pure component [P1] T/K,	system, single-phase liquid or two- 1, liquid 2, liquid Temperature	
	Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$,	system, single-phase liquid or two- 1, liquid 2, liquid Temperature Mole fraction of component 1	
Parameters:	Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ ,	system, single-phase liquid or two- 1, liquid 2, liquid Temperature	phase liquid-liquid (LL)
Parameters: Variables:	Two-component Pure component Pure component [P1] T/K , [X1] $x_{1}/-$, [Y1] H^E /Jmol ⁻¹ , Direct low-press 1. C5H ₁₀ O ₂ , Me	system, single-phase liquid or two- 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of H thyl butanoate	phase liquid-liquid (LL)
Parameters: Variables: Method: Components:	Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/}$, [Y1] $HE/Jmol^{-1}$, Direct low-press 1. C5H10O2, Me 2. C6H14O, Hexa	system, single-phase liquid or two- 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of H thyl butanoate	phase liquid-liquid (LL) E at variable x_1 and constant T
Parameters: Variables: Method: Components: [P1] = .29	Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $HE/Jmol^{-1}$, Direct low-press 1. C5H10O2, Me 2. C6H14O, Hext 8150E+03	system, single-phase liquid or two- 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of H thyl butanoate	phase liquid-liquid (LL) E at variable x_1 and constant T [Y1]
Parameters: Variables: Method: Components: [P1] = .29 [X1]	Two-component Pure component Pure component [P1] T/K, [X1] [X1] [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C5H10O2, Me 2. C6H14O, Hext 8150E+03 [Y1]	system, single-phase liquid or two- 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of H thyl butanoate	Phase liquid-liquid (LL) ^E at variable x ₁ and constant T [Y1] .200E+04
Parameters: Variables: Method: Components: [P1] = .29 [X1] .672000E-01	Two-component Pure component Pure component [P1] T/K, [X1] [X1] [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C5H10O2, Me 2. C6H14O, Hext 8150E+03 [Y1] .414000E+03	system, single-phase liquid or two- 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of H thyl butanoate	phase liquid-liquid (LL) ^E at variable x_1 and constant T [Y1] .200E+04 \circ [P1] = .298150E+03
Parameters: Variables: Method: Components: [P1] = .29 [X1] .672000E-01 .138200E+00	Two-component Pure component Pure component [P1] T/K, [X1] [X1] J. C5H10O2, Me 2. C6H14O, Hext 8150E+03 [Y1] .414000E+03 .759900E+03	system, single-phase liquid or two- 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of H thyl butanoate	phase liquid-liquid (LL) ^E at variable x_1 and constant T [Y1] .200E+04 \circ [P1] = .298150E+03
Parameters: Variables: Method: Components: [P1] = .29 [X1] .672000E-01	Two-component Pure component Pure component [P1] T/K, [X1] [X1] [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C5H10O2, Me 2. C6H14O, Hext 8150E+03 [Y1] .414000E+03	system, single-phase liquid or two- 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of H thyl butanoate	phase liquid-liquid (LL) ^E at variable x_1 and constant T [Y1] .200E+04 \circ [P1] = .298150E+03
Parameters: Variables: Method: Components: [P1] = .29 [X1] .672000E-01 .138200E+00 .209900E+00 .278500E+00 .344300E+00	Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressi 1. C5H ₁₀ O ₂ , Me 2. C ₆ H ₁₄ O, Hexa 8150E+03 [Y1] .414000E+03 .759900E+03 .107920E+04 .132610E+04 .151110E+04	system, single-phase liquid or two- 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of H thyl butanoate	phase liquid-liquid (LL) $E \text{ at variable } x_1 \text{ and constant } T$ [Y1] .200E+04 \circ [P1] = .298150E+03
Parameters: Variables: Method: Components: [P1] = .29 [X1] .672000E-01 .138200E+00 .209900E+00 .278500E+00 .344300E+00 .405400E+00	Two-component Pure component Pure component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. C5H10O2, Me 2. C6H14O, Hexa 8150E+03 [Y1] .414000E+03 .759900E+03 .107920E+04 .132610E+04 .151110E+04 .163740E+04	system, single-phase liquid or two- 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of H thyl butanoate	phase liquid-liquid (LL) ^E at variable x_1 and constant T [Y1] .200E+04 \circ [P1] = .298150E+03 $\circ^{\circ \circ \circ \circ} \circ_{\circ \circ}$
Parameters: Variables: Method: Components: [P1] = .29 [X1] .672000E-01 .138200E+00 .209900E+00 .278500E+00 .344300E+00 .405400E+00 .461100E+00	Two-component Pure component Pure c	system, single-phase liquid or two- 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of H thyl butanoate	phase liquid-liquid (LL) $E \text{ at variable } x_1 \text{ and constant } T$ [Y1] .200E+04 \circ [P1] = .298150E+03
Parameters: Variables: Method: Components: [P1] = .29 [X1] .672000E-01 .138200E+00 .209900E+00 .278500E+00 .405400E+00 .405400E+00 .510300E+00	Two-component Pure component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] HE/Jmol ⁻¹ , Direct low-pression 1. C5H10O2, Me 2. C6H14O, Hexa 8150E+03 [Y1] .414000E+03 .759900E+03 .107920E+04 .132610E+04 .151110E+04 .163740E+04 .171240E+04 .174560E+04	system, single-phase liquid or two- 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of H thyl butanoate	phase liquid-liquid (LL) $E \text{ at variable } x_1 \text{ and constant } T$ [Y1] .200E+04 \circ [P1] = .298150E+03
Parameters: Variables: Method: Components: [P1] = .29 [X1] .672000E-01 .138200E+00 .209900E+00 .278500E+00 .405400E+00 .401100E+00 .510300E+00 .554200E+00	Two-component Pure component Pure component Pure component Pure component Pure component [Y1] T/K, [Y1] L C5H10O2, Me 2. C6H14O, Hext 8150E+03 [Y1] .414000E+03 .759900E+03 .107920E+04 .132610E+04 .151110E+04 .163740E+04 .171240E+04 .175070E+04	system, single-phase liquid or two- 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of H thyl butanoate	phase liquid-liquid (LL) $E \text{ at variable } x_1 \text{ and constant } T$ [Y1] .200E+04 .150E+04 .150E+04 .150E+04
Parameters: Variables: Method: Components: [P1] = .29 [X1] .672000E-01 .138200E+00 .209900E+00 .278500E+00 .405400E+00 .405400E+00 .461100E+00 .510300E+00	Two-component Pure component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] HE/Jmol ⁻¹ , Direct low-pression 1. C5H10O2, Me 2. C6H14O, Hexa 8150E+03 [Y1] .414000E+03 .759900E+03 .107920E+04 .132610E+04 .151110E+04 .163740E+04 .171240E+04 .174560E+04	system, single-phase liquid or two- 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of H thyl butanoate	phase liquid-liquid (LL) $E \text{ at variable } x_1 \text{ and constant } T$ [Y1] .200E+04 \circ [P1] = .298150E+03
Parameters: Variables: Method: Components: [P1] = .29 [X1] .672000E-01 .138200E+00 .209900E+00 .278500E+00 .344300E+00 .405400E+00 .510300E+00 .600200E+00 .654100E+00 .712300E+00	Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C5H10O2, Me 2. C6H14O, Hexa 8150E+03 [Y1] .414000E+03 .759900E+03 .107920E+04 .132610E+04 .132610E+04 .171240E+04 .171240E+04 .175070E+04 .171960E+04 .152350E+04	system, single-phase liquid or two- 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of H thyl butanoate	phase liquid-liquid (LL) $E \text{ at variable } x_1 \text{ and constant } T$ [Y1] .200E+04 .150E+04
Parameters: Variables: Method: Components: [P1] = .29 [X1] .672000E-01 .138200E+00 .209900E+00 .278500E+00 .344300E+00 .344300E+00 .461100E+00 .510300E+00 .600200E+00 .654100E+00 .712300E+00 .772700E+00	Two-component Pure component Pure component Pure component Pure component Pure component Pure component [Y1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. C5H10O2, Me 2. C6H14O, Hexa 8150E+03 [Y1] .414000E+03 .759900E+03 .107920E+04 .132610E+04 .151110E+04 .163740E+04 .174560E+04 .17906E+04 .164790E+04 .152350E+04 .132830E+04	system, single-phase liquid or two- 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of H thyl butanoate	phase liquid-liquid (LL) $E \text{ at variable } x_1 \text{ and constant } T$ [Y1] .200E+04 .150E+04
Parameters: Variables: Method: Components: [P1] = .29 [X1] .672000E-01 .138200E+00 .209900E+00 .278500E+00 .344300E+00 .405400E+00 .405400E+00 .554200E+00 .654100E+00 .712300E+00 .772700E+00 .834700E+00	Two-component Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressi 1. C5H10O ₂ , Me 2. C6H14O, Hexa 8150E+03 [Y1] .414000E+03 .759900E+03 .107920E+04 .132610E+04 .151110E+04 .163740E+04 .171960E+04 .171960E+04 .172350E+04 .132830E+04 .132830E+04 .107720E+04	system, single-phase liquid or two- 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of H thyl butanoate	phase liquid-liquid (LL) $E \text{ at variable } x_1 \text{ and constant } T$ [Y1] .200E+04 .150E+04
Parameters: Variables: Method: Components: [P1] = .29 [X1] .672000E-01 .138200E+00 .209900E+00 .278500E+00 .405400E+00 .405400E+00 .554200E+00 .600200E+00 .654100E+00 .772700E+00 .834700E+00 .898200E+00	Two-component Pure component Pure component Pure component Pure component Pure component [Y1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. C5H10O2, Me 2. C6H14O, Hexa 8150E+03 [Y1] .414000E+03 .759900E+03 .107920E+04 .132610E+04 .151110E+04 .163740E+04 .171260E+04 .171960E+04 .152350E+04 .132830E+04 .107720E+04 .107720E+04 .747700E+03	system, single-phase liquid or two- 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of H thyl butanoate	phase liquid-liquid (LL) $E \text{ at variable } x_1 \text{ and constant } T$ $[Y1]$ $.200E+04$ $\circ [P1] = .298150E+03$ $0^{\circ} \circ $
Parameters: Variables: Method: Components: [P1] = .29 [X1] .672000E-01 .138200E+00 .209900E+00 .278500E+00 .344300E+00 .405400E+00 .405400E+00 .554200E+00 .654100E+00 .712300E+00 .772700E+00 .834700E+00	Two-component Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressi 1. C5H10O ₂ , Me 2. C6H14O, Hexa 8150E+03 [Y1] .414000E+03 .759900E+03 .107920E+04 .132610E+04 .151110E+04 .163740E+04 .171960E+04 .171960E+04 .172350E+04 .132830E+04 .132830E+04 .107720E+04	system, single-phase liquid or two- 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of H thyl butanoate	phase liquid-liquid (LL) $E \text{ at variable } x_1 \text{ and constant } T$ [Y1] .200E+04 .150E+04 .150E+04 .100E+04 .500E+03
Parameters: Variables: Method: Components: [P1] = .29 [X1] .672000E-01 .138200E+00 .209900E+00 .278500E+00 .405400E+00 .405400E+00 .554200E+00 .600200E+00 .654100E+00 .772700E+00 .834700E+00 .898200E+00	Two-component Pure component Pure component Pure component Pure component Pure component [Y1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. C5H10O2, Me 2. C6H14O, Hexa 8150E+03 [Y1] .414000E+03 .759900E+03 .107920E+04 .132610E+04 .151110E+04 .163740E+04 .171260E+04 .171960E+04 .152350E+04 .132830E+04 .107720E+04 .107720E+04 .747700E+03	system, single-phase liquid or two- 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of H thyl butanoate	phase liquid-liquid (LL) $E \text{ at variable } x_1 \text{ and constant } T$ $[Y1]$ $.200E+04$ $\circ [P1] = .298150E+03$ $0^{\circ} \circ $
Parameters: Variables: Method: Components: [P1] = .29 [X1] .672000E-01 .138200E+00 .209900E+00 .278500E+00 .405400E+00 .405400E+00 .554200E+00 .600200E+00 .654100E+00 .772700E+00 .834700E+00 .898200E+00	Two-component Pure component Pure component Pure component Pure component Pure component [Y1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. C5H10O2, Me 2. C6H14O, Hexa 8150E+03 [Y1] .414000E+03 .759900E+03 .107920E+04 .132610E+04 .151110E+04 .163740E+04 .171260E+04 .171960E+04 .152350E+04 .132830E+04 .107720E+04 .107720E+04 .747700E+03	system, single-phase liquid or two- 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of H thyl butanoate	phase liquid-liquid (LL) $E \text{ at variable } x_1 \text{ and constant } T$ [Y1] .200E+04 .150E+04 .150E+04 .100E+04 .500E+03
Parameters: Variables: Method: Components: [P1] = .29 [X1] .672000E-01 .138200E+00 .209900E+00 .278500E+00 .405400E+00 .405400E+00 .554200E+00 .600200E+00 .654100E+00 .772700E+00 .834700E+00 .898200E+00	Two-component Pure component Pure component Pure component Pure component Pure component [Y1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. C5H10O2, Me 2. C6H14O, Hexa 8150E+03 [Y1] .414000E+03 .759900E+03 .107920E+04 .132610E+04 .151110E+04 .163740E+04 .171260E+04 .171960E+04 .152350E+04 .132830E+04 .107720E+04 .107720E+04 .747700E+03	system, single-phase liquid or two- 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of H thyl butanoate	phase liquid-liquid (LL) $E \text{ at variable } x_1 \text{ and constant } T$ [Y1] .200E+04 .150E+04 .150E+04 .100E+04 .500E+03
Parameters: Variables: Method: Components: [P1] = .29 [X1] .672000E-01 .138200E+00 .209900E+00 .278500E+00 .405400E+00 .405400E+00 .554200E+00 .600200E+00 .654100E+00 .772700E+00 .834700E+00 .898200E+00	Two-component Pure component Pure component Pure component Pure component Pure component [Y1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. C5H10O2, Me 2. C6H14O, Hexa 8150E+03 [Y1] .414000E+03 .759900E+03 .107920E+04 .132610E+04 .151110E+04 .163740E+04 .171260E+04 .171960E+04 .152350E+04 .132830E+04 .107720E+04 .107720E+04 .747700E+03	system, single-phase liquid or two- 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of H thyl butanoate	phase liquid-liquid (LL) $E \text{ at variable } x_1 \text{ and constant } T$ [Y1] .200E+04 .200E+04 .150E+04 .150E+04 .100E+04 .000E+00
Parameters: Variables: Method: Components: [P1] = .29 [X1] .672000E-01 .138200E+00 .209900E+00 .278500E+00 .405400E+00 .405400E+00 .554200E+00 .600200E+00 .654100E+00 .772700E+00 .834700E+00 .898200E+00	Two-component Pure component Pure component Pure component Pure component Pure component [Y1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. C5H10O2, Me 2. C6H14O, Hexa 8150E+03 [Y1] .414000E+03 .759900E+03 .107920E+04 .132610E+04 .151110E+04 .163740E+04 .171260E+04 .171960E+04 .152350E+04 .132830E+04 .107720E+04 .107720E+04 .747700E+03	system, single-phase liquid or two- 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of H thyl butanoate	phase liquid-liquid (LL) E at variable x_1 and constant T [Y1] 200E+04 \circ [P1] = .298150E+03 $\circ^{\circ} \circ^{\circ} \circ_{\circ} \circ$
Parameters: Variables: Method: Components: [P1] = .29 [X1] .672000E-01 .138200E+00 .209900E+00 .278500E+00 .344300E+00 .405400E+00 .405400E+00 .554200E+00 .600200E+00 .712300E+00 .772700E+00 .834700E+00 .898200E+00	Two-component Pure component Pure component Pure component Pure component Pure component [Y1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. C5H10O2, Me 2. C6H14O, Hexa 8150E+03 [Y1] .414000E+03 .759900E+03 .107920E+04 .132610E+04 .151110E+04 .163740E+04 .171260E+04 .171960E+04 .152350E+04 .132830E+04 .107720E+04 .107720E+04 .747700E+03	system, single-phase liquid or two- 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of H thyl butanoate	phase liquid-liquid (LL) $E \text{ at variable } x_1 \text{ and constant } T$ [Y1] .200E+04 .200E+04 .150E+04 .150E+04 .100E+04 .000E+00

	LDATA SARL Fraz IHMSD10001 HF		AND SOLUTION	and the second sec	ORTJ0954.016
State:	Two-component s	system, single-pha	se liquid or two-pha	se liquid-liquid (LL)	
	Pure component	1, liquid	- •	/	
-	Pure component				
Parameters: Variables:	[P1] <i>T/</i> K, [X1] <i>x</i> ₁ /-,	Temperature Mole fraction o	f component 1		
AT HUDICS:	[Y1] HE/Jmol-1	Molar excess er	nthalpy		
Method:	Direct low-pressu	ire calorimetric m	easurement of H^E a	t variable x_1 and constant T	
Components:	1. C ₅ H ₁₀ O ₂ , Me 2. C ₈ H ₁₈ O, Oct	ethyl butanoate	nan geregel av gerlanden og skrivet som en som en som en skille af som en skille skrivet som en som en som en s		
[P1] = .298				[Y1]	
[X1]	[Y1]			.200E+04	
.862000E-01	.543900E+03		5		.0.0.0
.169400E+00	.940000E+03		1		0 ^{.000} 0
.249600E+00	.128740E+04			\$	Ö. Ö.
.324500E+00 .393600E+00	.154210E+04 .171680E+04		1	1500-104	6
.456600E+00	.182210E+04			.150E+04	
.512700E+00	.187420E+04				ò
.561900E+00	.188690E+04			Ŷ	
.605000E+00 .645200E+00	.186800E+04 .181580E+04				
.694900E+00	.181380E+04			.100E+04	0
.746800E+00	.154060E+04			0	
.800100E+00					0
.855600E+00 .907600E+00	.106680E+04 .739500E+03				.
.956100E+00	.739300E+03			.500E+03	
					Q
				○[P1] :	= .298150E+03
			,		
	a second and a second	1 m · · · · · · · · · · · · · · · · · ·		.000E+00	<u> </u>
					.50E+00
					[X1]
			II		
	ELDATA SARL Fra		ved. 3 AND SOLUTION	187 - Angele Branner - Marine A.	ORTJ0954.018
State:	Two-component	mutan sincle sh		 The second se Second second sec	
	rue component	system, single-pha	ase liquid or two-pha	ase liquid-liquid (LL)	
	Pure component	1, liquid	ase liquid or two-pha	ase liquid-liquid (LL)	
Denser	Pure component Pure component	1, liquid 2, liquid	ase liquid or two-ph	ase liquid-liquid (LL)	
Parameters: Variables:	Pure component Pure component [P1] T/K,	1, liquid 2, liquid Temperature		ase liquid-liquid (LL)	
Parameters: Variables:	Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$,	1, liquid 2, liquid Temperature Mole fraction Molar excess e	of component 1 nthalpy	ž ≱očstovych so objektov Zastovych so objektov Zastovala	
	Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$,	1, liquid 2, liquid Temperature Mole fraction Molar excess e	of component 1 nthalpy	ase liquid-liquid (LL) at variable x_1 and constant T	
Variables:	Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. C5H10O2, M	1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl butanoate	of component 1 nthalpy	ž ≱očstovych so objektov Zastovych so objektov Zastovala	
Variables: Method: Components:	Pure component Pure component [P1] T/K , [X1] $x_{1}/-$, [Y1] $H^{E}/Jmol^{-1}$, Direct low-press 1. C5H ₁₀ O ₂ , Mu 2. C ₁₀ H ₂₂ O, De	1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl butanoate	of component 1 nthalpy	at variable x_1 and constant T	
Variables: Method: Components: [P1] = .298	Pure component Pure component [P1] T/K , [X1] $x_{1}/-$, [Y1] $H^{E}/Jmol^{-1}$, Direct low-press 1. C5H10O2, Ma 2. C10H22O, De B150E+03	1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl butanoate	of component 1 nthalpy	at variable x_1 and constant T [Y1]	
Variables: Method: Components: [P1] = .298 [X1]	Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-presses 1. $C5H_{10}O_2$, Ma 2. $C_{10}H_{22}O$, De B150E+03 [Y1]	1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl butanoate	of component 1 nthalpy	IY1] .240E+04	
Variables: Method: Components: [P1] = .298 [X1] .993000E-01	Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-presses 1. $C5H_{10}O_2$, Ma 2. $C_{10}H_{22}O$, De B150E+03 [Y1] .630200E+03	1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl butanoate	of component 1 nthalpy	at variable x_1 and constant T [Y1]	150E+03
Variables: Method: Components: [P1] = .298 [X1]	Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-presses 1. $C5H_{10}O_2$, Ma 2. $C_{10}H_{22}O$, De B150E+03 [Y1]	1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl butanoate	of component 1 nthalpy	IY1] .240E+04	
Variables: Method: Components: [P1] = .298 [X1] .993000E-01 .200800E+00 .291800E+00 .375000E+00	Pure component Pure component Pure component [P1] T/K , [X1] $x_{1}/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. $C5H_{10}O_2$, Ma 2. $C_{10}H_{22}O$, De 3150E+03 [Y1] .630200E+03 .114670E+04 .154660E+04 .180310E+04	1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl butanoate	of component 1 nthalpy	IY1] .240E+04	
Variables: Method: Components: [P1] = .298 [X1] .993000E-01 .200800E+00 .291800E+00 .375000E+00 .447400E+00	Pure component Pure component Pure component [P1] T/K , [X1] $x_{1}/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. $C5H_{10}O_2$, Ma 2. $C_{10}H_{22}O$, De 3150E+03 [Y1] .630200E+03 .114670E+04 .154660E+04 .180310E+04 .196040E+04	1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl butanoate	of component 1 nthalpy	IY1] .240E+04	
Variables: Method: Components: [P1] = .298 [X1] .993000E-01 .200800E+00 .291800E+00 .375000E+00 .447400E+00 .512200E+00	Pure component Pure component Pure component [P1] T/K , [X1] $x_{1}/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. $C5H_{10}O_2$, Ma 2. $C_{10}H_{22}O$, De 3150E+03 [Y1] .630200E+03 .114670E+04 .154660E+04 .180310E+04 .196040E+04 .204520E+04	1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl butanoate	of component 1 nthalpy	[Y1] .240E+04 \circ [P1] = .298	
Variables: Method: Components: [P1] = .298 [X1] .993000E-01 .200800E+00 .291800E+00 .375000E+00 .447400E+00 .512200E+00 .539200E+00	Pure component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. $C5H_{10}O_2$, M. 2. $C_{10}H_{22}O$, De 3150E+03 [Y1] .630200E+03 .114670E+04 .154660E+04 .196040E+04 .204520E+04 .206670E+04	1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl butanoate	of component 1 nthalpy	[Y1] .240E+04 \circ [P1] = .298	
Variables: Method: Components: [P1] = .298 [X1] .993000E-01 .200800E+00 .291800E+00 .375000E+00 .447400E+00 .512200E+00 .539200E+00 .570100E+00	Pure component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. $C5H_{10}O_2$, M. 2. $C_{10}H_{22}O$, De 3150E+03 [Y1] .630200E+03 .114670E+04 .154660E+04 .196040E+04 .204520E+04 .206670E+04 .208090E+04	1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl butanoate	of component 1 nthalpy	[Y1] .240E+04 \circ [P1] = .298	o ^{ooa} o. _o o o
Variables: Method: Components: [P1] = .298 [X1] .993000E-01 .200800E+00 .291800E+00 .375000E+00 .447400E+00 .512200E+00 .539200E+00 .570100E+00 .653700E+00	Pure component Pure component Pure component [P1] T/K , [X1] $x_{1}/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-presse 1. $C5H_{10}O_2$, Ma 2. $C_{10}H_{22}O$, De 3150E+03 [Y1] .630200E+03 .114670E+04 .154660E+04 .196040E+04 .204520E+04 .206670E+04 .208090E+04 .205930E+04 .200790E+04	1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl butanoate	of component 1 nthalpy	$[Y1] \\ .240E+04 \\ .180E+04 \\ .180E+04 \\ .0 [P1] = .2983 \\ .0 \\ .0 \\ .0 \\ .0 \\ .0 \\ .0 \\ .0 \\ .$	0,00000,0 0,0000,0 0,0000,0 0,0000,0 0,0000,0 0,0000,0 0,0000,0 0,0000,0 0,0000,0 0,0000,0 0,0000,0 0,0000,0 0,000,0000
Variables: Method: Components: [P1] = .298 [X1] .993000E-01 .200800E+00 .291800E+00 .375000E+00 .447400E+00 .512200E+00 .539200E+00 .570100E+00 .653700E+00 .693800E+00	Pure component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressed 1. $C5H_{10}O_2$, Ma 2. $C_{10}H_{22}O$, De 3150E+03 [Y1] .630200E+03 .114670E+04 .154660E+04 .196040E+04 .204520E+04 .206670E+04 .206930E+04 .205930E+04 .200790E+04 .192500E+04	1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl butanoate	of component 1 nthalpy	[Y1] .240E+04 \circ [P1] = .298	0.00000.0 0.00000.0 0.00000.0 0.00000.0 0.000000
Variables: Method: Components: [P1] = .298 [X1] .993000E-01 .200800E+00 .291800E+00 .375000E+00 .447400E+00 .512200E+00 .539200E+00 .570100E+00 .653700E+00 .693800E+00 .739500E+00	Pure component Pure component Pure component [P1] T/K , [X1] $x_{1}/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. $C5H_{10}O_2$, Ma 2. $C_{10}H_{22}O$, De 3150E+03 .114670E+04 .154660E+04 .154660E+04 .196040E+04 .204520E+04 .206670E+04 .205930E+04 .205930E+04 .200790E+04 .179510E+04	1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl butanoate	of component 1 nthalpy	$[Y1] \\ .240E+04 \\ .180E+04 \\ .180E+04 \\ .0 [P1] = .2983 \\ .0 \\ .0 \\ .0 \\ .0 \\ .0 \\ .0 \\ .0 \\ .$	oo ⁰⁰⁰ 0.0. 0
Variables: Method: Components: [P1] = .298 [X1] .993000E-01 .200800E+00 .291800E+00 .375000E+00 .447400E+00 .512200E+00 .539200E+00 .570100E+00 .653700E+00 .693800E+00 .739500E+00 .786600E+00	Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C5H ₁₀ O ₂ , Ma 2. C ₁₀ H ₂₂ O, De 3150E+03 [Y1] .630200E+03 .114670E+04 .154660E+04 .196040E+04 .204520E+04 .206670E+04 .205930E+04 .205930E+04 .205930E+04 .192500E+04 .192500E+04 .192500E+04 .192500E+04 .192500E+04 .192500E+04	1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl butanoate	of component 1 nthalpy	$[Y1] \\ .240E+04 \\ .180E+04 \\ .180E+04 \\ .0 [P1] = .2983 \\ .0 \\ .0 \\ .0 \\ .0 \\ .0 \\ .0 \\ .0 \\ .$	00000.0. 0. 0. 0. 0.
Variables: Method: Components: [P1] = .298 [X1] .993000E-01 .200800E+00 .291800E+00 .375000E+00 .447400E+00 .539200E+00 .539200E+00 .53700E+00 .653700E+00 .693800E+00 .739500E+00 .739500E+00 .833600E+00	Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C5H ₁₀ O ₂ , Ma 2. C ₁₀ H ₂₂ O, De 3150E+03 [Y1] .630200E+03 .114670E+04 .154660E+04 .196040E+04 .204520E+04 .206670E+04 .205930E+04 .205930E+04 .200790E+04 .192500E+04 .192500E+04 .139520E+04 .139520E+04	1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl butanoate	of component 1 nthalpy	$[Y1] \\ .240E+04 \\ .180E+04 \\ .180E+04 \\ .0 [P1] = .2983 \\ .0 \\ .0 \\ .0 \\ .0 \\ .0 \\ .0 \\ .0 \\ .$	0,00000,0 0,0000,0 0,0000,0 0,0000,0 0,0000,0 0,0000,0 0,0000,0 0,0000,0 0,0000,0 0,0000,0 0,0000,0 0,0000,0 0,000,0000
Variables: Method: Components: [P1] = .298 [X1] .993000E-01 .200800E+00 .291800E+00 .375000E+00 .447400E+00 .512200E+00 .539200E+00 .570100E+00 .653700E+00 .693800E+00 .739500E+00 .786600E+00	Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C5H ₁₀ O ₂ , Ma 2. C ₁₀ H ₂₂ O, De 3150E+03 [Y1] .630200E+03 .114670E+04 .154660E+04 .196040E+04 .206670E+04 .206670E+04 .20690E+04 .205930E+04 .205930E+04 .192500E+04 .192500E+04 .139520E+04 .11930E+04	1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl butanoate	of component 1 nthalpy	$[Y1] \\ .240E+04 \\ .180E+04 \\ .120E+04 \\ .1$	o. 0000.0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
Variables: Method: Components: [P1] = .298 [X1] .993000E-01 .200800E+00 .291800E+00 .375000E+00 .447400E+00 .512200E+00 .539200E+00 .570100E+00 .693800E+00 .739500E+00 .739500E+00 .833600E+00 .83800E+00 .878900E+00	Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C5H ₁₀ O ₂ , Ma 2. C ₁₀ H ₂₂ O, De 3150E+03 [Y1] .630200E+03 .114670E+04 .154660E+04 .196040E+04 .204520E+04 .206670E+04 .205930E+04 .205930E+04 .200790E+04 .192500E+04 .192500E+04 .139520E+04	1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl butanoate	of component 1 nthalpy	$[Y1] \\ .240E+04 \\ .180E+04 \\ .180E+04 \\ .0 [P1] = .2983 \\ .0 \\ .0 \\ .0 \\ .0 \\ .0 \\ .0 \\ .0 \\ .$	0.0000.0 0 0
Variables: Method: Components: [P1] = .298 [X1] .993000E-01 .200800E+00 .291800E+00 .375000E+00 .447400E+00 .512200E+00 .539200E+00 .653700E+00 .693800E+00 .739500E+00 .739500E+00 .833600E+00 .83800E+00 .83800E+00 .83800E+00 .878900E+00 .923500E+00	Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C5H ₁₀ O ₂ , Ma 2. C ₁₀ H ₂₂ O, De 3150E+03 [Y1] .630200E+03 .114670E+04 .154660E+04 .196040E+04 .204520E+04 .206670E+04 .205930E+04 .205930E+04 .205930E+04 .192500E+04 .192500E+04 .1930E+04 .1930E+04 .1930E+04 .781900E+03	1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl butanoate	of component 1 nthalpy	$[Y1] \\ .240E+04 \\ .180E+04 \\ .120E+04 \\ .1$	0 0 0
Variables: Method: Components: [P1] = .298 [X1] .993000E-01 .200800E+00 .291800E+00 .375000E+00 .447400E+00 .512200E+00 .539200E+00 .653700E+00 .693800E+00 .739500E+00 .739500E+00 .833600E+00 .83800E+00 .83800E+00 .83800E+00 .878900E+00 .923500E+00	Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C5H ₁₀ O ₂ , Ma 2. C ₁₀ H ₂₂ O, De 3150E+03 [Y1] .630200E+03 .114670E+04 .154660E+04 .196040E+04 .204520E+04 .206670E+04 .205930E+04 .205930E+04 .205930E+04 .192500E+04 .192500E+04 .1930E+04 .1930E+04 .1930E+04 .781900E+03	1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl butanoate	of component 1 nthalpy	$[Y1] \\ .240E+04 \\ .180E+04 \\ .120E+04 \\ .1$	0,00 ^{0,0} ,0,0 0,0 0,0 0,0 0,0 0,0 0,0 0,0 0,0
Variables: Method: Components: [P1] = .298 [X1] .993000E-01 .200800E+00 .291800E+00 .375000E+00 .447400E+00 .512200E+00 .539200E+00 .653700E+00 .693800E+00 .739500E+00 .739500E+00 .833600E+00 .83800E+00 .83800E+00 .83800E+00 .878900E+00 .923500E+00	Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C5H ₁₀ O ₂ , Ma 2. C ₁₀ H ₂₂ O, De 3150E+03 [Y1] .630200E+03 .114670E+04 .154660E+04 .196040E+04 .204520E+04 .206670E+04 .205930E+04 .205930E+04 .205930E+04 .192500E+04 .192500E+04 .1930E+04 .1930E+04 .1930E+04 .781900E+03	1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl butanoate	of component 1 nthalpy	$[Y1] \\ .240E+04 \\ .180E+04 \\ .120E+04 \\ .1$	0,0000,0 0,000000
Variables: Method: Components: [P1] = .298 [X1] .993000E-01 .200800E+00 .291800E+00 .375000E+00 .447400E+00 .512200E+00 .539200E+00 .653700E+00 .693800E+00 .739500E+00 .739500E+00 .833600E+00 .83800E+00 .83800E+00 .83800E+00 .878900E+00 .923500E+00	Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C5H ₁₀ O ₂ , Ma 2. C ₁₀ H ₂₂ O, De 3150E+03 [Y1] .630200E+03 .114670E+04 .154660E+04 .196040E+04 .204520E+04 .206670E+04 .205930E+04 .205930E+04 .205930E+04 .192500E+04 .192500E+04 .1930E+04 .1930E+04 .1930E+04 .781900E+03	1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl butanoate	of component 1 nthalpy	$[Y1] \\ .240E+04 \\ .180E+04 \\ .120E+04 \\ .1$	
Variables: Method: Components: [P1] = .298 [X1] .993000E-01 .200800E+00 .291800E+00 .375000E+00 .447400E+00 .512200E+00 .539200E+00 .653700E+00 .693800E+00 .739500E+00 .739500E+00 .833600E+00 .83800E+00 .83800E+00 .83800E+00 .878900E+00 .923500E+00	Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C5H ₁₀ O ₂ , Ma 2. C ₁₀ H ₂₂ O, De 3150E+03 [Y1] .630200E+03 .114670E+04 .154660E+04 .196040E+04 .204520E+04 .206670E+04 .205930E+04 .205930E+04 .205930E+04 .192500E+04 .192500E+04 .1930E+04 .1930E+04 .1930E+04 .781900E+03	1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl butanoate	of component 1 nthalpy	$\begin{array}{c} \text{[Y1]} \\ .240\text{E+04} \\ .180\text{E+04} \\ .120\text{E+04} \\ .600\text{E+03} \\ \end{array}$	
Variables: Method: Components: [P1] = .298 [X1] .993000E-01 .200800E+00 .291800E+00 .375000E+00 .375000E+00 .539200E+00 .539200E+00 .653700E+00 .633600E+00 .836600E+00 .83660E+00 .878900E+00 .923500E+00	Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C5H ₁₀ O ₂ , Ma 2. C ₁₀ H ₂₂ O, De 3150E+03 [Y1] .630200E+03 .114670E+04 .154660E+04 .196040E+04 .204520E+04 .206670E+04 .205930E+04 .205930E+04 .205930E+04 .192500E+04 .192500E+04 .1930E+04 .1930E+04 .1930E+04 .781900E+03	1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl butanoate	of component 1 nthalpy	$\begin{array}{c} \text{[Y1]} \\ .240\text{E+04} \\ .180\text{E+04} \\ .120\text{E+04} \\ .600\text{E+03} \\ \end{array}$	
Variables: Method: Components: [P1] = .298 [X1] .993000E-01 .200800E+00 .291800E+00 .375000E+00 .375000E+00 .539200E+00 .539200E+00 .653700E+00 .633600E+00 .836600E+00 .83660E+00 .878900E+00 .923500E+00	Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C5H ₁₀ O ₂ , Ma 2. C ₁₀ H ₂₂ O, De 3150E+03 [Y1] .630200E+03 .114670E+04 .154660E+04 .196040E+04 .204520E+04 .206670E+04 .205930E+04 .205930E+04 .205930E+04 .192500E+04 .192500E+04 .1930E+04 .1930E+04 .1930E+04 .781900E+03	1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl butanoate	of component 1 nthalpy	$\begin{array}{c} \text{[Y1]} \\ .240\text{E+04} \\ .180\text{E+04} \\ .120\text{E+04} \\ .600\text{E+03} \\ \end{array}$	

		ce. All rights reserve			
Property Code:	[HMSD1000] HE.	AT OF MIXING	AND SOLUTION	1	ORTJ0954.023
			e liquid or two-ph	ase liquid-liquid (LL)	
	Pure component 1				
	Pure component 2 [P1] T/K,	Temperature			
Variables:	$[X1] x_1/-,$	Mole fraction of	component 1		
		Molar excess ent			
Method:	Direct low-pressu	re calorimetric me	asurement of $H^{\rm E}$	at variable x_1 and constant T	
	1. C ₆ H ₁₂ O ₂ , Me				
components.	2. C ₆ H ₁₄ O, Hex	an-1-ol			
[P1] = .298				[V1]	
[X1]	[Y1]			[Y1] .200E+04	
		<i>v</i>			
.484000E-01 .106500E+00	.297800E+03 .592100E+03			○ [P1] = .298150E+0	03
.167800E+00	.881200E+03				-O
.231800E+00	.113670E+04			,	· · O.,
.293300E+00	.134370E+04			.150E+04	٥.
.354100E+00	.150670E+04				
.405000E+00	.160830E+04			o	
.448400E+00	.166810E+04				N N
.485600E+00	.170070E+04			o	Ó.
.512400E+00 .558000E+00	.171120E+04 .171750E+04			.100E+04	\
.615700E+00					No. 1
.679100E+00				, o	ò.
.745600E+00					O
.814400E+00	.115890E+04				
.881800E+00	.824700E+03		4	.500E+03	- 0
.946500E+00	.433900E+03				<u> </u>
				o'	
		-			
1					
	1			.000E+00	
				.50E+	
					[X1]
L					
Copyright© 1995 I	CI DATA CADI E				
					ODT10054.025
Property Code:	[HMSD1000] HI	EAT OF MIXING	AND SOLUTIO	N	ORTJ0954.025
	[HMSD1000] HI Two-component	EAT OF MIXING system, single-pha	AND SOLUTIO	N nase liquid-liquid (LL)	ORTJ0954.025
Property Code:	[HMSD1000] HI Two-component Pure component	EAT OF MIXING system, single-pha 1, liquid	AND SOLUTIO	N 1ase liquid-liquid (LL)	ORTJ0954.025
Property Code:	[HMSD1000] HI Two-component Pure component Pure component	EAT OF MIXING system, single-pha 1, liquid	AND SOLUTIO	N nase liquid-liquid (LL)	ORTJ0954.025
Property Code: State:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-,	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o	AND SOLUTIO se liquid or two-p	N nase liquid-liquid (LL)	ORTJ0954.025
Property Code: State: Parameters:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] HE/Jmol ⁻¹ ,	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess er	AND SOLUTIO se liquid or two-p of component 1 nthalpy	nase liquid-liquid (LL)	ORTJ0954.025
Property Code: State: Parameters:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess er ure calorimetric m	AND SOLUTIO se liquid or two-p of component 1 nthalpy	N hase liquid-liquid (LL) \hat{r} at variable x_1 and constant T	ORTJ0954.025
Property Code: State: Parameters: Variables:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₂ O ₂ , M	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess er ure calorimetric m ethyl pentanoate	AND SOLUTIO se liquid or two-p of component 1 nthalpy	nase liquid-liquid (LL)	ORTJ0954.025
Property Code: State: Parameters: Variables: Method: Components:	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₂ O ₂ , M 2. C ₈ H ₁₈ O, Oct	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess er ure calorimetric m ethyl pentanoate	AND SOLUTIO se liquid or two-p of component 1 nthalpy	the mass and the mass of the	ORTJ0954.025
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₂ O ₂ , M 2. C ₈ H ₁₈ O, Oct 8150E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess er ure calorimetric m ethyl pentanoate	AND SOLUTIO se liquid or two-p of component 1 nthalpy	the provided here the set of the	ORTJ0954.025
Property Code: State: Parameters: Variables: Method: Components:	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₂ O ₂ , M 2. C ₈ H ₁₈ O, Oct 8150E+03 [Y1]	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess er ure calorimetric m ethyl pentanoate	AND SOLUTIO se liquid or two-p of component 1 nthalpy	the mass and the mass of the	ORTJ0954.025
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .482000E-01	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₂ O ₂ , M 2. C ₈ H ₁₈ O, Oct 8150E+03 [Y1] .303900E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess er ure calorimetric m ethyl pentanoate	AND SOLUTIO se liquid or two-p of component 1 nthalpy	ase liquid-liquid (LL) at variable x ₁ and constant T [Y1] .200E+04	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .482000E-01 .103200E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₂ O ₂ , M 2. C ₈ H ₁₈ O, Oct 8150E+03 [Y1] .303900E+03 .592900E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess er ure calorimetric m ethyl pentanoate	AND SOLUTIO se liquid or two-p of component 1 nthalpy	ase liquid-liquid (LL) at variable x ₁ and constant T [Y1] .200E+04	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .482000E-01 .103200E+00 .159900E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₂ O ₂ , M 2. C ₈ H ₁₈ O, Oct 8150E+03 [Y1] .303900E+03 .592900E+03 .874300E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess er ure calorimetric m ethyl pentanoate	AND SOLUTIO se liquid or two-p of component 1 nthalpy	ase liquid-liquid (LL) at variable x ₁ and constant T [Y1] .200E+04	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .482000E-01 .103200E+00 .159900E+00 .215400E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₂ O ₂ , M 2. C ₈ H ₁₈ O, Oct 8150E+03 [Y1] .303900E+03 .592900E+03 .592900E+03 .874300E+03 .111090E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess er ure calorimetric m ethyl pentanoate	AND SOLUTIO se liquid or two-p of component 1 nthalpy	ase liquid-liquid (LL) at variable x ₁ and constant T [Y1] .200E+04	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .482000E-01 .103200E+00 .159900E+00 .215400E+00 .270200E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₂ O ₂ , M 2. C ₈ H ₁₈ O, Oct 8150E+03 [Y1] .303900E+03 .592900E+03 .592900E+03 .592900E+03 .11090E+04 .130940E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess er ure calorimetric m ethyl pentanoate	AND SOLUTIO se liquid or two-p of component 1 nthalpy	ase liquid-liquid (LL) at variable x ₁ and constant T [Y1] .200E+04	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .482000E-01 .103200E+00 .215400E+00 .215400E+00 .270200E+00 .323500E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C6H ₁₂ O ₂ , M 2. C ₈ H ₁₈ O, Oct 8150E+03 [Y1] .303900E+03 .592900E+03 .874300E+04 .130940E+04 .130940E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess er ure calorimetric m ethyl pentanoate	AND SOLUTIO se liquid or two-p of component 1 nthalpy	ase liquid-liquid (LL) at variable x ₁ and constant T [Y1] .200E+04	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .482000E-01 .103200E+00 .215400E+00 .270200E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₂ O ₂ , M 2. C ₈ H ₁₈ O, Oct 8150E+03 [Y1] .303900E+03 .592900E+03 .592900E+03 .874300E+03 .11090E+04 .130940E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess er ure calorimetric m ethyl pentanoate	AND SOLUTIO se liquid or two-p of component 1 nthalpy	ase liquid-liquid (LL) at variable x ₁ and constant T [Y1] .200E+04	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .482000E-01 .103200E+00 .215400E+00 .215400E+00 .323500E+00 .376000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> 1/-, [Y1] <i>HE/J</i> mol ⁻¹ , Direct low-press 1. C6H12O2, M 2. C8H18O, Oct 8150E+03 [Y1] .303900E+03 .592900E+03 .592900E+03 .874300E+03 .111090E+04 .130940E+04 .159530E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess er ure calorimetric m ethyl pentanoate	AND SOLUTIO se liquid or two-p of component 1 nthalpy	ase liquid-liquid (LL) at variable x ₁ and constant T [Y1] .200E+04	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .482000E-01 .103200E+00 .215400E+00 .215400E+00 .376000E+00 .376000E+00 .424300E+00 .468800E+00 .510300E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₂ O ₂ , M 2. C ₈ H ₁₈ O, Oct 8150E+03 [Y1] .303900E+03 .592900E+03 .592900E+03 .874300E+03 .111090E+04 .130940E+04 .159530E+04 .173640E+04 .173640E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess er ure calorimetric m ethyl pentanoate	AND SOLUTIO se liquid or two-p of component 1 nthalpy	[Y1] $.200E+04$ $.150E+04$ $0 [P1] = .298150E+$ $0 (P1) = .298150E+$	03 •°°°°°°°°°°°°°°°°°°°°°°°°°°°°°°°°°°°°
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .482000E-01 .103200E+00 .215400E+00 .215400E+00 .270200E+00 .323500E+00 .468800E+00 .510300E+00 .550200E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C6H12O2, M 2. C8H18O, Oct 8150E+03 [Y1] .303900E+03 .592900E+03 .592900E+03 .592900E+03 .11090E+04 .130940E+04 .130940E+04 .159530E+04 .173640E+04 .175770E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess er ure calorimetric m ethyl pentanoate	AND SOLUTIO se liquid or two-p of component 1 nthalpy	ase liquid-liquid (LL) at variable x ₁ and constant T [Y1] .200E+04	03 •°°°°°°°°°°°°°°°°°°°°°°°°°°°°°°°°°°°°
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .482000E-01 .103200E+00 .215400E+00 .215400E+00 .376000E+00 .376000E+00 .424300E+00 .510300E+00 .550200E+00 .579300E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₂ O ₂ , M 2. C ₈ H ₁₈ O, Oct 8150E+03 [Y1] .303900E+03 .592900E+03 .592900E+03 .592900E+03 .592900E+03 .11090E+04 .130940E+04 .130940E+04 .130940E+04 .159530E+04 .173640E+04 .173580E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess er ure calorimetric m ethyl pentanoate	AND SOLUTIO se liquid or two-p of component 1 nthalpy	[Y1] $.200E+04$ $.150E+04$ $0 [P1] = .298150E+$ $0 (P1) = .298150E+$	03 •°°°°°°°°°°°°°°°°°°°°°°°°°°°°°°°°°°°°
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .482000E-01 .103200E+00 .159900E+00 .215400E+00 .270200E+00 .376000E+00 .424300E+00 .510300E+00 .579300E+00 .579300E+00 .621700E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C6H ₁₂ O ₂ , M 2. C ₈ H ₁₈ O, Oct 8150E+03 [Y1] .303900E+03 .592900E+03 .592900E+03 .592900E+03 .874300E+04 .130940E+04 .130940E+04 .130940E+04 .173640E+04 .173580E+04 .173580E+04 .170680E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess er ure calorimetric m ethyl pentanoate	AND SOLUTIO se liquid or two-p of component 1 nthalpy	[Y1] $.200E+04$ $.150E+04$ $0 [P1] = .298150E+$ $0 (P1) = .298150E+$	03 •°°°°°°°°°
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .482000E-01 .103200E+00 .215400E+00 .215400E+00 .270200E+00 .376000E+00 .468800E+00 .510300E+00 .550200E+00 .621700E+00 .663000E+00	[HMSD1000] HI Two-component Pure component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> 1/-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C6H12O ₂ , M 2. C8H18O, Oct 8150E+03 [Y1] .303900E+03 .592900E+03 .592900E+03 .592900E+03 .11090E+04 .130940E+04 .130940E+04 .130940E+04 .17650E+04 .176580E+04 .170680E+04 .170680E+04 .170680E+04 .170680E+04 .170680E+04 .170680E+04 .170680E+04 .170680E+04 .170680E+04 .165870E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess er ure calorimetric m ethyl pentanoate	AND SOLUTIO se liquid or two-p of component 1 nthalpy	[Y1] $.200E+04$ $.150E+04$ $0 [P1] = .298150E+$ $0 (P1) = .298150E+$	03 •°°°°°°°°°
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .482000E-01 .103200E+00 .159900E+00 .215400E+00 .376000E+00 .376000E+00 .510300E+00 .579300E+00 .579300E+00 .579300E+00 .663000E+00 .706400E+00	[HMSD1000] HI Two-component Pure component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₂ O ₂ , M 2. C ₈ H ₁₈ O, Oct 8150E+03 [Y1] .303900E+03 .592900E+03 .592900E+03 .874300E+04 .130940E+04 .130940E+04 .159530E+04 .168150E+04 .173640E+04 .173580E+04 .173580E+04 .165870E+04 .155770E+04 .157720E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess er ure calorimetric m ethyl pentanoate	AND SOLUTIO se liquid or two-p of component 1 nthalpy	hase liquid-liquid (LL) x_1 and constant T [Y1] .200E+04 .150E+04 .150E+04 .100E+04 .100E+04	03 •°°°°°°°°°
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .482000E-01 .103200E+00 .215400E+00 .215400E+00 .270200E+00 .376000E+00 .468800E+00 .510300E+00 .550200E+00 .621700E+00 .663000E+00	[HMSD1000] HI Two-component Pure component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₂ O ₂ , M 2. C ₈ H ₁₈ O, Oct 8150E+03 [Y1] .303900E+03 .592900E+03 .592900E+03 .874300E+04 .130940E+04 .130940E+04 .159530E+04 .168150E+04 .173640E+04 .173680E+04 .173580E+04 .165870E+04 .155770E+04 .157720E+04 .157720E+04 .148470E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess er ure calorimetric m ethyl pentanoate	AND SOLUTIO se liquid or two-p of component 1 nthalpy	[Y1] $.200E+04$ $.150E+04$ $0 [P1] = .298150E+$ $0 (P1) = .298150E+$	
Property Code: State: Variables: Variables: Method: Components: [P1] = .29 [X1] .482000E-01 .103200E+00 .215400E+00 .215400E+00 .376000E+00 .323500E+00 .376000E+00 .510300E+00 .550200E+00 .579300E+00 .663000E+00 .706400E+00 .744700E+00 .790000E+00 .834300E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C6H12O2, M 2. C8H18O, Oct 8150E+03 [Y1] .303900E+03 .592900E+03 .592900E+03 .592900E+03 .592900E+03 .592900E+03 .592900E+03 .592900E+03 .592900E+03 .592900E+04 .130940E+04 .130940E+04 .175770E+04 .175770E+04 .175780E+04 .175780E+04 .157720E+04 .133900E+04 .133900E+04 .15350E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess er ure calorimetric m ethyl pentanoate	AND SOLUTIO se liquid or two-p of component 1 nthalpy	asse liquid-liquid (LL) at variable x_1 and constant T [Y1] .200E+04 \circ [P1] = .298150E+ .150E+04 .150E+04 .100E+04 .00E+03	03 .°°°`°.o. .o. .o.
Property Code: State: Variables: Method: Components: [P1] = .29 [X1] .482000E+00 .103200E+00 .215400E+00 .215400E+00 .215400E+00 .376000E+00 .376000E+00 .510300E+00 .579300E+00 .579300E+00 .579300E+00 .706400E+00 .706400E+00 .744700E+00 .834300E+00 .834300E+00 .884700E+00	[HMSD1000] HI Two-component Pure component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C6H12O2, M 2. C8H18O, Oct 8150E+03 [Y1] .303900E+03 .592900E+03 .592900E+03 .592900E+03 .874300E+03 .11090E+04 .130940E+04 .130940E+04 .159530E+04 .173580E+04 .173580E+04 .173580E+04 .15350E+04 .15550E+04 .15550E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess er ure calorimetric m ethyl pentanoate	AND SOLUTIO se liquid or two-p of component 1 nthalpy	hase liquid-liquid (LL) x_1 and constant T [Y1] .200E+04 .150E+04 .150E+04 .100E+04 .100E+04	03 •°°°°°°°°°°°°°°°°°°°°°°°°°°°°°°°°°°°°
Property Code: State: Variables: Method: Components: [P1] = .29 [X1] .482000E-01 .103200E+00 .215400E+00 .215400E+00 .270200E+00 .376000E+00 .376000E+00 .550200E+00 .550200E+00 .550200E+00 .579300E+00 .706400E+00 .744700E+00 .884700E+00 .884700E+00 .927400E+00	[HMSD1000] HI Two-component Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C6H ₁₂ O ₂ , M 2. C ₈ H ₁₈ O, Oct 8150E+03 [Y1] .303900E+03 .592900E+03 .592900E+03 .874300E+03 .11090E+04 .130940E+04 .130940E+04 .159530E+04 .176680E+04 .176680E+04 .176680E+04 .157720E+04 .15350E+04.15350E+04 .15350E+04 .15350E+04.15350E+04 .15350E+04.15350E+04 .15350E+04.15350E+04 .15500E+050E+050E+050E+050E+050E	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess er ure calorimetric m ethyl pentanoate	AND SOLUTIO se liquid or two-p of component 1 nthalpy	asse liquid-liquid (LL) at variable x_1 and constant T [Y1] .200E+04 \circ [P1] = .298150E+ .150E+04 .150E+04 .100E+04 .00E+03	03 .°°°`°.°. .°°
Property Code: State: Variables: Method: Components: [P1] = .29 [X1] .482000E+00 .103200E+00 .215400E+00 .215400E+00 .215400E+00 .376000E+00 .376000E+00 .510300E+00 .579300E+00 .579300E+00 .579300E+00 .706400E+00 .706400E+00 .744700E+00 .834300E+00 .834300E+00 .884700E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C6H12O2, M 2. C8H18O, Oct 8150E+03 [Y1] .303900E+03 .592900E+03 .592900E+03 .874300E+03 .11090E+04 .130940E+04 .130940E+04 .159530E+04 .17660E+04 .176680E+04 .176680E+04 .170680E+04 .15770E+04 .15350E+04 .15350E+04 .15350E+04 .15350E+04 .15350E+04 .15350E+04 .15350E+04 .15350E+04 .15350E+04 .15350E+04 .15350E+04 .15350E+04 .15350E+04 .15350E+04 .15350E+04 .15350E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess er ure calorimetric m ethyl pentanoate	AND SOLUTIO se liquid or two-p of component 1 nthalpy	inase liquid-liquid (LL) inase li	03 .°°°`°.°. .°°
Property Code: State: Variables: Method: Components: [P1] = .29 [X1] .482000E-01 .103200E+00 .215400E+00 .215400E+00 .270200E+00 .376000E+00 .376000E+00 .550200E+00 .550200E+00 .550200E+00 .579300E+00 .706400E+00 .744700E+00 .884700E+00 .884700E+00 .927400E+00	[HMSD1000] HI Two-component Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C6H ₁₂ O ₂ , M 2. C ₈ H ₁₈ O, Oct 8150E+03 [Y1] .303900E+03 .592900E+03 .592900E+03 .874300E+03 .11090E+04 .130940E+04 .130940E+04 .159530E+04 .176680E+04 .176680E+04 .176680E+04 .157720E+04 .15350E+04.15350E+04 .15350E+04 .15350E+04.15350E+04 .15350E+04.15350E+04 .15350E+04.15350E+04 .15500E+050E+050E+050E+050E+050E	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess er ure calorimetric m ethyl pentanoate	AND SOLUTIO se liquid or two-p of component 1 nthalpy	asse liquid-liquid (LL) at variable x_1 and constant T [Y1] .200E+04 \circ [P1] = .298150E+ .150E+04 .150E+04 .100E+04 .00E+03	
Property Code: State: Variables: Method: Components: [P1] = .29 [X1] .482000E-01 .103200E+00 .215400E+00 .215400E+00 .270200E+00 .376000E+00 .376000E+00 .550200E+00 .550200E+00 .550200E+00 .579300E+00 .706400E+00 .744700E+00 .884700E+00 .884700E+00 .927400E+00	[HMSD1000] HI Two-component Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C6H ₁₂ O ₂ , M 2. C ₈ H ₁₈ O, Oct 8150E+03 [Y1] .303900E+03 .592900E+03 .592900E+03 .874300E+03 .11090E+04 .130940E+04 .130940E+04 .159530E+04 .176680E+04 .176680E+04 .176680E+04 .157720E+04 .15350E+04.15350E+04 .15350E+04 .15350E+04.15350E+04 .15350E+04.15350E+04 .15350E+04.15350E+04 .15500E+050E+050E+050E+050E+050E	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess er ure calorimetric m ethyl pentanoate	AND SOLUTIO se liquid or two-p of component 1 nthalpy	inase liquid-liquid (LL) inase li	
Property Code: State: Variables: Method: Components: [P1] = .29 [X1] .482000E-01 .103200E+00 .215400E+00 .215400E+00 .270200E+00 .376000E+00 .376000E+00 .550200E+00 .550200E+00 .550200E+00 .579300E+00 .706400E+00 .744700E+00 .884700E+00 .884700E+00 .927400E+00	[HMSD1000] HI Two-component Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C6H ₁₂ O ₂ , M 2. C ₈ H ₁₈ O, Oct 8150E+03 [Y1] .303900E+03 .592900E+03 .592900E+03 .592900E+03 .874300E+03 .11090E+04 .130940E+04 .130940E+04 .159530E+04 .176680E+04 .176680E+04 .173580E+04 .173580E+04 .15350E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess er ure calorimetric m ethyl pentanoate	AND SOLUTIO se liquid or two-p of component 1 nthalpy	inase liquid-liquid (LL) inase li	

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State:	Two-component s	system, single-pha	se liquid or two-ph	ase liquid-liquid	(LL)	OK130/34.02/
	Pure component		be inquite of the pr	inse inquite inquite		
	Pure component					
Parameters:	[P1] <i>T/</i> K,	Temperature				
Variables:	$[X1] x_{1/-},$	Mole fraction of	of component 1			
	[Y1] $H^{E}/Jmol^{-1}$,	Molar excess en	nthalpy	- A	d sources T	
Method:	and the second		easurement of $H^{\rm E}$	at variable x_1 and	d constant I	
Components:	1. C ₆ H ₁₂ O ₂ , Me 2. C ₁₀ H ₂₂ O, De	can-1-ol			1-1 1-1	
[P1] = .298	3150E+03			[Y1]		
[X1]	[Y1]			.200E+04		
.863000E-01	.513900E+03					
.170100E+00	.903900E+03				o o	
.255800E+00	.126240E+04				a	
.333200E+00	.151700E+04				Č a	
.405100E+00	.168870E+04			.150E+04	¢	-
.468300E+00	.178740E+04					
.529500E+00 .570000E+00	.182060E+04				0	
.613300E+00	.181670E+04 .179090E+04			1	0	
.659400E+00	.179090E+04					
.707900E+00	.161640E+04		f = -g	.100E+04		0
.758500E+00	.147770E+04				ø	
.809400E+00	.128790E+04				1	
.860900E+00	.103890E+04					0
.910300E+00 .957300E+00	.732900E+03					
.95/300E+00	.390800E+03		$b_{i} = \left(\frac{1}{2} \frac$.500E+03	¢.	-
				1	1	0
					○ [P1] = .298150E+03	
				0005.00		
			- 「「「「」」「「「」」「「」」	.000E+00	.50E+00	
1	3				.302+00	[X1]
	1					1211
		EAT OF MIXING	AND SOLUTION		1	ORTJ0954.032
Property Code:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-,	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction of	3 AND SOLUTIO ase liquid or two-ph of component 1		1	
Property Code: State: Parameters:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ ,	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e	3 AND SOLUTIO ase liquid or two-ph of component 1 nthalpy	ase liquid-liquid		
Property Code: State: Parameters: Variables: Method:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m	3 AND SOLUTIO ase liquid or two-ph of component 1	ase liquid-liquid		
Property Code: State: Parameters: Variables: Method: Components:	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hex 2. C ₈ H ₁₆ O ₂ , Ma	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid		
Property Code: State: Parameters: Variables: Method: Components:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hex 2. C ₈ H ₁₆ O ₂ , Ma 8150E+03	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid		
Property Code: State: Parameters: Variables: Method: Components:	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hex 2. C ₈ H ₁₆ O ₂ , Ma	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid at variable x_1 and	(LL)	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hez 2. C ₈ H ₁₆ O ₂ , Mo 8150E+03 [Y1] .512000E+03	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	tase liquid-liquid at variable x_1 and [Y1]	(LL)	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .654000E-01 .141400E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hez 2. C ₈ H ₁₆ O ₂ , Mo 8150E+03 [Y1] .512000E+03 .923100E+03	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	tase liquid-liquid at variable x_1 and [Y1]	(LL)	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .654000E-01 .141400E+00 .219900E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-presse 1. C ₆ H ₁₄ O, Hez 2. C ₈ H ₁₆ O ₂ , Me 8150E+03 [Y1] .512000E+03 .923100E+03 .125620E+04	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	tase liquid-liquid at variable x_1 and [Y1]	(LL)	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .654000E-01 .141400E+00 .219900E+00 .295900E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-presse 1. C ₆ H ₁₄ O, Hez 2. C ₈ H ₁₆ O ₂ , Me 8150E+03 [Y1] .512000E+03 .923100E+03 .125620E+04 .147650E+04	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	at variable x ₁ and [Y1] .180E+04	(LL)	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .654000E-01 .141400E+00 .219900E+00 .295900E+00 .367500E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-presse 1. C ₆ H ₁₄ O, Hez 2. C ₈ H ₁₆ O ₂ , Me 8150E+03 [Y1] .512000E+03 .923100E+03 .923100E+03 .125620E+04 .147650E+04 .160510E+04	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	tase liquid-liquid at variable x_1 and [Y1]	(LL)	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .654000E-01 .141400E+00 .219900E+00 .295900E+00 .367500E+00 .418400E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-presse 1. C ₆ H ₁₄ O, Hes 2. C ₈ H ₁₆ O ₂ , Me 8150E+03 [Y1] .512000E+03 .923100E+03 .923100E+03 .125620E+04 .147650E+04 .160510E+04 .164350E+04	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	at variable x ₁ and [Y1] .180E+04		
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .654000E-01 .141400E+00 .219900E+00 .295900E+00 .367500E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C₆H₁₄O , Hex 2. C₈H₁₆O₂ , Mex 8150E+03 [Y1] .512000E+03 .923100E+03 .125620E+04 .147650E+04 .164350E+04 .165400E+04	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	at variable x ₁ and [Y1] .180E+04	(LL)	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .654000E-01 .141400E+00 .219900E+00 .295900E+00 .367500E+00 .418400E+00 .461900E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-presse 1. C ₆ H ₁₄ O, Hes 2. C ₈ H ₁₆ O ₂ , Me 8150E+03 [Y1] .512000E+03 .923100E+03 .923100E+03 .125620E+04 .147650E+04 .160510E+04 .164350E+04	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	at variable x ₁ and [Y1] .180E+04	(LL)	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .654000E-01 .141400E+00 .215900E+00 .367500E+00 .418400E+00 .459600E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hea 2. C ₈ H ₁₆ O ₂ , Me 8150E+03 [Y1] .512000E+03 .923100E+03 .125620E+04 .147650E+04 .164350E+04 .165400E+04 .164260E+04	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	at variable x1 and [Y1] .180E+04 .135E+04	(LL)	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .294 [X1] .654000E-01 .141400E+00 .219900E+00 .367500E+00 .418400E+00 .461900E+00 .544200E+00 .589600E+00 .624200E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hea 2. C ₈ H ₁₆ O ₂ , Ma 8150E+03 [Y1] .512000E+03 .923100E+03 .125620E+04 .160510E+04 .164350E+04 .164260E+04 .164260E+04 .151600E+04 .151600E+04 .144830E+04	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	at variable x ₁ and [Y1] .180E+04	(LL)	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .654000E-01 .141400E+00 .295900E+00 .367500E+00 .367500E+00 .418400E+00 .461900E+00 .544200E+00 .589600E+00 .624200E+00 .668800E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hex 2. C ₈ H ₁₆ O ₂ , Ma 8150E+03 [Y1] .512000E+03 .923100E+03 .125620E+04 .16550E+04 .16550E+04 .164350E+04 .164260E+04 .151600E+04 .151600E+04 .13830E+04 .133830E+04	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	at variable x1 and [Y1] .180E+04 .135E+04	(LL)	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .654000E-01 .141400E+00 .219900E+00 .219900E+00 .295900E+00 .418400E+00 .418400E+00 .544200E+00 .589600E+00 .589600E+00 .589600E+00 .628200E+00 .68800E+00 .734500E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-pressi 1. C ₆ H ₁₄ O, Hea 2. C ₈ H ₁₆ O ₂ , Ma 8150E+03 [Y1] .512000E+03 .923100E+03 .923100E+03 .125620E+04 .147650E+04 .165400E+04 .165400E+04 .151600E+04 .151600E+04 .13830E+04 .114640E+04	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	at variable x1 and [Y1] .180E+04 .135E+04	(LL)	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .654000E-01 .141400E+00 .219900E+00 .295900E+00 .367500E+00 .418400E+00 .418400E+00 .544200E+00 .589600E+00 .589600E+00 .589600E+00 .668800E+00 .734500E+00 .805200E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] HE/Jmol-1, Direct low-pressi 1. C6H14O, Hea 2. C8H16O2, Ma 8150E+03 [Y1] .512000E+03 .923100E+03 .923100E+03 .125620E+04 .166510E+04 .166510E+04 .164260E+04 .158480E+04 .15480E+04 .13830E+04 .14640E+04 .886100E+03	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	at variable x1 and [Y1] .180E+04 .135E+04	(LL)	ORTJ0954.032
Property Code: State: Variables: Method: Components: [P1] = .29 [X1] .654000E-01 .141400E+00 .219900E+00 .295900E+00 .367500E+00 .418400E+00 .418400E+00 .544200E+00 .589600E+00 .589600E+00 .624200E+00 .668800E+00 .734500E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-pressi 1. C ₆ H ₁₄ O, Hea 2. C ₈ H ₁₆ O ₂ , Ma 8150E+03 [Y1] .512000E+03 .923100E+03 .923100E+03 .125620E+04 .147650E+04 .165400E+04 .165400E+04 .151600E+04 .151600E+04 .13830E+04 .114640E+04	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	at variable x1 and [Y1] .180E+04 .135E+04 .900E+03	(LL)	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .654000E-01 .141400E+00 .219900E+00 .295900E+00 .367500E+00 .418400E+00 .461900E+00 .499600E+00 .544200E+00 .668800E+00 .734500E+00 .805200E+00 .881000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] HE/Jmol-1, Direct low-pressi 1. C6H14O, Hea 2. C8H16O2, Ma 8150E+03 [Y1] .512000E+03 .923100E+03 .923100E+03 .125620E+04 .166510E+04 .166510E+04 .164350E+04 .164260E+04 .158480E+04 .151600E+04 .13830E+04 .13830E+04 .114640E+04 .886100E+03 .557200E+03	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	at variable x1 and [Y1] .180E+04 .135E+04	(LL)	ORTJ0954.032
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .654000E-01 .141400E+00 .219900E+00 .295900E+00 .367500E+00 .418400E+00 .461900E+00 .544200E+00 .544200E+00 .668800E+00 .734500E+00 .805200E+00 .881000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] HE/Jmol-1, Direct low-pressi 1. C6H14O, Hea 2. C8H16O2, Ma 8150E+03 [Y1] .512000E+03 .923100E+03 .923100E+03 .125620E+04 .166510E+04 .166510E+04 .164350E+04 .164260E+04 .158480E+04 .151600E+04 .13830E+04 .13830E+04 .114640E+04 .886100E+03 .557200E+03	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	at variable x1 and [Y1] .180E+04 .135E+04 .900E+03	(LL)	ORTJ0954.032
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .654000E-01 .141400E+00 .219900E+00 .295900E+00 .367500E+00 .418400E+00 .461900E+00 .544200E+00 .544200E+00 .668800E+00 .734500E+00 .805200E+00 .881000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] HE/Jmol-1, Direct low-pressi 1. C6H14O, Hea 2. C8H16O2, Ma 8150E+03 [Y1] .512000E+03 .923100E+03 .923100E+03 .125620E+04 .166510E+04 .166510E+04 .164350E+04 .164260E+04 .158480E+04 .151600E+04 .13830E+04 .13830E+04 .114640E+04 .886100E+03 .557200E+03	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	at variable x1 and [Y1] .180E+04 .135E+04 .900E+03	(LL)	ORTJ0954.032
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .654000E-01 .141400E+00 .219900E+00 .295900E+00 .367500E+00 .418400E+00 .461900E+00 .499600E+00 .544200E+00 .668800E+00 .734500E+00 .805200E+00 .881000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] HE/Jmol-1, Direct low-pressi 1. C6H14O, Hea 2. C8H16O2, Ma 8150E+03 [Y1] .512000E+03 .923100E+03 .923100E+03 .125620E+04 .166510E+04 .166510E+04 .164350E+04 .164260E+04 .158480E+04 .151600E+04 .13830E+04 .13830E+04 .114640E+04 .886100E+03 .557200E+03	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	at variable x1 and [Y1] .180E+04 .135E+04 .900E+03	(LL)	ORTJ0954.032
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .654000E-01 .141400E+00 .219900E+00 .295900E+00 .367500E+00 .418400E+00 .461900E+00 .499600E+00 .544200E+00 .668800E+00 .734500E+00 .805200E+00 .881000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] HE/Jmol-1, Direct low-pressi 1. C6H14O, Hea 2. C8H16O2, Ma 8150E+03 [Y1] .512000E+03 .923100E+03 .923100E+03 .125620E+04 .166510E+04 .166510E+04 .164350E+04 .164260E+04 .158480E+04 .151600E+04 .13830E+04 .13830E+04 .114640E+04 .886100E+03 .557200E+03	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	at variable x1 and [Y1] .180E+04 .135E+04 .900E+03	(LL)	ORTJ0954.032
Property Code: State: Variables: Method: Components: [P1] = .29 [X1] .654000E-01 .141400E+00 .219900E+00 .295900E+00 .367500E+00 .418400E+00 .461900E+00 .461900E+00 .544200E+00 .544200E+00 .668800E+00 .734500E+00 .805200E+00 .881000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] HE/Jmol-1, Direct low-pressi 1. C6H14O, Hea 2. C8H16O2, Ma 8150E+03 [Y1] .512000E+03 .923100E+03 .923100E+03 .125620E+04 .166510E+04 .166510E+04 .164350E+04 .164260E+04 .158480E+04 .151600E+04 .13830E+04 .13830E+04 .114640E+04 .886100E+03 .557200E+03	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	at variable x1 and [Y1] .180E+04 .135E+04 .900E+03 .450E+03	(LL)	ORTJ0954.032
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .654000E-01 .141400E+00 .219900E+00 .295900E+00 .367500E+00 .418400E+00 .461900E+00 .544200E+00 .544200E+00 .668800E+00 .734500E+00 .805200E+00 .881000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] HE/Jmol-1, Direct low-pressi 1. C6H14O, Hea 2. C8H16O2, Ma 8150E+03 [Y1] .512000E+03 .923100E+03 .923100E+03 .125620E+04 .166510E+04 .166510E+04 .164350E+04 .164260E+04 .158480E+04 .151600E+04 .13830E+04 .13830E+04 .114640E+04 .886100E+03 .557200E+03	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	at variable x1 and [Y1] .180E+04 .135E+04 .900E+03 .450E+03	(LL) d constant T $\circ^{\circ^{\circ^{\circ_{\circ_{\circ_{\circ_{\circ_{\circ_{\circ_{\circ}}}}}}}}} \circ \circ^{\circ_{\circ_{\circ_{\circ_{\circ}}}}} \circ \circ^{\circ_{\circ_{\circ_{\circ_{\circ}}}}} \circ \circ^{\circ_{\circ_{\circ_{\circ}}}} \circ \circ^{\circ_{\circ_{\circ_{\circ}}}} \circ \circ^{\circ_{\circ_{\circ_{\circ}}}} \circ \circ^{\circ_{\circ_{\circ_{\circ}}}} \circ \circ^{\circ_{\circ_{\circ}}} \circ \circ^{\circ_{\circ}} \circ^{\circ_{\circ}} \circ \circ^{\circ_{\circ}} \circ^{\circ_{\circ}} \circ \circ^{\circ_{\circ}} \circ^{\circ_$	ORTJ0954.032
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .654000E-01 .141400E+00 .219900E+00 .295900E+00 .367500E+00 .418400E+00 .589600E+00 .589600E+00 .668800E+00 .624200E+00 .668800E+00 .734500E+00 .805200E+00 .881000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] HE/Jmol-1, Direct low-pressi 1. C6H14O, Hea 2. C8H16O2, Ma 8150E+03 [Y1] .512000E+03 .923100E+03 .923100E+03 .125620E+04 .166510E+04 .166510E+04 .164350E+04 .164260E+04 .158480E+04 .151600E+04 .13830E+04 .13830E+04 .114640E+04 .886100E+03 .557200E+03	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	at variable x1 and [Y1] .180E+04 .135E+04 .900E+03 .450E+03	(LL) d constant T $\circ^{\circ^{\circ^{\circ_{\circ_{\circ_{\circ_{\circ_{\circ_{\circ_{\circ}}}}}}}}} \circ \circ^{\circ_{\circ_{\circ_{\circ_{\circ}}}}} \circ \circ^{\circ_{\circ_{\circ_{\circ_{\circ}}}}} \circ \circ^{\circ_{\circ_{\circ_{\circ}}}} \circ \circ^{\circ_{\circ_{\circ_{\circ}}}} \circ \circ^{\circ_{\circ_{\circ_{\circ}}}} \circ \circ^{\circ_{\circ_{\circ_{\circ}}}} \circ \circ^{\circ_{\circ_{\circ}}} \circ \circ^{\circ_{\circ}} \circ^{\circ_{\circ}} \circ \circ^{\circ_{\circ}} \circ^{\circ_{\circ}} \circ \circ^{\circ_{\circ}} \circ^{\circ_$	ORTJ0954.032

	LDATA SARL Fran					
Property Code:	[HMSD1000] HE	AT OF MIXING	AND SOLUTION	N		ORTJ0954.041
State:	Two-component s	ystem, single-phas	e liquid or two-ph	ase liquid-liqu	id (LL)	
	Pure component 1					
	Pure component 2					
	[P1] <i>T/</i> K,	Temperature				
Variables:	$[X1] x_1/-,$	Mole fraction of	component 1			
	[Y1] $H^{E}/Jmol^{-1}$,	Molar excess ent	thalpy			
	Direct low-pressu	and a state of the second s	easurement of H ^L	at variable x1	and constant T	
Components:	1. C ₆ H ₁₄ O, Hexa	an-1-ol				
	2. C ₁₀ H ₂₀ O ₂ , M	ethyl nonanoate				
[P1] = .298	3150E+03			[21]		
· · ·		Т		[Y1]		
[X1]	[Y1]			.180E+04	· · · · · · · · · · · · · · · · · · ·	
.756000E-01	.577500E+03					
.938000E-01	.696500E+03				0 ^{0.0} 0	
.162000E+00	.101790E+04					
.214100E+00	.121890E+04				, O O,	
.265300E+00	.138340E+04			.135E+04	. o a	_
.306600E+00	.149470E+04				$ \rangle = \langle \rangle$	
.353900E+00	.157820E+04				o o	
.379100E+00	.161160E+04				$ \rangle / \rangle$	
.437600E+00	.164770E+04					2
.486200E+00	.164450E+04			0007 - 02		
.526800E+00	.161970E+04			.900E+03	F /	\ 1
.569900E+00	.156730E+04					9.
.599500E+00	.149270E+04					
.632300E+00	.143590E+04				Ĭ	
.668300E+00	.136390E+04				ġ.	
.719600E+00	.123190E+04			.450E+03		
.780500E+00	.104030E+04					
.837200E+00	.818200E+03					
.902900E+00	.524500E+03				○ [P1] = .298150E+03	0
.959400E+00	.242100E+03					
				0007 . 00		
				.000E+00		
		n		.000E+00		
Property Code:	ELDATA SARL Fra [HMSD1000] HI	EAT OF MIXING	AND SOLUTIO	N		[X1]
Property Code: State: Parameters:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K,	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature	AND SOLUTIO se liquid or two-pl	N		
Property Code: State:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-,	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o	AND SOLUTIO se liquid or two-pl	N		
Property Code: State: Parameters: Variables:	[HMSD1000] HI Two-component Pure component [P1] T/K, [X1] x1/-, [Y1] HEJmol ⁻¹ ,	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en	AND SOLUTIO se liquid or two-pl of component 1 nthalpy	N hase liquid-liqu	iid (LL)	
Property Code: State: Parameters: Variables: Method:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [X1] H ^E /Jmol ⁻¹ , Direct low-press	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric m	AND SOLUTIO se liquid or two-pl of component 1 nthalpy	N hase liquid-liqu	iid (LL)	
Property Code: State: Parameters: Variables:	[HMSD1000] HI Two-component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Her	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric more can-1-ol	AND SOLUTIO se liquid or two-pl of component 1 thalpy easurement of H ^E	N hase liquid-liqu	iid (LL)	
Property Code: State: Parameters: Variables: Method: Components:	[HMSD1000] HI Two-component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hes 2. C ₁₂ H ₂₄ O ₂ , M	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric m	AND SOLUTIO se liquid or two-pl of component 1 thalpy easurement of H ^E	N hase liquid-liqu	iid (LL)	
Property Code: State: Parameters: Variables: Method:	[HMSD1000] HI Two-component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hes 2. C ₁₂ H ₂₄ O ₂ , M	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric more can-1-ol	AND SOLUTIO se liquid or two-pl of component 1 thalpy easurement of H ^E	N hase liquid-liqu	iid (LL)	
Property Code: State: Parameters: Variables: Method: Components:	[HMSD1000] HI Two-component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hes 2. C ₁₂ H ₂₄ O ₂ , M	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric more can-1-ol	AND SOLUTIO se liquid or two-pl of component 1 thalpy easurement of H ^E	N hase liquid-liqu ⁵ at variable x ₁	iid (LL)	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1]	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hez 2. C ₁₂ H ₂₄ O ₂ , M 8150E+03 [Y1]	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric more can-1-ol	AND SOLUTIO se liquid or two-pl of component 1 thalpy easurement of H ^E	N hase liquid-liqu ⁵ at variable x ₁ [Y1]	iid (LL)	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .881000E-01	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hes 2. C ₁₂ H ₂₄ O ₂ , M 8150E+03 [Y1] .651100E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric more can-1-ol	AND SOLUTIO se liquid or two-pl of component 1 thalpy easurement of H ^E	N hase liquid-liqu ⁵ at variable x ₁ [Y1]	and constant T	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .881000E-01 .184000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hea 2. C ₁₂ H ₂₄ O ₂ , M 8150E+03 [Y1] .651100E+03 .111490E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric more can-1-ol	AND SOLUTIO se liquid or two-pl of component 1 thalpy easurement of H ^E	N hase liquid-liqu ⁵ at variable x ₁ [Y1]	and constant T	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .881000E-01 .184000E+00 .278300E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hes 2. C ₁₂ H ₂₄ O ₂ , M 8150E+03 [Y1] .651100E+03 .111490E+04 .141420E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric more can-1-ol	AND SOLUTIO se liquid or two-pl of component 1 thalpy easurement of H ^E	N hase liquid-liqu ⁵ at variable x ₁ [Y1]	and constant T	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .881000E-01 .184000E+00 .278300E+00 .339400E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hez 2. C ₁₂ H ₂₄ O ₂ , M 8150E+03 [Y1] .651100E+03 .11490E+04 .141420E+04 .154170E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric more can-1-ol	AND SOLUTIO se liquid or two-pl of component 1 thalpy easurement of H ^E	N hase liquid-liqu at variable x ₁ [Y1] .180E+04	and constant T	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .881000E-01 .184000E+00 .378300E+00 .39400E+00 .391800E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hez 2. C ₁₂ H ₂₄ O ₂ , M 8150E+03 [Y1] .651100E+03 .111490E+04 .154170E+04 .160350E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric more can-1-ol	AND SOLUTIO se liquid or two-pl of component 1 thalpy easurement of H ^E	N hase liquid-liqu ⁵ at variable x ₁ [Y1]	and constant T	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .881000E+00 .278300E+00 .39400E+00 .391800E+00 .436200E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hes 2. C ₁₂ H ₂₄ O ₂ , M 8150E+03 [Y1] .651100E+03 .111490E+04 .154170E+04 .160350E+04 .162690E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric more can-1-ol	AND SOLUTIO se liquid or two-pl of component 1 thalpy easurement of H ^E	N hase liquid-liqu at variable x ₁ [Y1] .180E+04	and constant T	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .881000E-01 .184000E+00 .378300E+00 .339400E+00 .391800E+00 .436200E+00 .475100E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hea 2. C ₁₂ H ₂₄ O ₂ , M 8150E+03 [Y1] .651100E+03 .111490E+04 .154170E+04 .160350E+04 .162810E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric more can-1-ol	AND SOLUTIO se liquid or two-pl of component 1 thalpy easurement of H ^E	N hase liquid-liqu at variable x ₁ [Y1] .180E+04	and constant T	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .881000E-01 .184000E+00 .278300E+00 .39400E+00 .391800E+00 .436200E+00 .475100E+00 .508300E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hen 2. C ₁₂ H ₂₄ O ₂ , M 8150E+03 [Y1] .651100E+03 .111490E+04 .161420E+04 .162810E+04 .161420E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric more can-1-ol	AND SOLUTIO se liquid or two-pl of component 1 thalpy easurement of H ^E	N hase liquid-liqu at variable x ₁ [Y1] .180E+04	and constant T	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .881000E-01 .184000E+00 .278300E+00 .339400E+00 .339400E+00 .436200E+00 .508300E+00 .570500E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hes 2. C ₁₂ H ₂₄ O ₂ , M 8150E+03 [Y1] .651100E+03 .111490E+04 .161420E+04 .162810E+04 .162810E+04 .161420E+04 .161420E+04 .153330E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric more can-1-ol	AND SOLUTIO se liquid or two-pl of component 1 thalpy easurement of H ^E	N hase liquid-liqu at variable x ₁ [Y1] .180E+04	and constant T	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .881000E-01 .184000E+00 .278300E+00 .391800E+00 .391800E+00 .436200E+00 .508300E+00 .570500E+00 .603500E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hes 2. C ₁₂ H ₂₄ O ₂ , M 8150E+03 [Y1] .651100E+03 .111490E+04 .161420E+04 .162810E+04 .162810E+04 .161420E+04 .153330E+04 .148010E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric more can-1-ol	AND SOLUTIO se liquid or two-pl of component 1 thalpy easurement of H ^E	N hase liquid-liqu at variable x ₁ [Y1] .180E+04	and constant T	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .881000E-01 .184000E+00 .278300E+00 .39400E+00 .391800E+00 .436200E+00 .570500E+00 .639500E+00 .639500E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hez 2. C ₁₂ H ₂₄ O ₂ , M 8150E+03 [Y1] .651100E+03 .11490E+04 .161420E+04 .162810E+04 .162810E+04 .161420E+04 .153330E+04 .141920E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric more can-1-ol	AND SOLUTIO se liquid or two-pl of component 1 thalpy easurement of H ^E	N hase liquid-liqu 3 at variable x ₁ [Y1] .180E+04 .135E+04	and constant T	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .881000E-01 .184000E+00 .339400E+00 .391800E+00 .436200E+00 .436200E+00 .570500E+00 .603500E+00 .639500E+00 .676100E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hez 2. C ₁₂ H ₂₄ O ₂ , M 8150E+03 [Y1] .651100E+03 .111490E+04 .154170E+04 .160350E+04 .162810E+04 .161420E+04 .161420E+04 .148010E+04 .141920E+04 .134610E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric more can-1-ol	AND SOLUTIO se liquid or two-pl of component 1 thalpy easurement of H ^E	N hase liquid-liqu 3 at variable x ₁ [Y1] .180E+04 .135E+04	and constant T	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .881000E+00 .278300E+00 .39400E+00 .39400E+00 .391800E+00 .436200E+00 .508300E+00 .603500E+00 .63500E+00 .676100E+00 .721300E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hes 2. C ₁₂ H ₂₄ O ₂ , M 8150E+03 [Y1] .651100E+03 .111490E+04 .161420E+04 .162810E+04 .162810E+04 .162810E+04 .163330E+04 .16330E+04 .148010E+04 .13330E+04 .134610E+04 .123270E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric more can-1-ol	AND SOLUTIO se liquid or two-pl of component 1 thalpy easurement of H ^E	N hase liquid-liqu 3 at variable x ₁ [Y1] .180E+04 .135E+04	and constant T	ORTJ0954.050
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .881000E-01 .184000E+00 .278300E+00 .339400E+00 .339400E+00 .436200E+00 .570500E+00 .639500E+00 .639500E+00 .676100E+00 .721300E+00 .767600E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hes 2. C ₁₂ H ₂₄ O ₂ , M 8150E+03 [Y1] .651100E+03 .111490E+04 .161420E+04 .162810E+04 .162810E+04 .162810E+04 .162810E+04 .163330E+04 .148010E+04 .13330E+04 .134610E+04 .123270E+04 .109340E+04	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric more can-1-ol	AND SOLUTIO se liquid or two-pl of component 1 thalpy easurement of H ^E	N hase liquid-liqu 3 at variable x ₁ [Y1] .180E+04 .135E+04	and constant T	ORTJ0954.050
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .881000E-01 .184000E+00 .278300E+00 .391800E+00 .391800E+00 .391800E+00 .570500E+00 .603500E+00 .639500E+00 .676100E+00 .721300E+00 .721300E+00 .814700E+00	[HMSD1000] HI Two-component Pure component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hes 2. C ₁₂ H ₂₄ O ₂ , M 8150E+03 [Y1] .651100E+03 .111490E+04 .161350E+04 .162810E+04 .162810E+04 .162810E+04 .163330E+04 .16420E+04 .153330E+04 .141920E+04 .134610E+04 .134610E+04 .123270E+04 .09340E+04 .925200E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric more can-1-ol	AND SOLUTIO se liquid or two-pl of component 1 thalpy easurement of H ^E	N hase liquid-liqu at variable x ₁ [Y1] .180E+04 .135E+04 .900E+03	and constant T	ORTJ0954.050
Property Code: State: Variables: Variables: Variables: Method: Components: [P1] = .29 [X1] .881000E-01 .184000E+00 .278300E+00 .39400E+00 .391800E+00 .391800E+00 .570500E+00 .603500E+00 .639500E+00 .676100E+00 .721300E+00 .767600E+00 .881700E+00 .860900E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hes 2. C ₁₂ H ₂₄ O ₂ , M 8150E+03 [Y1] .651100E+03 .111490E+04 .161420E+04 .162690E+04 .162810E+04 .162810E+04 .163330E+04 .161420E+04 .153330E+04 .141920E+04 .141920E+04 .134610E+04 .13	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric more can-1-ol	AND SOLUTIO se liquid or two-pl of component 1 thalpy easurement of H ^E	N hase liquid-liqu 3 at variable x ₁ [Y1] .180E+04 .135E+04	and constant T	ORTJ0954.050
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .881000E-01 .184000E+00 .278300E+00 .39400E+00 .391800E+00 .391800E+00 .570500E+00 .635500E+00 .635500E+00 .676100E+00 .721300E+00 .767600E+00 .844700E+00 .844700E+00 .860900E+00 .905000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hez 2. C ₁₂ H ₂₄ O ₂ , M 8150E+03 [Y1] .651100E+03 .11490E+04 .161420E+04 .162810E+04 .162810E+04 .162810E+04 .162810E+04 .162810E+04 .162810E+04 .141920E+04 .141920E+04 .134610E+04 .123270E+04 .134610E+04 .123270E+04 .734500E+03 .734500E+03 .532500E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric more can-1-ol	AND SOLUTIO se liquid or two-pl of component 1 thalpy easurement of H ^E	N hase liquid-liqu at variable x ₁ [Y1] .180E+04 .135E+04 .900E+03	and constant T	ORTJ0954.050
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .881000E-01 .184000E+00 .39400E+00 .39400E+00 .391800E+00 .436200E+00 .603500E+00 .603500E+00 .676100E+00 .721300E+00 .767600E+00 .860900E+00 .905000E+00 .905100E+00 .905100E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hez 2. C ₁₂ H ₂₄ O ₂ , M 8150E+03 [Y1] .651100E+03 .111490E+04 .154170E+04 .160350E+04 .162810E+04 .162810E+04 .161420E+04 .161420E+04 .13330E+04 .148010E+04 .134610E+04 .134610E+04 .134610E+04 .134610E+04 .134500E+03 .734500E+03 .532500E+03 .363500E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo can-1-ol	AND SOLUTIO se liquid or two-pl of component 1 thalpy easurement of H ^E	N hase liquid-liqu at variable x ₁ [Y1] .180E+04 .135E+04 .900E+03	and constant <i>T</i>	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .881000E-01 .184000E+00 .278300E+00 .39400E+00 .391800E+00 .391800E+00 .570500E+00 .63500E+00 .63500E+00 .676100E+00 .721300E+00 .721300E+00 .84700E+00 .84700E+00 .84700E+00 .860900E+00 .905000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hez 2. C ₁₂ H ₂₄ O ₂ , M 8150E+03 [Y1] .651100E+03 .11490E+04 .161420E+04 .162810E+04 .162810E+04 .162810E+04 .162810E+04 .162810E+04 .162810E+04 .141920E+04 .141920E+04 .134610E+04 .123270E+04 .134610E+04 .123270E+04 .734500E+03 .734500E+03 .532500E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo can-1-ol	AND SOLUTIO se liquid or two-pl of component 1 thalpy easurement of H ^E	N hase liquid-liqu at variable x ₁ [Y1] .180E+04 .135E+04 .900E+03	and constant T	ORTJ0954.050
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .881000E-01 .184000E+00 .39400E+00 .39400E+00 .391800E+00 .436200E+00 .603500E+00 .603500E+00 .676100E+00 .721300E+00 .767600E+00 .860900E+00 .905000E+00 .905100E+00 .905100E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hez 2. C ₁₂ H ₂₄ O ₂ , M 8150E+03 [Y1] .651100E+03 .111490E+04 .154170E+04 .160350E+04 .162810E+04 .162810E+04 .161420E+04 .161420E+04 .13330E+04 .148010E+04 .134610E+04 .134610E+04 .134610E+04 .134610E+04 .134500E+03 .734500E+03 .532500E+03 .363500E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo can-1-ol	AND SOLUTIO se liquid or two-pl of component 1 thalpy easurement of H ^E	N hase liquid-liqu at variable x ₁ [Y1] .180E+04 .135E+04 .900E+03	and constant <i>T</i>	ORTJ0954.050
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .881000E-01 .184000E+00 .39400E+00 .39400E+00 .391800E+00 .436200E+00 .603500E+00 .603500E+00 .676100E+00 .721300E+00 .767600E+00 .860900E+00 .905000E+00 .905100E+00 .905100E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hez 2. C ₁₂ H ₂₄ O ₂ , M 8150E+03 [Y1] .651100E+03 .111490E+04 .154170E+04 .160350E+04 .162810E+04 .162810E+04 .161420E+04 .161420E+04 .13330E+04 .148010E+04 .134610E+04 .134610E+04 .134610E+04 .134610E+04 .134500E+03 .734500E+03 .532500E+03 .363500E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo can-1-ol	AND SOLUTIO se liquid or two-pl of component 1 thalpy easurement of H ^E	N hase liquid-liqu at variable x ₁ [Y1] .180E+04 .135E+04 .900E+03	and constant <i>T</i>	ORTJ0954.050
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .881000E-01 .184000E+00 .39400E+00 .39400E+00 .391800E+00 .436200E+00 .603500E+00 .603500E+00 .676100E+00 .721300E+00 .767600E+00 .860900E+00 .905000E+00 .905100E+00 .905100E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hez 2. C ₁₂ H ₂₄ O ₂ , M 8150E+03 [Y1] .651100E+03 .111490E+04 .154170E+04 .160350E+04 .162810E+04 .162810E+04 .161420E+04 .161420E+04 .13330E+04 .148010E+04 .134610E+04 .134610E+04 .134610E+04 .134610E+04 .134500E+03 .734500E+03 .532500E+03 .363500E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo can-1-ol	AND SOLUTIO se liquid or two-pl of component 1 thalpy easurement of H ^E	N hase liquid-liqu i at variable x1 [Y1] .180E+04 .135E+04 .900E+03 .450E+03	and constant <i>T</i>	ORTJ0954.050
Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .881000E-01 .184000E+00 .39400E+00 .39400E+00 .391800E+00 .436200E+00 .603500E+00 .603500E+00 .676100E+00 .721300E+00 .767600E+00 .860900E+00 .905000E+00 .905100E+00 .905100E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hez 2. C ₁₂ H ₂₄ O ₂ , M 8150E+03 [Y1] .651100E+03 .111490E+04 .154170E+04 .160350E+04 .162810E+04 .162810E+04 .161420E+04 .161420E+04 .13330E+04 .148010E+04 .134610E+04 .134610E+04 .134610E+04 .134610E+04 .134500E+03 .734500E+03 .532500E+03 .363500E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo can-1-ol	AND SOLUTIO se liquid or two-pl of component 1 thalpy easurement of H ^E	N hase liquid-liqu i at variable x1 [Y1] .180E+04 .135E+04 .900E+03 .450E+03	and constant <i>T</i>	ORTJ0954.050
Property Code: State: Variables: Method: Components: [P1] = .29 [X1] .881000E-01 .184000E+00 .39400E+00 .39400E+00 .391800E+00 .436200E+00 .436200E+00 .570500E+00 .639500E+00 .639500E+00 .721300E+00 .767600E+00 .860900E+00 .905000E+00 .972300E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hez 2. C ₁₂ H ₂₄ O ₂ , M 8150E+03 [Y1] .651100E+03 .111490E+04 .154170E+04 .160350E+04 .162810E+04 .162810E+04 .161420E+04 .161420E+04 .13330E+04 .148010E+04 .134610E+04 .134610E+04 .134610E+04 .134610E+04 .134500E+03 .734500E+03 .532500E+03 .363500E+03	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction o Molar excess en ure calorimetric mo can-1-ol	AND SOLUTIO se liquid or two-pl of component 1 thalpy easurement of H ^E	N hase liquid-liqu i at variable x1 [Y1] .180E+04 .135E+04 .900E+03 .450E+03	and constant <i>T</i>	ORTJ0954.050

roperty Code:	[HMSD1000] HE	nce. All rights reserved. AT OF MIXING	AND SOLUTION	N SPECIAL CONTRACT		RTJ0954.059
late:	Two-component s	system, single-pha	ase liquid or two-ph	ase liquid-liquid ([LL)	
	Pure component					
	Pure component					
	[P1] <i>T/</i> K,	Temperature	6			
ariables:	$[X1] x_1/-,$ $[Y1] H^E/Jmol^{-1},$	Mole fraction of	of component 1			
fethod:	Direct low-press	re calorimetric m	neasurement of $H^{\rm E}$	at variable r1 and	constant T	
and the second	1. C ₆ H ₁₄ O, Hex			at variable x1 and		
-	2. C14H28O2, M		ite			
[P1] = .298				[Y1]		
[X1]	[Y1]		and the second second	.180E+04		
.108500E+00	.656400E+03				P[P1] = .298150E + 03	
.209400E+00	.107530E+04					
.310900E+00 .398100E+00	.135820E+04 .150230E+04				o ^{o.} .o	
.472100E+00	.154480E+04			1057.04	0 000	
.530700E+00	.152400E+04		$\gamma_{\rm eff} = \gamma_{\rm eff} + \gamma_{\rm eff}$.135E+04	, o , o	1
.581400E+00	.147730E+04				a da Angela a San Nasara	
.625500E+00	.141190E+04					
.645400E+00	.138120E+04				o o	
.677300E+00	.130360E+04		10.000	.900E+03	\sim	
.722300E+00 .774500E+00	.117070E+04 .101760E+04		1 - 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1 -		/ Š	1
.774500E+00	.848200E+03		3		$-\sqrt{2}$	
.875500E+00	.645300E+03				0	
.923200E+00	.424300E+03				A second s	
.965300E+00	.210100E+03		a statistic	.450E+03	🛃 de la companya de la company	0
						X I
						N.
						2
	and the second	te a constant	P - EKA	.000E+00		
	14 1	1997 - NG 2			.50E+00	[X1]
	1	1				1411
			-			[]
Commisht@ 1005 E	I DATA SARI Em	All rights record				[]
	LDATA SARL Fra			J	OR	
	[HMSD1000] HI	EAT OF MIXING	G AND SOLUTION	N ase liquid-liquid (() TJ0954.068
Property Code:	[HMSD1000] HI Two-component Pure component	EAT OF MIXINC system, single-pha 1, liquid		1 ase liquid-liquid (
Property Code: State:	[HMSD1000] HI Two-component Pure component Pure component	EAT OF MIXINC system, single-pha 1, liquid 2, liquid	G AND SOLUTION	1 ase liquid-liquid (
Property Code: State: Parameters:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K,	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature	3 AND SOLUTION ase liquid or two-ph	ase liquid-liquid (
Property Code: State: Parameters:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-,	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction of	G AND SOLUTION ase liquid or two-ph of component 1	ase liquid-liquid (
Property Code: State: Parameters: /ariables:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ .	EAT OF MIXINC system, single-phi 1, liquid 2, liquid Temperature Mole fraction of Molar excess e	G AND SOLUTION ase liquid or two-ph of component 1	ase liquid-liquid (
Property Code: State: Parameters: /ariables: Aethod:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. C ₆ H ₁₄ O, Hex	EAT OF MIXINC system, single-phr 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid (
Property Code: State: Parameters: /ariables: /dethod: Components:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1}/-$, [Y1] H^{E}/Jmol^{-1} , Direct low-press 1. C ₆ H ₁₄ O, Hen 2. C ₁₆ H ₃₂ O ₂ , M	EAT OF MIXINC system, single-phr 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid (at variable x ₁ and		
Property Code:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1}/-$, [Y1] H^{E}/Jmol^{-1} , Direct low-press 1. C ₆ H ₁₄ O, Hen 2. C ₁₆ H ₃₂ O ₂ , M	EAT OF MIXINC system, single-phr 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid (
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₆ H ₁₄ O, Hea 2. C ₁₆ H ₃₂ O ₂ , M 3150E+03	EAT OF MIXINC system, single-phr 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid (at variable x ₁ and	LL)	
Property Code: State: Parameters: Variables: Variables: Method: Components: [P1] = .298 [X1] .100900E+00 .192500E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hex 2. C ₁₆ H ₃₂ O ₂ , M B150E+03 [Y1] .734000E+03 .118050E+04	EAT OF MIXINC system, single-phr 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid (at variable x ₁ and		
Property Code: State: Parameters: Variables: Variables: Method: Components: [P1] = .298 [X1] .100900E+00 .192500E+00 .279800E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hex 2. C ₁₆ H ₃₂ O ₂ , M B150E+03 [Y1] .734000E+03 .118050E+04 .146490E+04	EAT OF MIXINC system, single-phr 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid (at variable x ₁ and	LL)	
Property Code: State: Parameters: Variables: Variables: Method: Components: [P1] = .298 [X1] .100900E+00 .192500E+00 .279800E+00 .358600E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hex 2. C ₁₆ H ₃₂ O ₂ , M B150E+03 [Y1] .734000E+03 .118050E+04 .146490E+04 .161030E+04	EAT OF MIXINC system, single-phr 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid (at variable x ₁ and [Y1] .180E+04	LL)	
Property Code: State: Parameters: Variables: Variables: Vethod: Components: [P1] = .298 [X1] .100900E+00 .192500E+00 .279800E+00 .358600E+00 .428600E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hex 2. C ₁₆ H ₃₂ O ₂ , M B150E+03 [Y1] .734000E+03 .118050E+04 .146490E+04 .166620E+04	EAT OF MIXINC system, single-phr 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid (at variable x ₁ and	LL)	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .100900E+00 .192500E+00 .279800E+00 .358600E+00 .428600E+00 .493000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hex 2. C ₁₆ H ₃₂ O ₂ , M B150E+03 [Y1] .734000E+03 .118050E+04 .146490E+04 .166620E+04 .166830E+04	EAT OF MIXINC system, single-phr 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid (at variable x ₁ and [Y1] .180E+04	LL)	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .100900E+00 .192500E+00 .279800E+00 .358600E+00 .428600E+00 .493000E+00 .545500E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hen 2. C ₁₆ H ₃₂ O ₂ , M 3150E+03 [Y1] .734000E+03 .118050E+04 .146490E+04 .166620E+04 .166830E+04 .162410E+04	EAT OF MIXINC system, single-phr 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid (at variable x ₁ and [Y1] .180E+04	LL)	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .100900E+00 .192500E+00 .279800E+00 .358600E+00 .428600E+00 .493000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hex 2. C ₁₆ H ₃₂ O ₂ , M B150E+03 [Y1] .734000E+03 .118050E+04 .146490E+04 .166620E+04 .166830E+04	EAT OF MIXINC system, single-phr 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid (at variable x ₁ and [Y1] .180E+04	LL)	
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Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hea 2. C ₁₆ H ₃₂ O ₂ , M 3150E+03 [Y1] .734000E+03 .118050E+04 .146490E+04 .166830E+04 .166830E+04 .166230E+04 .162410E+04 .148480E+04 .140520E+04 .130190E+04	EAT OF MIXINC system, single-phr 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid (at variable x ₁ and [Y1] .180E+04	LL)	
Property Code: State: Parameters: Variables: Variables: Vethod: Components: [P1] = .298 [X1] .100900E+00 .192500E+00 .279800E+00 .428600E+00 .428600E+00 .545500E+00 .592200E+00 .631300E+00 .663400E+00 .702100E+00 .745200E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hen 2. C ₁₆ H ₃₂ O ₂ , M 3150E+03 [Y1] .734000E+03 .118050E+04 .146490E+04 .166830E+04 .166830E+04 .166830E+04 .148480E+04 .140520E+04 .130190E+04 .130190E+04 .117630E+04	EAT OF MIXINC system, single-phr 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid (at variable x ₁ and [Y1] .180E+04 .135E+04	LL)	
Property Code: State: Parameters: Variables: Variables: Variables: (P1] = .298 [X1] .100900E+00 .192500E+00 .279800E+00 .428600E+00 .545500E+00 .631300E+00 .63430E+00 .663400E+00 .745200E+00 .745200E+00 .793600E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₆ H ₁₄ O, Hea 2. C ₁₆ H ₃₂ O ₂ , M 3150E+03 [Y1] .734000E+03 .118050E+04 .18050E+04 .166830E+04 .166830E+04 .166830E+04 .166830E+04 .140520E+04 .130190E+04 .130190E+04 .101720E+04	EAT OF MIXINC system, single-phr 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid (at variable x ₁ and [Y1] .180E+04 .135E+04	LL)	
Property Code: State: Parameters: Variables: Variables: Method: Components: [P1] = .298 [X1] .100900E+00 .279800E+00 .279800E+00 .358600E+00 .493000E+00 .545500E+00 .631300E+00 .63200E+00 .745200E+00 .745200E+00 .793600E+00 .842000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressi 1. C ₆ H ₁₄ O, Hex 2. C ₁₆ H ₃₂ O ₂ , M 3150E+03 [Y1] .734000E+03 .118050E+04 .146490E+04 .166830E+04 .166830E+04 .166230E+04 .166230E+04 .130190E+04 .130190E+04 .101720E+04 .835500E+03	EAT OF MIXINC system, single-phr 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid (at variable x ₁ and [Y1] .180E+04 .135E+04	LL)	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .100900E+00 .192500E+00 .279800E+00 .358600E+00 .428600E+00 .592200E+00 .592200E+00 .63400E+00 .793600E+00 .884200E+00 .88400E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressi 1. C ₆ H ₁₄ O, Hea 2. C ₁₆ H ₃₂ O ₂ , M 3150E+03 [Y1] .734000E+03 .118050E+04 .146490E+04 .166830E+04 .166830E+04 .166210E+04 .166210E+04 .162410E+04 .130190E+04 .130190E+04 .101720E+04 .835500E+03 .629400E+03	EAT OF MIXINC system, single-phr 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 inthalpy neasurement of HE noate	ase liquid-liquid (at variable x ₁ and [Y1] .180E+04 .135E+04 .900E+03	LL)	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .100900E+00 .192500E+00 .279800E+00 .358600E+00 .428600E+00 .428600E+00 .592200E+00 .631300E+00 .702100E+00 .745200E+00 .793600E+00 .888400E+00 .888400E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressi 1. C ₆ H ₁₄ O, Hex 2. C ₁₆ H ₃₂ O ₂ , M 3150E+03 [Y1] .734000E+03 .118050E+04 .146490E+04 .166830E+04 .166830E+04 .166230E+04 .166230E+04 .130190E+04 .130190E+04 .101720E+04 .835500E+03	EAT OF MIXINC system, single-phr 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 nthalpy neasurement of H ^E	ase liquid-liquid (at variable x ₁ and [Y1] .180E+04 .135E+04	LL)	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .100900E+00 .192500E+00 .279800E+00 .358600E+00 .428600E+00 .592200E+00 .592200E+00 .63400E+00 .793600E+00 .884200E+00 .88400E+00	[HMSD1000] HI Two-component Pure component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] HE/Jmol-1, Direct low-pressi 1. C6H14O, Hen 2. C16H32O2, M 3150E+03 [Y1] .734000E+03 .118050E+04 .146490E+04 .166830E+04 .166830E+04 .166830E+04 .166830E+04 .166830E+04 .148480E+04 .148480E+04 .101720E+04 .835500E+03 .629400E+03 .408400E+03	EAT OF MIXINC system, single-phr 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 inthalpy neasurement of HE noate	ase liquid-liquid (at variable x ₁ and [Y1] .180E+04 .135E+04 .900E+03	LL)	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .100900E+00 .192500E+00 .279800E+00 .358600E+00 .428600E+00 .592200E+00 .592200E+00 .63400E+00 .793600E+00 .88400E+00 .88400E+00 .88400E+00 .888400E+00 .88400E+00 .888400E+00 .88400E+00 .888400E+00 .88400E+00 .888400E+00 .88400E+00	[HMSD1000] HI Two-component Pure component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] HE/Jmol-1, Direct low-pressi 1. C6H14O, Hen 2. C16H32O2, M 3150E+03 [Y1] .734000E+03 .118050E+04 .146490E+04 .166830E+04 .166830E+04 .166830E+04 .166830E+04 .166830E+04 .148480E+04 .148480E+04 .101720E+04 .835500E+03 .629400E+03 .408400E+03	EAT OF MIXINC system, single-phr 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 inthalpy neasurement of HE noate	ase liquid-liquid (at variable x ₁ and [Y1] .180E+04 .135E+04 .900E+03	LL)	and the second second
Property Code: State: Parameters: Variables: Variables: Variables: (P1] = .298 [X1] .100900E+00 .192500E+00 .279800E+00 .358600E+00 .428600E+00 .592200E+00 .592200E+00 .63400E+00 .745200E+00 .793600E+00 .888400E+00 .888400E+00 .888400E+00 .888400E+00 .888400E+00 .888400E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressi 1. C ₆ H ₁₄ O, Hea 2. C ₁₆ H ₃₂ O ₂ , M 3150E+03 [Y1] .734000E+03 .118050E+04 .146490E+04 .166830E+04 .166830E+04 .166830E+04 .166830E+04 .166830E+04 .148480E+04 .140520E+04 .101720E+04 .835500E+03 .629400E+03 .408400E+03	EAT OF MIXINC system, single-phr 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 inthalpy neasurement of HE noate	ase liquid-liquid (at variable x ₁ and [Y1] .180E+04 .135E+04 .900E+03	LL)	
Property Code: State: Parameters: /arlable: /arlables: /arlables: /arlable: /a	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressi 1. C ₆ H ₁₄ O, Hea 2. C ₁₆ H ₃₂ O ₂ , M 3150E+03 [Y1] .734000E+03 .118050E+04 .146490E+04 .166830E+04 .166830E+04 .166830E+04 .166830E+04 .166830E+04 .148480E+04 .140520E+04 .101720E+04 .835500E+03 .629400E+03 .408400E+03	EAT OF MIXINC system, single-phr 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 inthalpy neasurement of HE noate	ase liquid-liquid (at variable x ₁ and [Y1] .180E+04 .135E+04 .900E+03	LL)	
Property Code: State: Parameters: /ariables: /ariables: /ethod: Components: [P1] = .298 [X1] .100900E+00 .192500E+00 .279800E+00 .358600E+00 .428600E+00 .545500E+00 .592200E+00 .663400E+00 .793600E+00 .888400E+00 .888400E+00 .888400E+00 .888400E+00 .888400E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressi 1. C ₆ H ₁₄ O, Hea 2. C ₁₆ H ₃₂ O ₂ , M 3150E+03 [Y1] .734000E+03 .118050E+04 .146490E+04 .166830E+04 .166830E+04 .166830E+04 .166830E+04 .166830E+04 .148480E+04 .140520E+04 .101720E+04 .835500E+03 .629400E+03 .408400E+03	EAT OF MIXINC system, single-phr 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 inthalpy neasurement of HE noate	ase liquid-liquid (at variable x1 and [Y1] .180E+04 .135E+04 .900E+03 - .450E+03	LL)	ETJ0954.068
roperty Code: tate: arameters: ariables: fethod: components: [P1] = .298 [X1] .100900E+00 .192500E+00 .279800E+00 .279800E+00 .358600E+00 .428600E+00 .592200E+00 .663400E+00 .792600E+00 .793600E+00 .888400E+00 .888400E+00 .888400E+00 .931300E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressi 1. C ₆ H ₁₄ O, Hea 2. C ₁₆ H ₃₂ O ₂ , M 3150E+03 [Y1] .734000E+03 .118050E+04 .146490E+04 .166830E+04 .166830E+04 .166830E+04 .166830E+04 .166830E+04 .148480E+04 .140520E+04 .101720E+04 .835500E+03 .629400E+03 .408400E+03	EAT OF MIXINC system, single-phr 1, liquid 2, liquid Temperature Mole fraction of Molar excess e ure calorimetric m can-1-ol	G AND SOLUTION ase liquid or two-ph of component 1 inthalpy neasurement of HE noate	ase liquid-liquid (at variable x1 and [Y1] .180E+04 .135E+04 .900E+03 - .450E+03	Constant <i>T</i>	

	ELDATA SARL Fr [HMSD1000] H	EAT OF MIXING	G AND SOLUTIO		ORTJ0954.0
State:	Two-component	system, single-ph	ase liquid or two-ph		uid (LL)
	Pure component				
	Pure component				
Parameters: Variables:	[P1] <i>T/</i> K, [X1] <i>x</i> ₁ /-,	Temperature Mole fraction	of component 1		
WAR AND ILS.		, Molar excess e	enthalpy		
Method:	Direct low-press	ure calorimetric n	neasurement of $H^{\rm E}$	at variable x_1	and constant T
Components:	1. C ₈ H ₁₆ O ₂ , M	ethyl heptanoate	:		
[P 11 - 20	2. C ₈ H ₁₈ O, Oct 8150E+03	lan-1-ol	r		
	1			[Y1]	
[X1]	[Y1]		:	.200E+04	· · · · · · · · · · · · · · · · · · ·
.394000E-01 .839000E-01					○ [P1] = .298150E+03
.131500E+00					
.182100E+00					o ^{.oo} .o
.228700E+00			$ _{W^{1,p}(G)} \leq _{W^{1,p}(G)} < _{W^{1,p$.150E+04	
.274300E+00 .321200E+00					0
.365800E+00					
.406100E+00	.152290E+04				<u> </u>
.447500E+00				.100E+04	ø
.492900E+00 .550200E+00				110013104	
.599800E+00					
.630200E+00	.166690E+04		1		o [P1] = .298150E+03
.675200E+00 .721500E+00					
.768200E+00				.500E+03	- / - -
.816700E+00					À
.865200E+00					¢
.911200E+00 .959000E+00					V A
	101000D100				
	and the property of the	and the second second second second	and the second	.000E+00	
	а	production of the second se	and and the second s	.000E+00	.50E+00
	алан (тар бай соло) (тар бай	$\mu = 0$, $\mu = 1/2$, where the set of the set μ is μ , μ , μ , μ , μ	na an a	.000E+00	.50E+00 [X1
Copyright© 1995 F	LDATA SARL Fr	Ince. All rights reser	ved	.000E+00	
	ELDATA SARL Fra [HMSD1000] HI				
	[HMSD1000] HI Two-component	EAT OF MIXING system, single-ph	ved. 3 AND SOLUTION ase liquid or two-ph	1	[X1 ORTJ0954.0:
Property Code:	[HMSD1000] HI Two-component Pure component	EAT OF MIXING system, single-ph 1, liquid	G AND SOLUTION	1	[X1 ORTJ0954.0:
Property Code: State:	[HMSD1000] HI Two-component	EAT OF MIXING system, single-ph 1, liquid	G AND SOLUTION	1	[X1 ORTJ0954.0:
Property Code:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-,	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction	G AND SOLUTION ase liquid or two-ph of component 1	1	[X1 ORTJ0954.0:
Property Code: State: Paramęters: Variables:	[HMSD1000] HI Two-component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ .	EAT OF MIXING system, single-phi 1, liquid 2, liquid Temperature Mole fraction of Molar excess e	G AND SOLUTION ase liquid or two-ph of component 1 inthaloy	N ase liquid-liqui	[X1] id (LL)
Property Code: State: Paramęters: /ariables: /iethod:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press	EAT OF MIXING system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m	G AND SOLUTION ase liquid or two-ph of component 1 inthalpy measurement of H ^E	N ase liquid-liqui	[X1] id (LL)
Property Code: State: Parameters: /ariables: /dethod: Components:	[HMSD1000] HI Two-component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ .	EAT OF MIXING system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl heptanoate	G AND SOLUTION ase liquid or two-ph of component 1 inthalpy measurement of H ^E	N ase liquid-liqui	[X1] id (LL)
Property Code: State: Parameters: /ariables: /dethod: Components:	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-press 1. CgH ₁₆ O ₂ , Ma 2. C ₁₀ H ₂₂ O, De	EAT OF MIXING system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl heptanoate	G AND SOLUTION ase liquid or two-ph of component 1 inthalpy measurement of H ^E	N ase liquid-liqui ast variable x1 a	[X1] id (LL)
Property Code: State: Paramęters: /ariables: Method: Components:	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-press 1. CgH ₁₆ O ₂ , Ma 2. C ₁₀ H ₂₂ O, De	EAT OF MIXING system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl heptanoate	G AND SOLUTION ase liquid or two-ph of component 1 inthalpy measurement of H ^E	N ase liquid-liqui	[X1] id (LL)
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .673000E-01	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₈ H ₁₆ O ₂ , Ma 2. C ₁₀ H ₂₂ O, De B150E+03 [Y1] .382400E+03	EAT OF MIXING system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl heptanoate	G AND SOLUTION ase liquid or two-ph of component 1 inthalpy measurement of H ^E	N ase liquid-liqui at variable x1 a [Y1]	[X1] id (LL)
Property Code: State: Parameters: /ariables: /dethod: Components: [P1] = .298 [X1] .673000E-01 .136900E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₈ H ₁₆ O ₂ , Ma 2. C ₁₀ H ₂₂ O, De B150E+03 [Y1] .382400E+03 .703200E+03	EAT OF MIXING system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl heptanoate	G AND SOLUTION ase liquid or two-ph of component 1 inthalpy measurement of H ^E	N ase liquid-liqui at variable x1 a [Y1]	[X1] id (LL) and constant T • [P1] = .298150E+03
Property Code: State: Parameters: /ariables: //ariabl	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C8H16O ₂ , Ma 2. C10H22O, De B150E+03 [Y1] .382400E+03 .703200E+03 .100450E+04	EAT OF MIXING system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl heptanoate	G AND SOLUTION ase liquid or two-ph of component 1 inthalpy measurement of H ^E	N ase liquid-liqui at variable x1 a [Y1]	[X1] id (LL) and constant T • [P1] = .298150E+03
Property Code: State: Parameters: /ariables: /dethod: Components: [P1] = .298 [X1] .673000E-01 .136900E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₈ H ₁₆ O ₂ , Ma 2. C ₁₀ H ₂₂ O, De B150E+03 [Y1] .382400E+03 .703200E+03	EAT OF MIXING system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl heptanoate	G AND SOLUTION ase liquid or two-ph of component 1 inthalpy measurement of H ^E	N ase liquid-liqui at variable x ₁ a [Y1] .200E+04	[X1] id (LL) and constant T • [P1] = .298150E+03
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .673000E-01 .136900E+00 .208400E+00 .342000E+00 .402000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. CgH16O2, M 2. C10H22O, De 3150E+03 [Y1] .382400E+03 .703200E+03 .100450E+04 .124360E+04 .124360E+04 .155760E+04	EAT OF MIXING system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl heptanoate	G AND SOLUTION ase liquid or two-ph of component 1 inthalpy measurement of H ^E	N ase liquid-liqui at variable x1 a [Y1]	[X1] id (LL) and constant T • [P1] = .298150E+03
Property Code: State: Parameters: /ariables: /dethod: Components: [P1] = .298 [X1] .673000E-01 .136900E+00 .208400E+00 .277100E+00 .342000E+00 .342000E+00 .402000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. CgH ₁₆ O ₂ , Ma 2. C ₁₀ H ₂₂ O, De B150E+03 [Y1] .382400E+03 .703200E+03 .100450E+04 .124360E+04 .142730E+04 .155760E+04 .163780E+04	EAT OF MIXING system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl heptanoate	G AND SOLUTION ase liquid or two-ph of component 1 inthalpy measurement of H ^E	N ase liquid-liqui at variable x ₁ a [Y1] .200E+04	[X1] id (LL) orrjop54.02 orrj
Property Code: State: Parameters: /ariables: /dethod: Components: [P1] = .298 [X1] .673000E-01 .136900E+00 .208400E+00 .277100E+00 .342000E+00 .402000E+00 .455900E+00 .465800E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. CgH ₁₆ O ₂ , Ma 2. C ₁₀ H ₂₂ O, Da 3150E+03 [Y1] .382400E+03 .703200E+03 .100450E+04 .124360E+04 .142730E+04 .155760E+04 .163780E+04 .165070E+04	EAT OF MIXING system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl heptanoate	G AND SOLUTION ase liquid or two-ph of component 1 inthalpy measurement of H ^E	N ase liquid-liqui at variable x ₁ a [Y1] .200E+04	[X1] id (LL) and constant T • [P1] = .298150E+03
Property Code: State: Parameters: /ariables: /dethod: Components: [P1] = .298 [X1] .673000E-01 .136900E+00 .208400E+00 .277100E+00 .342000E+00 .342000E+00 .402000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. CgH ₁₆ O ₂ , Ma 2. C ₁₀ H ₂₂ O, De B150E+03 [Y1] .382400E+03 .703200E+03 .100450E+04 .124360E+04 .142730E+04 .155760E+04 .163780E+04	EAT OF MIXING system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl heptanoate	G AND SOLUTION ase liquid or two-ph of component 1 inthalpy measurement of HE	N ase liquid-liqui at variable x ₁ a [Y1] .200E+04 .150E+04	[X1] id (LL) and constant T • [P1] = .298150E+03
Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] HE/Jmol-1, Direct low-press 1. C8H16O2, Mo 2. C10H22O, De 3150E+03 [Y1] .382400E+03 .703200E+03 .100450E+04 .124360E+04 .142730E+04 .155760E+04 .166780E+04 .168760E+04 .166380E+04 .166380E+04	EAT OF MIXING system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl heptanoate	G AND SOLUTION ase liquid or two-ph of component 1 inthalpy measurement of H ^E	N ase liquid-liqui at variable x ₁ a [Y1] .200E+04	[X1] id (LL) and constant T • [P1] = .298150E+03
Property Code: State: Parameters: /ariables: //ariabl	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₈ H ₁₆ O ₂ , Ma 2. C ₁₀ H ₂₂ O, De 150E+03 [Y1] .382400E+03 .100450E+04 .124360E+04 .124360E+04 .166730E+04 .166730E+04 .166380E+04 .166380E+04 .166380E+04 .161470E+04	EAT OF MIXING system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl heptanoate	G AND SOLUTION ase liquid or two-ph of component 1 inthalpy measurement of HE	N ase liquid-liqui at variable x ₁ a [Y1] .200E+04 .150E+04	[X1] id (LL) o [P1] = .298150E+03 $0^{0^{-0^{-0}}}$
Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₈ H ₁₆ O ₂ , M 2. C ₁₀ H ₂₂ O, De 150E+03 [Y1] .382400E+03 .100450E+04 .124360E+04 .124360E+04 .165776E+04 .166730E+04 .166730E+04 .166730E+04 .166380E+04 .161470E+04 .151980E+04	EAT OF MIXING system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl heptanoate	G AND SOLUTION ase liquid or two-ph of component 1 inthalpy measurement of HE	N ase liquid-liqui at variable x ₁ a [Y1] .200E+04 .150E+04	[X1] id (LL) o [P1] = .298150E+03 $0^{0^{-0^{-0}}}$
Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₈ H ₁₆ O ₂ , Ma 2. C ₁₀ H ₂₂ O, De 150E+03 [Y1] .382400E+03 .100450E+04 .124360E+04 .124360E+04 .166730E+04 .166730E+04 .166380E+04 .166380E+04 .166380E+04 .161470E+04	EAT OF MIXING system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl heptanoate	G AND SOLUTION ase liquid or two-ph of component 1 inthalpy measurement of HE	N ase liquid-liqui at variable x ₁ a [Y1] .200E+04 .150E+04	[X1] id (LL) o [P1] = .298150E+03 $0^{0^{-0^{-0}}}$
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .673000E-01 .136900E+00 .208400E+00 .277100E+00 .402000E+00 .402000E+00 .455900E+00 .551900E+00 .551900E+00 .669400E+00 .708900E+00 .768000E+00 .828600E+00 .828600E+00 .888700E+00	[HMSD1000] HI Two-component Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. CgH ₁₆ O ₂ , Ma 2. C ₁₀ H ₂₂ O, Da St50E+03 [Y1] .382400E+03 .703200E+03 .100450E+04 .124360E+04 .124360E+04 .142730E+04 .165770E+04 .166930E+04 .166930E+04 .166380E+04 .151980E+04 .135990E+04 .135990E+04 .112670E+04 .813800E+03	EAT OF MIXING system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl heptanoate	G AND SOLUTION ase liquid or two-ph of component 1 inthalpy measurement of HE	N ase liquid-liqui at variable x ₁ a [Y1] .200E+04 .150E+04	[X1] id (LL) and constant T \circ [P1] = .298150E+03 $\circ^{\circ^{\circ^{\circ^{\circ^{\circ^{\circ^{\circ^{\circ^{\circ^{\circ^{\circ^{\circ^{\circ$
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .673000E-01 .136900E+00 .208400E+00 .207100E+00 .402000E+00 .402000E+00 .455900E+00 .506900E+00 .551900E+00 .60900E+00 .654200E+00 .708900E+00 .768000E+00 .828600E+00	[HMSD1000] HI Two-component Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. CgH ₁₆ O ₂ , Mi 2. C ₁₀ H ₂₂ O, De B150E+03 [Y1] .382400E+03 .703200E+03 .100450E+04 .124360E+04 .142730E+04 .165760E+04 .166930E+04 .166930E+04 .166380E+04 .166380E+04 .151980E+04 .151980E+04 .135990E+04 .112670E+04	EAT OF MIXING system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl heptanoate	G AND SOLUTION ase liquid or two-ph of component 1 inthalpy measurement of HE	N ase liquid-liqui at variable x ₁ a [Y1] .200E+04 .150E+04 .100E+04	[X1] id (LL) id (LL) \circ [P1] = .298150E+03 \circ $\circ^{\circ \circ \circ \circ} \circ$ \circ \circ \circ \circ \circ \circ \circ \circ \circ
Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HI Two-component Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. CgH ₁₆ O ₂ , Ma 2. C ₁₀ H ₂₂ O, Da St50E+03 [Y1] .382400E+03 .703200E+03 .100450E+04 .124360E+04 .124360E+04 .142730E+04 .165770E+04 .166930E+04 .166930E+04 .166380E+04 .151980E+04 .135990E+04 .135990E+04 .112670E+04 .813800E+03	EAT OF MIXING system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl heptanoate	G AND SOLUTION ase liquid or two-ph of component 1 inthalpy measurement of HE	N ase liquid-liqui at variable x ₁ a [Y1] .200E+04 .150E+04 .100E+04	[X1] id (LL) and constant T \circ [P1] = .298150E+03 $\circ^{\circ^{\circ^{\circ^{\circ^{\circ^{\circ^{\circ^{\circ^{\circ^{\circ^{\circ^{\circ^{\circ$
Property Code: State: Parameters: /ariables: /aria	[HMSD1000] HI Two-component Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. CgH ₁₆ O ₂ , Ma 2. C ₁₀ H ₂₂ O, Da St50E+03 [Y1] .382400E+03 .703200E+03 .100450E+04 .124360E+04 .124360E+04 .142730E+04 .165770E+04 .166930E+04 .166930E+04 .166380E+04 .151980E+04 .135990E+04 .135990E+04 .112670E+04 .813800E+03	EAT OF MIXING system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl heptanoate	G AND SOLUTION ase liquid or two-ph of component 1 inthalpy measurement of HE	N ase liquid-liqui at variable x ₁ a [Y1] .200E+04 .150E+04 .100E+04	[X1] id (LL) id (LL) \circ [P1] = .298150E+03 \circ $\circ^{\circ \circ \circ \circ} \circ$ \circ \circ \circ \circ \circ \circ \circ \circ \circ
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .673000E-01 .136900E+00 .208400E+00 .277100E+00 .402000E+00 .402000E+00 .455900E+00 .551900E+00 .551900E+00 .669400E+00 .708900E+00 .768000E+00 .828600E+00 .828600E+00 .888700E+00	[HMSD1000] HI Two-component Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. CgH ₁₆ O ₂ , Ma 2. C ₁₀ H ₂₂ O, Da St50E+03 [Y1] .382400E+03 .703200E+03 .100450E+04 .124360E+04 .124360E+04 .142730E+04 .165770E+04 .166930E+04 .166930E+04 .166380E+04 .151980E+04 .135990E+04 .135990E+04 .112670E+04 .813800E+03	EAT OF MIXING system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl heptanoate	G AND SOLUTION ase liquid or two-ph of component 1 inthalpy neasurement of HE	N ase liquid-liqui at variable x1 a [Y1] .200E+04 .150E+04 .100E+04 .500E+03	[X1] id (LL) id (LL) \circ [P1] = .298150E+03 \circ $\circ^{\circ \circ \circ \circ} \circ$ \circ \circ \circ \circ \circ \circ \circ \circ \circ
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .673000E-01 .136900E+00 .208400E+00 .277100E+00 .402000E+00 .402000E+00 .455900E+00 .551900E+00 .551900E+00 .669400E+00 .708900E+00 .768000E+00 .828600E+00 .828600E+00 .888700E+00	[HMSD1000] HI Two-component Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. CgH ₁₆ O ₂ , Ma 2. C ₁₀ H ₂₂ O, Da St50E+03 [Y1] .382400E+03 .703200E+03 .100450E+04 .124360E+04 .124360E+04 .142730E+04 .165770E+04 .166930E+04 .166930E+04 .166380E+04 .151980E+04 .135990E+04 .135990E+04 .112670E+04 .813800E+03	EAT OF MIXING system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl heptanoate	G AND SOLUTION ase liquid or two-ph of component 1 inthalpy measurement of HE	N ase liquid-liqui at variable x ₁ a [Y1] .200E+04 .150E+04 .100E+04	[X1] id (LL) o [P1] = .298150E+03
roperty Code: itate: arameters: ariables: fethod: components: [P1] = .298 [X1] .673000E-01 .136900E+00 .208400E+00 .207100E+00 .402000E+00 .402000E+00 .402000E+00 .551900E+00 .506900E+00 .506900E+00 .708900E+00 .708900E+00 .768000E+00 .828600E+00 .888700E+00	[HMSD1000] HI Two-component Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. CgH ₁₆ O ₂ , Ma 2. C ₁₀ H ₂₂ O, Da S150E+03 [Y1] .382400E+03 .703200E+03 .703200E+03 .100450E+04 .124360E+04 .142730E+04 .165760E+04 .166930E+04 .166930E+04 .166380E+04 .151980E+04 .135990E+04 .135990E+04 .112670E+04 .813800E+03	EAT OF MIXING system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m ethyl heptanoate	G AND SOLUTION ase liquid or two-ph of component 1 inthalpy neasurement of HE	N ase liquid-liqui at variable x1 a [Y1] .200E+04 .150E+04 .100E+04 .500E+03	[X1] id (LL) id (LL) \circ [P1] = .298150E+03 \circ $\circ^{\circ \circ \circ \circ} \circ$ \circ \circ \circ \circ \circ \circ \circ \circ \circ

		T OF MIXING AND S	SOLUTION			ORTJ0954.04
	wo-component sys	stem, single-phase liqui	d or two-phase	e liquid-liqui	d (LL)	
	ure component 1,					
	ure component 2,					
	P1] <i>T/</i> K,	Temperature				
riables: []	X1] $x_{1/-}$, X11 $HE(Imol-1)$	Mole fraction of comp Molar excess enthalpy	onent 1			
ethod: D	II] <i>H~/J</i> mol ⁻¹ ,	e calorimetric measurer	ment of HE at	variable r. a	nd constant T	
	and the state of the		nent of <i>n</i> ~ at	variable x1 a		
	C8H18O, Octar 2. C10H20O2, Me					
[P1] = .2981				rv1)	an a	
				[Y1]		
[X1]	[Y1]			.180E+04		
.597000E-01	.484500E+03				○ [P1] = .298150E+03	
.126300E+00	.866700E+03				0.0.0.0	
.193900E+00 .261500E+00	.117160E+04 .138290E+04				,o	
.325500E+00	.151410E+04			1055 . 04	0	
.384500E+00	.151410E+04			.135E+04	· · · · · · · · · · · · · · · · · · ·	-
.438600E+00	.160820E+04				Á á	
.487900E+00	.160040E+04				, ç	
.532600E+00	.156850E+04				/	9
.585500E+00	.149560E+04				/	8
.627600E+00	.142010E+04			.900E+03	.]	· -
.670100E+00	.133520E+04				ř	0
.711900E+00	.123650E+04				/	Y I
.755600E+00	.111260E+04				o [P1] = .298150E+03	
.800500E+00	.958900E+03					0
.845300E+00	.783700E+03			.450E+03	. ¢	<u> </u>
.888900E+00	.592200E+03					q
.930100E+00 .967500E+00	.389700E+03			1.1		
.90/300E+00	.192900E+03					0
				.000E+00		i i i i i i i i i i i i i i i i i i i
					.50E+00	
						[X1]
						1
Copyright© 1995 E	LDATA SARL Fran	nce. All rights reserved.				
	[HMSD1000] HF	AT OF MIXING AND	SOL LETION			ORTJ0954.052
			SOLUTION			
State:	Two-component s	system, single-phase liqu	id or two-phas	se liquid-liqu	id (LL)	
	Two-component s Pure component	system, single-phase liqu 1, liquid	id or two-phas	se liquid-liqu	id (LL)	
State:	Two-component s Pure component Pure component	system, single-phase liqu 1, liquid 2, liquid	id or two-phas	æ liquid-liqu	id (LL)	
State: Parameters:	Two-component s Pure component Pure component [P1] T/K,	system, single-phase liqu 1, liquid 2, liquid Temperature	uid or two-phas	se liquid-liqu	id (LL)	
State:	Two-components Pure component [P1] T/K, [X1] x ₁ /-,	system, single-phase liqu 1, liquid 2, liquid Temperature Mole fraction of com	uid or two-phas ponent 1	æ liquid-liqu	id (LL)	
State: Parameters: Variables:	Two-components Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$,	system, single-phase liqu 1, liquid 2, liquid Temperature Mole fraction of com Molar excess enthalp	uid or two-phas ponent 1 v			
State: Parameters: Variables: Method:	Two-components Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu	system, single-phase liqu 1, liquid 2, liquid Temperature Mole fraction of com Molar excess enthalp ure calorimetric measure	uid or two-phas ponent 1 v			
State: Parameters: Variables:	Two-components Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C8H18O, Octa	system, single-phase liqu 1, liquid 2, liquid Temperature Mole fraction of com Molar excess enthalp ure calorimetric measure	uid or two-phas ponent 1 v			
State: Parameters: Variables: Method: Components:	Two-components Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C8H18O, Octa	system, single-phase liqu 1, liquid 2, liquid Temperature Mole fraction of com Molar excess enthalp ure calorimetric measure an-1-ol	uid or two-phas ponent 1 v	variable x_1 a		
State: Parameters: Variables: Method: Components:	Two-components Pure components Pure components [P1] T/K , [X1] $x_{1}/-$, [Y1] $H^{E}/Jmol^{-1}$, Direct low-pressu 1. C ₈ H ₁₈ O, Octa 2. C ₁₂ H ₂₄ O ₂ , M	system, single-phase liqu 1, liquid 2, liquid Temperature Mole fraction of com Molar excess enthalp ure calorimetric measure an-1-ol	uid or two-phas ponent 1 v			
State: Parameters: Variables: Method: Components: [P1] = .29 [X1]	Two-component s Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C8H18O, Octt 2. C12H24O2, M 8150E+03 [Y1]	system, single-phase liqu 1, liquid 2, liquid Temperature Mole fraction of com Molar excess enthalp ure calorimetric measure an-1-ol	uid or two-phas ponent 1 v	variable x_1 (Y1)	and constant T	
State: Parameters: Variables: Method: Components: [P1] = .29	Two-component s Pure component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C8H18O, Octt 2. C12H24O2, M 8150E+03 [Y1] .449100E+03	system, single-phase liqu 1, liquid 2, liquid Temperature Mole fraction of com Molar excess enthalp ure calorimetric measure an-1-ol	uid or two-phas ponent 1 v	variable x_1 (Y1)	and constant T	
State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .586000E-01	Two-component s Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-pressu 1. C ₈ H ₁₈ O, Oct. 2. C ₁₂ H ₂₄ O ₂ , M 8150E+03 [Y1] .449100E+03 .810300E+03	system, single-phase liqu 1, liquid 2, liquid Temperature Mole fraction of com Molar excess enthalp ure calorimetric measure an-1-ol	uid or two-phas ponent 1 v	variable x_1 (Y1)	and constant T	
State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .586000E-01 .123600E+00 .188800E+00 .255300E+00	Two-component s Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-pressu 1. CgH1gO, Oct. 2. C12H24O2, M 8150E+03 [Y1] .449100E+03 .810300E+03 .109940E+04 .130590E+04	system, single-phase liqu 1, liquid 2, liquid Temperature Mole fraction of com Molar excess enthalp ure calorimetric measure an-1-ol	uid or two-phas ponent 1 v	variable x_1 (Y1)	and constant T	
State: Parameters: Variables: Method: Components: [P1] = .293 [X1] .586000E-01 .123600E+00 .188800E+00 .255300E+00 .316600E+00	Two-component s Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] HE/Jmol-1, Direct low-pressu 1. CgH1gO, Oct 2. C12H24O2, M 8150E+03 [Y1] .449100E+03 .810300E+03 .109940E+04 .130590E+04 .143320E+04	system, single-phase liqu 1, liquid 2, liquid Temperature Mole fraction of com Molar excess enthalp ure calorimetric measure an-1-ol	uid or two-phas ponent 1 v	variable x_1 (Y1)	and constant T	
State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .586000E-01 .123600E+00 .188800E+00 .255300E+00 .316600E+00 .375900E+00	Two-component s Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] HE/Jmol-1, Direct low-pressu 1. CgH1gO, Octa 2. C12H24O2, M 8150E+03 [Y1] .449100E+03 .810300E+03 .109940E+04 .130590E+04 .150750E+04	system, single-phase liqu 1, liquid 2, liquid Temperature Mole fraction of com Molar excess enthalp ure calorimetric measure an-1-ol	uid or two-phas ponent 1 v	[Y1] .180E+04	and constant T	
State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .586000E-01 .123600E+00 .188800E+00 .255300E+00 .316600E+00 .375900E+00 .428800E+00	Two-component s Pure component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-pressu 1. C ₈ H ₁₈ O, Oct. 2. C ₁₂ H ₂₄ O ₂ , M 8150E+03 [Y1] .449100E+03 .810300E+03 .109940E+04 .130590E+04 .150750E+04 .153530E+04	system, single-phase liqu 1, liquid 2, liquid Temperature Mole fraction of com Molar excess enthalp ure calorimetric measure an-1-ol	uid or two-phas ponent 1 v	[Y1] .180E+04	and constant T	
State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .586000E-01 .123600E+00 .188800E+00 .355300E+00 .316600E+00 .375900E+00 .428800E+00 .477000E+00	Two-component s Pure component Pure component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_8H_{18}O$, Oct. 2. $C_{12}H_{24}O_2$, M 8150E+03 [Y1] .449100E+03 .810300E+03 .109940E+04 .130590E+04 .150750E+04 .153530E+04 .153450E+04	system, single-phase liqu 1, liquid 2, liquid Temperature Mole fraction of com Molar excess enthalp ure calorimetric measure an-1-ol	uid or two-phas ponent 1 v	[Y1] .180E+04	and constant T	
State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .586000E-01 .123600E+00 .35300E+00 .316600E+00 .375900E+00 .428800E+00 .428800E+00 .522600E+00	Two-component s Pure component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_8H_{18}O$, Oct. 2. $C_{12}H_{24}O_2$, M 8150E+03 [Y1] .449100E+03 .810300E+03 .109940E+04 .130590E+04 .153530E+04 .153450E+04 .150990E+04	system, single-phase liqu 1, liquid 2, liquid Temperature Mole fraction of com Molar excess enthalp ure calorimetric measure an-1-ol	uid or two-phas ponent 1 v	[Y1] .180E+04	and constant T	
State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .586000E-01 .123600E+00 .123600E+00 .316600E+00 .376900E+00 .428800E+00 .428800E+00 .522600E+00 .563000E+00	Two-component s Pure component Pure component Pure component Pure component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_8H_{18}O$, Oct. 2. $C_{12}H_{24}O_2$, M 8150E+03 [Y1] .449100E+03 .810300E+03 .109940E+04 .130590E+04 .153530E+04 .153450E+04 .150990E+04 .146800E+04	system, single-phase liqu 1, liquid 2, liquid Temperature Mole fraction of com Molar excess enthalp ure calorimetric measure an-1-ol	uid or two-phas ponent 1 v	[Y1] .180E+04	ind constant T	
State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .586000E-01 .123600E+00 .188800E+00 .376900E+00 .376900E+00 .428800E+00 .428800E+00 .522600E+00 .563000E+00 .586800E+00	Two-component s Pure component Pure component Pure component Pure component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_8H_{18}O$, Oct. 2. $C_{12}H_{24}O_2$, M 8150E+03 [Y1] .449100E+03 .810300E+03 .109940E+04 .130590E+04 .150750E+04 .1503450E+04 .150990E+04 .143800E+04 .143110E+04	system, single-phase liqu 1, liquid 2, liquid Temperature Mole fraction of com Molar excess enthalp ure calorimetric measure an-1-ol	uid or two-phas ponent 1 v	[Y1] .180E+04 .135E+04	and constant T	
State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .586000E-01 .123600E+00 .188800E+00 .316600E+00 .375900E+00 .428800E+00 .522600E+00 .522600E+00 .563000E+00 .586800E+00 .586800E+00 .625200E+00	Two-components Pure component Pure component Pure component Pure component Pure component [P1] T/K, [X1] $x_1/-,$ [Y1] HE/Jmol ⁻¹ , Direct low-pressu 1. CgH1gO, Oct. 2. C12H24O2, M 8150E+03 [Y1] .449100E+03 .810300E+03 .109940E+04 .130590E+04 .150750E+04 .153450E+04 .153450E+04 .153450E+04 .143110E+04 .139190E+04	system, single-phase liqu 1, liquid 2, liquid Temperature Mole fraction of com Molar excess enthalp ure calorimetric measure an-1-ol	uid or two-phas ponent 1 v	[Y1] .180E+04 .135E+04	and constant T	
State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .586000E-01 .123600E+00 .188800E+00 .255300E+00 .316600E+00 .375900E+00 .428800E+00 .522600E+00 .522600E+00 .586800E+00 .625200E+00 .625200E+00 .654100E+00	Two-component s Pure component Pure component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. CgH1gO, Octa 2. C12H24O2, M 8150E+03 [Y1] .449100E+03 .810300E+03 .109940E+04 .130590E+04 .153530E+04 .153450E+04 .153450E+04 .150990E+04 .143110E+04 .139190E+04 .132870E+04	system, single-phase liqu 1, liquid 2, liquid Temperature Mole fraction of com Molar excess enthalp ure calorimetric measure an-1-ol	uid or two-phas ponent 1 v	[Y1] .180E+04 .135E+04	and constant T	
State: Parameters: Variables: Method: Components: [P1] = .293 [X1] .586000E-01 .123600E+00 .188800E+00 .255300E+00 .316600E+00 .375900E+00 .428800E+00 .522600E+00 .563000E+00 .625200E+00 .625200E+00 .654100E+00 .697500E+00 .742400E+00	Two-component s Pure component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] HE/Jmol-1, Direct low-pressu 1. CgH1gO, Oct. 2. C12H24O2, M 8150E+03 [Y1] .449100E+03 .810300E+03 .109940E+04 .130590E+04 .153530E+04 .153450E+04 .150990E+04 .14310E+04 .139190E+04 .132870E+04 .122590E+04 .122590E+04	system, single-phase liqu 1, liquid 2, liquid Temperature Mole fraction of com Molar excess enthalp ure calorimetric measure an-1-ol	uid or two-phas ponent 1 v	[Y1] .180E+04 .135E+04	and constant T	
State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .586000E-01 .123600E+00 .188800E+00 .255300E+00 .316600E+00 .375900E+00 .522600E+00 .563000E+00 .563000E+00 .697500E+00 .697500E+00 .742400E+00 .788800E+00 .788800E+00	Two-component s Pure component Pure component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_8H_{18}O$, Oct. 2. $C_{12}H_{24}O_2$, M 8150E+03 [Y1] .449100E+03 .810300E+03 .109940E+04 .130590E+04 .153530E+04 .153530E+04 .153450E+04 .153450E+04 .132870E+04 .132870E+04 .132870E+04 .132870E+04 .132870E+04 .132870E+04 .132870E+04 .132870E+04 .122590E+04 .10560E+04 .10560E+04	system, single-phase liqu 1, liquid 2, liquid Temperature Mole fraction of com Molar excess enthalp ure calorimetric measure an-1-ol	uid or two-phas ponent 1 v	[Y1] .180E+04 .135E+04	and constant T	
State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .586000E-01 .123600E+00 .123600E+00 .316600E+00 .375900E+00 .428800E+00 .522600E+00 .563000E+00 .586800E+00 .697500E+00 .742400E+00 .788800E+00 .788800E+00 .835000E+00	Two-component s Pure component s Pure component s Pure component s Pure component s [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_8H_{18}O$, Oct. 2. $C_{12}H_{24}O_2$, M 8150E+03 [Y1] .449100E+03 .810300E+03 .109940E+04 .130590E+04 .153530E+04 .153530E+04 .153450E+04 .153450E+04 .139190E+04 .132870E+04 .122590E+04 .10560E+04 .10560E+04 .397800E+03	system, single-phase liqu 1, liquid 2, liquid Temperature Mole fraction of com Molar excess enthalp an-1-ol fethyl undecanoate	uid or two-phas ponent 1 v	[Y1] .180E+04 .135E+04 .900E+03	and constant T	
State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .586000E-01 .123600E+00 .355300E+00 .316600E+00 .375900E+00 .428800E+00 .522600E+00 .563000E+00 .563000E+00 .586800E+00 .742400E+00 .788800E+00 .835000E+00 .835000E+00 .832100E+00 .822100E+00	Two-component s Pure component s Pure component s Pure component s Pure component s [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_8H_{18}O$, Oct. 2. $C_{12}H_{24}O_2$, M 8150E+03 [Y1] .449100E+03 .810300E+03 .109940E+04 .130590E+04 .153530E+04 .153530E+04 .153450E+04 .153450E+04 .153990E+04 .132870E+04 .132870E+04 .122590E+04 .10560E+04 .10560E+04 .9964400E+03 .797800E+03 .604200E+03	system, single-phase liqu 1, liquid 2, liquid Temperature Mole fraction of com Molar excess enthalp an-1-ol fethyl undecanoate	uid or two-phas ponent 1 v	[Y1] .180E+04 .135E+04 .900E+03	and constant T	
State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .586000E-01 .123600E+00 .123600E+00 .316600E+00 .375900E+00 .316600E+00 .375900E+00 .522600E+00 .563000E+00 .586800E+00 .586800E+00 .882100E+00 .882100E+00 .82200E+00 .8200E+00 .8200E+00	Two-component s Pure component s [Y1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_8H_{18}O$, Oct 2. $C_{12}H_{24}O_2$, M 8150E+03 [Y1] .449100E+03 .810300E+03 .810300E+04 .130590E+04 .153530E+04 .153530E+04 .153450E+04 .153450E+04 .153450E+04 .132870E+04 .132870E+04 .132870E+04 .122590E+04 .10560E+03 .797800E+03 .604200E+03 .604200E+03 .400300E+03	system, single-phase liqu 1, liquid 2, liquid Temperature Mole fraction of com Molar excess enthalp an-1-ol fethyl undecanoate	uid or two-phas ponent 1 v	[Y1] .180E+04 .135E+04 .900E+03	and constant T	
State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .586000E-01 .123600E+00 .355300E+00 .316600E+00 .375900E+00 .428800E+00 .522600E+00 .563000E+00 .563000E+00 .586800E+00 .742400E+00 .788800E+00 .835000E+00 .835000E+00 .832100E+00 .822100E+00	Two-component s Pure component s [Y1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_8H_{18}O$, Oct 2. $C_{12}H_{24}O_2$, M 8150E+03 [Y1] .449100E+03 .810300E+03 .810300E+04 .130590E+04 .153530E+04 .153530E+04 .153450E+04 .153450E+04 .153450E+04 .132870E+04 .132870E+04 .132870E+04 .122590E+04 .10560E+03 .797800E+03 .604200E+03 .604200E+03 .400300E+03	system, single-phase liqu 1, liquid 2, liquid Temperature Mole fraction of com Molar excess enthalp an-1-ol fethyl undecanoate	uid or two-phas ponent 1 v	[Y1] .180E+04 .135E+04 .900E+03	and constant T	
State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .586000E-01 .123600E+00 .123600E+00 .316600E+00 .375900E+00 .316600E+00 .375900E+00 .522600E+00 .563000E+00 .586800E+00 .586800E+00 .882100E+00 .882100E+00 .82200E+00 .8200E+00 .8200E+00	Two-component s Pure component s [Y1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_8H_{18}O$, Oct 2. $C_{12}H_{24}O_2$, M 8150E+03 [Y1] .449100E+03 .810300E+03 .810300E+04 .130590E+04 .153530E+04 .153530E+04 .153450E+04 .153450E+04 .153450E+04 .132870E+04 .132870E+04 .132870E+04 .122590E+04 .10560E+03 .797800E+03 .604200E+03 .604200E+03 .400300E+03	system, single-phase liqu 1, liquid 2, liquid Temperature Mole fraction of com Molar excess enthalp an-1-ol fethyl undecanoate	uid or two-phas ponent 1 v	[Y1] .180E+04 .135E+04 .900E+03	and constant T	
State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .586000E-01 .123600E+00 .123600E+00 .316600E+00 .375900E+00 .316600E+00 .375900E+00 .522600E+00 .563000E+00 .586800E+00 .586800E+00 .882100E+00 .882100E+00 .82200E+00 .8200E+00 .8200E+00	Two-component s Pure component s [Y1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_8H_{18}O$, Oct 2. $C_{12}H_{24}O_2$, M 8150E+03 [Y1] .449100E+03 .810300E+03 .810300E+04 .130590E+04 .153530E+04 .153530E+04 .153450E+04 .153450E+04 .153450E+04 .132870E+04 .132870E+04 .132870E+04 .122590E+04 .10560E+03 .797800E+03 .604200E+03 .604200E+03 .400300E+03	system, single-phase liqu 1, liquid 2, liquid Temperature Mole fraction of com Molar excess enthalp an-1-ol fethyl undecanoate	uid or two-phas ponent 1 v	[Y1] .180E+04 .135E+04 .900E+03 .450E+03	and constant T	
State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .586000E-01 .123600E+00 .123600E+00 .316600E+00 .375900E+00 .316600E+00 .375900E+00 .522600E+00 .563000E+00 .586800E+00 .625200E+00 .625200E+00 .788800E+00 .832100E+00 .832100E+00 .82200E+00 .8200E+00 .8200	Two-component s Pure component s [Y1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_8H_{18}O$, Oct 2. $C_{12}H_{24}O_2$, M 8150E+03 [Y1] .449100E+03 .810300E+03 .810300E+04 .130590E+04 .153530E+04 .153530E+04 .153450E+04 .153450E+04 .153450E+04 .132870E+04 .132870E+04 .132870E+04 .122590E+04 .10560E+03 .797800E+03 .604200E+03 .604200E+03 .400300E+03	system, single-phase liqu 1, liquid 2, liquid Temperature Mole fraction of com Molar excess enthalp an-1-ol fethyl undecanoate	uid or two-phas ponent 1 v	[Y1] .180E+04 .135E+04 .900E+03 .450E+03	o [P1] = .298150E+03	

		EAT OF MIXIN				ORTJ0954.
State:			hase liquid or two-	phase liquid-liqu	iid (LL)	
	Pure componen					
D	Pure component					
Parameters:	[P1] <i>T/</i> K,	Temperature				
Variables:	[X1] $x_1/-$,	Mole fraction , Molar excess	of component 1			
Method:	Direct low-press	sure calorimetric	measurement of H	E at variable x1	and constant T	
Components:	1. C ₈ H ₁₈ O, Oc			1		
-	2. C14H28O2, 1		oate			
[P1] = .29	8150E+03			[Y1]		
[X1]	[Y1]			.180E+04		
.648000E-01	.454500E+03			1	- (71) 2001505 02	
.136800E+00					○ [P1] = .298150E+03	
.206200E+00						
.275300E+00						
.339800E+00				.135E+04	0 0	
.401600E+00				.1556+04		o 1
.457000E+00					<u> </u>	·.
.506700E+00						Ŭ.
.551600E+00					9	0
.588500E+00				1	/	
.626700E+00				.900E+03	. /	0 ⁰ 00
.656900E+00					ò	
.698500E+00	.131070E+04				Ĭ.	0
.746100E+00					1	
.748100E+00	.109130E+04					<u> </u>
.793200E+00 .837900E+00					- (
				.450E+03	- ġ	Q -
.878400E+00 .912800E+00	.629200E+03 .471400E+03				1	· · · ·
.912800E+00						o
.975500E+00	.306700E+03				1	
.973300E+00	.145500E+03				[9
			21.54	.000E+00		
					.50E+00	
		1				IX1
						[X1
Convright@ 1995 F	I DATA SARI F	nce All rights rese				[X1
	LDATA SARL Fra			N		
roperty Code:	[HMSD1000] HI	EAT OF MIXIN	G AND SOLUTIO			
roperty Code: state:	[HMSD1000] HI Two-component	EAT OF MIXIN system, single-ph			d (LL)	
roperty Code: state:	[HMSD1000] HI Two-component Pure component	EAT OF MIXING system, single-ph 1, liquid	G AND SOLUTIO		d (LL)	
Property Code: State:	[HMSD1000] HI Two-component Pure component Pure component	EAT OF MIXIN system, single-ph 1, liquid 2, liquid	G AND SOLUTIO		d (LL)	
Property Code: State: Parameters:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K,	EAT OF MIXIN system, single-ph 1, liquid 2, liquid Temperature	G AND SOLUTIC ase liquid or two-p		d (LL)	
roperty Code: itate: arameters: ariables:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$,	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction	G AND SOLUTIC ase liquid or two-p of component 1		d (LL)	
roperty Code: itale: arameters: ariables:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ .	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess of	G AND SOLUTIC ase liquid or two-p of component 1	ohase liquid-liqui		
roperty Code: tate: arameters: ariables: lethod: omponents:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/}$ -, [Y1] $H^{E}/Jmol^{-1}$, Direct low-press 1. C ₈ H ₁₈ O, Oct	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess of the calorimetric man-1-ol	G AND SOLUTIC ase liquid or two-p of component 1 enthalpy neasurement of H ^I	ohase liquid-liqui		
Property Code: State: Parameters: ariables: Station: Components:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₈ H ₁₈ O, Oct 2. C ₁₆ H ₃₂ O ₂ , M	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess of the calorimetric man-1-ol	G AND SOLUTIC ase liquid or two-p of component 1 enthalpy neasurement of H ^I	bhase liquid-liqui ³ at variable x ₁ a		
roperty Code: tate: arameters: ariables: fethod: omponents: [P1] = .298	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₈ H ₁₈ O, Octa 2. C ₁₆ H ₃₂ O ₂ , M 150E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess of the calorimetric man-1-ol	G AND SOLUTIC ase liquid or two-p of component 1 enthalpy neasurement of H ^I	bhase liquid-liqui ³ at variable x ₁ an [Y1]		
Property Code: itate: arameters: ariables: fethod: components: [P1] = .298 [X1]	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^{E}/Jmol^{-1}$, Direct low-pressu 1. C ₈ H ₁₈ O, Oct 2. C ₁₆ H ₃₂ O ₂ , M 150E+03 [Y1]	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess of the calorimetric man-1-ol	G AND SOLUTIC ase liquid or two-p of component 1 enthalpy neasurement of H ^I	bhase liquid-liqui ³ at variable x ₁ a	nd constant T	ORTJ0954.07
roperty Code: tate: arameters: ariables: fethod: omponents: [P1] = .298 [X1] .894000E-01	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^{E}/Jmol^{-1}$, Direct low-pressu 1. C8H18O, Oct 2. C16H32O2, M 150E+03 [Y1] .682700E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess of the calorimetric man-1-ol	G AND SOLUTIC ase liquid or two-p of component 1 enthalpy neasurement of H ^I	bhase liquid-liqui ³ at variable x ₁ an [Y1]	nd constant T	ORTJ0954.07
roperty Code: tate: arameters: ariables: fethod: omponents: [P1] = .298 [X1] .894000E-01	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^{E}/Jmol^{-1}$, Direct low-pressu 1. C ₈ H ₁₈ O, Oct 2. C ₁₆ H ₃₂ O ₂ , M 150E+03 [Y1]	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess of the calorimetric man-1-ol	G AND SOLUTIC ase liquid or two-p of component 1 enthalpy neasurement of H ^I	bhase liquid-liqui ³ at variable x ₁ an [Y1]	nd constant T	ORTJ0954.07
roperty Code: tate: arameters: ariables: [ethod: omponents: [P1] = .298 [X1] .894000E-01 .169100E+00 .240500E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^{E}/Jmol^{-1}$, Direct low-pressu 1. C8H18O, Oct 2. C16H32O2, M 150E+03 [Y1] .682700E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess of the calorimetric man-1-ol	G AND SOLUTIC ase liquid or two-p of component 1 enthalpy neasurement of H ^I	bhase liquid-liqui ³ at variable x ₁ an [Y1]	nd constant T	ORTJ0954.0
roperty Code: tate: arameters: ariables: [ethod: omponents: [P1] = .298 [X1] .894000E-01 .169100E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^{E}/Jmol^{-1}$, Direct low-pressu 1. C8H18O, Oct 2. C16H32O2, M 150E+03 [Y1] .682700E+03 .106790E+04	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess of the calorimetric man-1-ol	G AND SOLUTIC ase liquid or two-p of component 1 enthalpy neasurement of H ^I	bhase liquid-liqui ³ at variable x ₁ an [Y1]	nd constant T	ORTJ0954.07
roperty Code: tate: arameters: ariables: [ethod: omponents: [P1] = .298 [X1] .894000E-01 .169100E+00 .240500E+00 .301700E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^{E}/Jmol^{-1}$, Direct low-pressu 1. C8H18O, Oct 2. C16H32O2, M 150E+03 [Y1] .682700E+03 .106790E+04 .133420E+04	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess of the calorimetric man-1-ol	G AND SOLUTIC ase liquid or two-p of component 1 enthalpy neasurement of H ^I	bhase liquid-liqui at variable x ₁ an [Y1] .180E+04	nd constant T	ORTJ0954.07
roperty Code: tate: arameters: ariables: [ethod: omponents: [P1] = .298 [X1] .894000E-01 .169100E+00 .240500E+00 .301700E+00 .359900E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^{E}/Jmol^{-1}$, Direct low-pressu 1. C8H18O, Oct 2. C16H32O2, M 150E+03 [Y1] .682700E+03 .106790E+04 .133420E+04 .148920E+04	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess of the calorimetric man-1-ol	G AND SOLUTIC ase liquid or two-p of component 1 enthalpy neasurement of H ^I	bhase liquid-liqui ³ at variable x ₁ an [Y1]	nd constant T	ORTJ0954.07
roperty Code: tate: arameters: ariables: [ethod: omponents: [P1] = .298 [X1] .894000E-01 .169100E+00 .240500E+00 .301700E+00 .359900E+00 .412700E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^{E}/Jmol^{-1}$, Direct low-pressu 1. C8H18O, Octa 2. C16H32O2, M 150E+03 [Y1] .682700E+03 .106790E+04 .133420E+04 .148920E+04 .157470E+04 .160590E+04	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess of the calorimetric man-1-ol	G AND SOLUTIC ase liquid or two-p of component 1 enthalpy neasurement of H ^I	bhase liquid-liqui at variable x ₁ an [Y1] .180E+04	nd constant T	ORTJ0954.07
roperty Code: tate: arameters: ariables: [ethod: omponents: [P1] = .298 [X1] .894000E-01 .169100E+00 .240500E+00 .301700E+00 .359900E+00 .412700E+00 .460400E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressu 1. CgH1gO, Oct 2. C16H32O2, M 150E+03 [Y1] .682700E+03 .106790E+04 .133420E+04 .133420E+04 .157470E+04 .160590E+04 .160340E+04	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess of the calorimetric man-1-ol	G AND SOLUTIC ase liquid or two-p of component 1 enthalpy neasurement of H ^I	bhase liquid-liqui at variable x ₁ an [Y1] .180E+04	nd constant T	ORTJ0954.07
Property Code: state: Parameters: ariables: fethod: Components: [P1] = .298 [X1] .894000E-01 .169100E+00 .301700E+00 .359900E+00 .412700E+00 .460400E+00 .502300E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressu 1. C8H18O, Oct 2. C16H32O2, M 150E+03 [Y1] .682700E+03 .106790E+04 .133420E+04 .148920E+04 .160390E+04 .160340E+04 .157990E+04	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess of the calorimetric man-1-ol	G AND SOLUTIC ase liquid or two-p of component 1 enthalpy neasurement of H ^I	bhase liquid-liqui at variable x ₁ an [Y1] .180E+04	nd constant T	ORTJ0954.07
roperty Code: tate: arameters: ariables: fethod: omponents: [P1] = .298 [X1] .894000E-01 .169100E+00 .240500E+00 .301700E+00 .3059900E+00 .412700E+00 .460400E+00 .502300E+00 .544400E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. CgH1gO, Oct 2. C16H32O2, M 150E+03 [Y1] .682700E+03 .106790E+04 .133420E+04 .133420E+04 .160590E+04 .160340E+04 .157990E+04 .154500E+04	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess of the calorimetric man-1-ol	G AND SOLUTIC ase liquid or two-p of component 1 enthalpy neasurement of H ^I	Phase liquid-liqui at variable x ₁ at [Y1] .180E+04 .135E+04	nd constant T	ORTJ0954.07
roperty Code: tate: arameters: ariables: fethod: omponents: [P1] = .298 [X1] .894000E-01 .169100E+00 .240500E+00 .301700E+00 .305900E+00 .412700E+00 .460400E+00 .502300E+00 .544400E+00 .583200E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressu 1. C8H18O, Oct 2. C16H32O2, M 150E+03 [Y1] .682700E+03 .106790E+04 .133420E+04 .150590E+04 .160340E+04 .157990E+04 .154500E+04 .149150E+04	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess of the calorimetric man-1-ol	G AND SOLUTIC ase liquid or two-p of component 1 enthalpy neasurement of H ^I	bhase liquid-liqui at variable x ₁ an [Y1] .180E+04	nd constant T	ORTJ0954.0
roperty Code: tate: arameters: ariables: fethod: omponents: [P1] = .298 [X1] .894000E-01 .169100E+00 .240500E+00 .301700E+00 .412700E+00 .412700E+00 .502300E+00 .502300E+00 .583200E+00 .618700E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressu 1. CgH1gO, Oct 2. C16H32O2, M 150E+03 [Y1] .682700E+03 .106790E+04 .133420E+04 .154500E+04 .157990E+04 .154500E+04 .149150E+04 .142180E+04	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess of the calorimetric man-1-ol	G AND SOLUTIC ase liquid or two-p of component 1 enthalpy neasurement of H ^I	Phase liquid-liqui at variable x ₁ at [Y1] .180E+04 .135E+04	nd constant T	ORTJ0954.07
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roperty Code: tate: arameters: ariables: fethod: omponents: [P1] = .298 [X1] .894000E-01 .169100E+00 .240500E+00 .301700E+00 .305900E+00 .412700E+00 .502300E+00 .544400E+00 .583200E+00 .618700E+00 .656800E+00 .703200E+00	[HMSD1000] HI Two-component Pure component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. CgH1gO, Oct 2. C16H32O2, M 150E+03 [Y1] .682700E+03 .106790E+04 .13420E+04 .160590E+04 .160590E+04 .160340E+04 .154500E+04 .154500E+04 .149150E+04 .134140E+04 .123700E+04	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess of the calorimetric man-1-ol	G AND SOLUTIC ase liquid or two-p of component 1 enthalpy neasurement of H ^I	^E at variable x ₁ at [Y1] .180E+04 .135E+04	nd constant T	ORTJ0954.07
roperty Code: tate: arameters: ariables: fethod: omponents: [P1] = .298 [X1] .894000E-01 .169100E+00 .240500E+00 .301700E+00 .301700E+00 .4060400E+00 .502300E+00 .542400E+00 .583200E+00 .618700E+00 .618700E+00 .618700E+00 .757200E+00	[HMSD1000] HI Two-component Pure component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. CgH1gO, Oct 2. C16H32O2, M 150E+03 [Y1] .682700E+03 .106790E+04 .133420E+04 .133420E+04 .160340E+04 .160340E+04 .157990E+04 .154500E+04 .154500E+04 .134140E+04 .123700E+04 .106670E+04	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess of the calorimetric man-1-ol	G AND SOLUTIC ase liquid or two-p of component 1 enthalpy neasurement of H ^I	^E at variable x ₁ at [Y1] .180E+04 .135E+04	nd constant T	ORTJ0954.07
roperty Code: tate: arameters: ariables: fethod: omponents: [P1] = .298 [X1] .894000E-01 .169100E+00 .240500E+00 .301700E+00 .301700E+00 .412700E+00 .502300E+00 .544400E+00 .583200E+00 .618700E+00 .618700E+00 .656800E+00 .757200E+00 .812000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. CgH1gO, Oct 2. C16H32O2, M 150E+03 [Y1] .682700E+03 .106790E+04 .133420E+04 .157470E+04 .160590E+04 .160590E+04 .154500E+04 .154500E+04 .154500E+04 .154500E+04 .134140E+04 .123700E+04 .106670E+04 .890200E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess of the calorimetric man-1-ol	G AND SOLUTIC ase liquid or two-p of component 1 enthalpy neasurement of H ^I	^E at variable x ₁ at [Y1] .180E+04 .135E+04 .900E+03	nd constant T	ORTJ0954.07
roperty Code: tate: arameters: ariables: fethod: omponents: [P1] = .298 [X1] .894000E-01 .169100E+00 .240500E+00 .301900E+00 .301900E+00 .412700E+00 .502300E+00 .544400E+00 .532200E+00 .656800E+00 .757200E+00 .856800E+00 .856800E+00 .856800E+00 .856800E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₈ H ₁₈ O, Oct 2. C ₁₆ H ₃₂ O ₂ , M 150E+03 [Y1] .682700E+03 .106790E+04 .133420E+04 .13420E+04 .160390E+04 .160390E+04 .160340E+04 .157990E+04 .154500E+04 .134140E+04 .123700E+04 .106670E+04 .890200E+03 .683100E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess of the calorimetric man-1-ol	G AND SOLUTIC ase liquid or two-p of component 1 enthalpy neasurement of H ^I	^E at variable x ₁ at [Y1] .180E+04 .135E+04	nd constant T	ORTJ0954.07
roperty Code: iate: arameters: ariables: fethod: components: [P1] = .298 [X1] .894000E-01 .169100E+00 .240500E+00 .301700E+00 .301700E+00 .412700E+00 .502300E+00 .544400E+00 .583200E+00 .583200E+00 .568800E+00 .757200E+00 .81200E+00 .81200E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. CgH1gO, Oct 2. C16H32O2, M 150E+03 [Y1] .682700E+03 .106790E+04 .133420E+04 .157470E+04 .160390E+04 .160390E+04 .154500E+04 .154500E+04 .154500E+04 .154500E+04 .123700E+04 .123700E+04 .106670E+04 .106670E+04 .890200E+03 .683100E+03 .450000E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess of the calorimetric man-1-ol	G AND SOLUTIC ase liquid or two-p of component 1 enthalpy neasurement of H ^I	^E at variable x ₁ at [Y1] .180E+04 .135E+04 .900E+03	nd constant T	0
roperty Code: iate: arameters: ariables: fethod: components: [P1] = .298 [X1] .894000E-01 .169100E+00 .240500E+00 .301700E+00 .301700E+00 .412700E+00 .502300E+00 .544400E+00 .53220E+00 .656800E+00 .757200E+00 .856800E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₈ H ₁₈ O, Oct 2. C ₁₆ H ₃₂ O ₂ , M 150E+03 [Y1] .682700E+03 .106790E+04 .133420E+04 .13420E+04 .160390E+04 .160390E+04 .160340E+04 .157990E+04 .154500E+04 .134140E+04 .123700E+04 .106670E+04 .890200E+03 .683100E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess of the calorimetric man-1-ol	G AND SOLUTIC ase liquid or two-p of component 1 enthalpy neasurement of H ^I	^E at variable x ₁ at [Y1] .180E+04 .135E+04 .900E+03	nd constant T	ORTJ0954.07
roperty Code: iate: arameters: ariables: fethod: components: [P1] = .298 [X1] .894000E-01 .169100E+00 .240500E+00 .301700E+00 .301700E+00 .412700E+00 .502300E+00 .544400E+00 .583200E+00 .583200E+00 .568800E+00 .757200E+00 .81200E+00 .81200E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. CgH1gO, Oct 2. C16H32O2, M 150E+03 [Y1] .682700E+03 .106790E+04 .133420E+04 .157470E+04 .160390E+04 .160390E+04 .154500E+04 .154500E+04 .154500E+04 .154500E+04 .123700E+04 .123700E+04 .106670E+04 .106670E+04 .890200E+03 .683100E+03 .450000E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess of the calorimetric man-1-ol	G AND SOLUTIC ase liquid or two-p of component 1 enthalpy neasurement of H ^I	^E at variable x ₁ at [Y1] .180E+04 .135E+04 .900E+03	nd constant T	ORTJ0954.07
roperty Code: tate: arameters: ariables: fethod: omponents: [P1] = .298 [X1] .894000E-01 .169100E+00 .240500E+00 .240500E+00 .301700E+00 .412700E+00 .412700E+00 .502300E+00 .544400E+00 .583200E+00 .656800E+00 .757200E+00 .856800E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. CgH1gO, Oct 2. C16H32O2, M 150E+03 [Y1] .682700E+03 .106790E+04 .133420E+04 .157470E+04 .160390E+04 .160390E+04 .154500E+04 .154500E+04 .154500E+04 .154500E+04 .123700E+04 .123700E+04 .106670E+04 .106670E+04 .890200E+03 .683100E+03 .450000E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess of the calorimetric man-1-ol	G AND SOLUTIC ase liquid or two-p of component 1 enthalpy neasurement of H ^I	^E at variable x ₁ at [Y1] .180E+04 .135E+04 .900E+03	nd constant T	ORTJ0954.07
roperty Code: tate: arameters: ariables: fethod: omponents: [P1] = .298 [X1] .894000E-01 .169100E+00 .240500E+00 .240500E+00 .301700E+00 .412700E+00 .412700E+00 .502300E+00 .544400E+00 .583200E+00 .656800E+00 .757200E+00 .856800E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. CgH1gO, Oct 2. C16H32O2, M 150E+03 [Y1] .682700E+03 .106790E+04 .133420E+04 .157470E+04 .160390E+04 .160390E+04 .154500E+04 .154500E+04 .154500E+04 .154500E+04 .123700E+04 .123700E+04 .106670E+04 .106670E+04 .890200E+03 .683100E+03 .450000E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess of the calorimetric man-1-ol	G AND SOLUTIC ase liquid or two-p of component 1 enthalpy neasurement of H ^I	^E at variable x ₁ at [Y1] .180E+04 .135E+04 .900E+03	nd constant T	ORTJ0954.07
roperty Code: tate: arameters: ariables: fethod: omponents: [P1] = .298 [X1] .894000E-01 .169100E+00 .240500E+00 .240500E+00 .301700E+00 .412700E+00 .412700E+00 .502300E+00 .544400E+00 .583200E+00 .656800E+00 .757200E+00 .856800E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. CgH1gO, Oct 2. C16H32O2, M 150E+03 [Y1] .682700E+03 .106790E+04 .133420E+04 .157470E+04 .160390E+04 .160390E+04 .154500E+04 .154500E+04 .154500E+04 .154500E+04 .123700E+04 .123700E+04 .106670E+04 .106670E+04 .890200E+03 .683100E+03 .450000E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess of the calorimetric man-1-ol	G AND SOLUTIC ase liquid or two-p of component 1 enthalpy neasurement of H ^I	E at variable x1 at [Y1] .180E+04 .135E+04 .900E+03 .450E+03	o [P1] = .298150E+03	ORTJ0954.07
roperty Code: tate: arameters: ariables: fethod: omponents: [P1] = .298 [X1] .894000E-01 .169100E+00 .240500E+00 .240500E+00 .301700E+00 .412700E+00 .412700E+00 .502300E+00 .544400E+00 .583200E+00 .656800E+00 .757200E+00 .856800E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00 .812000E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. CgH1gO, Oct 2. C16H32O2, M 150E+03 [Y1] .682700E+03 .106790E+04 .133420E+04 .157470E+04 .160390E+04 .160390E+04 .154500E+04 .154500E+04 .154500E+04 .154500E+04 .123700E+04 .123700E+04 .106670E+04 .106670E+04 .890200E+03 .683100E+03 .450000E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess of the calorimetric man-1-ol	G AND SOLUTIC ase liquid or two-p of component 1 enthalpy neasurement of H ^I	E at variable x1 at [Y1] .180E+04 .135E+04 .900E+03 .450E+03	nd constant T	ORTJ0954.07

Property Code:	[HMSD1000] H	ance. All rights reserved. EAT OF MIXING AND SOLU'	ΓΙΟΝ	ORTJ0954.045
State:	Two-component	system, single-phase liquid or tw	o-phase liquid-liquid (LL)	
	Pure component	1, liquid		
	Pure component			
Parameters: Variables:	[P1] <i>T/</i> K, [X1] <i>x</i> ₁ /-,	Temperature Mole fraction of component 1		
ai labics.	[Y1] H^{E} /Jmol ⁻¹ ,	Molar excess enthalpy		
Method:	Direct low-press	ure calorimetric measurement of	$H^{\rm E}$ at variable x_1 and constant T	
Components:	1. C ₁₀ H ₂₀ O ₂ , M 2. C ₁₀ H ₂₂ O, D	Aethyl nonanoate		
[P1] = .29	8150E+03		13/41	
[X1]	[Y1]		[Y1] .180E+04	
.567000E-01	.309000E+03			,
.123400E+00	.509000E+03		○ [P1] = .298150E+03	
.190700E+00	.879400E+03		0.000.	
.256400E+00	.110220E+04		.135E+04	
.318400E+00	.127370E+04		.135E+04	, o
.374900E+00 .428400E+00	.139310E+04 .147510E+04		o o	
.478000E+00	.152520E+04			0
.522600E+00	.154740E+04		°	
.563200E+00			.900E+03	
.608700E+00			.5002+03	0
.669500E+00 .733800E+00	.148370E+04 .136130E+04			
.800100E+00	.116300E+04			
.867500E+00	.869700E+03		O	Q
.937200E+00	.489800E+03		.450E+03	° -
			0	
			.000E+00	
			.50E+00	
				[X1]
			ľ	
		nce. All rights reserved.		
Property Code:	[HMSD1000] HI	EAT OF MIXING AND SOLUT		ORTJ0954.054
Property Code:	[HMSD1000] HE Two-component	EAT OF MIXING AND SOLUT system, single-phase liquid or two	ION p-phase liquid-liquid (LL)	ORTJ0954.054
Property Code:	[HMSD1000] HE Two-component Pure component	EAT OF MIXING AND SOLUT system, single-phase liquid or two 1, liquid	TON p-phase liquid-liquid (LL)	ORTJ0954.054
Property Code: State: Parameters:	[HMSD1000] HE Two-component	EAT OF MIXING AND SOLUT system, single-phase liquid or two 1, liquid 2, liquid Temperature	p-phase liquid-liquid (LL)	ORTJ0954.054
Property Code: State: Parameters:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$,	EAT OF MIXING AND SOLUT system, single-phase liquid or two 1, liquid 2, liquid Temperature Mole fraction of component 1	p-phase liquid-liquid (LL)	ORTJ0954.054
Property Code: State: Parameters: Variables:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$,	EAT OF MIXING AND SOLUT system, single-phase liquid or two 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy	p-phase liquid-liquid (LL)	ORTJ0954.054
roperty Code: iate: arameters: ariables: fethod: omponents:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₁₀ H ₂₂ O, De	EAT OF MIXING AND SOLUT system, single-phase liquid or two 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of can-1-ol	p-phase liquid-liquid (LL)	ORTJ0954.054
Property Code: State: Parameters: ariables: fethod: Components:	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₁₀ H ₂₂ O, De 2. C ₁₂ H ₂₄ O ₂ , M	EAT OF MIXING AND SOLUT system, single-phase liquid or two 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of	p-phase liquid-liquid (LL)	ORTJ0954.054
roperty Code: itate: arameters: ariables: fethod: components: [P1] = .298	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₁₀ H ₂₂ O, De 2. C ₁₂ H ₂₄ O ₂ , M 150E+03	EAT OF MIXING AND SOLUT system, single-phase liquid or two 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of can-1-ol	p-phase liquid-liquid (LL) H^{E} at variable x_{1} and constant T [Y1]	ORTJ0954.054
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1]	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₁₀ H ₂₂ O, De 2. C ₁₂ H ₂₄ O ₂ , M S150E+03 [Y1]	EAT OF MIXING AND SOLUT system, single-phase liquid or two 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of can-1-ol	b-phase liquid-liquid (LL) H^{E} at variable x_{1} and constant T [Y1] .180E+04	ORTJ0954.054
Property Code: State: Parameters: Variables: Aethod: Components: [P1] = .298 [X1] .664000E-01	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₁₀ H ₂₂ O, De 2. C ₁₂ H ₂₄ O ₂ , M S150E+03 [Y1] .514700E+03	EAT OF MIXING AND SOLUT system, single-phase liquid or two 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of can-1-ol	p-phase liquid-liquid (LL) H^{E} at variable x_{1} and constant T [Y1]	ORTJ0954.054
Property Code: State: Parameters: Variables: fethod: Components: [P1] = .298 [X1] .664000E-01 .139300E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-pressu 1. C ₁₀ H ₂₂ O, De 2. C ₁₂ H ₂₄ O ₂ , M S150E+03 [Y1] .514700E+03 .897800E+03	EAT OF MIXING AND SOLUT system, single-phase liquid or two 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of can-1-ol	b-phase liquid-liquid (LL) $\frac{H^{E} \text{ at variable } x_{1} \text{ and constant } T}{[Y1]}$ $[Y1]$ $.180E+04$ $\circ [P1] = .298150E+03$	ORTJ0954.054
Property Code: State: Parameters: Variables: fethod: Components: [P1] = .298 [X1] .664000E-01 .139300E+00 .211800E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₁₀ H ₂₂ O, De 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .514700E+03 .897800E+03 .119150E+04	EAT OF MIXING AND SOLUT system, single-phase liquid or two 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of can-1-ol	b-phase liquid-liquid (LL) $\frac{H^{E} \text{ at variable } x_{1} \text{ and constant } T}{[Y1]}$ $[Y1]$ $.180E+04$ $\circ [P1] = .298150E+03$	ORTJ0954.054
roperty Code: itate: arameters: ariables: fethod: components: [P1] = .298 [X1] .664000E-01 .139300E+00 .211800E+00 .283300E+00 .347900E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H^E</i> /Jmol ⁻¹ , Direct low-pressu 1. C ₁₀ H ₂₂ O, De 2. C ₁₂ H ₂₄ O ₂ , M C150E+03 [Y1] .514700E+03 .897800E+03 .119150E+04 .138170E+04 .148320E+04	EAT OF MIXING AND SOLUT system, single-phase liquid or two 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of can-1-ol	b-phase liquid-liquid (LL) $\frac{H^{E} \text{ at variable } x_{1} \text{ and constant } T}{[Y1]}$ $[Y1]$ $.180E+04$ $\circ [P1] = .298150E+03$	ORTJ0954.054
Property Code: State: Parameters: Variables: fethod: Components: [P1] = .298 [X1] .664000E-01 .139300E+00 .211800E+00 .283300E+00 .347900E+00 .409300E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₁₀ H ₂₂ O, De 2. C ₁₂ H ₂₄ O ₂ , M C150E+03 [Y1] .514700E+03 .897800E+03 .119150E+04 .138170E+04 .148320E+04 .152950E+04	EAT OF MIXING AND SOLUT system, single-phase liquid or two 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of can-1-ol	b-phase liquid-liquid (LL) $\frac{H^{E} \text{ at variable } x_{1} \text{ and constant } T}{[Y1]}$ $[Y1]$ $.180E+04$ $\circ [P1] = .298150E+03$	ORTJ0954.054
Property Code: State: Parameters: Variables: fethod: Components: [P1] = .298 [X1] .664000E-01 .139300E+00 .211800E+00 .283300E+00 .347900E+00 .409300E+00 .465100E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₁₀ H ₂₂ O, De 2. C ₁₂ H ₂₄ O ₂ , M C150E+03 [Y1] .514700E+03 .897800E+03 .119150E+04 .138170E+04 .148320E+04 .152950E+04 .153000E+04	EAT OF MIXING AND SOLUT system, single-phase liquid or two 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of can-1-ol	$H^{E} \text{ at variable } x_{1} \text{ and constant } T$ $[Y1]$ $.180E+04$ $\circ [P1] = .298150E+03$ $\circ [\circ .0.0.0.0]$	ORTJ0954.054
Property Code: State: Parameters: Variables: fethod: Components: [P1] = .298 [X1] .664000E-01 .139300E+00 .211800E+00 .283300E+00 .347900E+00 .409300E+00 .465100E+00 .514700E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₁₀ H ₂₂ O, De 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .514700E+03 .897800E+03 .119150E+04 .138170E+04 .152950E+04 .153000E+04 .149850E+04	EAT OF MIXING AND SOLUT system, single-phase liquid or two 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of can-1-ol	b-phase liquid-liquid (LL) $\frac{H^{E} \text{ at variable } x_{1} \text{ and constant } T}{[Y1]}$ $[Y1]$ $.180E+04$ $\circ [P1] = .298150E+03$	ORTJ0954.054
Property Code: State: Parameters: Variables: /ethod: Components: [P1] = .298 [X1] .664000E-01 .139300E+00 .211800E+00 .283300E+00 .347900E+00 .409300E+00 .514700E+00 .558900E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₁₀ H ₂₂ O, De 2. C ₁₂ H ₂₄ O ₂ , M 3150E+03 [Y1] .514700E+03 .897800E+03 .119150E+04 .138170E+04 .148320E+04 .152950E+04 .149850E+04 .144830E+04	EAT OF MIXING AND SOLUT system, single-phase liquid or two 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of can-1-ol	$\frac{H^{E} \text{ at variable } x_{1} \text{ and constant } T}{[Y1]}$ $[Y1]$ $.180E+04$ $\circ [P1] = .298150E+03$ $\circ \circ $	ORTJ0954.054
Property Code: State: Parameters: Variables: fethod: Components: [P1] = .298 [X1] .664000E-01 .139300E+00 .211800E+00 .283300E+00 .347900E+00 .409300E+00 .465100E+00 .514700E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H</i> ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₁₀ H ₂₂ O, De 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .514700E+03 .897800E+03 .119150E+04 .138170E+04 .152950E+04 .153000E+04 .149850E+04	EAT OF MIXING AND SOLUT system, single-phase liquid or two 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of can-1-ol	b-phase liquid-liquid (LL) $\frac{H^{E} \text{ at variable } x_{1} \text{ and constant } T}{[Y1]}$ $[Y1]$ $.180E+04$ $\circ [P1] = .298150E+03$	ORTJ0954.054
roperty Code: itate: arameters: ariables: fethod: components: [P1] = .298 [X1] .664000E-01 .139300E+00 .211800E+00 .283300E+00 .347900E+00 .514700E+00 .558900E+00 .598500E+00 .662900E+00 .717800E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>HE</i> /Jmol ⁻¹ , Direct low-press 1. C ₁₀ H ₂₂ O, De 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .514700E+03 .897800E+03 .119150E+04 .138170E+04 .148320E+04 .152950E+04 .153000E+04 .144830E+04 .126930E+04 .126930E+04 .114050E+04	EAT OF MIXING AND SOLUT system, single-phase liquid or two 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of can-1-ol	$\frac{H^{E} \text{ at variable } x_{1} \text{ and constant } T}{[Y1]}$ $[Y1]$ $.180E+04$ $\circ [P1] = .298150E+03$ $\circ \circ $	ORTJ0954.054
Property Code: State: Parameters: Variables: Aethod: Components: [P1] = .298 [X1] .664000E-01 .139300E+00 .211800E+00 .283300E+00 .347900E+00 .514700E+00 .558900E+00 .598500E+00 .717800E+00 .775100E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₁₀ H ₂₂ O, De 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .514700E+03 .897800E+03 .119150E+04 .138170E+04 .148320E+04 .152950E+04 .153000E+04 .149850E+04 .14830E+04 .126930E+04 .114050E+04 .126930E+04 .114050E+04 .114050E+04	EAT OF MIXING AND SOLUT system, single-phase liquid or two 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of can-1-ol	$\frac{H^{E} \text{ at variable } x_{1} \text{ and constant } T}{[Y1]}$ $[Y1]$ $.180E+04$ $\circ [P1] = .298150E+03$ $\circ \circ $	ORTJ0954.054
Property Code: State: Parameters: Variables: (ethod: Components: [P1] = .298 [X1] .664000E-01 .139300E+00 .211800E+00 .283300E+00 .347900E+00 .558900E+00 .558900E+00 .598500E+00 .775100E+00 .775100E+00 .834500E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₁₀ H ₂₂ O, De 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .514700E+03 .897800E+03 .119150E+04 .138170E+04 .14830E+04 .14830E+04 .14830E+04 .14830E+04 .126930E+04 .126930E+04 .114050E+04 .126930E+04 .114050E+04 .126930E+04 .114050E+04 .162400E+03 .762400E+03	EAT OF MIXING AND SOLUT system, single-phase liquid or two 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of can-1-ol	$\frac{H^{E} \text{ at variable } x_{1} \text{ and constant } T}{[Y1]}$ $[Y1]$ $.180E+04$ $\circ [P1] = .298150E+03$ $\circ \circ $	ORTJ0954.054
Property Code: State: Parameters: Variables: Aethod: Components: [P1] = .298 [X1] .664000E-01 .139300E+00 .211800E+00 .247900E+00 .409300E+00 .514700E+00 .598500E+00 .598500E+00 .598500E+00 .717800E+00 .834500E+00 .834500E+00 .893400E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H^E</i> /Jmol ⁻¹ , Direct low-pressu 1. C ₁₀ H ₂₂ O, De 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .514700E+03 .897800E+03 .119150E+04 .138170E+04 .14830E+04 .152950E+04 .14830E+04 .14830E+04 .14830E+04 .126930E	EAT OF MIXING AND SOLUT system, single-phase liquid or two 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of can-1-ol	$H^{E} \text{ at variable } x_{1} \text{ and constant } T$ $[Y1]$ $.180E+04$ $\circ [P1] = .298150E+03$ $.135E+04$ $.900E+03$	ORTJ0954.054
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .664000E-01 .139300E+00 .211800E+00 .283300E+00 .347900E+00 .409300E+00 .518900E+00 .598500E+00 .598500E+00 .775100E+00 .834500E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₁₀ H ₂₂ O, De 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .514700E+03 .897800E+03 .119150E+04 .138170E+04 .14830E+04 .14830E+04 .14830E+04 .14830E+04 .126930E+04 .126930E+04 .114050E+04 .126930E+04 .114050E+04 .126930E+04 .114050E+04 .162400E+03 .762400E+03	EAT OF MIXING AND SOLUT system, single-phase liquid or two 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of can-1-ol	$\frac{H^{E} \text{ at variable } x_{1} \text{ and constant } T}{[Y1]}$ $[Y1]$ $.180E+04$ $\circ [P1] = .298150E+03$ $\circ \circ $	ORTJ0954.054
Property Code: State: Parameters: Variables: (ethod: Components: [P1] = .298 [X1] .664000E-01 .139300E+00 .211800E+00 .2409300E+00 .409300E+00 .514700E+00 .598500E+00 .598500E+00 .598500E+00 .717800E+00 .775100E+00 .834500E+00 .834500E+00 .834500E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H^E</i> /Jmol ⁻¹ , Direct low-pressu 1. C ₁₀ H ₂₂ O, De 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .514700E+03 .897800E+03 .119150E+04 .138170E+04 .14830E+04 .152950E+04 .14830E+04 .14830E+04 .14830E+04 .126930E	EAT OF MIXING AND SOLUT system, single-phase liquid or two 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of can-1-ol	$H^{E} \text{ at variable } x_{1} \text{ and constant } T$ $[Y1]$ $.180E+04$ $\circ [P1] = .298150E+03$ $.135E+04$ $.900E+03$	ORTJ0954.054
Property Code: State: Parameters: Variables: (ethod: Components: [P1] = .298 [X1] .664000E-01 .139300E+00 .211800E+00 .2409300E+00 .409300E+00 .514700E+00 .598500E+00 .598500E+00 .598500E+00 .717800E+00 .775100E+00 .834500E+00 .834500E+00 .834500E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H^E</i> /Jmol ⁻¹ , Direct low-pressu 1. C ₁₀ H ₂₂ O, De 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .514700E+03 .897800E+03 .119150E+04 .138170E+04 .14830E+04 .152950E+04 .14830E+04 .14830E+04 .14830E+04 .126930E	EAT OF MIXING AND SOLUT system, single-phase liquid or two 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of can-1-ol	$H^{E} \text{ at variable } x_{1} \text{ and constant } T$ $[Y1]$ $.180E+04$ $\circ [P1] = .298150E+03$ $.135E+04$ $.900E+03$	ORTJ0954.054
Property Code: State: Parameters: Variables: Aethod: Components: [P1] = .298 [X1] .664000E-01 .139300E+00 .211800E+00 .247900E+00 .409300E+00 .514700E+00 .598500E+00 .598500E+00 .598500E+00 .717800E+00 .834500E+00 .834500E+00 .893400E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H^E</i> /Jmol ⁻¹ , Direct low-pressu 1. C ₁₀ H ₂₂ O, De 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .514700E+03 .897800E+03 .119150E+04 .138170E+04 .14830E+04 .152950E+04 .14830E+04 .14830E+04 .14830E+04 .126930E	EAT OF MIXING AND SOLUT system, single-phase liquid or two 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of can-1-ol	$H^{E} \text{ at variable } x_{1} \text{ and constant } T$ $[Y1]$ $.180E+04$ $\circ [P1] = .298150E+03$ $.135E+04$ $.900E+03$	ORTJ0954.054
Property Code: State: Parameters: Variables: fethod: Components: [P1] = .298 [X1] .664000E-01 .139300E+00 .211800E+00 .247900E+00 .409300E+00 .514700E+00 .598500E+00 .598500E+00 .717800E+00 .775100E+00 .834500E+00 .834500E+00 .834500E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H^E</i> /Jmol ⁻¹ , Direct low-pressu 1. C ₁₀ H ₂₂ O, De 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .514700E+03 .897800E+03 .119150E+04 .138170E+04 .14830E+04 .152950E+04 .14830E+04 .14830E+04 .14830E+04 .126930E	EAT OF MIXING AND SOLUT system, single-phase liquid or two 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of can-1-ol	$\frac{H^{E} \text{ at variable } x_{1} \text{ and constant } T}{[Y1]}$ $[Y1]$ $.180E+04$ $\circ [P1] = .298150E+03$ $.135E+04$ $.900E+03$ $.450E+03$ $.000E+00$	ORTJ0954.054
roperty Code: itate: arameters: ariables: fethod: components: [P1] = .298 [X1] .664000E-01 .139300E+00 .211800E+00 .283300E+00 .347900E+00 .54700E+00 .514700E+00 .598500E+00 .662900E+00 .717800E+00 .775100E+00 .834500E+00 .834500E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H^E</i> /Jmol ⁻¹ , Direct low-pressu 1. C ₁₀ H ₂₂ O, De 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .514700E+03 .897800E+03 .119150E+04 .138170E+04 .14830E+04 .152950E+04 .14830E+04 .14830E+04 .14830E+04 .126930E	EAT OF MIXING AND SOLUT system, single-phase liquid or two 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of can-1-ol	$\frac{H^{E} \text{ at variable } x_{1} \text{ and constant } T}{[Y1]}$ $[Y1]$ $.180E+04$ $\circ [P1] = .298150E+03$ $.135E+04$ $.900E+03$ $.450E+03$	
roperty Code: ate: ariables: ethod: omponents: [P1] = .298 [X1] 664000E-01 139300E+00 211800E+00 247900E+00 347900E+00 409300E+00 558900E+00 598500E+00 662900E+00 775100E+00 834500E+00 893400E+00	[HMSD1000] HI Two-component Pure component Pure component [P1] <i>T/K</i> , [X1] <i>x</i> ₁ /-, [Y1] <i>H^E</i> /Jmol ⁻¹ , Direct low-pressu 1. C ₁₀ H ₂₂ O, De 2. C ₁₂ H ₂₄ O ₂ , M 150E+03 [Y1] .514700E+03 .897800E+03 .119150E+04 .138170E+04 .14830E+04 .152950E+04 .14830E+04 .14830E+04 .14830E+04 .126930E	EAT OF MIXING AND SOLUT system, single-phase liquid or two 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of can-1-ol	$\frac{H^{E} \text{ at variable } x_{1} \text{ and constant } T}{[Y1]}$ $[Y1]$ $.180E+04$ $\circ [P1] = .298150E+03$ $.135E+04$ $.900E+03$ $.450E+03$ $.000E+00$	ORTJ0954.054

