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Excess enthalpies of 1,1,2,2-tetrachloroethane + n-alkanes. Measurement and comparison with the DISQUAC model

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Enthalpy-of-mixing measurements are reported at 298.15 K for 1,1,2,2-tetrachloroethane + n-alkanes (pentane through heptadecane). All the mixtures are endothermic with molar excess enthalpies increasing regularly with the chain length of the n-alkane. The experimental data are in good agreement with the values predicted by the DISQUAC group contribution model for n-alkanes containing less than eight C atoms. The discrepancies increase with the chain length of the n-alkane up to 10% (in the central range of composition) for heptadecane.

1. INTRODUCTION

In continuation of our systematic experimental studies on the excess molar enthalpies H^E of mixtures containing chloroalkanes (ORTJ0915), we have determined H^E of 1,1,2,2-tetrachloroethane + n-alkanes (pentane through heptadecane). H^E measurements have been published previously only for 1,1,2,2tetrachloroethane + n-hexane (PARJ04870). These data, along with data on vapor-liquid equilibria (FARJ0950) and excess volumes (LINJ0950), will be used to test the applicability of various groupcontribution models.

2. EXPERIMENTAL SECTION

2.1. Apparatus and Procedure

The experimental data were taken at atmospheric pressure by means of a Calvet type microcalorimeter, model MS-80D (SETARAM, Lyon, France) with a stainless steel batch mixing cell (volume ca. 8 cm³) and with negligible vapor phase. The temperature T was maintained constant to within 0.02 K at (298.15 ± 0.02) ITS-90. K. All temperatures are on The microcalorimeter was calibrated electrically after each measurement (see ORTJ0881). Check measurements on cyclohexane + hexane and benzene + heptadecane are in agreement to within 1 % (over central range of concentration) with the data reported in (MCGM0690) and (DIAM0742). The estimated uncertainties in the mole fraction composition x_i and H^E are, respectively, $\sigma(x_i) = 0.0005$ and $\sigma(H^E) = 0.02 |H^E|$ (over central range of concentration).

2.2. Materials

 $C_2H_2Cl_4$, 1,1,2,2-Tetrachloroethane Aldrich Chem. Co., Inc. (Milwaukee, WI, USA) material of stated purity > 99 mole %, was degassed ultrasonically, dried over molecular sieves Type 3A (reference 69828, from Fluka), and used without further purification. n(D,298.15 K) = 1.4918; $\rho_i(298.15 \text{ K})/\text{kg m}^{-3} = 1588.37$.

C₅H₁₂, Pentane. Fluka AG (Buchs, Switzerland) 'puriss' grade material of stated GLC purity > 99.5 mole %, purified as above; n(D, 298.15 K) = 1.3547; $\rho_i(298.15 \text{ K})/\text{kg m}^3 = 621.31$.

C₆H₁₄, Hexane. Fluka AG (Buchs, Switzerland) 'puriss' grade material of stated GLC purity > 99.5 mole %, purified as above; n(D, 298.15 K) = 1.3723; $\rho_i(298.15 \text{ K})/\text{kg m}^{-3} = 654.71$.

C₇H₁₆, Heptane. Fluka AG (Buchs, Switzerland) 'puriss' grade material of stated GLC purity > 99.5 mole %, purified as above; n(D, 298.15 K) = 1.3851; $\rho_i(298.15 \text{ K})/\text{kg m}^{-3} = 679.46$.

C₈H₁₈, Octane. Fluka AG (Buchs, Switzerland) 'puriss' grade material of stated GLC purity > 99.5 mole %, purified as above; n(D, 298.15 K) = 1.3951; $\rho_i(298.15 \text{ K})/\text{kg m}^{-3} = 698.29$.

C₉H₂₀, Nonane. Fluka AG (Buchs, Switzerland) 'purum' grade material of stated GLC purity > 99.0 mole %, purified as above; n(D, 298.15 K) = 1.4033; $\rho_i(298.15 \text{ K})/\text{kg m}^{-3} = 713.85$.

C₁₀H₂₂, Decane. Fluka AG (Buchs, Switzerland) 'purum' grade material of stated GLC purity > 99.0 mole %, purified as above; n(D, 298.15 K) = 1.4098; $\rho_i(298.15 \text{ K})/\text{kg m}^{-3} = 726.13$.

C₁₁H₂₄, Undecane. Fluka AG (Buchs, Switzerland) 'purum' grade material of stated GLC purity > 98.0 mole %, purified as above; n(D, 298.15 K) = 1.4154; $\rho_i(298.15 \text{ K})/\text{kg m}^{-3} = 736.80$.

 $C_{12}H_{26}$, Dodecane. Fluka AG (Buchs, Switzerland) 'purum' grade material of stated GLC purity > 98.0 mole %, purified as above; n(D, 298.15 K) = 1.4196; $\rho_i(298.15 \text{ K})/\text{kg m}^{-3} = 745.19$.

 $C_{13}H_{28}$, Tridecane. Fluka AG (Buchs, Switzerland) 'puriss' grade material of stated GLC purity > 99.5 mole %, purified as above; n(D, 298.15 K) = 1.4238; $\rho_i(298.15 \text{ K})/\text{kg m}^{-3} = 752.79$.

C₁₄H₃₀, Tetradecane. Fluka AG (Buchs, Switzerland) 'puriss' grade material of stated GLC purity > 99.5 mole %, purified as above; n(D, 298.15 K) = 1.4271; $\rho_i(298.15 \text{ K})/\text{kg m}^{-3} = 759.36$.

C₁₅H₃₂, Pentadecane. Fluka AG (Buchs, Switzerland) 'purum' grade material of stated GLC purity > 98 mole %, purified as above; n(D, 298.15 K) = 1.4298; $\rho_i(298.15 \text{ K})/\text{kg m}^{-3} = 764.80$.

C₁₆H₃₄, Hexadecane. Fluka AG (Buchs, Switzerland) 'purum' grade material of stated GLC purity > 98 mole %, purified as above; n(D, 298.15 K) = 1.4325; $\rho_i(298.15 \text{ K})/\text{kg m}^{-3} = 770.10$.

C₁₇**H**₃₆, **Heptadecane**. Fluka AG (Buchs, Switzerland) 'purum' grade material of stated GLC purity > 99 mole %, purified as above; n(D, 298.15 K) = 1.4347; $\rho_i(298.15 \text{ K})/\text{kg m}^{-3} = 774.33$.

3. RESULTS

The direct experimental H^E values are tabulated and graphed in the Appendix and saved on disk as Standard ELDATA Files **ORTJ0953.001** through **ORTJ0953.013**.

The data were fitted to Eq. (1):

$$H^{E}_{calc}/J \text{ mol}^{-1} = x_{1}x_{2}\Sigma A_{i}[x_{1}/(x_{1} + kx_{2})]^{i-1}$$
(1)

all points weighted equally. With an adjusted coefficient k and n = 4 coefficients A_i the standard deviations $\sigma(H^E)$, defined by Eq.(2):

$$\sigma(H^E) = [\Sigma(H^E_{calc} - H^E)^2 / (N - n)]^{1/2}$$
(2)

where N is the number of experimental values, are less than 10 J mol⁻¹ (ca. 0.4 % at $x_1 = 0.5$).

4. DISCUSSION AND CONCLUSIONS

All the mixtures are endothermic with H^E increasing regularly with the chain length of the n-alkane. Our results for 1,1,2,2-tetrachloroethane + n-hexane are in excellent agreement (ca 1 % at $x_1 = 0.5$) with the literature data (**PARJ04870**). The experimental equimolar H^E values for short-chain n-alkanes agree within better than 4 % with DISQUAC predictions, using previously published parameters (KEHH0880). It is interesting to note that these parameters were estimated from structure-property correlations taking into account the intramolecular proximity effect of the -CHCl₂ groups. Characteristic discrepancies (up to 10 %) are noted in mixtures with long-chain n-alkanes. These are usually attributed to the perturbation of the conformational order of long-chain n-alkanes when mixed with globular molecules such as 1,1,2,2tetrachloroethane (PATD0760).

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Y1 [$h^{E/B}$ mol ⁻¹ , Molar excess enthalpy Direct low-pressure calorimetric measurement of H^{E} at variable x_1 and constant T Components: 1. C2H2Cl ₂ , 1,1,2,2-Tetrachloroethane 2. C3H12, Pentane [Y1] Image: transmission of		[HMSD0001] HE	AT OF MIXING	AND SOLUTIO	N		ORTJ0953.001
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Convight@ 1995 EL.DATA SARL France. All rights reserved. .000E+00 .000E+03 .000E+00 .000E+03 .000E+00 .105E+04 .105E+04 .105E+04 .00E+00 .000E+00	.949000E+00				ó		
Image: Constraint of 1995 ELDATA SARL France. All rights reserved. .000E+00 .50E+00 [X1] Copyright@ 1995 ELDATA SARL France. All rights reserved. .000E+00 .50E+00 [X1] Copyright@ 1995 ELDATA SARL France. All rights reserved. .000E+00 .000E+00 .50E+00 [X1] Copyright@ 1995 ELDATA SARL France. All rights reserved. .000E+00 .000E+00 .000E+00 .000E+00 .000E+00 .00E+00 .00E+00 <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td>0</td>							0
Image: Constraint of 1995 ELDATA SARL France. All rights reserved. .000E+00 .50E+00 [X1] Copyright@ 1995 ELDATA SARL France. All rights reserved. .000E+00 .50E+00 [X1] Copyright@ 1995 ELDATA SARL France. All rights reserved. .000E+00 .000E+00 .50E+00 [X1] Copyright@ 1995 ELDATA SARL France. All rights reserved. .000E+00 .000E+00 .000E+00 .000E+00 .000E+00 .00E+00 .00E+00 <td></td> <td></td> <td></td> <td></td> <td></td> <td>\circ [P1] = .298150E+03</td> <td></td>						\circ [P1] = .298150E+03	
Image: Constraints Constraints Constraints Constraints Property Code: [HMSD0001] HEAT OF MIXING AND SOLUTION ORTJ0953.00 Prove component 3, liquid Pure component 1, liquid ORTJ0953.00 Parameters: [Y1] 7/K, Temperature Mole fraction of component 1 /arrameters: [Y1] 7/K, Temperature Mole fraction of component 1 /arrameters: [Y1] 7/F, Mole fraction of component 1 Importance excess enthalpy /dethod: Direct low-pressure calorimetric measurement of H ^E at variable x1 and constant T Components: 2C4H14, Hexane [Y1] Index excess enthalpy /dethod: Direct low-pressure calorimetric measurement of H ^E at variable x1 and constant T 200400E+00 .580400E+03 [Y1] .102192.014, 11,2,2-Tetrachloroethane 2.04900E+03 [Y1] .1032500E+00 .103040E+03 [Y1] .105E+04 .005E+04 .273300E +00 .109040E+04 .105E+04 .005E+04 .005E+04 .59100E+00 .11620E+04 .005E+04 .00E+04 .00E+04 .00E+04 .593300E+00 .117920E+04					.000E+00		
Image: Constraint Property Code: IMMSD0001 JHEAT OF MIXING AND SOLUTION ORT J0953.00 State: Two-component system, single-phase liquid Pure component 2, liquid ORT J0953.00 Parameters: [P1] 17K, Temperature //artables: Temperature [P1] 7K, Mole fraction of component 1 [Y1] <i>HE</i> /Jmol ⁻¹ . Molar excess enthalpy //dethod: Direct low-pressure calorimetric measurement of <i>HE</i> at variable x1 and constant <i>T</i> Components: 1. C2H2(A, 1, 1, 2, 2-Tetrachloroethane 2. C6H14. Hexane [P1] = .298150E+03 [Y1] (X1] [Y1] [X1] X[1] [Y1] .140E+04 .2. C6H14. Hexane [Y1] .140E+04 [P1] = .298150E+03 [Y1] .140E+04 .2. C37300E +00 .975700E+03 .339800E+00 .105E+04 .2. C4900E+04 .1005E+04 .105E+04 .000E+03 .339800E+00 .118430E+04 .105E+04 .000E+03 .593300E+00 .118430E+04 .30900E+03 .3300E+03 .593300E+00 .107590E+04 .300E+03 .300E+03 .593300E+00 .118450E+04 .000E+04 .000E+03 .593300E+00 .975700E+03 .300E+0						.50E+00	
Property Code: [HMSD0001] HEAT OF MIXING AND SOLUTION ORT J0953.00 State: Two-component system, single-phase liquid Pure component 2, liquid Pure component 2, liquid Parameters: [P1] 7/K Temperature (X1] xl/, Mole fraction of component 1 [Y1] H ^E /Jmol ⁻¹ , Molar excess enthalpy Vetlod: Direct low-pressure calorimetric measurement of H ^E at variable x1 and constant T Components: 1. C2H2CL4, 1,1,2,2-Tetrachloroethane 2. C4H14, Hexane [Y1] [P1] 7.000 ±-03							[X1]
Property Code: [HMSD0001] HEAT OF MIXING AND SOLUTION ORT J0953.00 State: Two-component system, single-phase liquid Pure component 2, liquid Pure component 2, liquid Parameters: [P1] 7/K Temperature (X1] xl/, Mole fraction of component 1 [Y1] H ^E /Jmol ⁻¹ , Molar excess enthalpy Vetlod: Direct low-pressure calorimetric measurement of H ^E at variable x1 and constant T Components: 1. C2H2CL4, 1,1,2,2-Tetrachloroethane 2. C4H14, Hexane [Y1] [P1] 7.000 ±-03							
State: Two-component system, single-phase liquid Pure component 1, liquid Pure component 2, liquid Parameters: [P1] 7/K. Temperature Mole fraction of component 1 [Y1] $H^E/Jmol^{-1}$, Molar excess enthalpy Vethod: Direct low-pressure calorimetric measurement of H^E at variable x_1 and constant T Components: I. $C_2H_2Cl_4$, 1,1,2,2-Tetrachloroethane 2. C_6H_14 , Hexane [Y1] [Y1] I. $C_2H_2Cl_4$, 1,1,2,2-Tetrachloroethane 2. C_6H_14 , Hexane [Y1] [X1] [Y1] I. $C_2H_2Cl_4$, 1,1,2,2-Tetrachloroethane 2. C_6H_14 , Hexane [P1] = .298150E+03 [Y1] I.140E+04 [P1] = .298150E+00 S0800E+03 [Y1] .132500E+00 .103700E+03 [Y1] .140E+04 .105E+04 .005E+04 .457100E+00 .116250E+04 .105E+04 .005E+03 .522600E+00 .116250E+04 .30300E+00 .1052E+04 .00E+03 .00E+03 .593300E+00 .11490E+04 057500E+03 055E+04 00E+03	Const. L. M. Const.			- La di seria di seconda di second			
Pure component 1, liquid Pure component 2, liquid Parameters: [P1] 7/K, Temperature [P1] T/K , Mole fraction of component 1 [Y1] $H^E/Jmol^{-1}$, Mole racess enthalpy Method: Direct low-pressure calorimetric measurement of H^E at variable x_1 and constant T Components: 1. $C_2H_2Cl_4$, 1,1,2,2-Tetrachloroethane 2. C_{cH1_4} , Hexane [P1] = .298150E+03 [X1] [Y1] [X1] [Y1] .140E+04 .105E+00 .80800E+03 .204900E+00 .975700E+03 .339800E+00 .116250E+04 .409900E+00 .116250E+04 .557500E+00 .117920E+04 .557500E+00 .117920E+04 .5525600E+00 .117920E+04 .5525600E+00 .117920E+04 .552500E+00 .117920E+04 .593300E+00 .177800E+03 .3300E+00 .381300E+03 .3500E+00 .381300E+03 .3500E+00 .381300E+03 .3500E+00 .381300E+03 .555800E+00 .555800E+03 .555800E+00 .55680E+03 .555800E+00 .55680E+03 .555800E+00 .55680E+03 .555800E+00 .55680E+03 .555800E+00 .55680E+03 .555800E+00 .55680E+03 .555800E+00 .55680E+03 .555800E+00 .55680E+03 .55580E+00 .55680E+03 .55580E+00 .55680E+03 .555800E+00 .55680E+03 .555800E+00 .55680E+03 .555800E+00 .55680E+03 .555800E+00 .55680E+03 .55880E+00 .55680E+03 .55880E+00 .55680E+03 .55880E+00 .55680E+03 .55880E+00 .55680E+03 .55880E+00 .55680E+03 .55880E+00 .55680E+03 .55880E+00 .55680E+03 .55880	Copyright© 1995]	ELDATA SARL Fra	nce. All rights reser	rved.	NT		ODT10052.00
Pure component 2, liquid Parameters: [P1] T/K , Temperature [Y1] T/L , Mole fraction of component 1 [Y1] $H^E/Imol^{-1}$, Mole fraction of component 1 [Y1] $H^E/Imol^{-1}$, Mole fraction of component 1 [Y1] $H^E/Imol^{-1}$, Mole fraction of H^E at variable x_1 and constant T Components: 1. C_2H ₂ Cl4, L1,2,2-Tetrachloroethane 2. C_6H ₁₄ . Hexane [P1] = .298150E+03 [Y1] [X1] [Y1]	Property Code:	[HMSD0001] HI	EAT OF MIXING	G AND SOLUTIO	N		ORTJ0953.002
/ariables: [X1] $x_1/-,$ Mole fraction of component 1 [Y1] $H^E/Imol^{-1}$, Molar excess enthalpy Method: Direct low-pressure calorimetric measurement of H^E at variable x_1 and constant T Components: I. $C_2H_2Cl_4$, 1,1,2,2-Tetrachloroethane 2. C_6H_{14} , Hexane [Y1] [P1] = .298150E+03 [Y1] [R1] [Y1] [Y1] .32500E+00 .800800E+03 .317800E+03 .273300E+00 .800800E+03 .30800E+03 .273300E+00 .105040E+04 .105E+04 .400900E+00 .116250E+04 .105E+04 .457100E+00 .118540E+04 .700E+03 .593300E+00 .118409E+04 .700E+03 .593300E+00 .118540E+04 .700E+03 .593300E+00 .11430E+04 .700E+03 .593300E+00 .117920E+04 .3500E+03 .593300E+00 .118540E+04 .350E+03 .7000E+00 .56600E+03 .350E+03 .904900E+00 .56600E+03 .350E+03 .905800E+00 .192200E+03 .50E+00 .50E+00	Copyright© 1995) Property Code: State:	[HMSD0001] HI Two-component	EAT OF MIXING system, single-ph	G AND SOLUTIO	N		ORTJ0953.002
Viethod: Direct low-pressure calorimetric measurement of H^E at variable x_1 and constant T Components: I. $C_2H_2Cl_4$, $1, 1, 2, 2$ – Tetrachloroethane 2. C_6H_{14} , Hexame [Y1] [X1] [Y1] IX1 [Y1] IX2500E+00 .580400E+03 .204900E+00 .105250E+04 .30980E+00 .10940E+04 .105250E+04 .105250E+04 .400900E+00 .118420E+04 .507500E+00 .112309E+04 .552300E+00 .117920E+04 .556500E+00 .107590E+04 .688900E+00 .38100E+03 .3500E+00 .38100E+03 .350E+00 .38100E+03 .350E+00 .392100E+03	Property Code:	[HMSD0001] HI Two-component Pure component Pure component	EAT OF MIXING system, single-ph 1, liquid 2, liquid	G AND SOLUTIO	N		ORTJ0953.002
Method: Direct low-pressure calorimetric measurement of H^E at variable x_1 and constant T Components: 1. $C_2H_2Cl_4$, $L_1,L_2,2-Tetrachloroethane$ 2. C_6H_14 , Hexane Iteration [P1] = .298150E+03 [Y1] [X1] [Y1] .140E+04 .635000E-01 .317800E+03 [Y1] .132500E+00 .580400E+03 .137800E+03 .204900E+00 .800800E+03 .105E+04 .105E+04 .47100E+00 .114970E+04 .105E+04 .105E+04 .507500E+00 .120390E+04 .700E+03 .339800E+00 .107590E+04 .59100E+00 .118540E+04 .700E+03 .700E+03 .700E+03 .593300E+00 .117920E+04 .700E+03 .350E+03 .350E+03 .975000E+00 .727800E+03 .350E+03 .350E+03 .350E+03 .350E+03 .955800E+00 .192200E+03 .350E+03 .300E+03 .300E+03 .300E+03 .50E+00 .50E+03	Property Code: State: Parameters:	[HMSD0001] HI Two-component Pure component Pure component [P1] T/K,	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature	G AND SOLUTIO ase liquid	N		ORTJ0953.00
Components: 1. $C_2H_2Cl_4$, $1,1,2,2-Tetrachloroethane 2. C_6H_{14}, Hexane [P1] = .298150E+03 [Y1] [X1] [Y1] .140E+04 .635000E-01 .317800E+03 .317800E+03 .132500E+00 .580400E+03 .140E+04 .773300E+00 .975700E+03 .105E+04 .273300E+00 .10940E+04 .105E+04 .400900E+00 .116250E+04 .105E+04 .507500E+00 .120390E+04 .105E+04 .507500E+00 .11840E+04 .3075700E+03 .522600E+00 .117920E+04 .700E+03 .593300E+00 .114490E+04 .700E+03 .742300E+00 .865500E+03 .350E+03 .951000E+00 .272800E+03 .350E+03 .955800E+00 .192200E+03 .350E+03 .955800E+00 .192200E+03 .350E+03 $	Property Code: State:	[HMSD0001] HI Two-component Pure component Pure component [P1] <i>T/</i> K, [X1] x ₁ /-,	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction	G AND SOLUTIO ase liquid of component 1	N		ORTJ0953.00
[P1] = .298150E+03 [Y1] [X1] [Y1] .635000E-01 .317800E+03 .132500E+00 .580400E+03 .204900E+00 .800800E+03 .204900E+00 .109040E+04 .339800E+00 .109040E+04 .400900E+00 .116250E+04 .457100E+00 .1104250E+04 .507500E+00 .120390E+04 .507500E+00 .120390E+04 .507500E+00 .110490E+04 .507500E+00 .110920E+04 .50800E+00 .117920E+04 .53800E+00 .107590E+04 .638800E+00 .975700E+03 .742300E+00 .865500E+03 .796000E+00 .727800E+03 .351000E+00 .381300E+03 .955800E+00 .192200E+03 .955800E+00 .192200E+03 .955800E+00 .192200E+03	Property Code: State: Parameters: Variables:	[HMSD0001] HJ Two-component Pure component [P1] <i>T/</i> K, [X1] <i>x</i> ₁ /-, [Y1] <i>H^E</i> /Jmol ⁻¹ .	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess of	G AND SOLUTIO ase liquid of component 1 enthalpy		ant T	ORTJ0953.00
[X1] [Y1] .140E+04 .635000E-01 .317800E+03 .140E+04 .132500E+00 .580400E+03 .140E+04 .204900E+00 .800800E+03 .109040E+04 .2039800E+00 .109040E+04 .105E+04 .400900E+00 .116250E+04 .105E+04 .457100E+00 .118540E+04 .105E+04 .507500E+00 .120390E+04 .105E+04 .552600E+00 .117920E+04 .700E+03 .538300E+00 .107590E+04 .700E+03 .638800E+00 .975700E+03 .350E+03 .742300E+00 .366500E+03 .350E+03 .904900E+00 .381300E+03 .350E+03 .955800E+00 .192200E+03 .350E+03 .955800E+00 .192200E+03 .350E+03	Property Code: State: Parameters: Variables: Method:	[HMSD0001] HI Two-component Pure component [P1] T/K, [X1] x1/-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₂ H ₂ Cl ₄ , 1,1	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction , Molar excess e ure calorimetric m ,2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 enthalpy neasurement of HE		ant T	ORTJ0953.00
.635000E-01 .317800E+03 .132500E+00 .580400E+03 .204900E+00 .800800E+03 .273300E+00 .975700E+03 .339800E+00 .109040E+04 .40990E+00 .116250E+04 .457100E+00 .119470E+04 .507500E+00 .119470E+04 .507500E+00 .119470E+04 .507500E+00 .119470E+04 .507500E+00 .117920E+04 .532600E+00 .117920E+04 .593300E+00 .107590E+04 .638000E+00 .107590E+04 .638000E+00 .865500E+03 .700E+03 .350E+03 .796000E+00 .381300E+03 .955800E+00 .192200E+03 .955800E+00 .192200E+03 .955800E+00 .192200E+03 .955800E+00 .192200E+03 .955800E+00 .50E+03	Property Code: State: Parameters: Variables: Method: Components:	[HMSD0001] HI Two-component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. C ₂ H ₂ Cl ₄ , 1,1 2. C ₆ H ₁₄ , Hexa	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction , Molar excess e ure calorimetric m ,2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 enthalpy neasurement of HE		ant T	ORTJ0953.002
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	Property Code: State: Parameters: Variables: Method: Components: [P1] = .29	[HMSD0001] HI Two-component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^{E}/Jmol^{-1}$, Direct low-press 1. C ₂ H ₂ Cl ₄ , 1,1 2. C ₆ H ₁₄ , Hexa 8150E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction , Molar excess e ure calorimetric m ,2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 enthalpy neasurement of HE	at variable x_1 and const	ant T	ORTJ0953.00
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1]	[HMSD0001] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^{E}/Jmol^{-1}$, Direct low-press 1. C ₂ H ₂ Cl ₄ , 1,1 2. C ₆ H ₁₄ , Hexa 8150E+03 [Y1]	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction , Molar excess e ure calorimetric m ,2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 enthalpy neasurement of HE	at variable x_1 and const [Y1]	ant T	ORTJ0953.00
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .635000E-01	$[HMSD0001] HITwo-componentPure componentPure component[P1] T/K,[X1] x1/-,[Y1] H^E/Jmol-1,Direct low-press1. C2H2Cl4, 1,12. C6H14, Hexa8150E+03[Y1].317800E+03$	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction , Molar excess e ure calorimetric m ,2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 enthalpy neasurement of HE	at variable x_1 and const [Y1]	ant T	ORTJ0953.003
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .635000E-01 .132500E+00	$[HMSD0001] HITwo-componentPure componentPure component[P1] T/K,[X1] x1/-,[Y1] H^E/Jmol-1,Direct low-press1. C2H2Cl4, 1,12. C6H14, Hexa8150E+03[Y1].317800E+03.580400E+03$	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction , Molar excess e ure calorimetric m ,2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 enthalpy neasurement of HE	at variable x_1 and const [Y1]		ORTJ0953.003
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .635000E-01 .132500E+00 .204900E+00	[HMSD0001] HITwo-componentPure componentPure component[P1] T/K,[X1] x1/-,[Y1] HE/Jmol-1,Direct low-press1. C2H2Cl4, 1,12. C6H14, Hexa8150E+03[Y1].317800E+03.580400E+03.800800E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction , Molar excess e ure calorimetric m ,2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 enthalpy neasurement of HE	at variable x_1 and const [Y1]		ORTJ0953.00
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .635000E-01 .132500E+00 .204900E+00 .273300E+00	$[HMSD0001] HITwo-componentPure componentPure component[P1] T/K,[X1] x1/-,[Y1] H^E/Jmol-1,Direct low-press1. C2H2Cl4, 1,12. C6H14, Hexa8150E+03[Y1].317800E+03.580400E+03.800800E+03.975700E+03$	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction , Molar excess e ure calorimetric m ,2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 enthalpy neasurement of HE	[Y1] .140E+04		ORTJ0953.00
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	Property Code: State: Parameters: Variables: Method: Components: [P1] = .292 [X1] .635000E-01 .132500E+00 .204900E+00 .204900E+00 .339800E+00	[HMSD0001] HI Two-component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-press 1. C ₂ H ₂ Cl ₄ , 1,1 2. C ₆ H ₁₄ , Hexa 8150E+03 [Y1] .317800E+03 .580400E+03 .800800E+03 .975700E+03 .109040E+04	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction , Molar excess e ure calorimetric m ,2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 enthalpy neasurement of HE	[Y1] .140E+04		ORTJ0953.00
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	Property Code: State: Parameters: Variables: Method: Components: [P1] = .292 [X1] .635000E-01 .132500E+00 .204900E+00 .204900E+00 .339800E+00 .400900E+00 .457100E+00	[HMSD0001] HITwo-componentPure componentPure component[P1] T/K,[X1] x1/-,[Y1] HE/Jmol-1,Direct low-press1. C2H2Cl4, 1,12. C6H14, Hexa8150E+03[Y1].317800E+03.580400E+03.800800E+03.975700E+03.109040E+04.116250E+04	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction , Molar excess e ure calorimetric n ,2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 enthalpy neasurement of HE	[Y1] .140E+04		ORTJ0953.00
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	Property Code: State: Parameters: Variables: Method: Components: [P1] = .292 [X1] .635000E-01 .132500E+00 .204900E+00 .203900E+00 .339800E+00 .400900E+00 .407100E+00 .507500E+00	[HMSD0001] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-press 1. C ₂ H ₂ Cl ₄ , 1,1 2. C ₆ H ₁₄ , Hexa 8150E+03 [Y1] .317800E+03 .580400E+03 .800800E+03 .800800E+03 .975700E+03 .109040E+04 .116250E+04 .119470E+04 .120390E+04	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction , Molar excess e ure calorimetric n ,2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 enthalpy neasurement of HE	[Y1] .140E+04		ORTJ0953.00
.638800E+00 .107590E+04 .689000E+00 .975700E+03 .742300E+00 .865500E+03 .796000E+00 .727800E+03 .851000E+00 .381300E+03 .904900E+00 .381300E+03 .955800E+00 .192200E+03 .000E+00 .50E+00	Property Code: State: Variables: Method: Components: [P1] = .292 [X1] .635000E-01 .132500E+00 .204900E+00 .273300E+00 .339800E+00 .409900E+00 .457100E+00 .507500E+00 .549100E+00	$[HMSD0001] HITwo-componentPure componentPure component[P1] T/K,[X1] x_{1/-},[Y1] H^E/Jmol-1,Direct low-press1. C2H2Cl4, 1, 12. C6H14, Hexa8150E+03[Y1].317800E+03.580400E+03.800800E+03.800800E+03.975700E+03.109040E+04.116250E+04.119470E+04.120390E+04.118540E+04$	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction , Molar excess e ure calorimetric n ,2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 enthalpy neasurement of HE	[Y1] .140E+04		ORTJ0953.00
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .635000E-01 .132500E+00 .204900E+00 .339800E+00 .400900E+00 .400900E+00 .507500E+00 .549100E+00	$[HMSD0001] HITwo-componentPure componentPure component[P1] T/K,[X1] x_{1/-},[Y1] H^E/Jmol-1,Direct low-press1. C2H2Cl4, 1,12. C6H14, Hexa8150E+03[Y1].317800E+03.580400E+03.800800E+03.800800E+03.975700E+04.116250E+04.119470E+04.120390E+04.118540E+04.117920E+04$	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction , Molar excess e ure calorimetric n ,2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 enthalpy neasurement of HE	[Y1] .140E+04 .105E+04		ORTJ0953.00
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	Property Code: State: Parameters: Variables: Method: Components: [P1] = .29/ [X1] .635000E-01 .132500E+00 .204900E+00 .273300E+00 .400900E+00 .409000E+00 .507500E+00 .549100E+00 .552600E+00 .593300E+00	$[HMSD0001] HI Two-component Pure component Pure component [P1] T/K, [X1] x_{1/-},[Y1] H^E/Jmol-1,Direct low-press1. C2H2Cl4, 1,12. C6H14, Hexa8150E+03[Y1].317800E+03.800800E+03.800800E+03.800800E+03.800800E+03.109040E+04.116250E+04.116250E+04.119470E+04.118540E+04.11490E+04$	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction , Molar excess e ure calorimetric n ,2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 enthalpy neasurement of HE	[Y1] .140E+04 .105E+04		
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .635000E-01 .132500E+00 .204900E+00 .273300E+00 .339800E+00 .400900E+00 .507500E+00 .549100E+00 .552600E+00 .593300E+00 .638800E+00	$[HMSD0001] HI Two-component Pure component Pure component [P1] T/K, [X1] x_{1/-},[Y1] H^E/Jmol-1,Direct low-press1. C2H2Cl4, 1,12. C6H14, Hexa8150E+03[Y1].317800E+03.800800E+03.800800E+03.800800E+03.975700E+03.109040E+04.116250E+04.116250E+04.118540E+04.117920E+04.11490E+04.107590E+04$	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction , Molar excess e ure calorimetric n ,2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 enthalpy neasurement of HE	[Y1] .140E+04 .105E+04		
$\begin{array}{c c} .904900E+00 \\ .955800E+00 \\ .192200E+03 \\ .000E+00 \\ \hline & \\ .000E+00 \\ \hline & \\ .50E+00 \\ \hline \end{array}$	Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .635000E-01 .132500E+00 .204900E+00 .204900E+00 .339800E+00 .400900E+00 .57500E+00 .549100E+00 .552600E+00 .593300E+00 .689000E+00 .689000E+00 .742300E+00	$[HMSD0001] HI Two-component Pure component Pure component [P1] T/K, [X1] x_{1/-},[Y1] H^E/Jmol^{-1},Direct low-press1. C2H2Cl4, 1,12. C6H14, Hexa8150E+03[Y1].317800E+03.580400E+03.580400E+03.580400E+03.800800E+03.975700E+03.109040E+04.116250E+04.119470E+04.119470E+04.117920E+04.117920E+04.107590E+03.865500E+03$	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction , Molar excess e ure calorimetric n ,2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 enthalpy neasurement of HE	[Y1] .140E+04 .105E+04		
.955800E+00 .192200E+03 .000E+00 .192200E+03 .000E+00 .50E+00	Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .635000E-01 .132500E+00 .204900E+00 .204900E+00 .39800E+00 .507500E+00 .549100E+00 .552600E+00 .53800E+00 .689000E+00 .742300E+00 .796000E+00	$[HMSD0001] HI Two-component Pure component Pure component [P1] T/K, [X1] x_{1/-},[Y1] H^E/Jmol^{-1},Direct low-press1. C2H2Cl4, 1,12. C6H14, Hexa8150E+03[Y1].317800E+03.580400E+03.580400E+03.580400E+03.800800E+03.975700E+03.109040E+04.116250E+04.119470E+04.119470E+04.117920E$	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction , Molar excess e ure calorimetric n ,2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 enthalpy neasurement of HE	[Y1] .140E+04 .105E+04 .700E+03		
○ [P1] = .298150E+03 .50E+00	Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .635000E-01 .132500E+00 .204900E+00 .204900E+00 .39800E+00 .400900E+00 .57500E+00 .549100E+00 .552600E+00 .593300E+00 .689000E+00 .742300E+00 .796000E+00 .851000E+00	[HMSD0001] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] HE/Jmol-1, Direct low-press 1. C2H2Cl4, 1,1 2. C6H14, Hexa 8150E+03 [Y1] .317800E+03 .580400E+03 .580400E+03 .800800E+03 .975700E+03 .109040E+04 .116250E+04 .119470E+04 .11920E+04 .117920E+04 .117920E+04 .107590E+03 .865500E+03 .727800E+03 .566600E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction , Molar excess e ure calorimetric n ,2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 enthalpy neasurement of HE	[Y1] .140E+04 .105E+04 .700E+03		
○ [P1] = .298150E+03 .000E+00	Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .635000E-01 .132500E+00 .204900E+00 .204900E+00 .339800E+00 .400900E+00 .549100E+00 .549100E+00 .593300E+00 .638800E+00 .638000E+00 .638000E+00 .638000E+00 .638000E+00 .6381000E+00 .904900E+00	[HMSD0001] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] HE/Jmol-1, Direct low-press 1. C2H2Cl4, 1,1 2. C6H14, Hexa 8150E+03 [Y1] .317800E+03 .580400E+03 .580400E+03 .800800E+03 .975700E+03 .109040E+04 .116250E+04 .119470E+04 .119470E+04 .120390E+04 .117590E+04 .107590E+04 .107590E+03 .865500E+03 .727800E+03 .566600E+03 .381300E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction , Molar excess e ure calorimetric n ,2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 enthalpy neasurement of HE	[Y1] .140E+04 .105E+04 .700E+03		
.000E+00	Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .635000E-01 .132500E+00 .204900E+00 .204900E+00 .339800E+00 .400900E+00 .549100E+00 .549100E+00 .593300E+00 .638800E+00 .638000E+00 .638000E+00 .638000E+00 .638000E+00 .6381000E+00 .904900E+00	[HMSD0001] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] HE/Jmol-1, Direct low-press 1. C2H2Cl4, 1,1 2. C6H14, Hexa 8150E+03 [Y1] .317800E+03 .580400E+03 .580400E+03 .800800E+03 .975700E+03 .109040E+04 .116250E+04 .119470E+04 .119470E+04 .120390E+04 .117590E+04 .107590E+04 .107590E+03 .865500E+03 .727800E+03 .566600E+03 .381300E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction , Molar excess e ure calorimetric n ,2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 enthalpy neasurement of HE	[Y1] .140E+04 .105E+04 .700E+03		
.50E+00	Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .635000E-01 .132500E+00 .204900E+00 .204900E+00 .339800E+00 .400900E+00 .549100E+00 .549100E+00 .593300E+00 .638800E+00 .638000E+00 .638000E+00 .638000E+00 .638000E+00 .6381000E+00 .904900E+00	[HMSD0001] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] HE/Jmol-1, Direct low-press 1. C2H2Cl4, 1,1 2. C6H14, Hexa 8150E+03 [Y1] .317800E+03 .580400E+03 .580400E+03 .800800E+03 .975700E+03 .109040E+04 .116250E+04 .119470E+04 .119470E+04 .120390E+04 .117590E+04 .107590E+04 .107590E+03 .865500E+03 .727800E+03 .566600E+03 .381300E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction , Molar excess e ure calorimetric n ,2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 enthalpy neasurement of HE	[Y1] .140E+04 .105E+04 .700E+03		
	Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .635000E-01 .132500E+00 .204900E+00 .204900E+00 .339800E+00 .400900E+00 .549100E+00 .549100E+00 .593300E+00 .638800E+00 .638000E+00 .638000E+00 .638000E+00 .638000E+00 .6381000E+00 .904900E+00	[HMSD0001] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] HE/Jmol-1, Direct low-press 1. C2H2Cl4, 1,1 2. C6H14, Hexa 8150E+03 [Y1] .317800E+03 .580400E+03 .580400E+03 .800800E+03 .975700E+03 .109040E+04 .116250E+04 .119470E+04 .119470E+04 .120390E+04 .117590E+04 .107590E+04 .107590E+03 .865500E+03 .727800E+03 .566600E+03 .381300E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction , Molar excess e ure calorimetric n ,2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 enthalpy neasurement of HE	[Y1] .140E+04 .105E+04 .700E+03 .350E+03		
[]	Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .635000E-01 .132500E+00 .204900E+00 .204900E+00 .339800E+00 .400900E+00 .549100E+00 .549100E+00 .593300E+00 .638800E+00 .638000E+00 .638000E+00 .638000E+00 .638000E+00 .6381000E+00 .904900E+00	[HMSD0001] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] HE/Jmol-1, Direct low-press 1. C2H2Cl4, 1,1 2. C6H14, Hexa 8150E+03 [Y1] .317800E+03 .580400E+03 .580400E+03 .800800E+03 .975700E+03 .109040E+04 .116250E+04 .119470E+04 .119470E+04 .120390E+04 .117590E+04 .107590E+04 .107590E+03 .865500E+03 .727800E+03 .566600E+03 .381300E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction , Molar excess e ure calorimetric n ,2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 enthalpy neasurement of HE	[Y1] .140E+04 .105E+04 .700E+03 .350E+03	○ [P1] = .298150E+03	
	Property Code: State: Parameters: Variables: Method: Components: [P1] = .29 [X1] .635000E-01 .132500E+00 .204900E+00 .204900E+00 .39800E+00 .400900E+00 .597500E+00 .59300E+00 .59300E+00 .638800E+00 .638800E+00 .638000E+00 .742300E+00 .796000E+00 .904900E+00	[HMSD0001] HI Two-component Pure component Pure component [P1] T/K, [X1] x1/-, [Y1] HE/Jmol-1, Direct low-press 1. C2H2Cl4, 1,1 2. C6H14, Hexa 8150E+03 [Y1] .317800E+03 .580400E+03 .580400E+03 .800800E+03 .975700E+03 .109040E+04 .116250E+04 .119470E+04 .119470E+04 .120390E+04 .117590E+04 .107590E+04 .107590E+03 .865500E+03 .727800E+03 .566600E+03 .381300E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction , Molar excess e ure calorimetric n ,2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 enthalpy neasurement of HE	[Y1] .140E+04 .105E+04 .700E+03 .350E+03	○ [P1] = .298150E+03	

State: Parameters:	[1111020001]112		
Parameters:	Two-component s	AT OF MIXING AND SOLUTIO	N ORTJ0953.
Parameters:	Pure component		
	Pure component 2		
	[P1] <i>T/</i> K,	Temperature	
ariables:	[X1] $x_{1/-}$,	Mole fraction of component 1	
Method:	[YI] H ^D /Jmol ⁻¹ , Direct low-pressu	Molar excess enthalpy re calorimetric measurement of H^E	at variable r_1 and constant T
		2,2-Tetrachloroethane	
	2. C7H16, Hepta	ne	
[P1] = .298	150E+03		[¥1]
[X1]	[Y1]		.140E+04 .105E+04 .700E+03 .350E+03
.732000E-01	.370200E+03		
.152100E+00	.652700E+03		, o' , o, o, o
.230600E+00	.913800E+03		0 0
.304300E+00	.108630E+04		8
.372800E+00	.120080E+04		.105E+04
.436300E+00 .493400E+00	.127100E+04 .130100E+04		
.543200E+00	.130070E+04		o 0
.587800E+00	.127430E+04		
.627000E+00	.123650E+04		ò, l
.640200E+00	.121390E+04		.700E+03 -
.678100E+00	.115210E+04		
.725800E+00	.106020E+04		
.772700E+00	.932000E+03		
.822300E+00 .872000E+00	.768700E+03 .600400E+03		0
.919200E+00	.400000E+03		.350E+03 - 9
.963100E+00	.205900E+03		
	.2037001103		
			-(D1) = -202150E + 02
			\circ [P1] = .298150E+03
			.000E+00
			.50E+00 [X
			L
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Property Code:		EAT OF MIXING AND SOLUTIO	ORTJ0953.
Property Code: State:	Two-component	EAT OF MIXING AND SOLUTIO system, single-phase liquid	ORTJ0953.
Property Code: State:	Two-component Pure component	EAT OF MIXING AND SOLUTIO system, single-phase liquid 1, liquid	ORTJ0953.
Property Code: State:	Two-component Pure component Pure component	EAT OF MIXING AND SOLUTIO system, single-phase liquid 1, liquid 2, liquid	ORTJ0953.
Property Code: State: Parameters:	Two-component Pure component Pure component [P1] T/K,	EAT OF MIXING AND SOLUTIO system, single-phase liquid 1, liquid 2, liquid Temperature	ORTJ0953.
Property Code: State: Parameters: Variables:	Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$,	EAT OF MIXING AND SOLUTIO system, single-phase liquid 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy	
Property Code: State: Parameters: Variables: Method:	Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu	EAT OF MIXING AND SOLUTIO system, single-phase liquid 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of HE	
Property Code: State: Parameters: Variables: Method: Components:	Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressi 1. C ₂ H ₂ Cl ₄ , 1,1,	EAT OF MIXING AND SOLUTIO system, single-phase liquid 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of HE 2,2-Tetrachloroethane	
Property Code: State: Parameters: Variables: Method: Components:	Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₂ H ₂ Cl ₄ , 1,1, 2. C ₈ H ₁₈ , Octar	EAT OF MIXING AND SOLUTIO system, single-phase liquid 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of HE 2,2-Tetrachloroethane	$\frac{1}{2}$ at variable x_1 and constant T
Property Code: State: Parameters: Variables: Method: Components:	Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₂ H ₂ Cl ₄ , 1,1, 2. C ₈ H ₁₈ , Octar	EAT OF MIXING AND SOLUTIO system, single-phase liquid 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of HE 2,2-Tetrachloroethane	E at variable x_1 and constant T [Y1]
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .618000E-01	Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. C_8H_{18} , Octar 150E+03 [Y1] .313300E+03	EAT OF MIXING AND SOLUTIO system, single-phase liquid 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of HE 2,2-Tetrachloroethane	E at variable x_1 and constant T [Y1]
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .618000E-01 .134200E+00	Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. C_8H_{18} , Octar 150E+03 [Y1] .313300E+03 .625700E+03	EAT OF MIXING AND SOLUTIO system, single-phase liquid 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of HE 2,2-Tetrachloroethane	E at variable x_1 and constant T [Y1]
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .618000E-01 .134200E+00 .208800E+00	Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. C2H2Cl4, 1,1, 2. C8H18, Octar 150E+03 [Y1] .313300E+03 .625700E+03 .889300E+03	EAT OF MIXING AND SOLUTIO system, single-phase liquid 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of HE 2,2-Tetrachloroethane	E at variable x_1 and constant T [Y1]
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .618000E-01 .134200E+00 .208800E+00 .283200E+00	Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C2H2Cl4, 1,1, 2. C8H18, Octar 150E+03 [Y1] .313300E+03 .625700E+03 .889300E+03 .108520E+04	EAT OF MIXING AND SOLUTIO system, single-phase liquid 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of HE 2,2-Tetrachloroethane	E at variable x_1 and constant T [Y1]
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .618000E-01 .134200E+00 .208800E+00 .283200E+00 .351300E+00	Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C2H2Cl4, 1,1, 2. C8H18, Octar 150E+03 [Y1] .313300E+03 .625700E+03 .889300E+03 .108520E+04 .123120E+04	EAT OF MIXING AND SOLUTIO system, single-phase liquid 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of HE 2,2-Tetrachloroethane	E at variable x_1 and constant T [Y1]
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .618000E-01 .134200E+00 .208800E+00 .283200E+00 .351300E+00 .417400E+00	Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. C2H2Cl4, 1,1, 2. C8H18, Octar 150E+03 [Y1] .313300E+03 .625700E+03 .889300E+03 .108520E+04 .123120E+04	EAT OF MIXING AND SOLUTIO system, single-phase liquid 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of HE 2,2-Tetrachloroethane	E at variable x_1 and constant T [Y1]
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .618000E-01 .134200E+00 .208800E+00 .283200E+00 .351300E+00 .417400E+00 .476100E+00	Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C2H2Cl4, 1,1, 2. C8H18, Octar 150E+03 [Y1] .313300E+03 .625700E+03 .889300E+03 .108520E+04 .123120E+04 .138510E+04	EAT OF MIXING AND SOLUTIO system, single-phase liquid 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of HE 2,2-Tetrachloroethane	E at variable x_1 and constant T [Y1]
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .618000E-01 .134200E+00 .208800E+00 .283200E+00 .351300E+00 .417400E+00 .529300E+00	Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. C2H2Cl4, 1,1, 2. C8H18, Octar 150E+03 [Y1] .313300E+03 .625700E+03 .889300E+03 .108520E+04 .123120E+04 .138510E+04 .140930E+04	EAT OF MIXING AND SOLUTIO system, single-phase liquid 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of HE 2,2-Tetrachloroethane	E at variable x_1 and constant T [Y1] .1500E+04 .1125E+04
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .618000E-01 .134200E+00 .208800E+00 .208800E+00 .351300E+00 .417400E+00 .476100E+00 .529300E+00 .576100E+00	Two-component Pure component Pure component Pure component [Y1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. C_8H_{18} , Octar 150E+03 [Y1] .313300E+03 .625700E+03 .889300E+03 .108520E+04 .123120E+04 .138510E+04 .140930E+04	EAT OF MIXING AND SOLUTIO system, single-phase liquid 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of HE 2,2-Tetrachloroethane	E at variable x_1 and constant T [Y1] .1500E+04 .1125E+04
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .618000E-01 .134200E+00 .208800E+00 .283200E+00 .351300E+00 .417400E+00 .529300E+00	Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. C2H2Cl4, 1,1, 2. C8H18, Octar 150E+03 [Y1] .313300E+03 .625700E+03 .889300E+03 .108520E+04 .123120E+04 .138510E+04 .140930E+04	EAT OF MIXING AND SOLUTIO system, single-phase liquid 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of HE 2,2-Tetrachloroethane	E at variable x_1 and constant T [Y1] .1500E+04 .1125E+04
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .618000E-01 .134200E+00 .208800E+00 .208800E+00 .351300E+00 .417400E+00 .476100E+00 .529300E+00 .576100E+00 .617500E+00	Two-component Pure component Pure component Pure component [Y1] T/K , [X1] $x_1/-$, [Y1] $HE/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1,2, 2. C_8H_{18} , Octar 150E+03 [Y1] .313300E+03 .625700E+03 .89300E+03 .108520E+04 .132670E+04 .138510E+04 .140930E+04 .140160E+04	EAT OF MIXING AND SOLUTIO system, single-phase liquid 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of HE 2,2-Tetrachloroethane	E at variable x_1 and constant T [Y1] .1500E+04 .1125E+04
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .618000E-01 .134200E+00 .208800E+00 .208800E+00 .351300E+00 .417400E+00 .529300E+00 .576100E+00 .617500E+00 .648100E+00 .692300E+00 .738900E+00	Two-component Pure component Pure component P11 T/K, [X1] $x_1/-$, [Y1] HE/Jmol ⁻¹ , Direct low-pressu 1. C2H2Cl4, 1,1, 2. C8H18, Octar 150E+03 [Y1] .313300E+03 .625700E+03 .889300E+03 .108520E+04 .132670E+04 .132670E+04 .133660E+04 .133660E+04 .133660E+04 .124270E+04 .15250E+04	EAT OF MIXING AND SOLUTIO system, single-phase liquid 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of HE 2,2-Tetrachloroethane	E at variable x_1 and constant T [Y1] .1500E+04 .1125E+04
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .618000E-01 .134200E+00 .208800E+00 .283200E+00 .351300E+00 .417400E+00 .529300E+00 .576100E+00 .617500E+00 .617500E+00 .648100E+00 .692300E+00 .738900E+00 .785800E+00	Two-component Pure component Pure component P11 T/K, [X1] $x_1/-$, [Y1] HE/Jmol ⁻¹ , Direct low-pressu 1. C2H2Cl4, 1,1, 2. C8H18, Octar 150E+03 [Y1] .313300E+03 .625700E+03 .889300E+03 .108520E+04 .123120E+04 .132670E+04 .132670E+04 .133660E+04 .133660E+04 .133660E+04 .15250E+04 .15250E+04 .103500E+04	EAT OF MIXING AND SOLUTIO system, single-phase liquid 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of HE 2,2-Tetrachloroethane	E at variable x_1 and constant T $\begin{bmatrix} Y1] \\ .1500E+04 \\ .1125E+04 \\ .7500E+03 \\ 0 \end{bmatrix}$
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .618000E-01 .134200E+00 .208800E+00 .208800E+00 .351300E+00 .417400E+00 .529300E+00 .576100E+00 .576100E+00 .648100E+00 .692300E+00 .738900E+00 .785800E+00 .785800E+00 .833000E+00	Two-component Pure component Pure component Pure component [Y1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. C_8H_{18} , Octar 150E+03 [Y1] .313300E+03 .625700E+03 .889300E+03 .108520E+04 .123120E+04 .132670E+04 .13360E+04 .132670E+04 .133660E+04 .137160E+04 .15250E+04 .103500E+04 .849800E+03	EAT OF MIXING AND SOLUTIO system, single-phase liquid 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of HE 2,2-Tetrachloroethane	E at variable x_1 and constant T $\begin{bmatrix} Y1] \\ .1500E+04 \\ .1125E+04 \\ .7500E+03 \\ 0 \end{bmatrix}$
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .618000E-01 .134200E+00 .208800E+00 .208800E+00 .351300E+00 .417400E+00 .529300E+00 .576100E+00 .648100E+00 .648100E+00 .648100E+00 .632300E+00 .738900E+00 .785800E+00 .833000E+00 .879400E+00	Two-component Pure component Pure component P11 T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C2H2Cl4, 1,1, 2. C3H18, Octar 150E+03 [Y1] .313300E+03 .625700E+03 .889300E+03 .108520E+04 .132670E+04 .138510E+04 .138510E+04 .140930E+04 .137160E+04 .137660E+04 .132670E+04 .132500E+04 .103500E+04 .15250E+04 .103500E+04 .103500E+04 .661100E+03	EAT OF MIXING AND SOLUTIO system, single-phase liquid 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of HE 2,2-Tetrachloroethane	E at variable x_1 and constant T $\begin{bmatrix} Y1] \\ .1500E+04 \\ .1125E+04 \\ .7500E+03 \\ 0 \end{bmatrix}$
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .618000E-01 .134200E+00 .208800E+00 .208800E+00 .351300E+00 .417400E+00 .529300E+00 .576100E+00 .617500E+00 .648100E+00 .692300E+00 .738900E+00 .738900E+00 .738900E+00 .833000E+00 .879400E+00 .923700E+00	Two-component Pure component Pure component P11 T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C2H2Cl4, 1,1, 2. C3BH18, Octar 150E+03 [Y1] .313300E+03 .625700E+03 .889300E+03 .108520E+04 .123120E+04 .132670E+04 .132670E+04 .140930E+04 .140160E+04 .13660E+04 .132660E+04 .15250E+04 .103500E+04 .15250E+04 .103500E+04 .661100E+03 .661100E+03 .442900E+03 .641200E+03	EAT OF MIXING AND SOLUTIO system, single-phase liquid 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of HE 2,2-Tetrachloroethane	E at variable x_1 and constant T $\begin{bmatrix} Y1] \\ .1500E+04 \\ .1125E+04 \\ .7500E+03 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\$
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .618000E-01 .134200E+00 .208800E+00 .208800E+00 .351300E+00 .417400E+00 .529300E+00 .576100E+00 .648100E+00 .648100E+00 .648100E+00 .632300E+00 .738900E+00 .785800E+00 .833000E+00 .879400E+00	Two-component Pure component Pure component P11 T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C2H2Cl4, 1,1, 2. C3H18, Octar 150E+03 [Y1] .313300E+03 .625700E+03 .889300E+03 .108520E+04 .132670E+04 .138510E+04 .138510E+04 .140930E+04 .137160E+04 .137660E+04 .132670E+04 .132500E+04 .103500E+04 .15250E+04 .103500E+04 .103500E+04 .661100E+03	EAT OF MIXING AND SOLUTIO system, single-phase liquid 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of HE 2,2-Tetrachloroethane	E at variable x_1 and constant T $\begin{bmatrix} Y1] \\ .1500E+04 \\ .1125E+04 \\ .7500E+03 \\ 0 \end{bmatrix}$
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .618000E-01 .134200E+00 .208800E+00 .208800E+00 .351300E+00 .417400E+00 .529300E+00 .576100E+00 .617500E+00 .648100E+00 .692300E+00 .738900E+00 .738900E+00 .738900E+00 .833000E+00 .879400E+00 .923700E+00	Two-component Pure component Pure component P11 T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C2H2Cl4, 1,1, 2. C3BH18, Octar 150E+03 [Y1] .313300E+03 .625700E+03 .889300E+03 .108520E+04 .123120E+04 .132670E+04 .132670E+04 .140930E+04 .140160E+04 .13660E+04 .132660E+04 .15250E+04 .103500E+04 .15250E+04 .103500E+04 .661100E+03 .661100E+03 .442900E+03 .641200E+03	EAT OF MIXING AND SOLUTIO system, single-phase liquid 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of HE 2,2-Tetrachloroethane	E at variable x_1 and constant T [Y1] .1500E+04 .1125E+04 .7500E+03 .3750E+03
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .618000E-01 .134200E+00 .208800E+00 .208800E+00 .351300E+00 .417400E+00 .529300E+00 .576100E+00 .617500E+00 .648100E+00 .692300E+00 .738900E+00 .738900E+00 .738900E+00 .833000E+00 .879400E+00 .923700E+00	Two-component Pure component Pure component P11 T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C2H2Cl4, 1,1, 2. C3BH18, Octar 150E+03 [Y1] .313300E+03 .625700E+03 .889300E+03 .108520E+04 .123120E+04 .132670E+04 .132670E+04 .140930E+04 .140160E+04 .13660E+04 .132660E+04 .15250E+04 .103500E+04 .15250E+04 .103500E+04 .661100E+03 .661100E+03 .442900E+03 .641200E+03	EAT OF MIXING AND SOLUTIO system, single-phase liquid 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of HE 2,2-Tetrachloroethane	E at variable x_1 and constant T [Y1] .1500E+04 .1125E+04 .7500E+03 .3750E+03 \circ [P1] = .298150E+03
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .618000E-01 .134200E+00 .208800E+00 .208800E+00 .351300E+00 .417400E+00 .529300E+00 .576100E+00 .648100E+00 .648100E+00 .692300E+00 .738900E+00 .738900E+00 .738900E+00 .833000E+00 .879400E+00 .923700E+00	Two-component Pure component Pure component P11 T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C2H2Cl4, 1,1, 2. C3BH18, Octar 150E+03 [Y1] .313300E+03 .625700E+03 .889300E+03 .108520E+04 .123120E+04 .132670E+04 .132670E+04 .140930E+04 .140160E+04 .13660E+04 .132660E+04 .15250E+04 .103500E+04 .15250E+04 .103500E+04 .661100E+03 .661100E+03 .442900E+03 .641200E+03	EAT OF MIXING AND SOLUTIO system, single-phase liquid 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of HE 2,2-Tetrachloroethane	^E at variable x_1 and constant T [Y1] .1500E+04 .1125E+04 .7500E+03 .3750E+03 .0000E+00 .0000E+00
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .618000E-01 .134200E+00 .208800E+00 .208800E+00 .208800E+00 .351300E+00 .417400E+00 .529300E+00 .576100E+00 .648100E+00 .648100E+00 .648100E+00 .692300E+00 .738900E+00 .738900E+00 .833000E+00 .879400E+00 .923700E+00	Two-component Pure component Pure component P11 T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C2H2Cl4, 1,1, 2. C3BH18, Octar 150E+03 [Y1] .313300E+03 .625700E+03 .889300E+03 .108520E+04 .123120E+04 .132670E+04 .132670E+04 .138510E+04 .140930E+04 .140930E+04 .140160E+04 .13660E+04 .15250E+04 .15250E+04 .103500E+04 .661100E+03 .661100E+03 .442900E+03 .641200E+03	EAT OF MIXING AND SOLUTIO system, single-phase liquid 1, liquid 2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy ure calorimetric measurement of HE 2,2-Tetrachloroethane	E at variable x_1 and constant T [Y1] .1500E+04 .1125E+04 .7500E+03 .3750E+03 \circ [P1] = .298150E+03

			AND SOLUTIO	N		ORTJ0953.005
	Two-component s		ase liquid			
	Pure component 2 Pure component 2					
	[P1] <i>T</i> /K,	Temperature				
	$[X1] x_1/-,$	Mole fraction of	of component 1			
	$[Y1]$ H^E /Jmol ⁻¹ ,	Molar excess e	nthalpy			
A REAL PROPERTY AND ADDRESS OF THE OWNER OWNER OF THE OWNER OWN				at variable x_1 and c	onstant T	
	1. C ₂ H ₂ Cl ₄ , 1,1, 2. C ₉ H ₂₀ , Nonai		ethane			
[P1] = .298				(3/1)		
[X1]	[Y1]			[Y1]		
.893000E-01	.488200E+03			.160E+04		
.172100E+00	.790700E+03				, , , , , , , , , , , , , , , , , , ,	
.257900E+00	.106130E+04				0	
.336900E+00	.123620E+04				ío,	
.409800E+00	.137860E+04			.120E+04	0 0	
.473900E+00	.145580E+04					0 0 0
.531600E+00 .581300E+00	.148870E+04 .148640E+04				ø	o.
.583500E+00	.148040E+04					
.623000E+00	.145190E+04					9
.664200E+00	.139650E+04			.800E+03	¢.	-
.707900E+00	.131510E+04				1	0
.752300E+00	.120490E+04					
.797100E+00 .842900E+00	.106350E+04 .886100E+03				,	
.887800E+00	.679800E+03			.400E+03		ġ.
.929500E+00	.453300E+03			.40012+03		
.967100E+00	.228100E+03					
						0
		1 B			\circ [P1] = .298150E+03	
				.000E+00		
					.50E+00	(3/4)
Property Code:		EAT OF MIXING	G AND SOLUTIO	N	.50E+00	
Property Code:	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$,	EAT OF MIXING system, single-pha 1, liquid 2, liquid Temperature Mole fraction of	G AND SOLUTIO ase liquid of component 1	N	.50E+00	[X1] ORTJ0953.00
Property Code: State: Parameters: Variables:	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] H^E /Jmol ⁻¹ .	EAT OF MIXINC system, single-ph: 1, liquid 2, liquid Temperature Mole fraction Molar excess e	G AND SOLUTIO ase liquid of component 1 enthalpy			
Property Code: State: Parameters: Variables: Method:	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu	EAT OF MIXINC system, single-pha 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric m	G AND SOLUTIO ase liquid of component 1 inthalpy neasurement of <i>HE</i>	N at variable x ₁ and c		
Property Code: State: Parameters: Variables: Method:	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] H^E /Jmol ⁻¹ .	AT OF MIXINC system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 inthalpy neasurement of <i>HE</i>			
Property Code: State: Parameters: Variables: Method:	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₂ H ₂ Cl ₄ , 1,1, 2. C ₁₀ H ₂₂ , Dece	AT OF MIXINC system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 inthalpy neasurement of <i>HE</i>	at variable x_1 and c	onstant T	ORTJ0953.00
Property Code: State: Parameters: Variables: Method: Components:	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₂ H ₂ Cl ₄ , 1,1, 2. C ₁₀ H ₂₂ , Dece	AT OF MIXINC system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 inthalpy neasurement of <i>HE</i>		onstant T	ORTJ0953.00
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .780000E-01	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. $C_2H_2Cl_4$, 1,1, 2. $C_{10}H_{22}$, Decc B150E+03 [Y1] .407700E+03	AT OF MIXINC system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 inthalpy neasurement of <i>HE</i>	at variable x_1 and control of the second se	onstant T	ORTJ0953.00
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .780000E-01 .152000E+00	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-press 1. $C_2H_2Cl_4$, 1,1, 2. $C_{10}H_{22}$, Decc B150E+03 [Y1] .407700E+03 .715600E+03	AT OF MIXINC system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 inthalpy neasurement of <i>HE</i>	at variable x_1 and control of the second se	onstant T	ORTJ0953.00
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .780000E-01 .152000E+00 .220200E+00	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. $C_{10}H_{22}$, Decc B150E+03 [Y1] .407700E+03 .715600E+03 .985100E+03	AT OF MIXINC system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 inthalpy neasurement of <i>HE</i>	at variable x_1 and control of the second se	onstant T	ORTJ0953.00
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .780000E-01 .152000E+00 .220200E+00 .285900E+00	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. $C_{10}H_{22}$, Decc B150E+03 [Y1] .407700E+03 .715600E+03 .985100E+03 .116740E+04	AT OF MIXINC system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 inthalpy neasurement of <i>HE</i>	at variable x ₁ and c [Y1] .160E+04	onstant T	ORTJ0953.00
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .780000E-01 .152000E+00 .220200E+00 .285900E+00 .348100E+00	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. $C_{10}H_{22}$, Dece B150E+03 [Y1] .407700E+03 .715600E+03 .985100E+03 .116740E+04 .133850E+04	AT OF MIXINC system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 inthalpy neasurement of <i>HE</i>	at variable x_1 and control of the second se	onstant T	ORTJ0953.00
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .780000E - 01 .152000E + 00 .220200E + 00 .285900E + 00 .348100E + 00 .405400E + 00 .458200E + 00	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. $C_{10}H_{22}$, Dece B150E+03 [Y1] .407700E+03 .715600E+03 .715600E+03 .985100E+03 .116740E+04 .133850E+04 .145230E+04 .152110E+04	AT OF MIXINC system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 inthalpy neasurement of <i>HE</i>	at variable x ₁ and c [Y1] .160E+04		ORTJ0953.00
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .78000E - 01 .152000E + 00 .220200E + 00 .348100E + 00 .405400E + 00 .458200E + 00 .505700E + 00	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. $C_{10}H_{22}$, Dece 3150E+03 [Y1] .407700E+03 .715600E+03 .116740E+04 .133850E+04 .145230E+04 .152110E+04 .156000E+04	AT OF MIXINC system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 inthalpy neasurement of <i>HE</i>	at variable x ₁ and c [Y1] .160E+04	onstant T	ORTJ0953.00
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .78000E - 01 .152000E + 00 .220200E + 00 .245900E + 00 .348100E + 00 .405400E + 00 .505700E + 00 .542700E + 00	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. $C_{10}H_{22}$, Deca 3150E+03 [Y1] .407700E+03 .715600E+03 .116740E+04 .133850E+04 .132850E+04 .152110E+04 .157110E+04	AT OF MIXINC system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 inthalpy neasurement of <i>HE</i>	at variable x ₁ and c [Y1] .160E+04	onstant T	ORTJ0953.00
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .78000E - 01 .152000E + 00 .220200E + 00 .348100E + 00 .405400E + 00 .458200E + 00 .505700E + 00 .542700E + 00 .613000E + 00	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. $C_{10}H_{22}$, Deca 3150E+03 [Y1] .407700E+03 .715600E+03 .116740E+04 .133850E+04 .145230E+04 .152110E+04 .157110E+04 .154120E+04	AT OF MIXINC system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 inthalpy neasurement of <i>HE</i>	at variable x ₁ and c [Y1] .160E+04	onstant T	ORTJ0953.00
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .780000E-01 .152000E+00 .220200E+00 .285900E+00 .348100E+00 .458200E+00 .505700E+00 .542700E+00 .542700E+00 .613000E+00 .650900E+00	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. $C_{10}H_{22}$, Deca 3150E+03 [Y1] .407700E+03 .715600E+03 .985100E+03 .116740E+04 .133850E+04 .145230E+04 .152110E+04 .154120E+04 .154120E+04 .149500E+04	AT OF MIXINC system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 inthalpy neasurement of <i>HE</i>	[Y1] .160E+04 .120E+04	onstant T	ORTJ0953.00
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .780000E-01 .152000E+00 .20200E+00 .285900E+00 .348100E+00 .405400E+00 .505700E+00 .542700E+00 .542700E+00 .650900E+00 .690900E+00 .732300E+00	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. $C_{10}H_{22}$, Deca 3150E+03 [Y1] .407700E+03 .715600E+03 .116740E+04 .133850E+04 .145230E+04 .152110E+04 .157110E+04 .154120E+04	AT OF MIXINC system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 inthalpy neasurement of <i>HE</i>	[Y1] .160E+04 .120E+04	onstant T	ORTJ0953.00
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .780000E-01 .152000E+00 .220200E+00 .285900E+00 .348100E+00 .405400E+00 .505700E+00 .505700E+00 .650900E+00 .650900E+00 .650900E+00 .732300E+00 .774600E+00	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. $C_{10}H_{22}$, Deca 3150E+03 [Y1] .407700E+03 .715600E+03 .715600E+03 .985100E+03 .116740E+04 .133850E+04 .145230E+04 .152110E+04 .157110E+04 .154120E+04 .149500E+04 .142770E+04 .133520E+04 .121290E+04	AT OF MIXINC system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 inthalpy neasurement of <i>HE</i>	[Y1] .160E+04 .120E+04	onstant T	ORTJ0953.00
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .780000E-01 .152000E+00 .20200E+00 .20200E+00 .348100E+00 .405400E+00 .505700E+00 .505700E+00 .613000E+00 .650900E+00 .732300E+00 .774600E+00 .817000E+00	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. $C_{10}H_{22}$, Deca B150E+03 [Y1] .407700E+03 .715600E+03 .715600E+03 .116740E+04 .133850E+04 .145230E+04 .152110E+04 .155110E+04 .154120E+04 .154120E+04 .142770E+04 .133520E+04 .121290E+04 .106160E+04	AT OF MIXINC system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 inthalpy neasurement of <i>HE</i>	[Y1] .160E+04 .120E+04 .800E+03	onstant T	ORTJ0953.00
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .780000E-01 .152000E+00 .220200E+00 .220200E+00 .248100E+00 .405400E+00 .505700E+00 .505700E+00 .613000E+00 .630900E+00 .774600E+00 .817000E+00 .817000E+00 .859000E+00	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. $C_{10}H_{22}$, Deca B150E+03 [Y1] .407700E+03 .715600E+03 .715600E+03 .985100E+03 .116740E+04 .133850E+04 .152110E+04 .1557110E+04 .154120E+04 .154120E+04 .154120E+04 .133520E+04 .133520E+04 .121290E+04 .106160E+04 .879900E+03	AT OF MIXINC system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 inthalpy neasurement of <i>HE</i>	[Y1] .160E+04 .120E+04	onstant T	ORTJ0953.00
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .780000E-01 .152000E+00 .20200E+00 .20200E+00 .348100E+00 .405400E+00 .505700E+00 .505700E+00 .613000E+00 .650900E+00 .732300E+00 .774600E+00 .817000E+00	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. $C_{10}H_{22}$, Deca B150E+03 [Y1] .407700E+03 .715600E+03 .715600E+03 .985100E+03 .116740E+04 .133850E+04 .152110E+04 .1557110E+04 .154120E+04 .154120E+04 .154120E+04 .133520E+04 .121290E+04 .106160E+04 .879900E+03 .673100E+03	AT OF MIXINC system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 inthalpy neasurement of <i>HE</i>	[Y1] .160E+04 .120E+04 .800E+03	onstant T	ORTJ0953.00
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .780000E - 01 .152000E + 00 .20200E + 00 .20200E + 00 .348100E + 00 .405400E + 00 .505700E + 00 .505700E + 00 .613000E + 00 .650900E + 00 .774600E + 00 .817000E + 00 .859000E + 00 .859000E + 00 .859000E + 00 .899200E + 00	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. $C_{10}H_{22}$, Deca B150E+03 [Y1] .407700E+03 .715600E+03 .715600E+03 .985100E+03 .116740E+04 .133850E+04 .152110E+04 .1557110E+04 .154120E+04 .154120E+04 .154120E+04 .133520E+04 .133520E+04 .121290E+04 .106160E+04 .879900E+03	AT OF MIXINC system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 inthalpy neasurement of <i>HE</i>	[Y1] .160E+04 .120E+04 .800E+03	onstant T	ORTJ0953.00
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .780000E - 01 .152000E + 00 .20200E + 00 .20200E + 00 .348100E + 00 .405400E + 00 .542700E + 00 .542700E + 00 .542700E + 00 .650900E + 00 .732300E + 00 .817000E + 00 .859000E + 00 .859000E + 00 .859000E + 00 .859000E + 00 .899200E + 00 .899200E + 00 .899200E + 00 .899200E + 00	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. $C_{10}H_{22}$, Dece 3150E+03 [Y1] .407700E+03 .715600E+03 .715600E+03 .116740E+04 .13850E+04 .152110E+04 .156000E+04 .154120E+04 .154120E+04 .154120E+04 .154120E+04 .154120E+04 .1212900E+04 .121290E+04 .106160E+04 .879900E+03 .673100E+03 .673100E+03 .448800E+03	AT OF MIXINC system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 inthalpy neasurement of <i>HE</i>	[Y1] .160E+04 .120E+04 .800E+03	onstant <i>T</i>	ORTJ0953.00
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .780000E - 01 .152000E + 00 .20200E + 00 .20200E + 00 .348100E + 00 .405400E + 00 .542700E + 00 .542700E + 00 .542700E + 00 .650900E + 00 .732300E + 00 .817000E + 00 .859000E + 00 .859000E + 00 .859000E + 00 .859000E + 00 .899200E + 00 .899200E + 00 .899200E + 00 .899200E + 00	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. $C_{10}H_{22}$, Dece 3150E+03 [Y1] .407700E+03 .715600E+03 .715600E+03 .116740E+04 .13850E+04 .152110E+04 .156000E+04 .154120E+04 .154120E+04 .154120E+04 .154120E+04 .154120E+04 .1212900E+04 .121290E+04 .106160E+04 .879900E+03 .673100E+03 .673100E+03 .448800E+03	AT OF MIXINC system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 inthalpy neasurement of <i>HE</i>	at variable x1 and c [Y1] .160E+04 .120E+04 .800E+03 .400E+03	onstant T	ORTJ0953.00
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .780000E - 01 .152000E + 00 .20200E + 00 .20200E + 00 .348100E + 00 .405400E + 00 .542700E + 00 .542700E + 00 .542700E + 00 .650900E + 00 .732300E + 00 .817000E + 00 .859000E + 00 .859000E + 00 .859000E + 00 .859000E + 00 .899200E + 00 .899200E + 00 .899200E + 00 .899200E + 00	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. $C_{10}H_{22}$, Dece 3150E+03 [Y1] .407700E+03 .715600E+03 .715600E+03 .116740E+04 .13850E+04 .152110E+04 .156000E+04 .154120E+04 .154120E+04 .154120E+04 .154120E+04 .154120E+04 .1212900E+04 .121290E+04 .106160E+04 .879900E+03 .673100E+03 .673100E+03 .448800E+03	AT OF MIXINC system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 inthalpy neasurement of <i>HE</i>	[Y1] .160E+04 .120E+04 .800E+03	onstant <i>T</i>	ORTJ0953.00
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .780000E - 01 .152000E + 00 .20200E + 00 .20200E + 00 .348100E + 00 .405400E + 00 .542700E + 00 .54270E + 00	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. $C_{10}H_{22}$, Dece 3150E+03 [Y1] .407700E+03 .715600E+03 .715600E+03 .116740E+04 .13850E+04 .152110E+04 .156000E+04 .154120E+04 .154120E+04 .154120E+04 .154120E+04 .154120E+04 .1212900E+04 .121290E+04 .106160E+04 .879900E+03 .673100E+03 .673100E+03 .448800E+03	AT OF MIXINC system, single-phi 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTIO ase liquid of component 1 inthalpy neasurement of <i>HE</i>	at variable x1 and c [Y1] .160E+04 .120E+04 .800E+03 .400E+03	onstant <i>T</i>	ORTJ0953.00



	LDATA SARL Fra		wed. G AND SOLUTIO	N	ORTJ0953.009
State:	Two-component				OR130933.009
	Pure component				
	Pure component				
Parameters:	[P1] <i>T/</i> K,	Temperature			
Variables:	$[X1] x_1/-,$	Mole fraction	of component 1		
20. A. A	[Y1] HE/Jmol ⁻¹ ,	Molar excess e	enthalpy	at variable x_1 and constant	T
Method: Components:	1. C2H2Cl4, 1,1		and the second	at variable x1 and constant	
_	2. C13H28, Trid				
	8150E+03			[Y1]	
[X1]	[Y1]			.180E+04	00.
.804000E-01	.436600E+03				0 ⁰⁰⁰ 0
.164000E+00	.797000E+03				0 0
.242000E+00					o ò
.311700E+00 .374000E+00	.136620E+04 .153910E+04				0
.430600E+00				.135E+04	,
.481800E+00					e e
527200E+00					
.568000E+00	.177850E+04			0	0
.615000E+00					
.655100E+00				.900E+03	
.691400E+00				ő	y
.729600E+00					
.769400E+00	.142720E+04				0
.809300E+00	.128060E+04				
.849500E+00				.450E+03	<u></u>
.889900E+00 .929600E+00					
.967000E+00	.314700E+03				<u>°</u>
507000L100	JATTOLTUS				
					D[P1] = .298150E + 03
				.000E+00 £	1
					.50E+00
	No. of Concession, Name				[X1]
Convright@ 1995 F	T DATA SADI Em				
		nce. All rights reser			
Property Code:	[HMSD0001] HE	EAT OF MIXING	G AND SOLUTIO	٧	ORTJ0953.010
	[HMSD0001] HE Two-component	EAT OF MIXINO system, single-ph	G AND SOLUTIO	N	ORTJ0953.010
Property Code:	[HMSD0001] HE Two-component Pure component	EAT OF MIXINO system, single-ph 1, liquid	G AND SOLUTIO	N	ORTJ0953.010
Property Code: State:	[HMSD0001] HE Two-component Pure component Pure component	EAT OF MIXING system, single-ph 1, liquid 2, liquid	G AND SOLUTIO	4	ORTJ0953.010
Property Code: State: Parameters:	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K,	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature	G AND SOLUTIO ase liquid	8	ORTJ0953.010
Property Code: State: Parameters:	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$,	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction	G AND SOLUTION ase liquid of component 1	8	ORTJ0953.010
Property Code: State: Parameters: Variables:	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$,	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e	G AND SOLUTION ase liquid of component 1 enthalpy		
Property Code: State: Parameters: Variables: Method:	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e ure calorimetric n	G AND SOLUTION ase liquid of component 1 enthalpy neasurement of H ^E	N at variable x_1 and constant	
Property Code: State: Parameters: Variables: Method: Components:	[HMSD0001] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₂ H ₂ Cl ₄ , 1,1, 2. C ₁₄ H ₃₀ , Tetra	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTION ase liquid of component 1 enthalpy neasurement of H ^E		
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298	[HMSD0001] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₂ H ₂ Cl ₄ , 1,1, 2. C ₁₄ H ₃₀ , Tetra	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTION ase liquid of component 1 enthalpy neasurement of H ^E		
Property Code: State: Parameters: Variables: Method: Components:	[HMSD0001] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₂ H ₂ Cl ₄ , 1,1, 2. C ₁₄ H ₃₀ , Tetra	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTION ase liquid of component 1 enthalpy neasurement of H ^E	at variable x_1 and constant	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. C ₂ H ₂ Cl ₄ , 1,1, 2. C ₁₄ H ₃₀ , Tetra S150E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTION ase liquid of component 1 enthalpy neasurement of H ^E	at variable x_1 and constant [Y1]	<u>T</u>
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .899000E-01 .170800E+00	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. $C_{14}H_{30}$, Tetra [Y1]	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTION ase liquid of component 1 enthalpy neasurement of H ^E	at variable x_1 and constant [Y1]	<u>T</u>
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .899000E-01	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. $C_{14}H_{30}$, Tetra B150E+03 [Y1] .484400E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTION ase liquid of component 1 enthalpy neasurement of H ^E	at variable x_1 and constant [Y1]	<u>T</u>
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .899000E-01 .170800E+00 .247300E+00 .316300E+00	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. $C_{14}H_{30}$, Tetre 150E+03 [Y1] .484400E+03 .844900E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTION ase liquid of component 1 enthalpy neasurement of H ^E	at variable x_1 and constant [Y1]	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .899000E-01 .170800E+00 .247300E+00 .316300E+00 .378600E+00	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-pressu 1. C ₂ H ₂ Cl ₄ , 1,1, 2. C ₁₄ H ₃₀ , Tetre 150E+03 [Y1] .484400E+03 .844900E+03 .116560E+04	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTION ase liquid of component 1 enthalpy neasurement of H ^E	at variable x_1 and constant [Y1]	<u>T</u>
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .899000E-01 .170800E+00 .247300E+00 .316300E+00 .378600E+00 .435500E+00	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₂ H ₂ Cl ₄ , 1,1, 2. C ₁₄ H ₃₀ , Tetre B150E+03 [Y1] .484400E+03 .844900E+03 .116560E+04 .140910E+04 .158690E+04 .171380E+04	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTION ase liquid of component 1 enthalpy neasurement of H ^E	at variable x ₁ and constant [Y1] .200E+04	<u>T</u>
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .899000E -01 .170800E +00 .316300E +00 .378600E +00 .435500E +00 .486200E +00	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. $C_{14}H_{30}$, Tetre 2150E+03 [Y1] .484400E+03 .844900E+03 .116560E+04 .116560E+04 .158690E+04 .171380E+04 .179480E+04	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTION ase liquid of component 1 enthalpy neasurement of H ^E	at variable x ₁ and constant [Y1] .200E+04	<u>T</u>
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .899000E-01 .170800E+00 .247300E+00 .316300E+00 .378600E+00 .435500E+00 .486200E+00 .532200E+00	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₂ H ₂ Cl ₄ , 1,1, 2. C ₁₄ H ₃₀ , Tetre B150E+03 [Y1] .484400E+03 .844900E+03 .116560E+04 .116560E+04 .158690E+04 .171380E+04 .179480E+04 .183820E+04	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTION ase liquid of component 1 enthalpy neasurement of H ^E	at variable x ₁ and constant [Y1] .200E+04	<u>T</u>
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .899000E-01 .170800E+00 .247300E+00 .378600E+00 .435500E+00 .435500E+00 .532200E+00 .572900E+00	[HMSD0001] HE Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] H ^E /Jmol ⁻¹ , Direct low-pressu 1. C ₂ H ₂ Cl ₄ , 1,1, 2. C ₁₄ H ₃₀ , Tetre B150E+03 [Y1] .484400E+03 .844900E+03 .116560E+04 .158690E+04 .158690E+04 .179480E+04 .179480E+04 .183820E+04 .185020E+04	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTION ase liquid of component 1 enthalpy neasurement of H ^E	at variable x ₁ and constant [Y1] .200E+04	<u>T</u>
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .899000E-01 .170800E+00 .316300E+00 .378600E+00 .378600E+00 .435500E+00 .532200E+00 .572900E+00 .609800E+00	[HMSD0001] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-pressu 1. C ₂ H ₂ Cl ₄ , 1,1, 2. C ₁ 4H ₃₀ , Tetra B150E+03 [Y1] .484400E+03 .844900E+03 .116560E+04 .140910E+04 .158690E+04 .179480E+04 .183820E+04 .185020E+04 .184010E+04	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTION ase liquid of component 1 enthalpy neasurement of H ^E	at variable x1 and constant [Y1] .200E+04 .150E+04	<u>T</u>
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .899000E-01 .170800E+00 .247300E+00 .378600E+00 .378600E+00 .532200E+00 .572900E+00 .609800E+00 .649700E+00	[HMSD0001] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-pressu 1. C ₂ H ₂ Cl ₄ , 1,1, 2. C ₁ 4H ₃₀ , Tetra 3.150E+03 [Y1] .484400E+03 .116560E+04 .158690E+04 .158690E+04 .171380E+04 .179480E+04 .183820E+04 .185020E+04 .184010E+04 .178520E+04	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTION ase liquid of component 1 enthalpy neasurement of H ^E	at variable x ₁ and constant [Y1] .200E+04	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .899000E-01 .170800E+00 .247300E+00 .378600E+00 .378600E+00 .435500E+00 .532200E+00 .572900E+00 .609800E+00 .649700E+00 .701100E+00	[HMSD0001] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-pressu 1. C ₂ H ₂ Cl ₄ , 1,1, 2. C ₁ 4H ₃₀ , Tetra 150E+03 [Y1] .484400E+03 .116560E+04 .158690E+04 .158690E+04 .17380E+04 .179480E+04 .183820E+04 .185020E+04 .184010E+04 .178520E+04 .168240E+04	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTION ase liquid of component 1 enthalpy neasurement of H ^E	at variable x1 and constant [Y1] .200E+04 .150E+04	<u>T</u>
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .899000E-01 .170800E+00 .247300E+00 .316300E+00 .378600E+00 .378600E+00 .532200E+00 .572900E+00 .649700E+00 .649700E+00 .738400E+00 .738400E+00	[HMSD0001] HI Two-component Pure component Pure component [P1] T/K, [X1] x ₁ /-, [Y1] HE/Jmol ⁻¹ , Direct low-pressu 1. C ₂ H ₂ Cl ₄ , 1,1, 2. C ₁ 4H ₃₀ , Tetra 150E+03 [Y1] .484400E+03 .844900E+03 .116560E+04 .158690E+04 .158690E+04 .17380E+04 .179480E+04 .183820E+04 .185020E+04 .184010E+04 .178520E+04 .168240E+04 .158540E+04	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTION ase liquid of component 1 enthalpy neasurement of H ^E	at variable x1 and constant [Y1] .200E+04 .150E+04	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .899000E-01 .170800E+00 .247300E+00 .316300E+00 .378600E+00 .378600E+00 .572900E+00 .572900E+00 .609800E+00 .701100E+00 .738400E+00 .738400E+00 .776900E+00	[HMSD0001] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. C_14H_{30} , Tetra 150E+03 [Y1] .484400E+03 .844900E+03 .116560E+04 .158690E+04 .158690E+04 .179480E+04 .179480E+04 .185020E+04 .185020E+04 .18520E+04 .168240E+04 .158540E+04 .158540E+04 .146430E+04	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTION ase liquid of component 1 enthalpy neasurement of H ^E	at variable x1 and constant [Y1] .200E+04 .150E+04	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .899000E-01 .170800E+00 .247300E+00 .316300E+00 .378600E+00 .435500E+00 .532200E+00 .532200E+00 .572900E+00 .649700E+00 .701100E+00 .738400E+00 .776900E+00 .816000E+00	[HMSD0001] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. C_14H_{30} , Tetra 150E+03 [Y1] .484400E+03 .844900E+03 .116560E+04 .158690E+04 .158690E+04 .171380E+04 .179480E+04 .18820E+04 .18820E+04 .18820E+04 .188540E+04 .158540E+04 .158540E+04 .131050E+04	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTION ase liquid of component 1 enthalpy neasurement of H ^E	at variable x1 and constant [Y1] .200E+04 .150E+04 .100E+04	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .899000E-01 .170800E+00 .247300E+00 .316300E+00 .378600E+00 .378600E+00 .572900E+00 .572900E+00 .572900E+00 .701100E+00 .738400E+00 .776900E+00 .816000E+00 .854500E+00	[HMSD0001] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. C_14H_{30} , Tetra 150E+03 [Y1] .484400E+03 .844900E+03 .116560E+04 .158690E+04 .158690E+04 .171380E+04 .183820E+04 .183820E+04 .18520E+04 .168240E+04 .158540E+04 .158540E+04 .131050E+04 .112240E+04	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTION ase liquid of component 1 enthalpy neasurement of H ^E	at variable x1 and constant [Y1] .200E+04 .150E+04	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .899000E-01 .170800E+00 .247300E+00 .316300E+00 .378600E+00 .378600E+00 .532200E+00 .572900E+00 .609800E+00 .609800E+00 .738400E+00 .736900E+00 .816000E+00 .854500E+00 .894000E+00	[HMSD0001] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. C_14H_{30} , Tetra 150E+03 [Y1] .484400E+03 .844900E+03 .116560E+04 .158690E+04 .158690E+04 .179480E+04 .183820E+04 .18520E+04 .18520E+04 .18520E+04 .168240E+04 .158540E+04 .158540E+04 .131050E+04 .112240E+04 .888900E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTION ase liquid of component 1 enthalpy neasurement of H ^E	at variable x1 and constant [Y1] .200E+04 .150E+04 .100E+04	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .899000E-01 .170800E+00 .247300E+00 .316300E+00 .378600E+00 .378600E+00 .572900E+00 .572900E+00 .572900E+00 .701100E+00 .738400E+00 .776900E+00 .816000E+00 .854500E+00	[HMSD0001] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. C_14H_{30} , Tetra 150E+03 [Y1] .484400E+03 .844900E+03 .116560E+04 .16560E+04 .171380E+04 .179480E+04 .18820E+04 .185020E+04 .18520E+04 .18540E+04 .158540E+04 .158540E+04 .13050E+04 .112240E+04 .888900E+03 .618300E+03 .618300E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTION ase liquid of component 1 enthalpy neasurement of H ^E	at variable x1 and constant [Y1] .200E+04 .150E+04 .100E+04	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .899000E-01 .170800E+00 .247300E+00 .316300E+00 .378600E+00 .378600E+00 .572900E+00 .572900E+00 .609800E+00 .701100E+00 .738400E+00 .854500E+00 .854500E+00 .894000E+00 .894000E+00 .931800E+00	[HMSD0001] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. C_14H_{30} , Tetra 150E+03 [Y1] .484400E+03 .844900E+03 .116560E+04 .158690E+04 .158690E+04 .179480E+04 .183820E+04 .18520E+04 .18520E+04 .18520E+04 .168240E+04 .158540E+04 .158540E+04 .131050E+04 .112240E+04 .888900E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTION ase liquid of component 1 enthalpy neasurement of H ^E	at variable x1 and constant [Y1] .200E+04 .150E+04 .150E+04 .100E+04 .00E+03	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .899000E-01 .170800E+00 .247300E+00 .316300E+00 .378600E+00 .378600E+00 .572900E+00 .572900E+00 .609800E+00 .701100E+00 .738400E+00 .854500E+00 .854500E+00 .894000E+00 .894000E+00 .931800E+00	[HMSD0001] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. C_14H_{30} , Tetra 150E+03 [Y1] .484400E+03 .844900E+03 .116560E+04 .16560E+04 .171380E+04 .179480E+04 .18820E+04 .185020E+04 .18520E+04 .18540E+04 .158540E+04 .158540E+04 .13050E+04 .112240E+04 .888900E+03 .618300E+03 .618300E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTION ase liquid of component 1 enthalpy neasurement of H ^E	at variable x1 and constant [Y1] .200E+04 .150E+04 .100E+04 .100E+04 .500E+03	
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .899000E-01 .170800E+00 .247300E+00 .316300E+00 .378600E+00 .378600E+00 .572900E+00 .572900E+00 .609800E+00 .701100E+00 .738400E+00 .854500E+00 .854500E+00 .894000E+00 .894000E+00 .931800E+00	[HMSD0001] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. C_14H_{30} , Tetra 150E+03 [Y1] .484400E+03 .844900E+03 .116560E+04 .16560E+04 .171380E+04 .179480E+04 .18820E+04 .185020E+04 .18520E+04 .18540E+04 .158540E+04 .158540E+04 .13050E+04 .112240E+04 .888900E+03 .618300E+03 .618300E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTION ase liquid of component 1 enthalpy neasurement of H ^E	at variable x1 and constant [Y1] .200E+04 .150E+04 .150E+04 .100E+04 .00E+03	T
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .899000E-01 .170800E+00 .247300E+00 .316300E+00 .378600E+00 .378600E+00 .572900E+00 .572900E+00 .609800E+00 .701100E+00 .738400E+00 .854500E+00 .854500E+00 .894000E+00 .894000E+00 .931800E+00	[HMSD0001] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. C_14H_{30} , Tetra 150E+03 [Y1] .484400E+03 .844900E+03 .116560E+04 .16560E+04 .171380E+04 .179480E+04 .18820E+04 .185020E+04 .18520E+04 .18540E+04 .158540E+04 .158540E+04 .13050E+04 .112240E+04 .888900E+03 .618300E+03 .618300E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTION ase liquid of component 1 enthalpy neasurement of H ^E	at variable x1 and constant [Y1] .200E+04 .150E+04 .100E+04 .100E+04 .500E+03	T $(P1] = .298150E + 03$.50E+00
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .899000E-01 .170800E+00 .247300E+00 .316300E+00 .378600E+00 .378600E+00 .572900E+00 .572900E+00 .609800E+00 .701100E+00 .738400E+00 .854500E+00 .854500E+00 .894000E+00 .894000E+00 .931800E+00	[HMSD0001] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. C_14H_{30} , Tetra 150E+03 [Y1] .484400E+03 .844900E+03 .116560E+04 .16560E+04 .171380E+04 .179480E+04 .18820E+04 .185020E+04 .18520E+04 .18540E+04 .158540E+04 .158540E+04 .13050E+04 .112240E+04 .888900E+03 .618300E+03 .618300E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTION ase liquid of component 1 enthalpy neasurement of H ^E	at variable x1 and constant [Y1] .200E+04 .150E+04 .100E+04 .100E+04 .500E+03	T
Property Code: State: Parameters: Variables: Method: Components: [P1] = .298 [X1] .899000E-01 .170800E+00 .247300E+00 .316300E+00 .378600E+00 .378600E+00 .572900E+00 .572900E+00 .609800E+00 .701100E+00 .738400E+00 .854500E+00 .854500E+00 .894000E+00 .894000E+00 .931800E+00	[HMSD0001] HI Two-component Pure component Pure component [P1] T/K , [X1] $x_{1/-}$, [Y1] $H^E/Jmol^{-1}$, Direct low-pressu 1. $C_2H_2Cl_4$, 1,1, 2. C_14H_{30} , Tetra 150E+03 [Y1] .484400E+03 .844900E+03 .116560E+04 .16560E+04 .171380E+04 .179480E+04 .18820E+04 .185020E+04 .18520E+04 .18540E+04 .158540E+04 .158540E+04 .13050E+04 .112240E+04 .888900E+03 .618300E+03 .618300E+03	EAT OF MIXING system, single-ph 1, liquid 2, liquid Temperature Mole fraction Molar excess e tre calorimetric m 2,2-Tetrachloro	G AND SOLUTION ase liquid of component 1 enthalpy neasurement of H ^E	at variable x1 and constant [Y1] .200E+04 .150E+04 .100E+04 .100E+04 .500E+03	T $(P1] = .298150E + 03$.50E+00



Copyright© 1995 F Property Code: State: Parameters: Variables:	Two-component s Pure component 1 Pure component 2 [P1] T/K , [X1] $x_1/-$, [Y1] $H^E/Jmol^{-1}$,	2, liquid Temperature Mole fraction of component 1 Molar excess enthalpy	
Method:	ne na se a	re calorimetric measurement of HE	^{<i>L</i>} at variable x_1 and constant <i>T</i>
Components:	2. C17H36, Hept	2,2 — Tetrachloroethane adecane	
[P1] = .290	8150E+03		[Y1]
[X1]	[Y1]		.220E+04
.141800E+00 .251300E+00 .335600E+00 .402000E+00 .509500E+00 .509500E+00 .553900E+00 .648800E+00 .668900E+00 .734600E+00 .804600E+00 .804600E+00 .875400E+00 .909400E+00 .909400E+00 .909400E+00	.199360E+04 .200310E+04 .197420E+04 .191470E+04 .185430E+04 .185430E+04 .165870E+04 .135260E+04 .135260E+04 .114630E+04 .905200E+03 .625900E+03		$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$