

## Towards mild conditions by predictive catalysis *via* sterics in the Ru-catalyzed hydrogenation of thioesters

Michele Tomasini<sup>a</sup>, Josep Duran<sup>a</sup>, Sílvia Simon<sup>a</sup>, Luis Miguel Azofra<sup>b,\*</sup>, Albert Poater<sup>a,\*</sup>

<sup>a</sup> Institut de Química Computacional i Catàlisi and Departament de Química, Universitat de Girona, c/ Maria Aurèlia Capmany 69, 17003 Girona, Catalonia, Spain

<sup>b</sup> Instituto de Estudios Ambientales y Recursos Naturales (i-UNAT), Universidad de Las Palmas de Gran Canaria (ULPGC), Campus de Tafira, 35017 Las Palmas de Gran Canaria, Spain

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### ABSTRACT

The Milstein's reported discovery of hydrogenation of thioesters directly toward thiols and alcohols catalyzed by a Ru-acridine complex has been studied here by DFT calculations to know the origin of the different performance depending on the nature of the substituents. Unveiling the reaction mechanism leads to a deeper understanding of the steric and electronic properties on the nature of the limiting step of the reaction. Steric maps and Conceptual DFT have been the tools to rationalize the reactivity patterns. In addition, the nature of the catalyst has been studied, replacing the substituents on the phosphorous atoms by less sterically demanding groups with the aim to move to milder reaction conditions.

### Introduction

In the field of the industrial chemistry, moving from stoichiometric to catalytic reactions represents a primary objective not always achievable. The hydrogenation of thioesters often lies in the stoichiometric consumption of the hydride reagents [1,2], reducing them into thiols and alcohols but also generating waste and presenting low selectivity when thioesters are part of organic substrates with a higher molecular complexity. Undoubtedly, this represents a bottleneck in the applicability of this reaction on biological substrates. In Nature, the four-electrons reduction of thioesters by NAD(P)H in the terminal steps of non-ribosomal peptide synthetase and polyketide synthase allows the biosynthesis of specific alcohols [3–5] from bio-based feedstocks.

Within the sustainable green homogeneous catalytic chemistry, the old methods using stoichiometric amounts of hydride reagents have been replaced by metal-catalyzed reactions for a wide range of substrate transformations [6–10]. While the hydrogenative reactions may lead to the reduction of the organic substrates [11–14], in particular carbamates [15–18], amides [19–21], and any carboxylic derivative group [22–25], here the focus will be on thioesters and the incapacity to hydrogenate them in the past.

In 2020, Milstein and collaborators reported a complex based on ruthenium acridine (**Ru-1**), capable of reducing thioesters, thio-carbamates, and thioamides [26]. As shown at Fig. 1a, using

hexanethiol, **Ru-1** is transformed into a hydride-thiol Ru based complex (**Ru-2**). In addition (Fig. 1b), in presence of a thioester substrate, **Ru-1** generates the corresponding aldehyde and another ruthenium complex, **Ru-3**. As shown at Fig. 1c, **Ru-3** has the ability to heterolytically break H<sub>2</sub> under mild conditions, and by reaction with the thioester substrate, the corresponding alcohol and thiol products are generated. Then all efforts were made to convert the already important stoichiometric outputs to catalytic ones. From **Ru-1**, even increasing the pressure of H<sub>2</sub> up to 40 atm, it was not possible to consume the thioester reagent, but the increase in temperature up to 408.15 K allowed to reach up to a full conversion, with yields of 94% of the alcohol and of 96% thiol, completely omitting side reactions. Increasing up to 423.15 K and 10 bar (H<sub>2</sub>) the temperature and pressure, respectively, those yields increase up to 95 and 99% (Fig. 1d). Furthermore, the substitution of the quasi linear CH<sub>2</sub>CH<sub>2</sub>Ph of substrate **1a** by the shorter, but at the same time bulkier *t*-butyl group (**1h**) entailed a drop of 30% of yield (Fig. 1e). In addition, it was demonstrated experimentally how hydrogen gas pressure governs selectivity toward hydrogenation or dehydrogenation, together with mechanistic insights [27]. Accordingly, a competing dehydrogenative mechanism was discussed [28–30]. The thermodynamical preference was not enough because of the prohibitive kinetics due to the high acidity of thiol compared to alcohol. This is translated in the higher stability of ruthenium thiolate intermediate with respect to ruthenium alkoxide intermediate. In addition, with the goal of

\* Corresponding authors.

E-mail addresses: [luismiguel.azofra@ulpgc.es](mailto:luismiguel.azofra@ulpgc.es) (L.M. Azofra), [albert.poater@udg.edu](mailto:albert.poater@udg.edu) (A. Poater).

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hydrogenation of thioesters, undesired competitive reaction pathways like the dehydrogenative coupling of alcohol to ester as well as the Tishchenko reaction coupling aldehyde to ester were found out to be not kinetically favored [31,32].

Herein, we investigate the reaction pathway [33] of the catalytic hydrogenation of a series of thioesters by means of sterics through density functional theory (DFT) calculations.

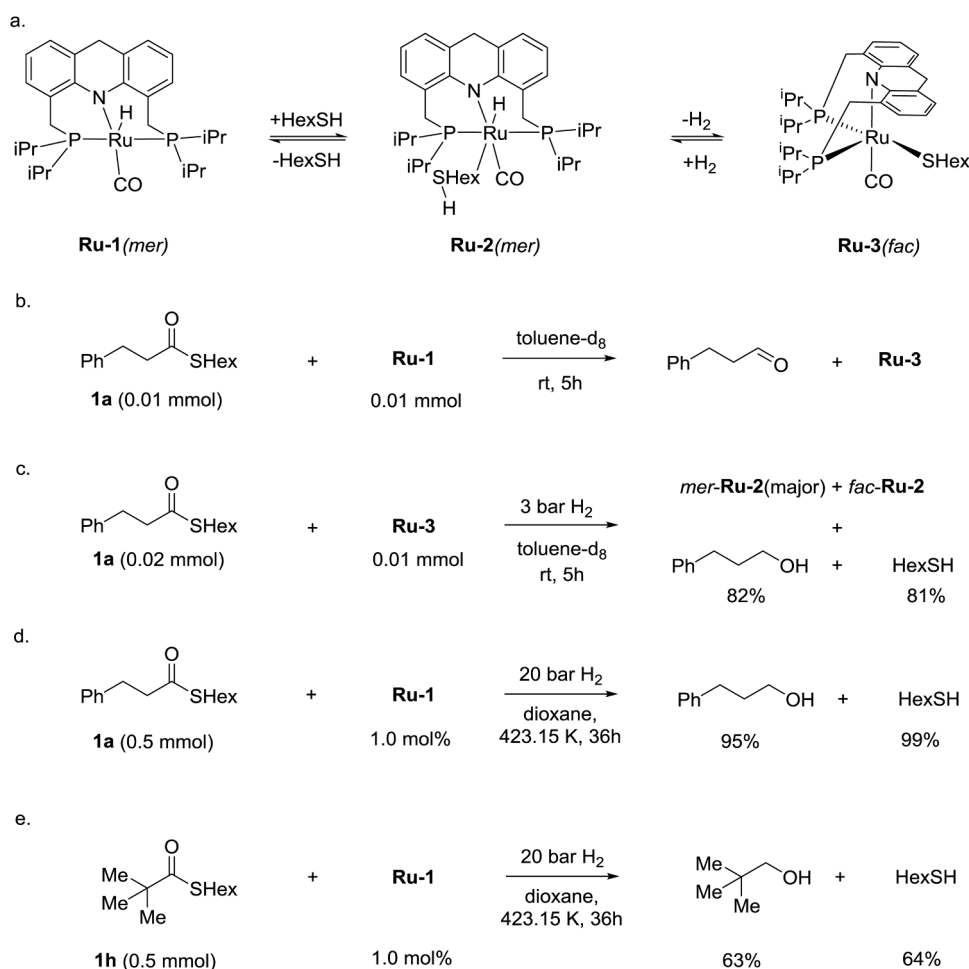
### Computational details

DFT calculations were performed using the facilities provided by the Gaussian16 package [34]. For geometry optimization, the GGA-based BP86 functional was used [35,36], including explicit dispersion corrections to the energy through the Grimme D3BJ method [37]. All geometry optimizations were performed without symmetry constraints in the gas phase. The located stationary points were characterized as minima or transition states by analytical frequency calculations. The split-valence basis set Def2-SVP from Ahlrichs and co-workers was used for non-metal atoms [38], while for ruthenium, the small-core, quasi-relativistic Stuttgart/Dresden effective core potential (SDD) was employed [39–41]. For single-point energy refinements, the hybrid GGA-based B3LYP functional was used [42,43] with the Def2-TZVP basis set [44,45]. At this stage, solvent effects were introduced by means of the universal solvation model based on density (SMD) variation of IEFPCM by Truhlar and co-workers [46], using 1,4-dioxane as solvent. Gibbs energies were calculated as the sum of the electronic energies at the B3LYP-D3BJ-SMD(1,4-dioxane)/Def2-TZVP~SDD//BP

86-D3BJ/Def2-SVP~SDD level of theory plus the zero-point energies (ZPE) and thermal corrections calculated at the BP86-D3BJ/Def2-SVP~SDD computational level in vacuum. All free energies refer to standard Gibbs energies in a 1 M standard-state concentration for all species [47–49], i.e., the change of the conventional 1 atm standard state for gas phase calculations to a standard state of 1 M concentration in solution entails corrections of 1.9 and 3.0 kcal/mol at 298.15 and 423.15 K, respectively [50–52].

### Results and discussion

The reaction mechanism of the Ru-catalyzed thioester hydrogenation by Milstein and co-workers [26,27] has been unveiled by means of density functional theory (DFT) (See Fig. 2). The process starts with the coordination between the thioester *S*-methyl propanethioate (as model substrate) with the ruthenium-acridine complex **fac-Ru**, which presents a vacancy site at the ruthenium center. A significant destabilization of 16.7 kcal/mol is seen leading to a highly sterically impeded complex **1** which allows [53–56], however, the subsequent hydride transfer from ruthenium to the  $sp^2$  carbon of the entering carbonyl group, i.e., the insertion of the thioester into the Ru-H bond of the catalyst [57], overcoming an energy barrier of 12.6 kcal/mol (**TS1**). A relatively unstable hexacoordinated Ru intermediate **2** bearing an agostic interaction is formed, which evolves to the more favored pentacoordinated complex **2a**, breaking the agostic interaction and releasing 7.7 kcal/mol. In this context, the calculation of the sterical hindrance by means of the % $V_{\text{Bur}}$  index defined by Cavallo and co-workers [58–60] decreases from 79.3 to



**Fig. 1.** (a) PNP pincer Ru-based complexes; stoichiometric transformation of thioester (b) to aldehyde by Ru-1 and (c) to alcohol by Ru-3; (d) catalytic transformation of thioester **1a** and (e) of thioester **1h** to evaluate the steric effects.

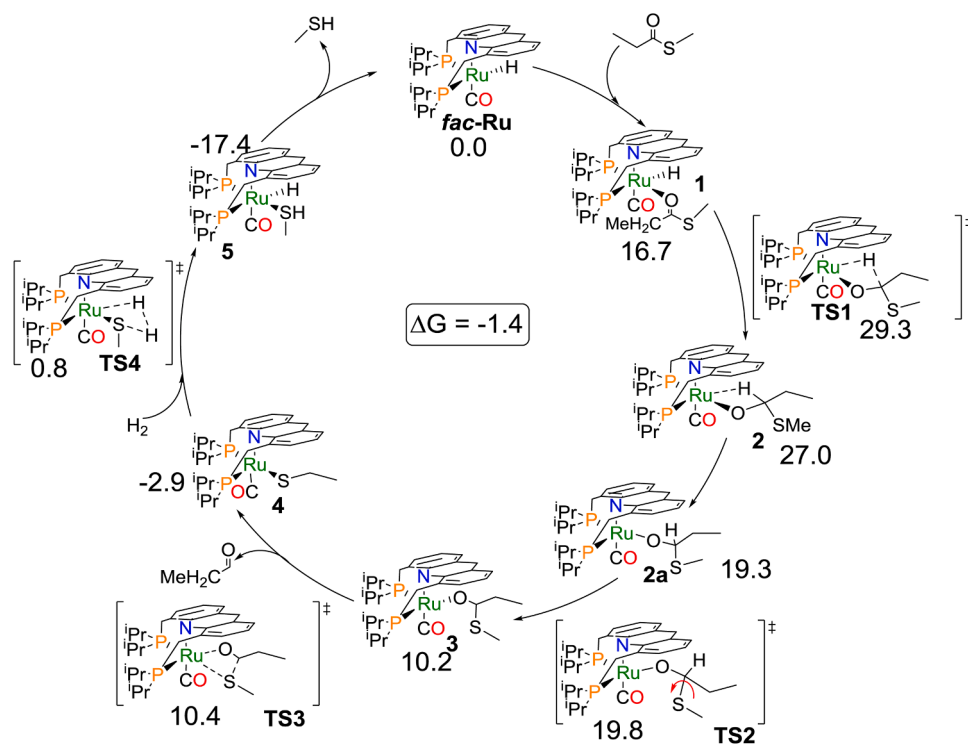


Fig. 2. Reaction mechanism for the Ru-catalyzed thioester hydrogenation using *fac*-Ru as catalyst (Relative Gibbs energies in kcal/mol calculated at 298.15 K).

71.4% [61,62]. Next, the nearly barrierless rotational movement around the Ru–O–C–S dihedral angle in **TS2** facilitates the isomerization of complex **2a** into complex **3**, and guides to the subsequent C–S bond cleavage through **TS3** and the release of an aldehyde moiety that leads to the formation of intermediate **4**. The latter thioalkyl transfer via **TS3** is also a kinetically irrelevant process with a very low energy barrier of just 0.2 kcal/mol. To close the catalytic cycle, the former *fac*-Ru complex is then regenerated through hydrogenation of complex **4** by molecular hydrogen. The heterolytic H–H bond cleavage [63–65] with a kinetic cost of 3.7 kcal/mol via **TS4** leads to the formation of the hydride intermediate **5**, prone to release a thiol product in an overall exergonic reaction with a reaction free energy of 1.4 kcal/mol. Although not shown at Fig. 2, complex **5** will be also the active species for the aldehyde hydrogenation into alcohol (previously released) through a so-called **TS5** to regenerate complex **4**, however this should overcome a significant energy barrier of 36.9 kcal/mol.

Overall, the rate-determining step (rds) is imposed by **TS1**. Although a relative barrier of 12.6 kcal/mol is seen with respect complex **1**, according to Shaik and Kozuch [66], the rate determining intermediate as reference is the lowest in energy before the rds, so **TS1** is the single transition state that is responsible for the turnover frequency (TOF) being at 29.3 kcal/mol with respect *fac*-Ru.

Since the catalyst performance is actually optimized at 423.15 K,  $\Delta G$  values at Fig. 2 have been recalculated at this temperature. (See Fig. S1 from the Supporting Information). The value of the rds changes to 33.7 kcal/mol for this case. It should be noted that a comparison of  $\Delta G$  values at both temperatures explain why at mild conditions the reaction cannot take place: it is necessary to increase the temperature, and although it involves a slight increase in the kinetic cost of the rds, the temperature allows to supply it.

Knowing that the catalytic performance drops for thioesters with higher sterical alkyl groups in alpha to the carbonyl group, substrates **II** (*S*-methyl *t*-butylpropanethioate), **III** [*S*-(*t*-butyl) propanethioate], and **IV** [*S*-(*t*-butyl) *t*-butylpropanethioate] at Scheme 1 have been also considered. Focusing just on **TS1** (rds), the introduction of a *t*-butyl (*t*-Bu) group in the sulfur substituent (**III**) increases the energy barrier by

1.4 kcal/mol, while this is 9.5 kcal/mol if the *t*-Bu substituent is bonded directly to the keto group (**II**). When both sides of substrate **I** are substituted with *t*-Bu groups (**IV**), the barrier increases by 9.8 kcal/mol. Looking at the geometry of **TS1** for each case (Fig. 3), once added the *t*-Bu group(s), it is clear that the sterical hindrance is larger when this bulky substituent is next to the keto group.

Undoubtedly, this high energy barrier is principally caused by the steric hindrance between the substituents of thioesters and the two isopropyl (*i*-Pr) groups on the phosphorous atoms of the PNP pincer ligand. For that reason, % $V_{\text{Bur}}$  between the substituents and the *i*-Pr groups has been calculated for **TS1** with values of 75.7, 82.1, 80.3 and 84.8% for **I**–**IV** series, respectively. Steric maps in Fig. 4 confirm that the

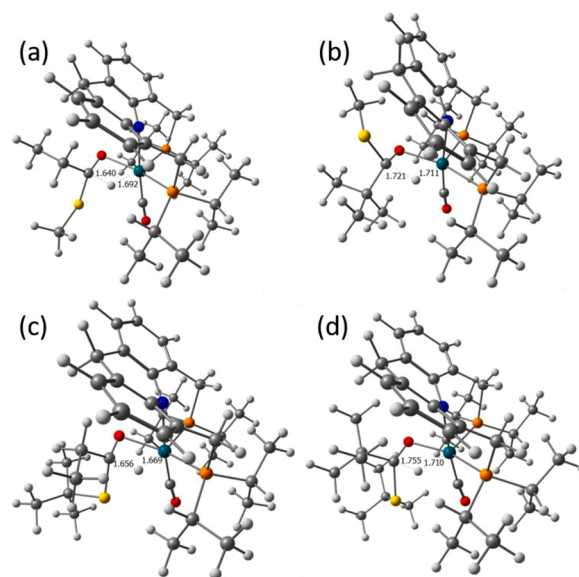


Fig. 3. Rate determining transition state **TS1** for (a) **I**, (b) **II**, (c) **III**, and (d) **IV** substrates. Selected distances are shown in Å.

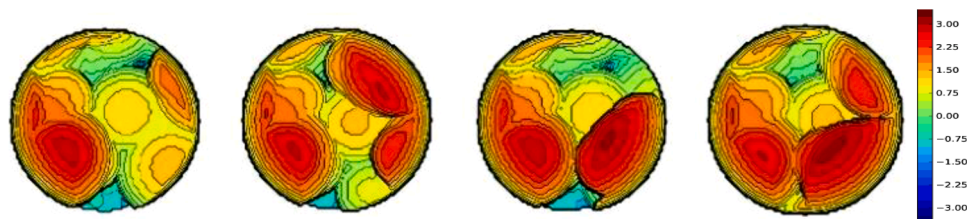


Fig. 4. Topographic steric maps (plane  $xy$ ) with the metal in the  $z$  axis of the TS1 for I-IV substrates (from left to right), with a radius of 3.5 Å.

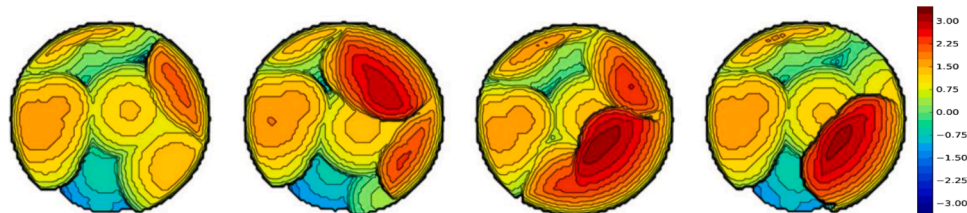
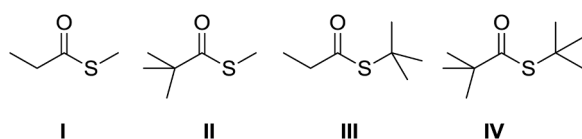


Fig. 5. Topographic steric maps (plane  $xy$ ) with the metal in the  $z$  axis of the TS1 for I-IV substrates (from left to right), with a radius of 3.5 Å, using *fac*-Ru with methyls on the P atoms of the PNP pincer ligand.



Scheme 1. Scope of substrates.

left groove corresponding to the substituent on the sulfur has a low or even null impact on the active center of TS1 [67], while on the right groove, the *t*-Bu group has a significant change [68]. It should be noted that the steric maps for substrate III would seem that the quadrant on the right and bottom is very obstructed, but this fact is offset by the one above. Quantifying by quadrants, the value of this for substrate III is 68.6%, even lower than for I (70.5%). For comparison, in substrates II and IV this increases to 89.7 and 79.6%, respectively.

In the frame of the Conceptual DFT analysis [69], the chemical hardness of intermediate 1 was evaluated, as well as for the I-IV substrates separately. In general rules, substrate IV is much less reactive than I, with II and III in between, at the electronic level [70,71,72,73]. Hardness values are 69.0, 71.5, 70.3, and 72.2 kcal/mol for complexed I-IV substrates at the intermediate 1. Interestingly, we did not observe any trend for the substrates separately, revealing that what plays a major role is the interaction of the substrates with the catalyst. Even though the *t*-Bu groups have a predominant sterical importance, the electronic nature is also capable of explain the different reactivity between the thioester substrates, following the same trend. We also carried out supporting calculations to analyze the effect of the non-covalent interactions between substrates and *fac*-Ru [74]. In this regard, NCIplots calculations by Contreras et al. [75,76] were performed, but no significant differences were appreciated between the four different substrates [77,78].

In an attempt to move to milder conditions, predictive catalytic analysis was employed by simple substitution of the *i*-Pr groups in the phosphines of the PNP pincer ligand by the less sterically demanding hydrogen and methyl groups. Interestingly, the TS1 rds drop from 29.3 kcal/mol to just 16.4 and 16.2 kcal/mol, respectively, for substrate I. In addition, for substrates II-IV these values are of just 22.7, 17.6 and 22.5 kcal/mol, respectively, for the catalyst with the phosphines substituted with methyl groups. These free energy barriers are more affordable at

room temperature. In addition, steric maps and % $V_{\text{Bur}}$  provides a clear explanation about this drop of kinetics demand [79,80]. In detail, the %  $V_{\text{Bur}}$  for TS1 decreases from 75.7 to 68.4% for substrate I, and with a similar decrease of around 7–8% for the other substrates. The steric maps in Fig. 5 give an even clearer view of the lower steric demand by substituting the *i*-Pr groups by methyls of the PNP pincer ligand, specially on the left.

In an attempt to put together the sterics with the electronics, following the scheme of Falivene and Cavallo [81], multilinear regressions were tested with the recognized low amount set of data for such an analysis. Despite the low statistical significance, the agreement was found to be 0.76 for % $V_{\text{Bur}}$  and the energy of the LUMO of TS1. However, still the main contribution is due to sterics since the agreement with just % $V_{\text{Bur}}$  is 0.8888 [82].

## Conclusions

By DFT calculations, we have unveiled the reaction mechanism of the catalytic hydrogenation of thioesters to form thiols and alcohols for a series of substrates with different bulky and not bulky substituents, in particular *t*-Bu groups. The results confirmed that the insertion of *t*-Bu groups to the substrate structure was dramatic next to the keto of the thioester chemical group, whereas innocent on the sulfur ligand. We also conducted further predictive calculations modifying the structure of the PNP replacing the *i*-Pr groups on both phosphorous atoms by methyl groups and hydrogen atoms in order to provide a route to milder conditions. Steric maps indicate that the different catalytic performance evaluated here is mainly due to sterics, although Conceptual DFT also confirms the trend since bulky *t*-Bu groups also increase the chemical hardness [83], and, by application of the Principle of Maximum Hardness (PMH) [84], decrease the chemical reactivity.

## Authors' contribution

**Michele Tomasini:** Calculations, Visualization, Data management, Writing – original draft. **Josep Duran:** Visualization, Data management, Writing – original draft. **Silvia Simon:** Visualization, Data management, Writing – original draft. **Luis Miguel Azofra:** Conceptualization, Writing – review & editing, Funding acquisition. **Albert Poater:** Conceptualization, Writing – original draft, review & editing, Supervision, Funding acquisition.

## Declaration of Competing Interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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## Supplementary materials

Supplementary material associated with this article can be found, in the online version, at doi:10.1016/j.mcat.2021.111692.

## Appendix A. Supplementary data

Supplementary material related to this article can be found, in the online version, at doi:https://doi.org/10.1016/j.mcat.2021.XXXXXX.

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